

Kavli Institute for Theoretical Physics  
University of California, Santa Barbara

# Fluid-Mediated Particle Transport in Geophysical Flows

Sep 23, 2013 - Dec 20, 2013

## **Kinetic theory applied to debris flow**

***Michele Larcher***

Department of Civil, Environmental and Mechanical Engineering

University of Trento, Italy

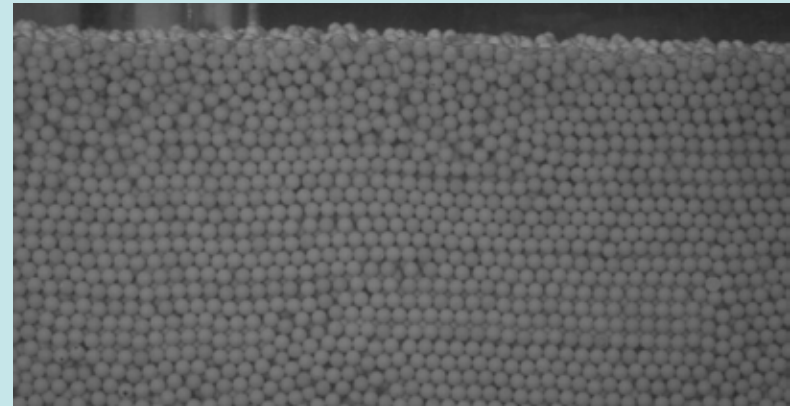
October 24, 2013

# Ingredients

Nature



Experiments



Theory

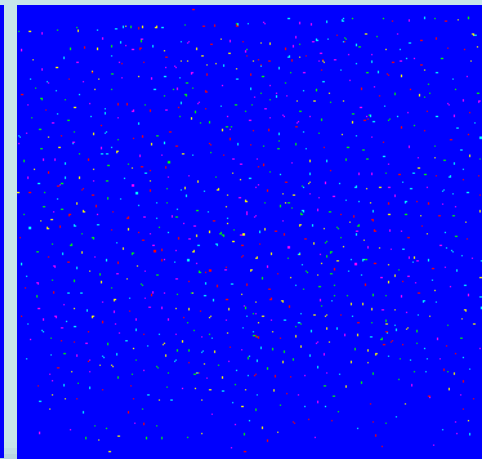
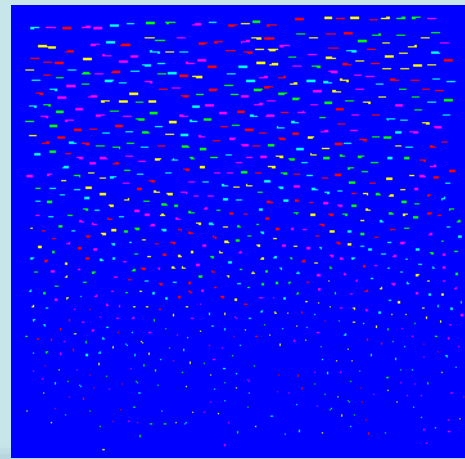
*velocity* = ...

*flow depth* = ...

*concentration* = ...

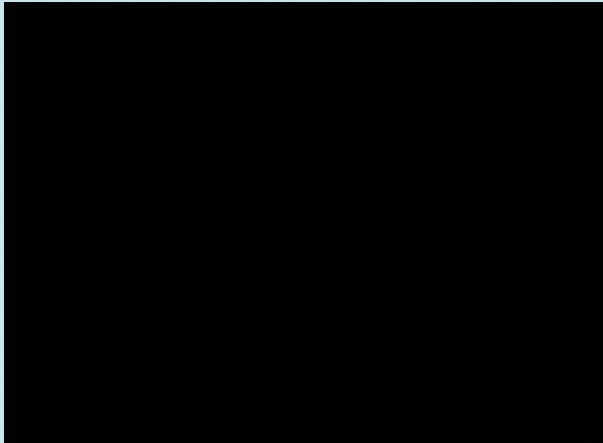
*total volume* = ...

Experimental methods



# Ingredients

Nature



Experiments

Aronne Armanini, Univ. of Trento

Luigi Fraccarollo, Univ. of Trento

Theory

Jim Jenkins, Cornell University

Experimental methods

Hervé Capart, National Taiwan Univ.

Benoit Spinewine, Univ. catholique de Louvain

# Experiments

## Recirculating flume



Journal of Fluid Mechanics 532, 269-319 (2005)

Journal of Hydraulic Research 45, 59-71 (2007)

Granular Matter, 9, 145-157 (2007)

Powder Technology, 182: 218-227 (2008)

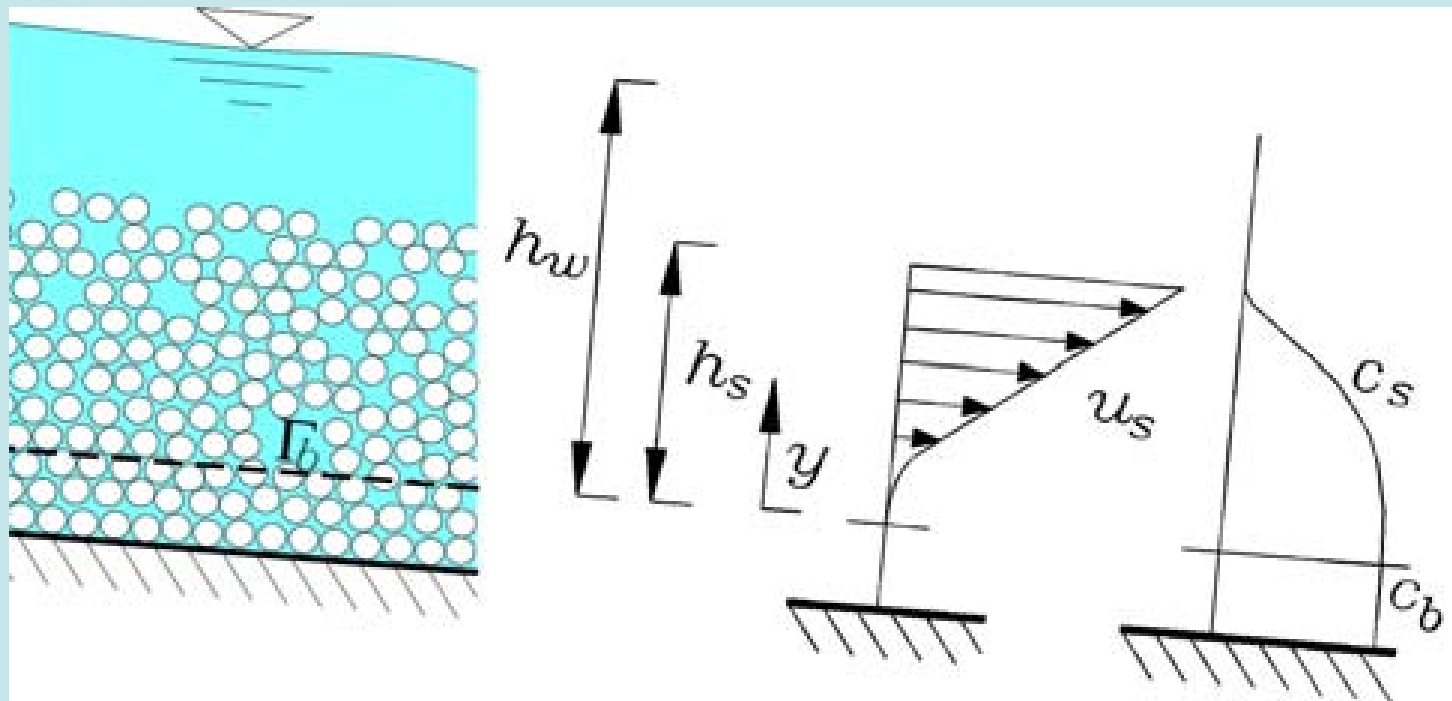
Physical Review E, 79, 051306 (2009)

# Experiments

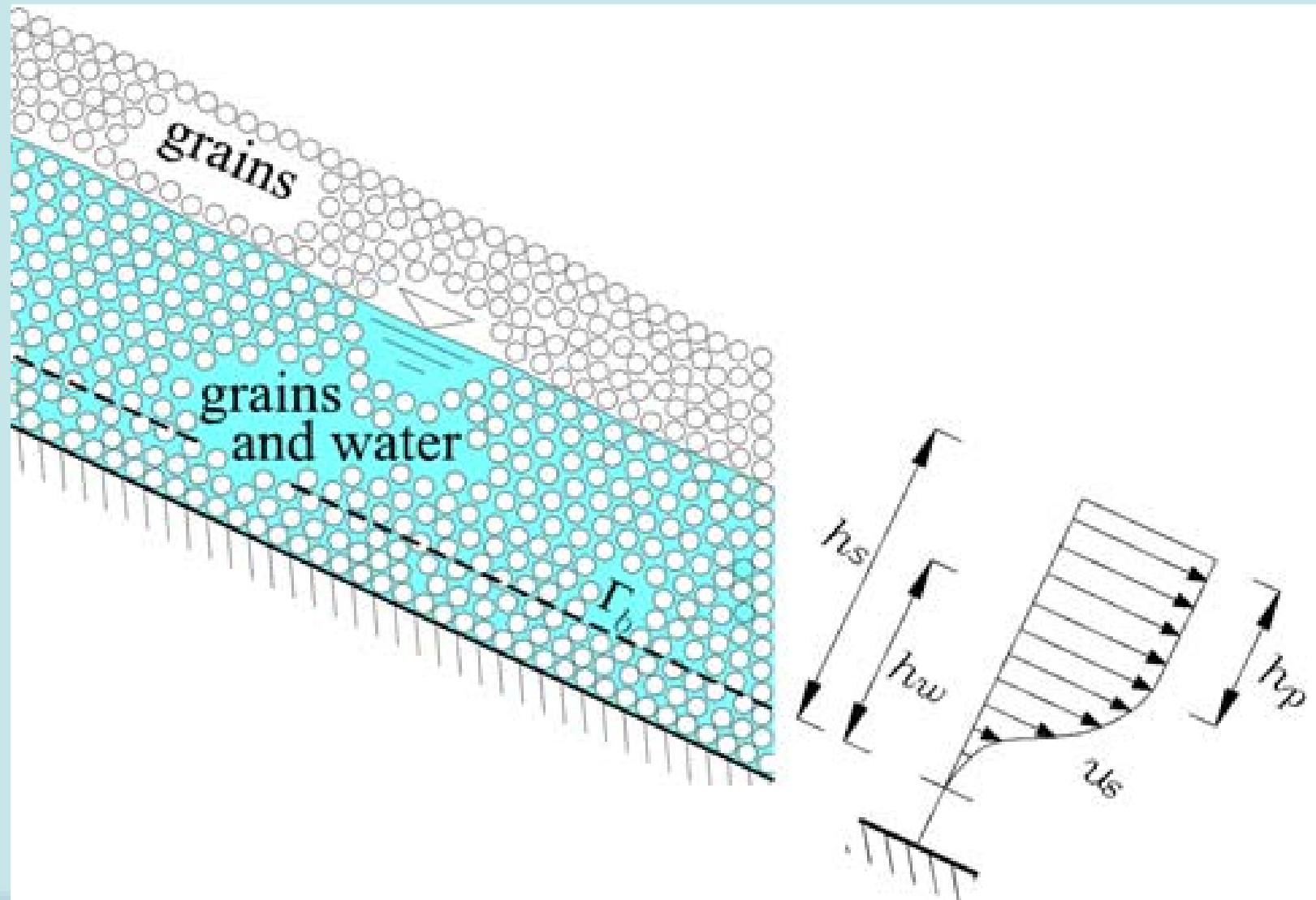
## Steady, Fully-Developed Flow over a mobile bed

- Over-saturated: water depth greater than grain depth
- Saturated: water depth equal to grain depth
- Under-saturated: water depth less than grain depth

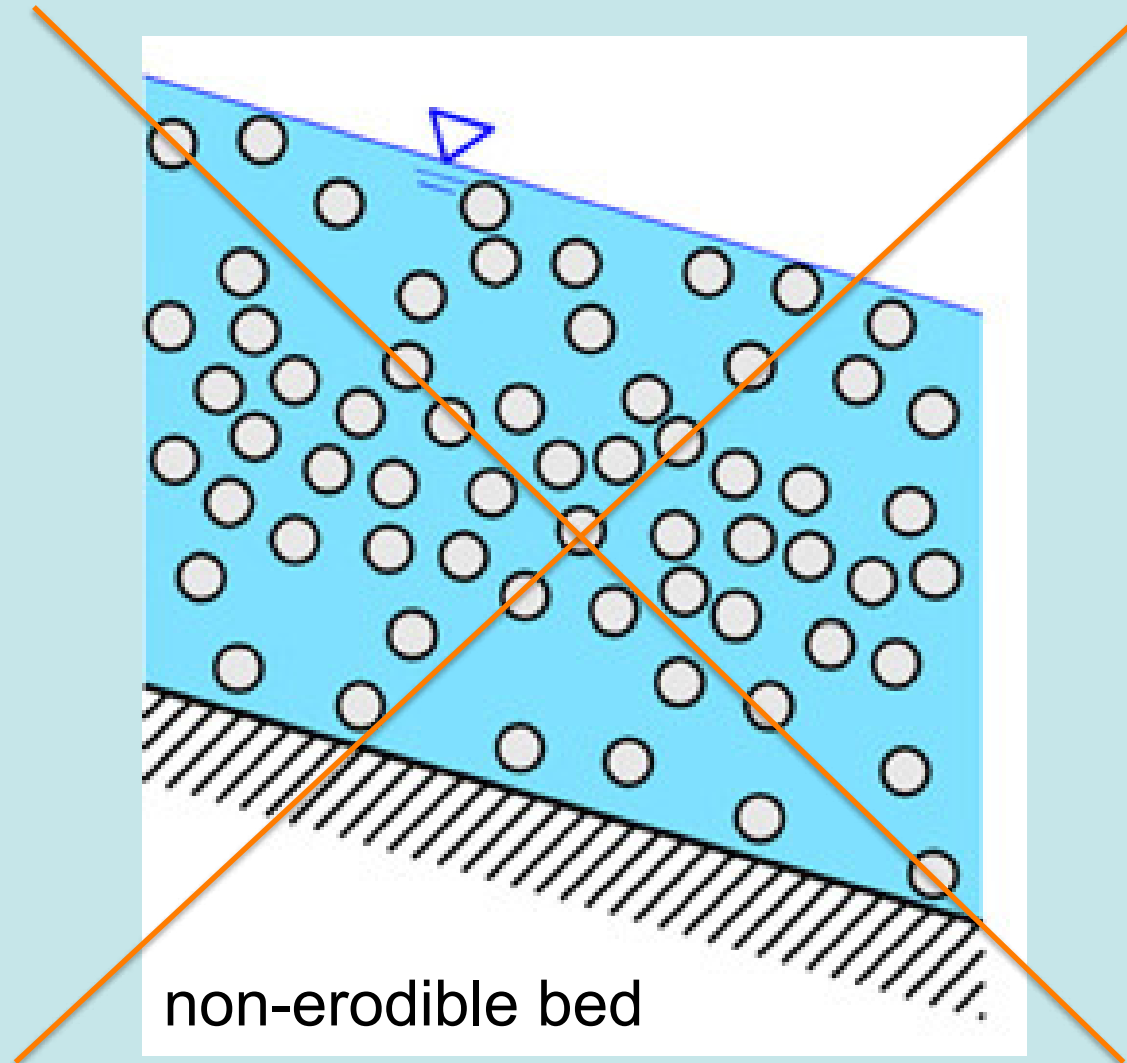
# Experiments



# Experiments

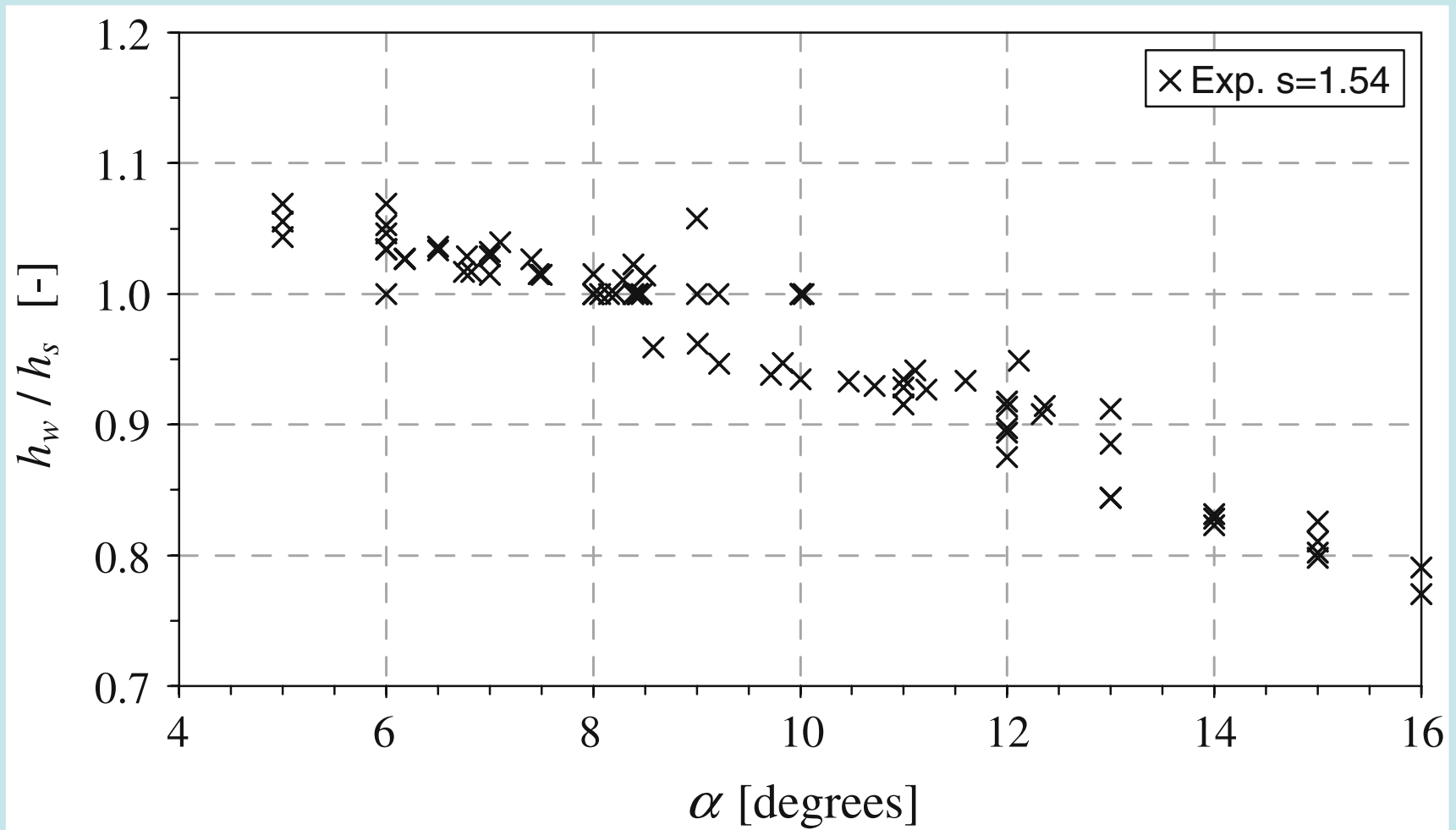


# Experiments

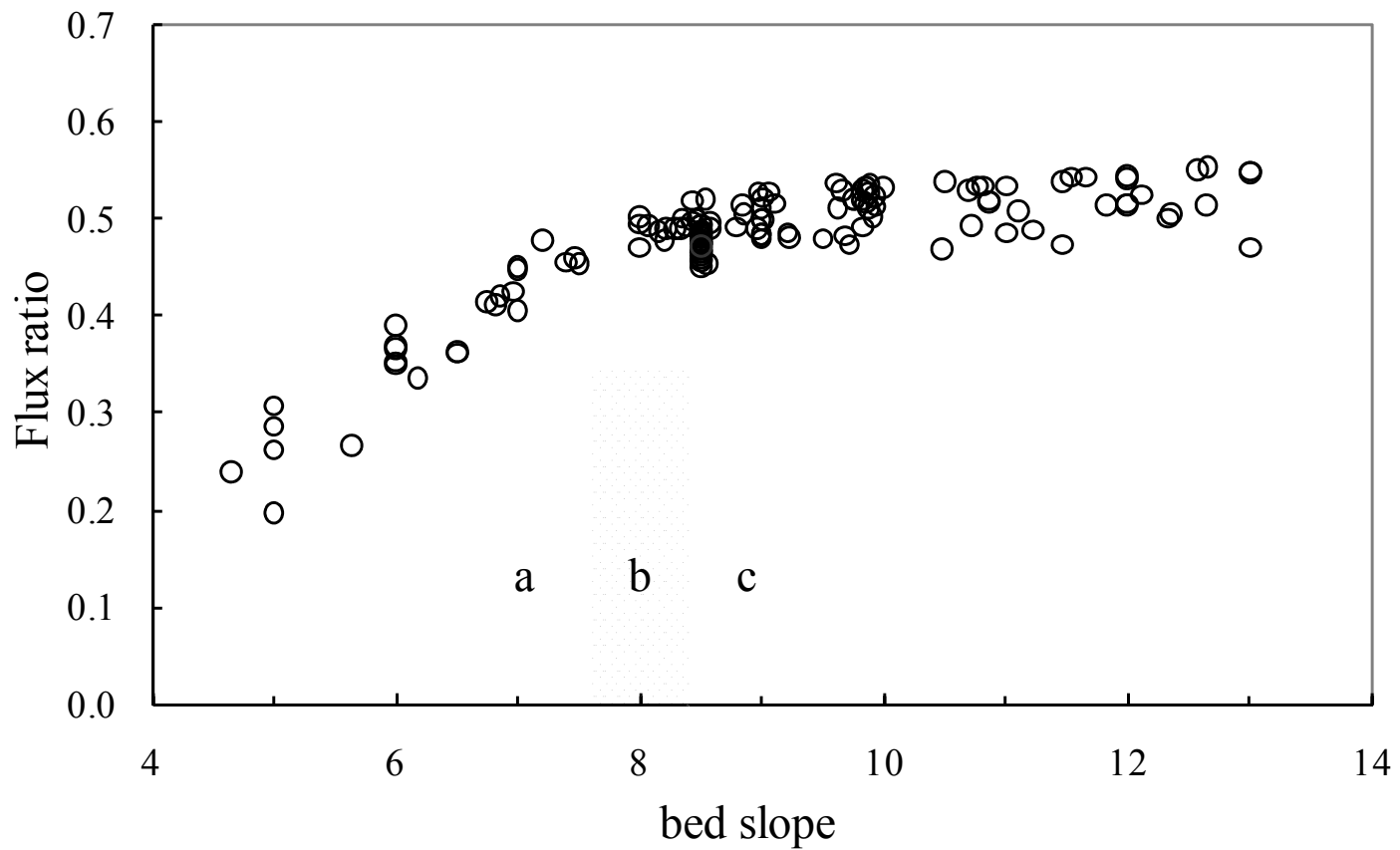
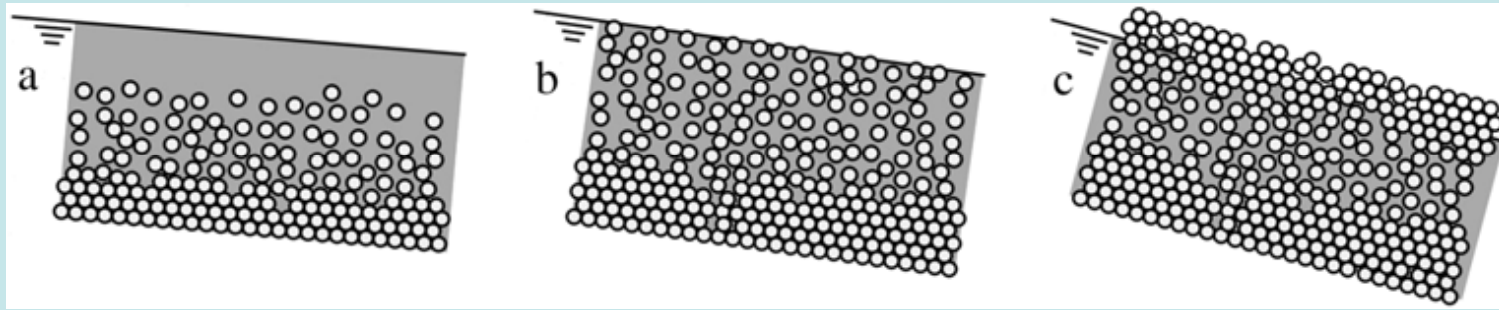




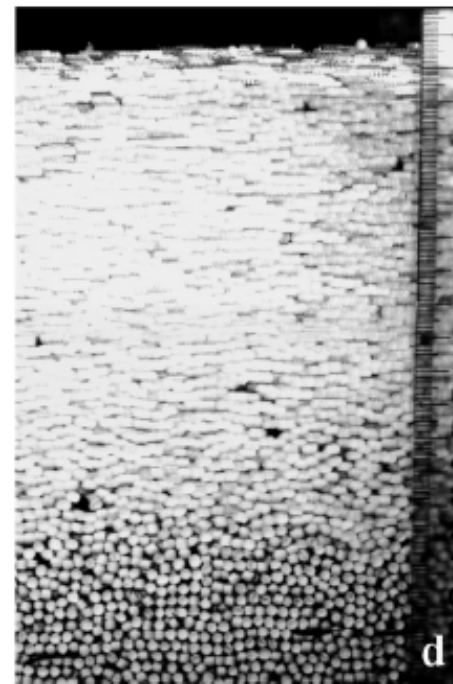
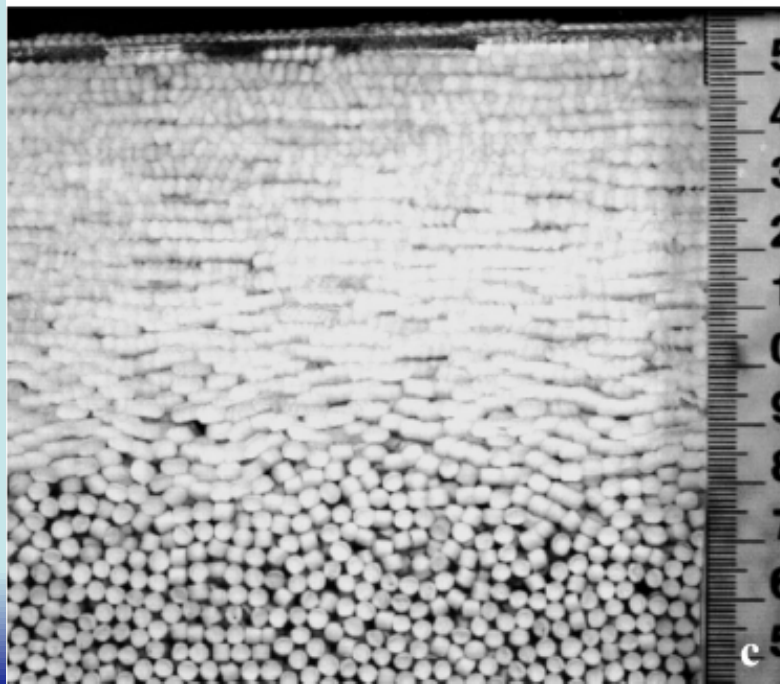
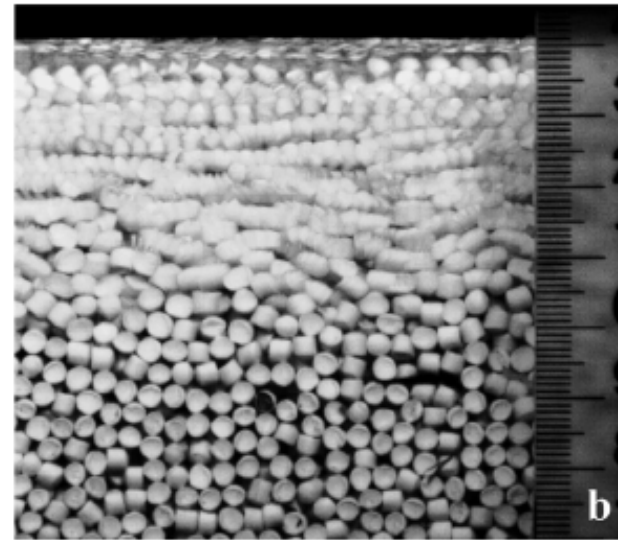
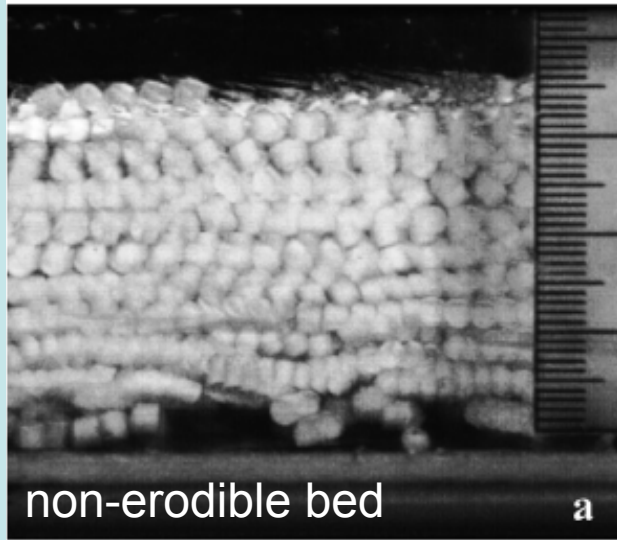
# Experiments



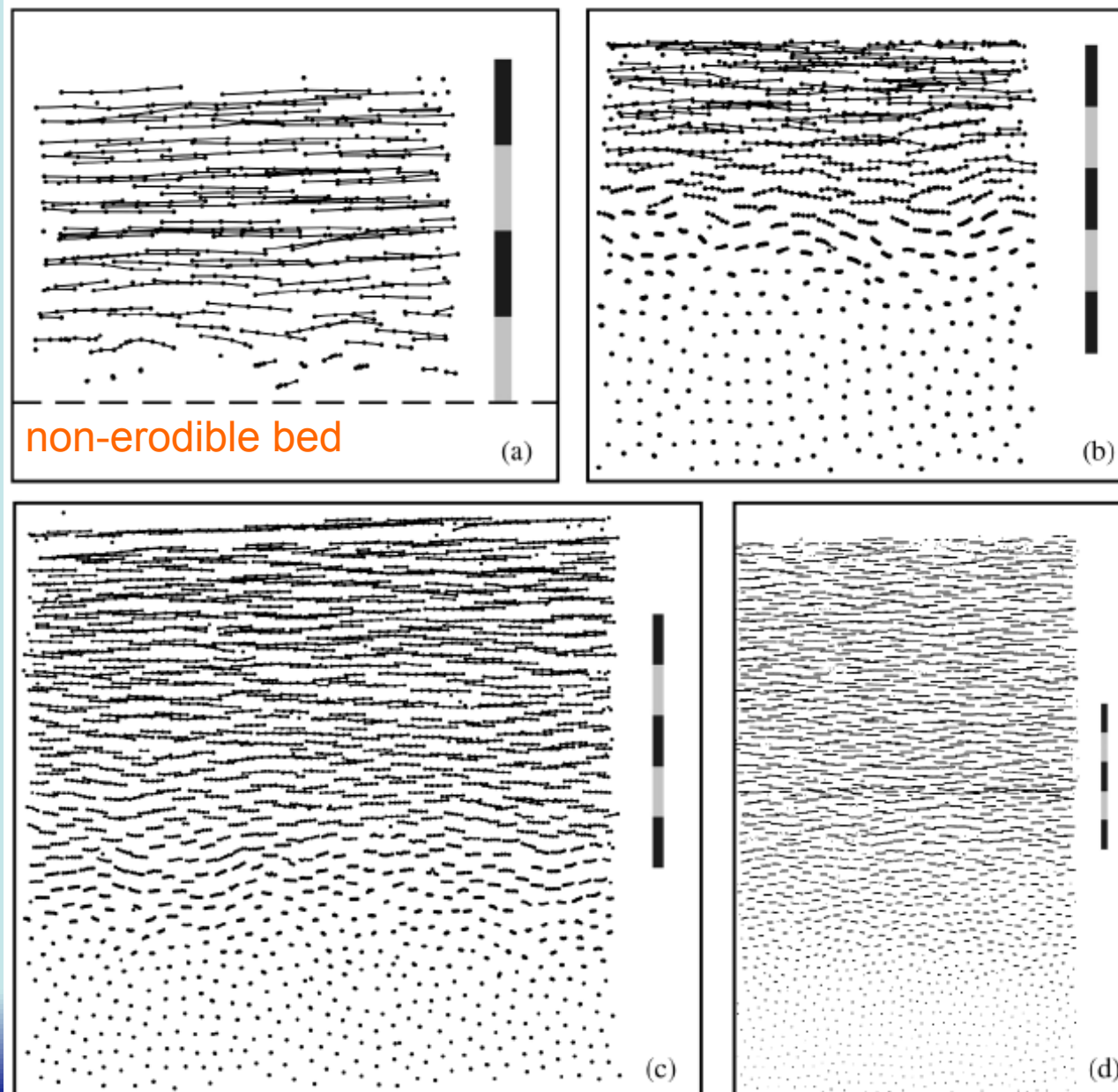
# Experiments



# Experiments

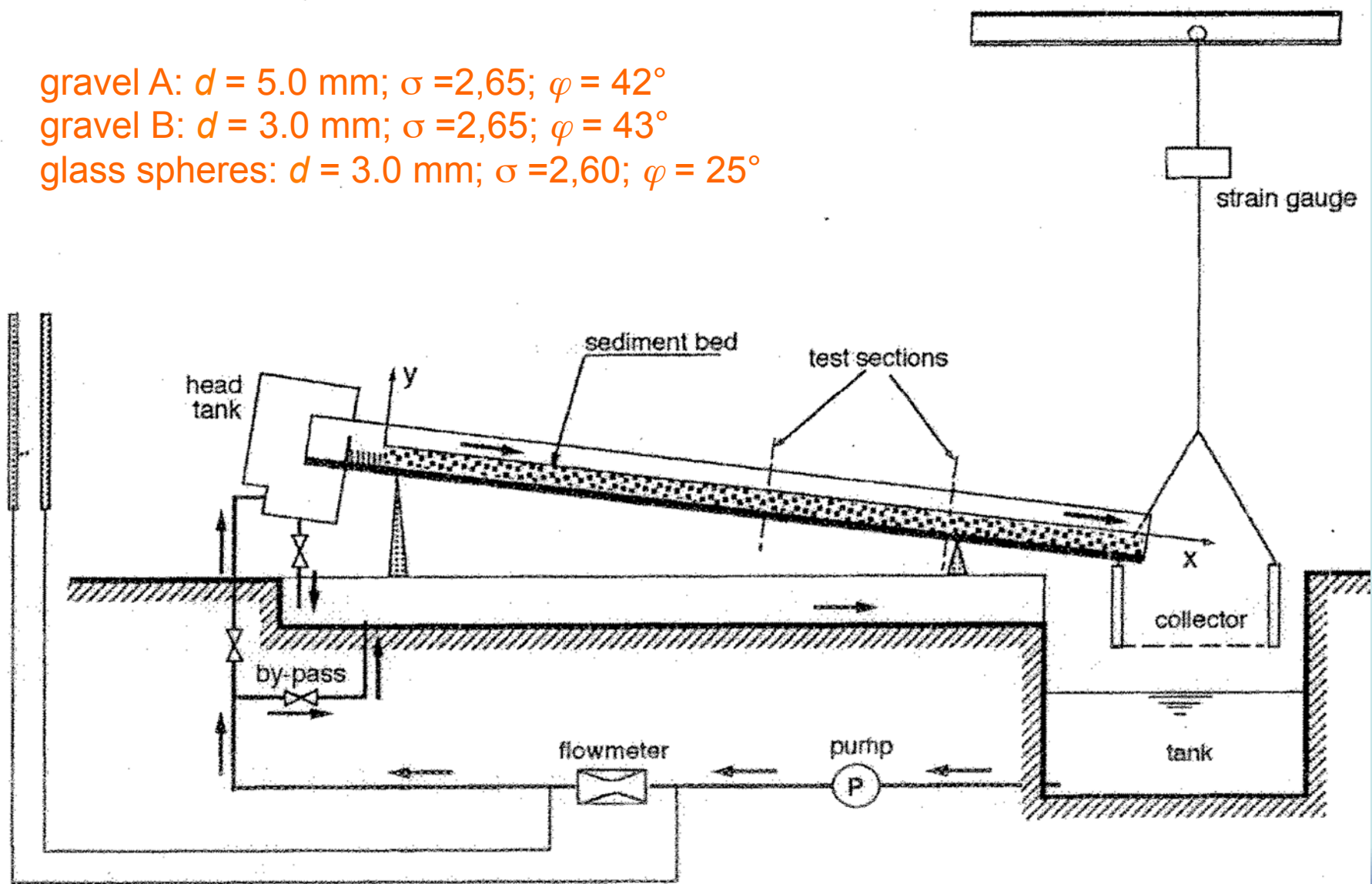


# Experiments



# Other experiments

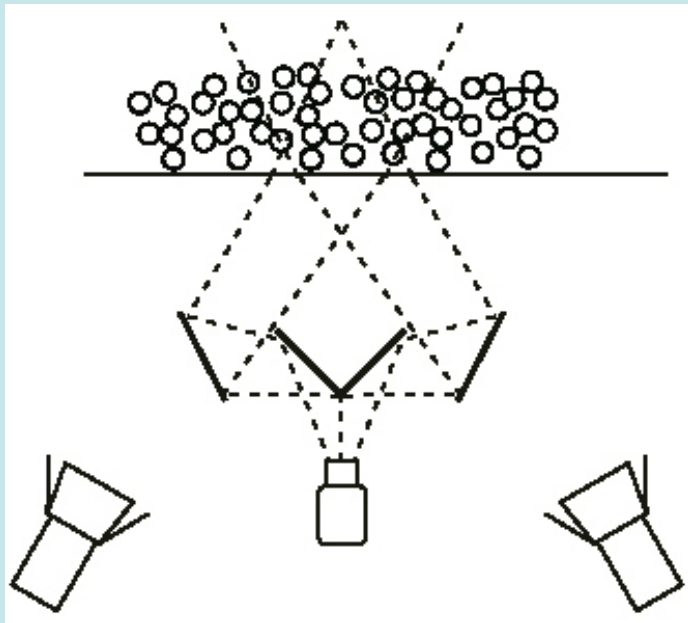
gravel A:  $d = 5.0$  mm;  $\sigma = 2,65$ ;  $\varphi = 42^\circ$   
gravel B:  $d = 3.0$  mm;  $\sigma = 2,65$ ;  $\varphi = 43^\circ$   
glass spheres:  $d = 3.0$  mm;  $\sigma = 2,60$ ;  $\varphi = 25^\circ$



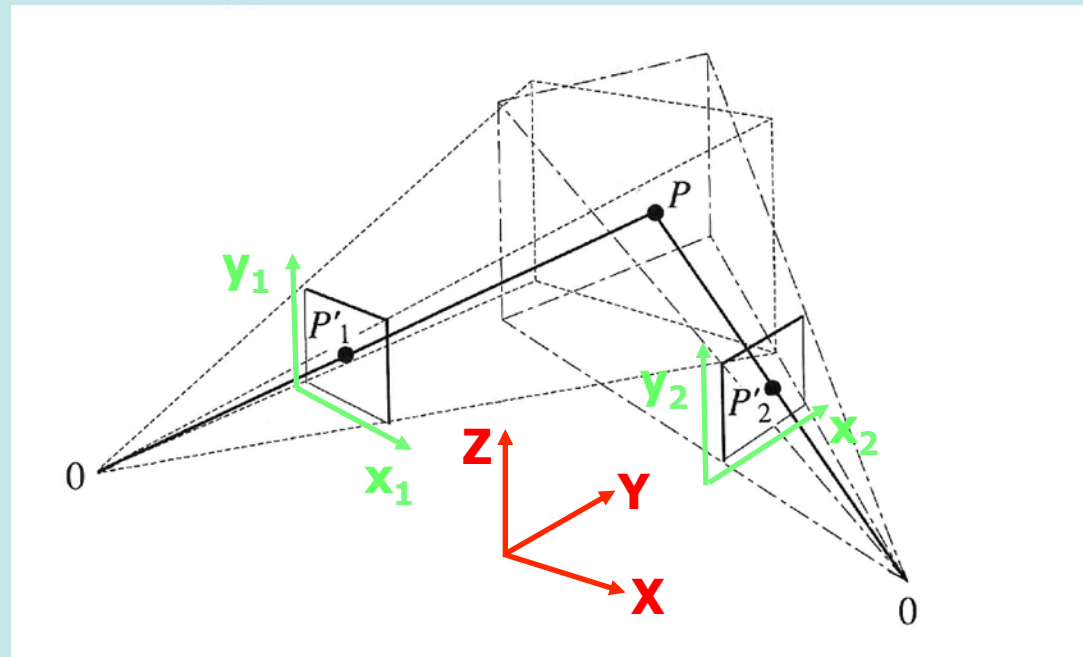


# Experimental methods

## Voronoi 3D tracking velocimetry



# Experimental methods

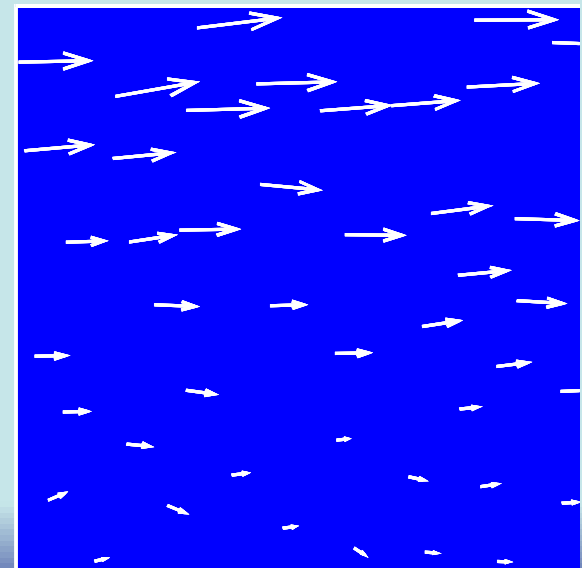
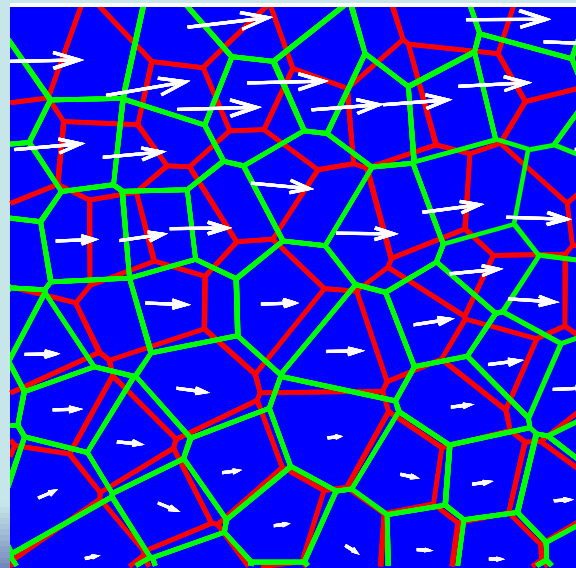
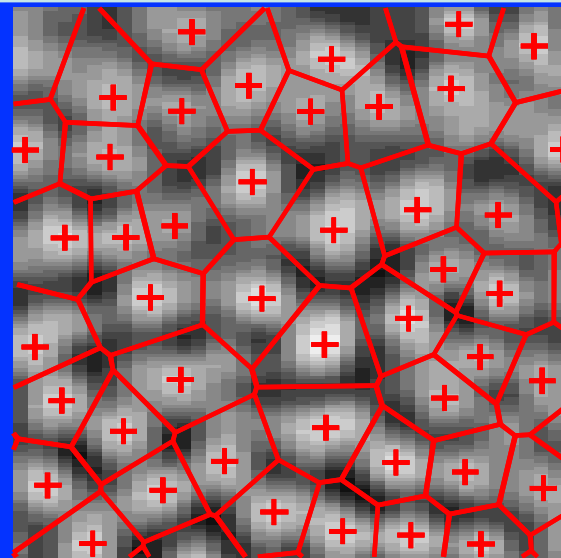
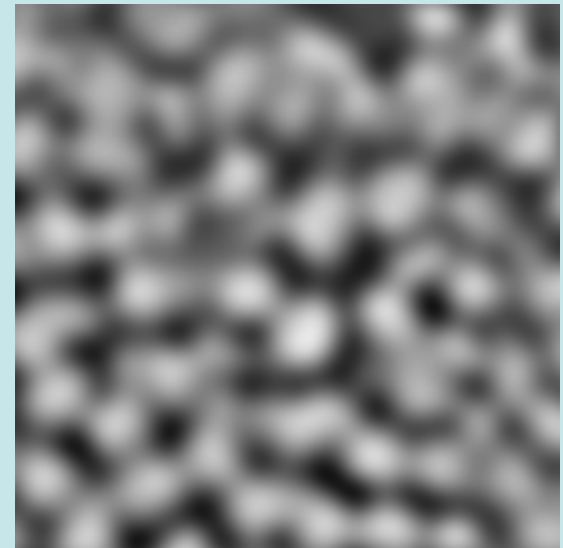
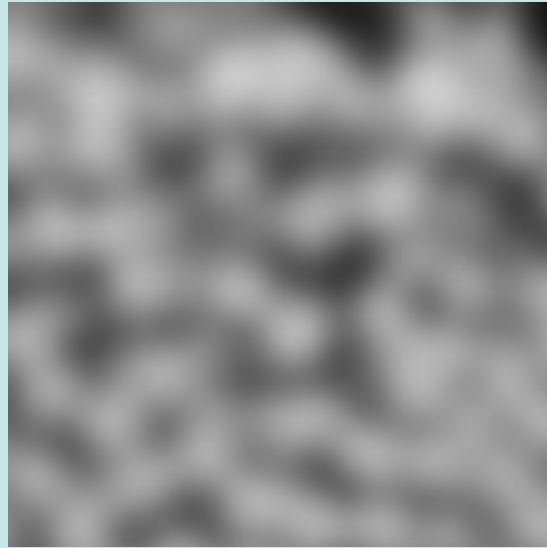
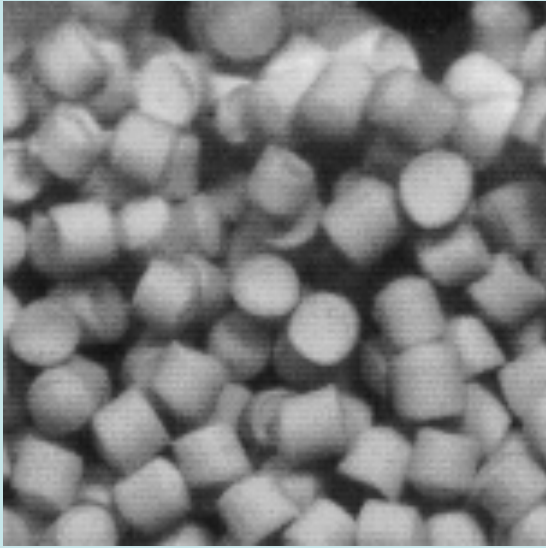


$(x_1, y_1)$   $(x_2, y_2)$  : Image coord.

$(X, Y, Z)$  : World coordinates

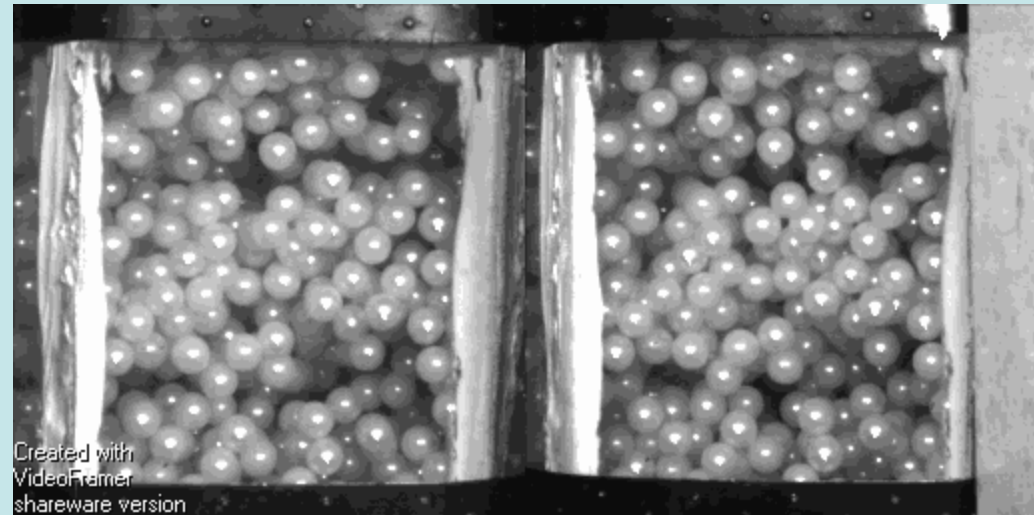
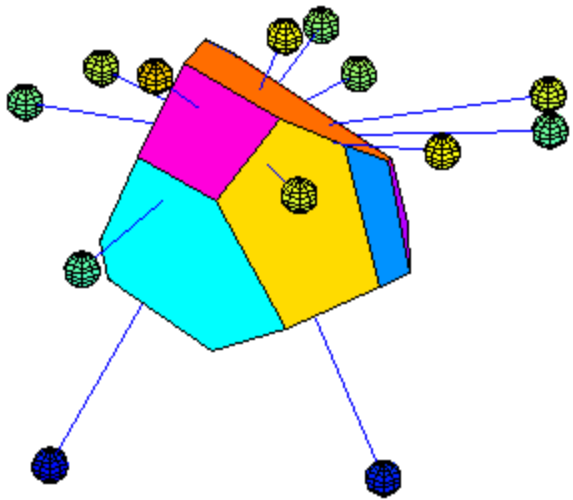
$$\left. \begin{array}{l} (x_1, y_1) \ (x_2, y_2) : \text{Image coord.} \\ (X, Y, Z) : \text{World coordinates} \end{array} \right\} [x \ y]^T = P \cdot [X \ Y \ Z \ 1]^T$$

# Experimental methods

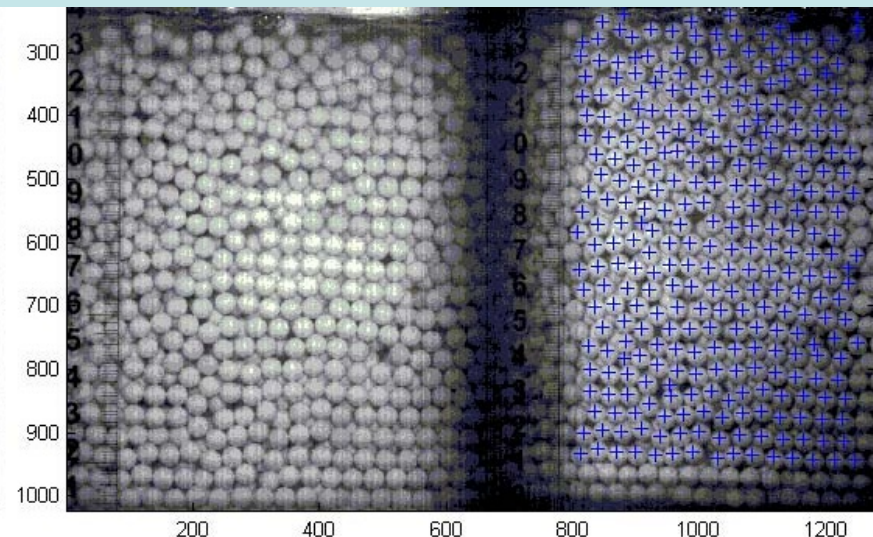
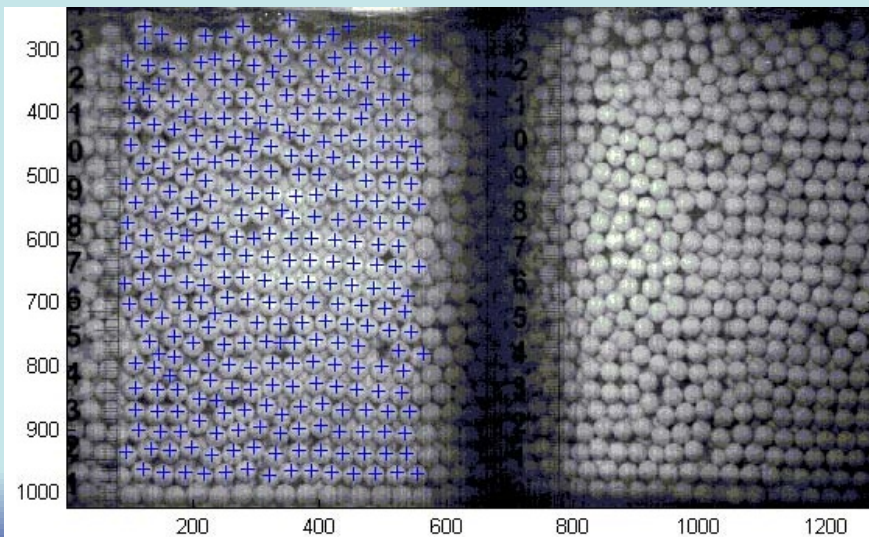
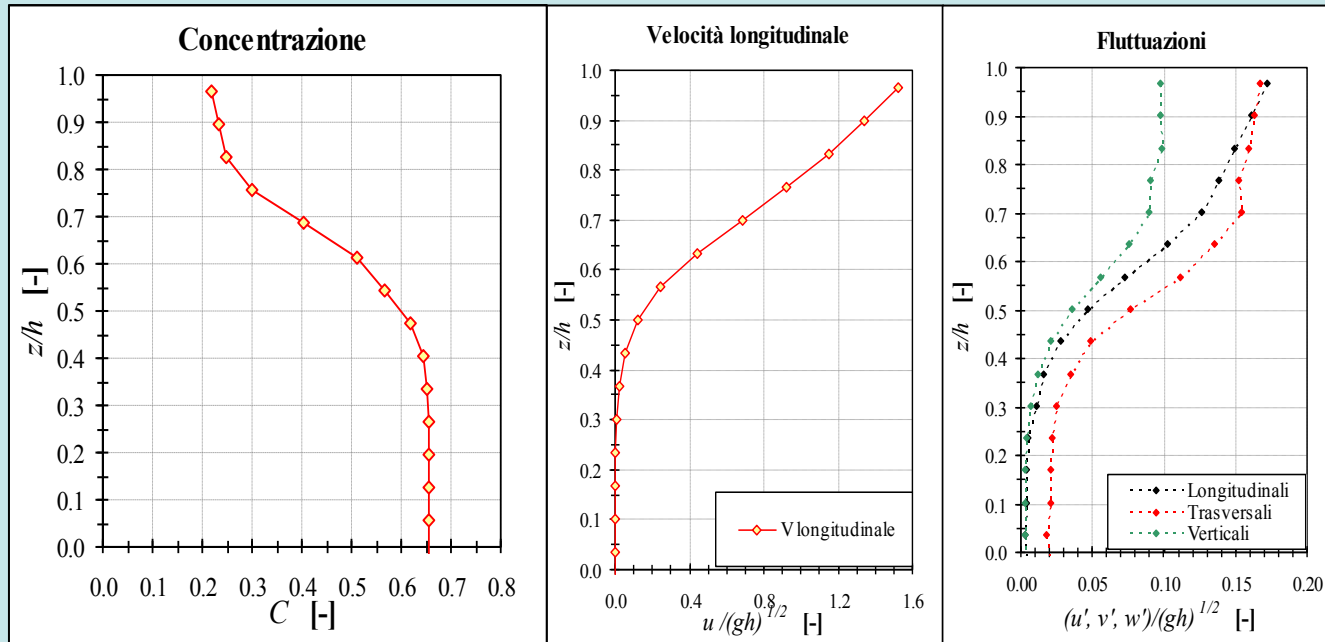




# Experimental methods

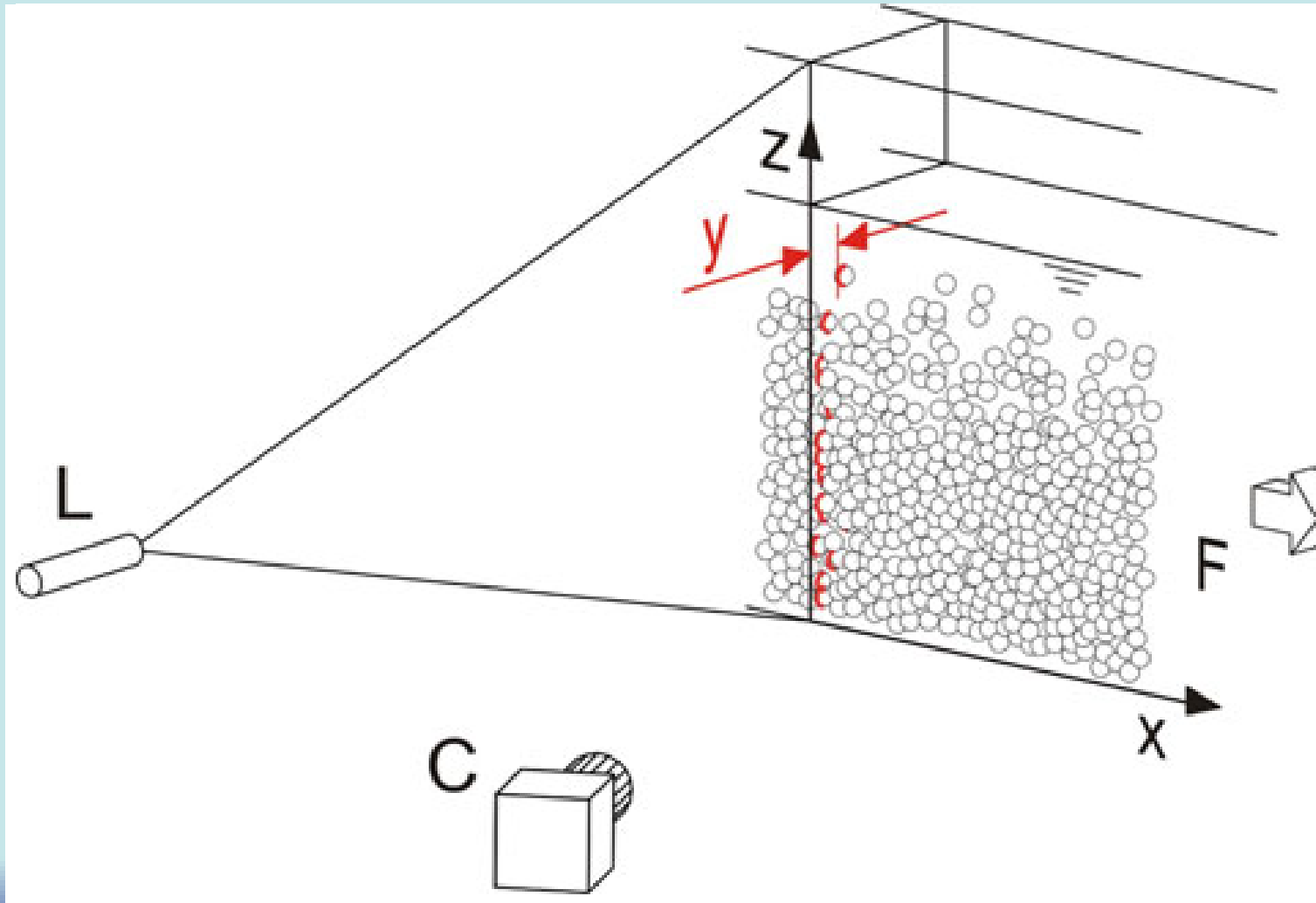


# Experimental methods

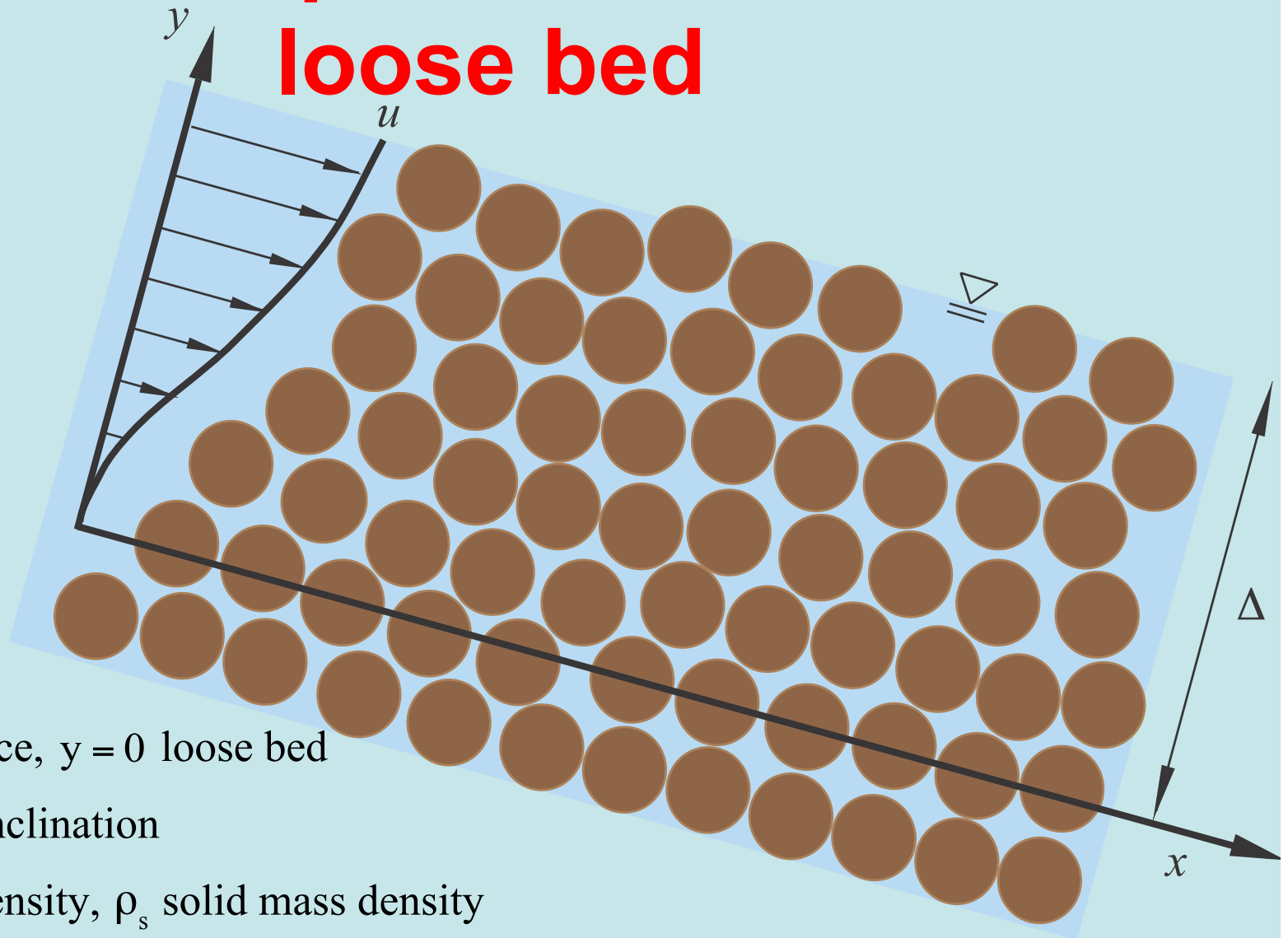


# Experimental methods

## Laserstripe method



# Saturated particle flow over a loose bed



$y = \Delta$  free surface,  $y = 0$  loose bed

$\theta$  free surface inclination

$\rho_f$  fluid mass density,  $\rho_s$  solid mass density

$\sigma = \rho_s / \rho_f$  grain specific mass,  $\nu$  grain concentration

$g$  gravitational acceleration,  $\hat{g} = (\sigma - 1)g / \sigma$  buoyant gravity

Advances in Water Resources (submitted)

# Fluid

$U$  fluid velocity,  $\eta$  fluid viscosity

$$R = \rho_f d (\hat{g}d)^{1/2} / \eta \text{ Reynolds number}$$

# Particles

$u$  grain average velocity

$C$  grain fluctuation velocity

$T = \langle C^2 \rangle / 3$  granular temperature

$St = \sigma T^{1/2} R / 9(\hat{g}d)^{1/2}$  Stokes number

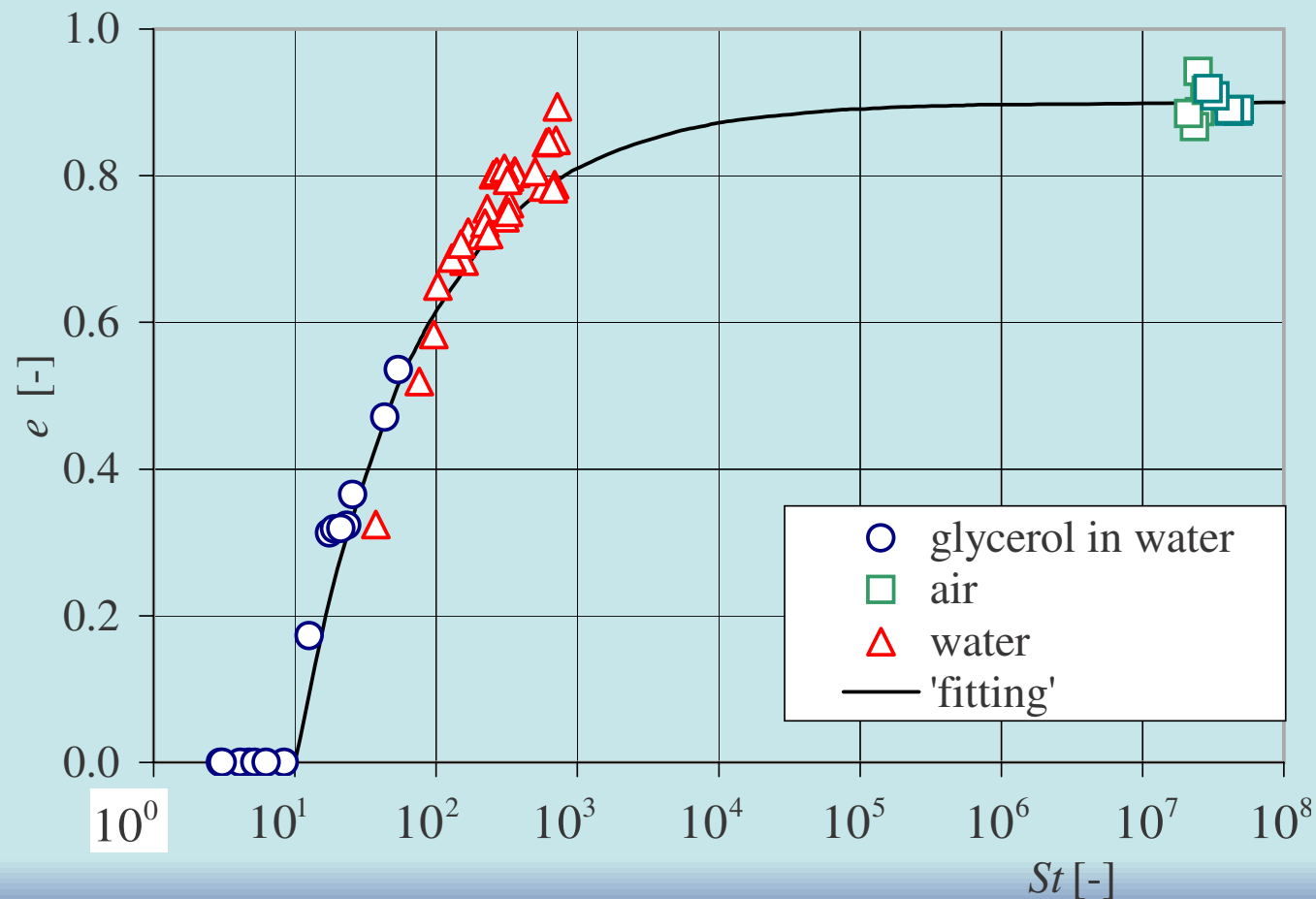
$\varepsilon$  dry restitution coefficient

$\alpha$  bed yield stress ratio

Make lengths dimensionless by grain diameter  $d$ ,  
velocities by  $(\hat{g}d)^{1/2}$ , and stresses by  $\rho_s \hat{g}d$ .

# Velocity dependent restitution

$$e = \max\left(\varepsilon - 6.9 \frac{1 + \varepsilon}{St}, 0\right)$$



# Goals

Given the angle of inclination, predict the **depth** of a saturated flow, the **total volume flux**, and the **range of inclinations** for which saturated flows are possible.

# Parameters

$$\sigma = 1.54 \quad d = 0.37 \text{ cm} \quad \varepsilon = 0.50 \quad W = 54d$$

$$\mu_w = 0.15 \quad c = 0.52 \quad \alpha = 0.60$$

# Fluid Momentum Balance

transverse:

$$P' = -\frac{1-\nu}{\sigma-1} \cos \phi$$

flow:

$$S' = -\frac{1-\nu}{\sigma-1} \sin \phi \frac{\sigma}{\sigma-1} + \frac{\nu D}{\sigma} (U - u)$$

$$D = \frac{1}{(1-\nu)^{3.1}} \left( 0.3 |U - u| + \frac{18.3}{R} \right)$$



# Grain Momentum Balance

transverse:

$$p' = -\nu \cos \phi$$

flow:

$$s' = -\nu \sin \phi \frac{\sigma}{\sigma - 1} + 2\mu_w \frac{p}{W} - \frac{\nu D}{\sigma} (U - u)$$

Diagram annotations:  
- An orange arrow labeled "wall friction" points to the term  $2\mu_w \frac{p}{W}$ .  
- An orange arrow labeled "chute width" points to the term  $\frac{p}{W}$ .

$$D = \frac{1}{(1 - \nu)^{3.1}} \left( 0.3 |U - u| + \frac{18.3}{R} \right)$$

# Depth of flow

$$\frac{d}{dy}(s + S) = -\sin \phi \frac{v(\sigma - 1) + 1}{\sigma - 1} + 2\mu_w \frac{p}{W}.$$

$$p = v \cos \phi (\Delta - y)$$

neglect the fluid shear stress in the dense flow:

$$\frac{s}{p} = \tan \phi \frac{v(\sigma - 1) + 1}{v(\sigma - 1)} - \frac{\mu_w}{W} \frac{p}{v \cos \phi}$$

obtain the dependence of s/p on y:

$$\frac{s}{p} = \tan \phi \frac{v(\sigma - 1) + 1}{v(\sigma - 1)} - \frac{\mu_w}{W} (\Delta - y)$$

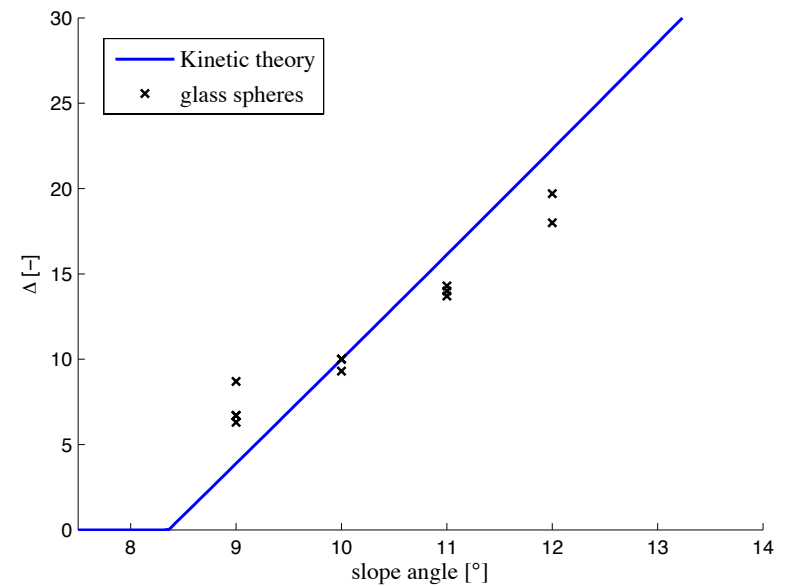
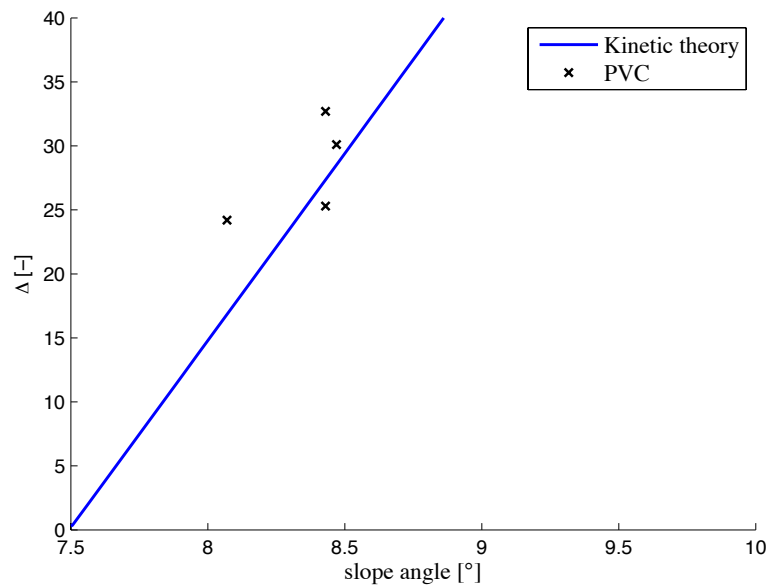
# ...depth of flow

At the bed ( $y = 0$ ),  $s/p = \alpha$ , so:

$$\alpha = \tan \phi \frac{\nu(\sigma - 1) + 1}{\nu(\sigma - 1)} - \frac{\mu_w}{W} \Delta$$

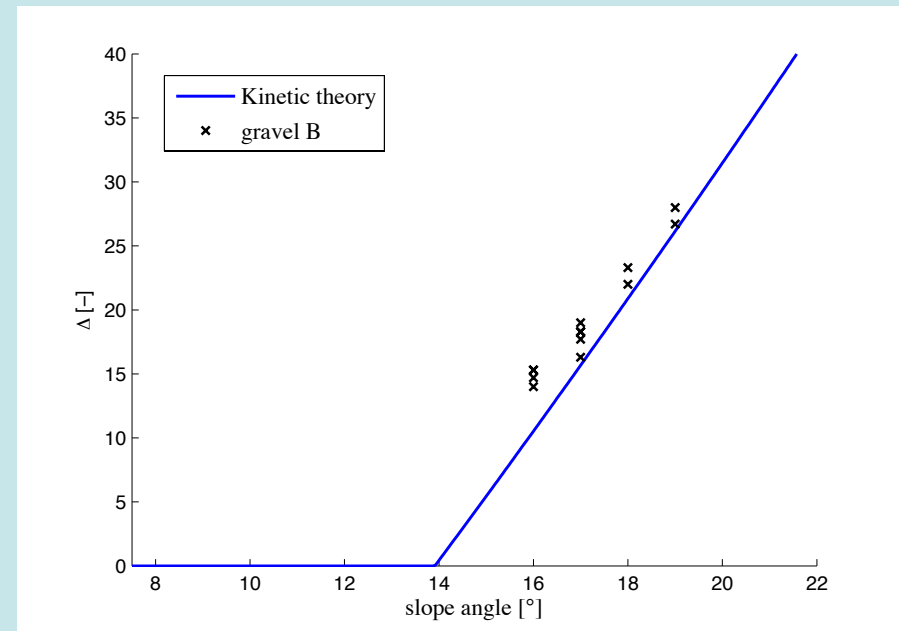
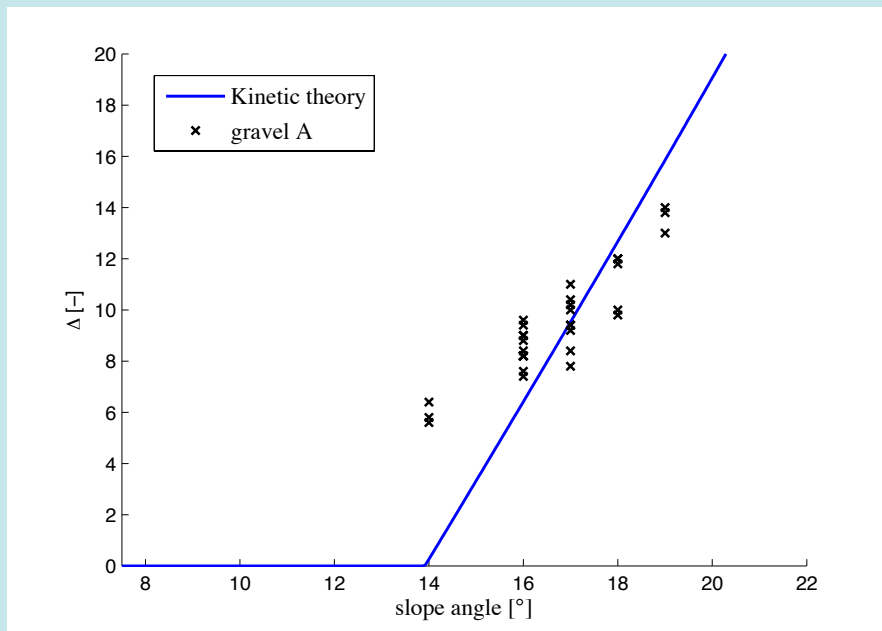
or:

$$\Delta = \frac{W}{\mu_w} \left\{ \tan \phi \left[ 1 + \frac{1}{\nu(\sigma - 1)} \right] - \alpha \right\}$$



# ...depth of flow

$$\Delta = \frac{W}{\mu_w} \left\{ \tan \phi \left[ 1 + \frac{1}{\nu(\sigma - 1)} \right] - \alpha \right\}$$



# Particle Energy Balance

$$su' - \Gamma = 0$$

$$s = \mu u'$$

$$p = 2(1+e)vGT$$

$$\mu = \frac{4J}{5\pi^{1/2}(1+e)} \frac{p}{T^{1/2}} \quad J = \frac{(1+e)}{2} + \frac{\pi}{4} \frac{(3e-1)(1+e)^2}{[24-(1-e)(11-e)]} \quad G = \frac{0.59c}{0.60-c}$$

collisional dissipation:

$$\Gamma = \frac{12}{\pi^{1/2}} \frac{vG}{L} (1-e^2) T^{3/2}$$

*Jenkins (2006, 2007)*

cluster size:

$$L = \frac{1}{2} \hat{c} G^{1/3} \frac{u'}{T^{1/2}}$$

# Concentration

Eliminate  $L$  from the energy balance and solve for  $u'/T^{1/2}$  :

$$\frac{u'}{T^{1/2}} = \frac{15}{J} \frac{1 - e^2}{\hat{c}G^{1/3}}$$

Use this to eliminate  $u'/T^{1/2}$  from the shear stress with  $s/p$ :

$$\frac{s}{p} = \left[ \frac{192}{25\pi^{3/2}} \frac{J^2(1-e)}{\hat{c}(1+e)^2} \right]^{1/3} \frac{1}{G^{1/9}} = \tan \phi \frac{\nu(\sigma - 1) + 1}{\nu(\sigma - 1)} - \frac{\mu_w}{W} (\Delta - y)$$

and substitute in:

$$\nu = \frac{0.63G}{0.60 + G}$$

# Temperature

Solve the pressure for  $T$  and obtain its variation with depth:

$$T = \frac{p}{2(1+e)vG} = \frac{\cos \phi(\Delta - y)}{2(1+e)G}$$

# Velocity

Invert the shear stress and integrate (crudely, linear profile with  $u_0 = 0$ ):

$$u' = \frac{5\pi^{1/2}}{4J} (1+e) \frac{s}{p} T^{1/2} \qquad u_{\Delta} = \frac{5\pi^{1/2}}{8} \frac{(1+e_0)T_0^{1/2}}{J_0} \alpha \Delta$$

# Velocity: a more exact integration

$$\bar{G} = \left[ \frac{192}{25\pi^{3/2}} \frac{\bar{J}^2(1-\bar{e})}{\hat{c}(1+\bar{e})^2(s/p)^3} \right]^3 \quad \bar{e} = e_0 / 2 \quad \frac{\bar{s}}{p} = \tan \phi \frac{\nu(\sigma-1)+1}{\nu(\sigma-1)} - \frac{\mu_w}{W} \frac{\Delta}{2}$$

equation to be integrated:

$$u' = \frac{5\pi^{1/2}}{4\bar{J}} (1+e) \frac{s}{p} T^{1/2}$$

velocity profile:

$$u(y) = \frac{5\pi^{1/2}}{4\bar{J}\sqrt{2\bar{G}}} \left(1 + \frac{e_0}{2}\right)^{1/2} (\cos \phi)^{1/2} \left\{ \frac{2}{5} \frac{\mu_w}{W} [(\Delta - y)^{5/2} - \Delta^{5/2}] - \frac{2}{3} \tan \phi \frac{\nu(\sigma-1)+1}{\nu(\sigma-1)} [(\Delta - y)^{3/2} - \Delta^{3/2}] \right\}$$



# Total Volume Flux

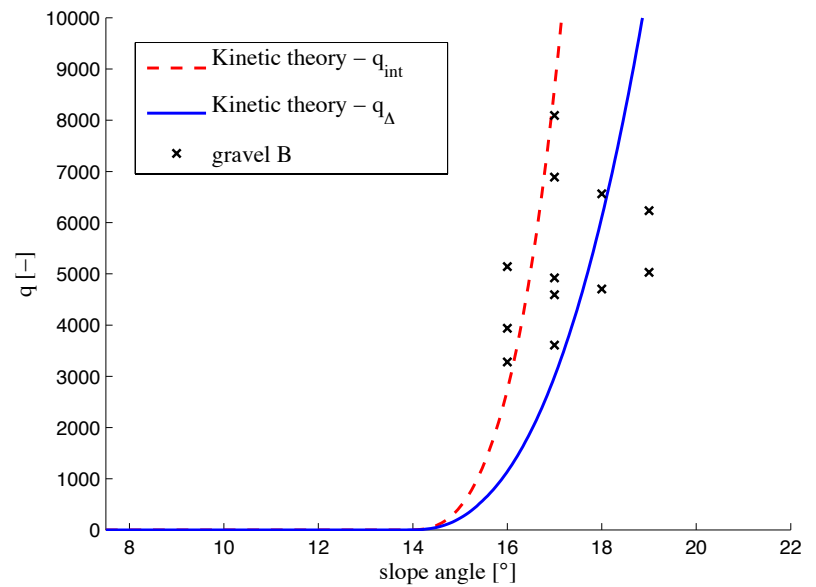
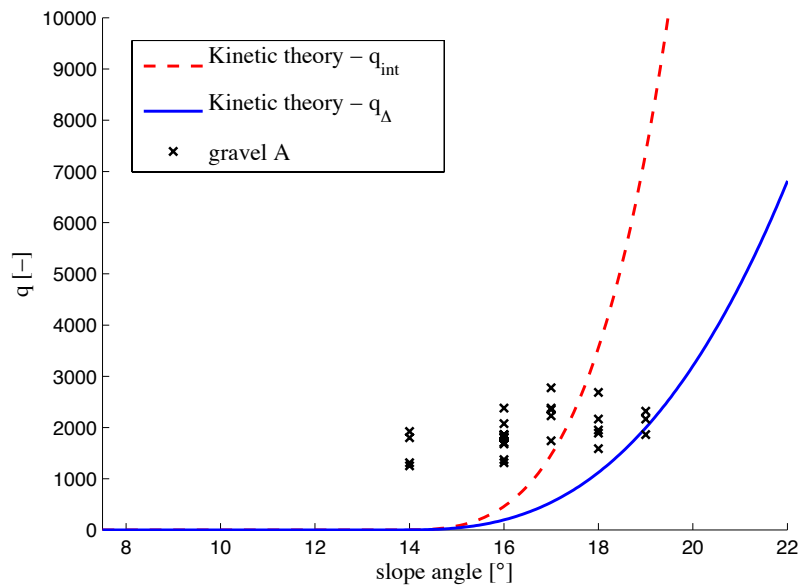
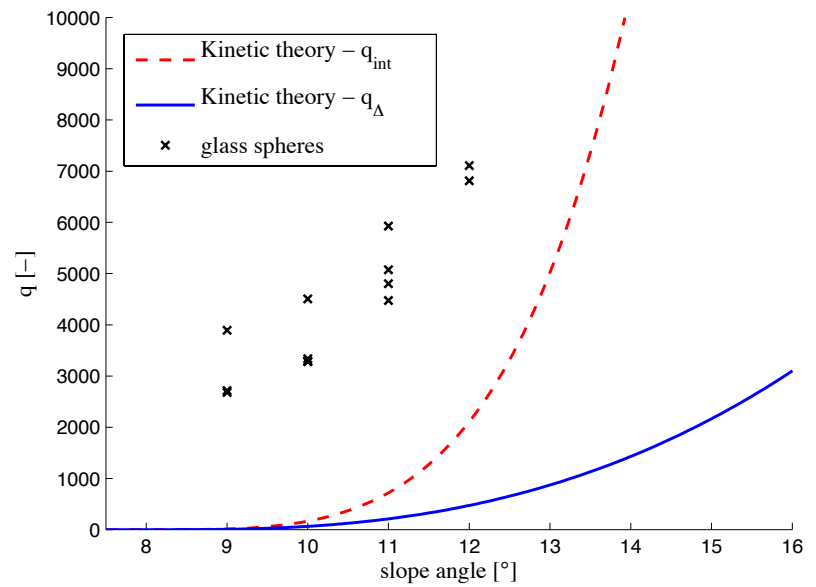
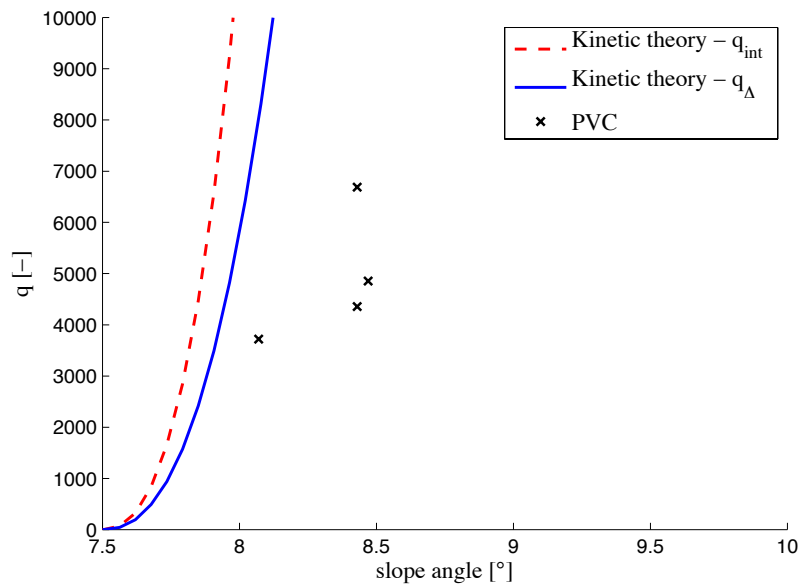
Integrate again  $u_\Delta$ :

$$q_\Delta = \frac{1}{2} W u_\Delta \Delta$$

or, more exactly:

$$\begin{aligned} q_{\text{int}} &= W \int_0^\Delta u(y) dy = \\ &= \frac{5\pi^{1/2} W}{4\bar{J}\sqrt{2\bar{G}}} \left(1 + \frac{e_0}{2}\right)^{1/2} (\cos\phi)^{1/2} \left\{ \frac{2}{5} \left(1 + \frac{1}{\nu(\sigma-1)}\right) \Delta^{5/2} \tan\phi - \frac{2}{7} \frac{\mu_w}{W} \Delta^{7/2} \right\} \end{aligned}$$

# Total Volume Flux



# Extent of inclination

$$L = \frac{1}{2} \hat{c} G^{1/3} \frac{u'}{T^{1/2}}$$

$$u' = \frac{5\pi^{1/2}}{4J} (1+e) \frac{s}{p} T^{1/2}$$

$$\frac{s}{p} = \left[ \frac{192}{25\pi^{3/2}} \frac{J^2(1-e)}{\hat{c}(1+e)^2} \right]^{1/3} \frac{1}{G^{1/9}}$$

$$L = \frac{24J}{5\pi} \frac{1-e}{1+e} \left( \frac{p}{s} \right)^2$$

Top:

$$L = 1$$

$$k \equiv \frac{s_{\Delta}}{p_{\Delta}} = \left[ \frac{24}{5\pi} J_{\Delta} \frac{(1-e_{\Delta})}{(1+e_{\Delta})} \right]^{1/2}$$

Bed: Yield

$$\frac{s_0}{p_0} = \alpha$$

## ...extent of inclination

$$\frac{\nu(\sigma - 1)}{1 + \nu(\sigma - 1)} \alpha \leq \tan \phi \leq \frac{\nu(\sigma - 1)}{1 + \nu(\sigma - 1)} k$$

observed

predicted

PVC:

$$7.5^\circ < \phi < 9^\circ$$

$$7.5^\circ < \phi < 10.2^\circ$$

sand:

$$14^\circ < \phi < 20^\circ$$

$$14^\circ < \phi < 22^\circ$$

glass:

$$9^\circ < \phi < 12^\circ$$

$$8^\circ < \phi < 21^\circ$$



# Conclusion



A relatively simple theory based on a velocity-dependent coefficient of restitution and an extension of the kinetic theory to very dense, very dissipative grain interactions has the capability of reproducing the depth, volume flux, and range of inclination angle for dense, saturated, fluid-particle flows

Extend to under-saturated and oversaturated flows, mixtures, and unsteady, developing flows.



Benoit Spinewine



Jim Jenkins



Hervé Capart



Aronne Armanini

Thank you  
*M.L.L.*  
[michele.larcher@unitn.it](mailto:michele.larcher@unitn.it)



Luigi Fraccarollo