

Two transitions in suspensions: Contact networks in shear thickening & Inertial flow transitions

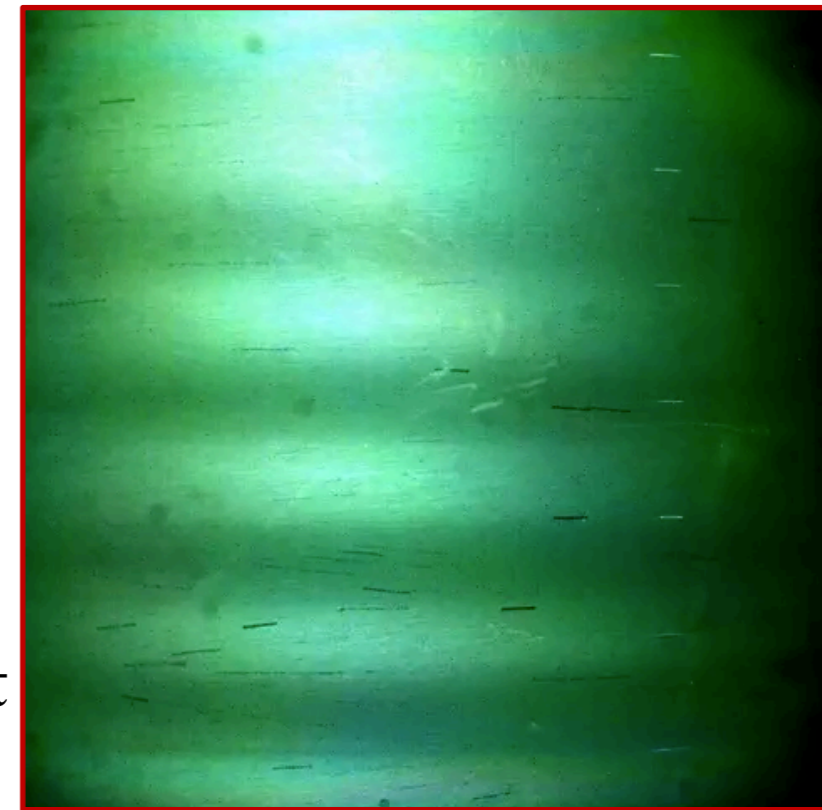
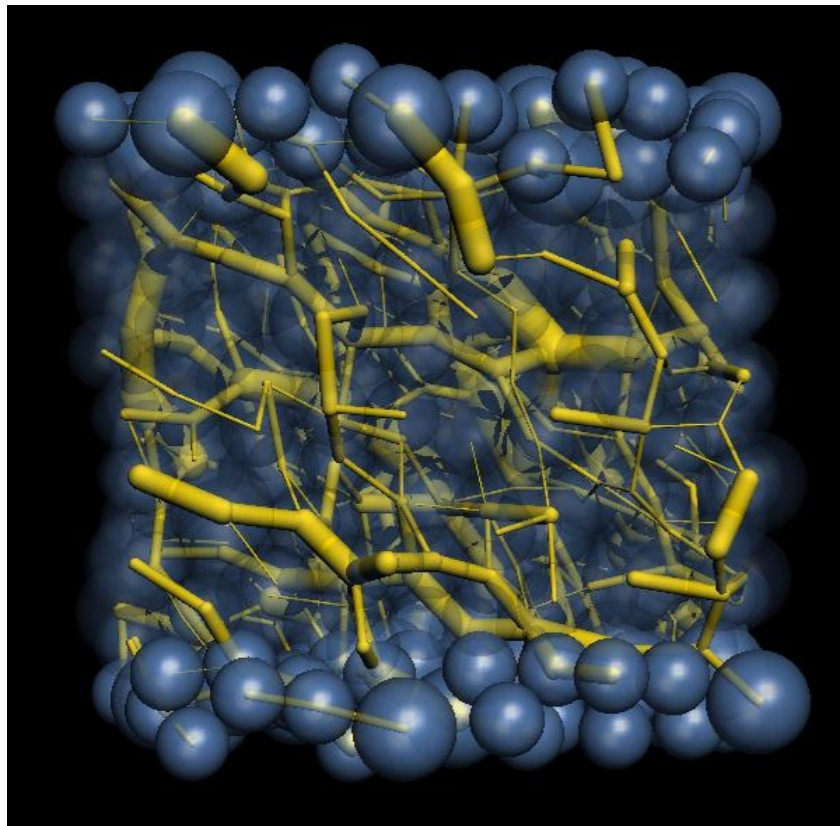
Jeff Morris

Levich Institute

and Chemical Engineering

CUNY City College of New York

morris@ccny.cuny.edu



KITP

**Multiphase Flows in
Geophysics and the Environment
November 2, 2022**

Presenting the work of

**Omer Sedes (NovoSenso), Aritra Santra (soon at IIT / ISM Dhanbad)
Madhu Majji (MIT, post-doc), Lina Baroudi (Manhattan College)**

Special credit to Romain Mari (CNRS Grenoble), Ryohei Seto (Wenzhou Inst.)

With colleagues

Mort Denn, Bulbul Chakraborty (Brandeis Univ.), Sanjoy Banerjee

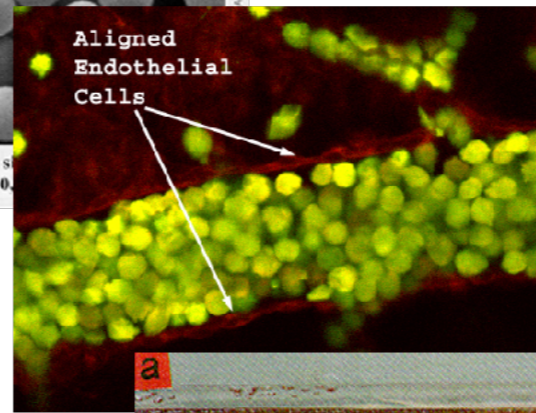
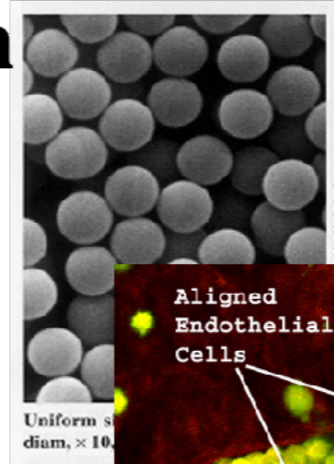
Supported by

US National Science Foundation, Mondelez & Halliburton

Suspensions

Nanoparticle
dispersions
&
colloids

10nm - 1 μm

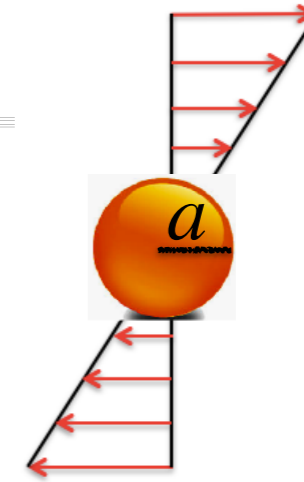
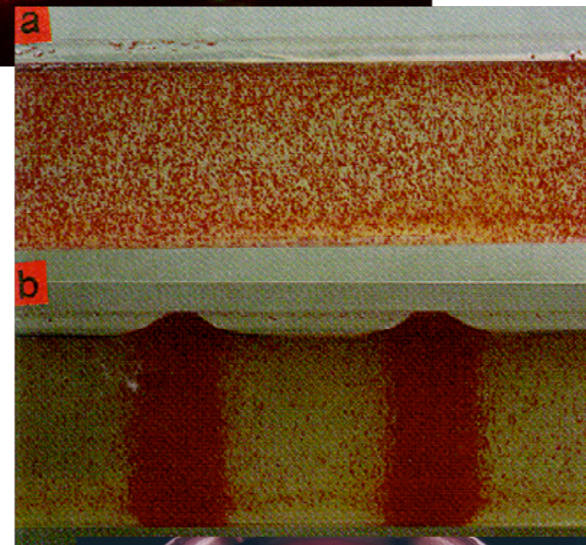


Blood cells

Noncolloidal
dispersions

Wet granular
material
(sand)

1 mm



$$u_x = \dot{\gamma}y$$

$$Re_p = \frac{\rho \dot{\gamma} a^2}{\eta}$$

Suspensions in nature ...



Jan 9 2018. Montecito
Image: Mike Eliason via AP.

Jan 9 2018. San Luis Obispo

Fluid mechanics of suspensions has major consequences!
Property and flow models are needed.

Complexity can be enormous.

Model material: “near-hard-sphere” suspensions.

Morris *Phys. Rev. Fluids* 2020

Flow transitions in suspensions

Hoffman
Trans. Soc. Rheol. 1972

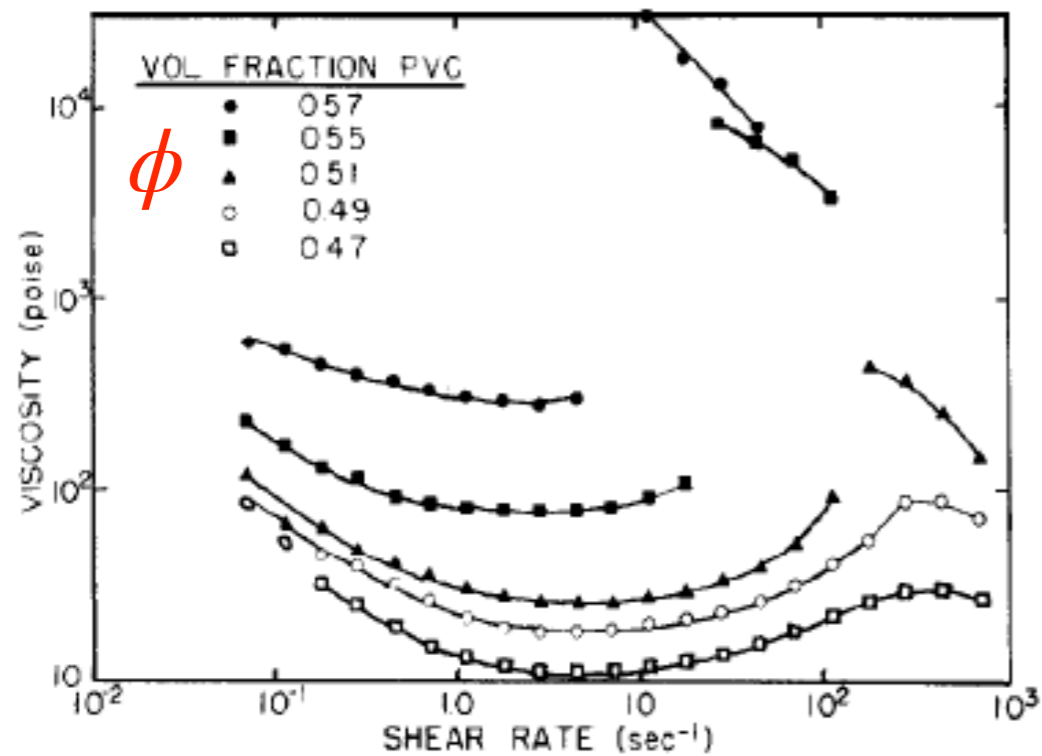


Fig. 4. Effect of volume fraction of 1.25 μ PVC in dioctyl phthalate upon viscosity discontinuity at 25°C.

Rheological property transition:

abrupt shear thickening

SIMULATIONS

$\phi > 0.5$

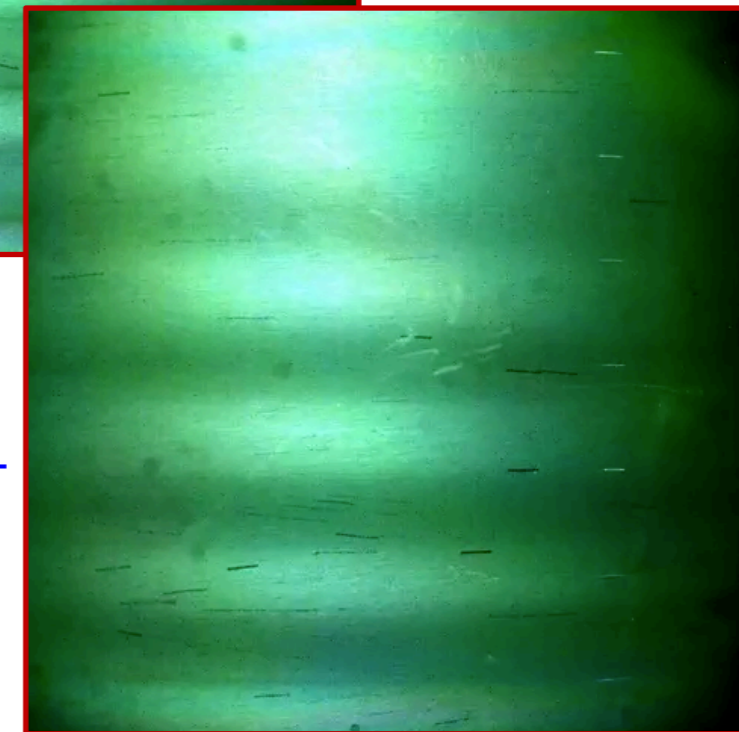
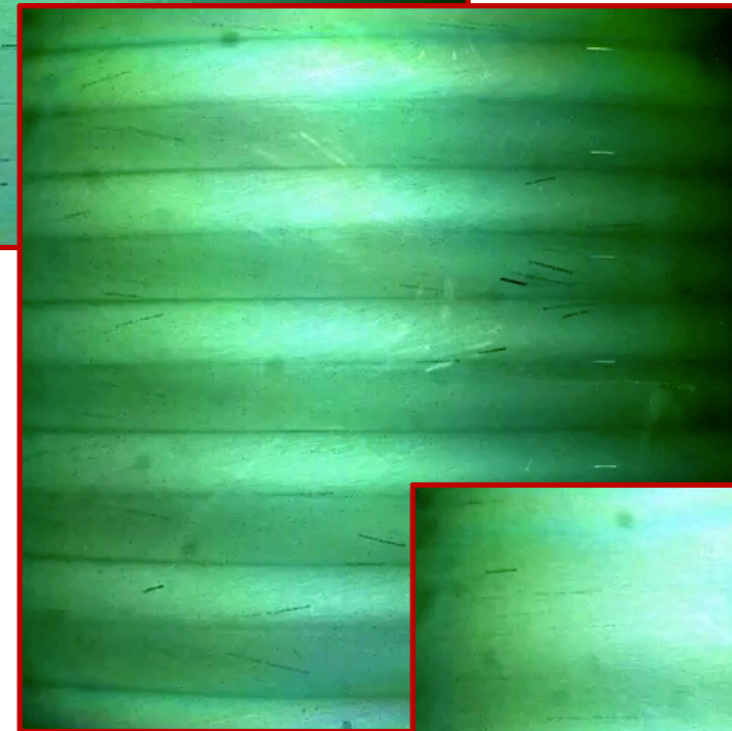
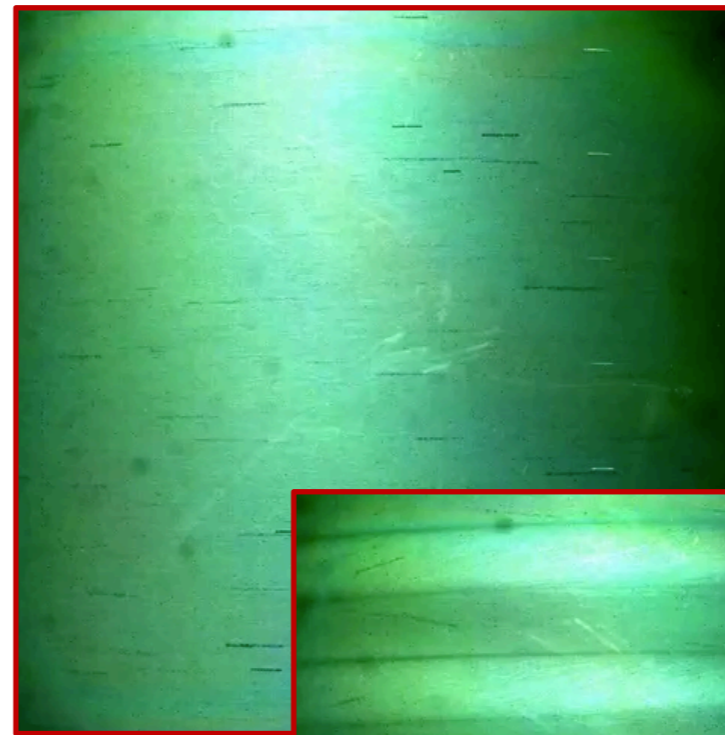
*Inertially-driven
flow state transition:*

suspension

Taylor-Couette flows

EXPERIMENTS

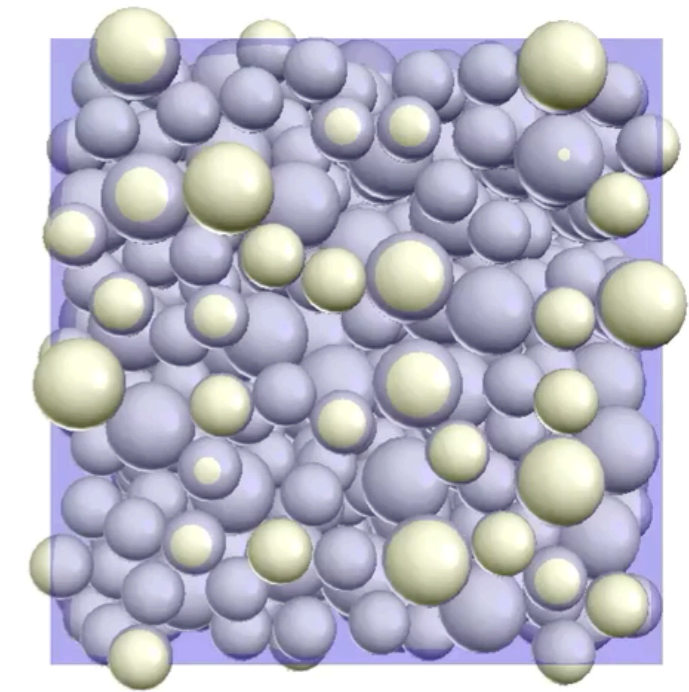
$0 < \phi \leq 0.4$



Simulation method

Lubrication flow + frictional DEM (LF-DEM)

- Hydrodynamic interactions: *Lubrication only*
- Contact model—discrete-element modeling (DEM): *Friction at contact* (Cundall & Strack 1979)
- Conservative force: *Stabilizing repulsion*
Charge or polymer coating



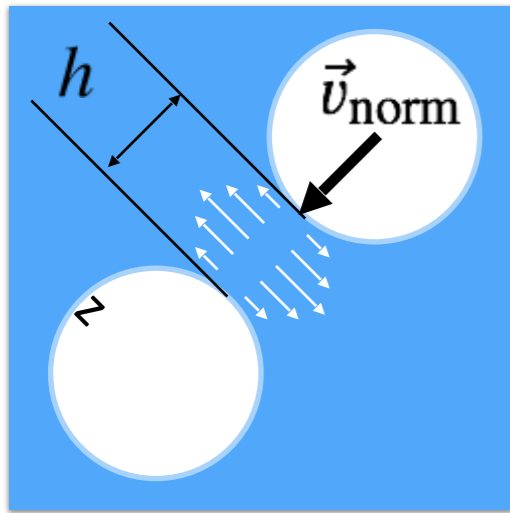
Overdamped motion ($Re = Re_p = 0$): balance forces and torques

$$0 = F_H + F_C + F_R$$

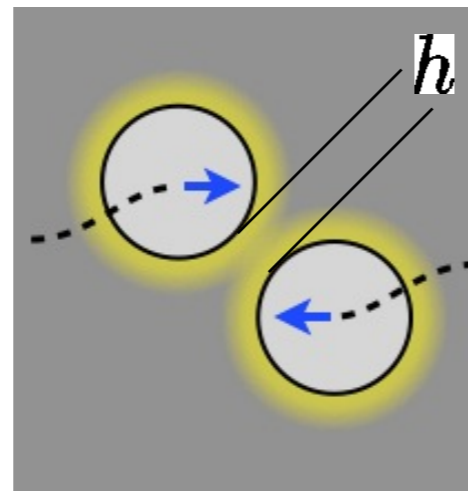
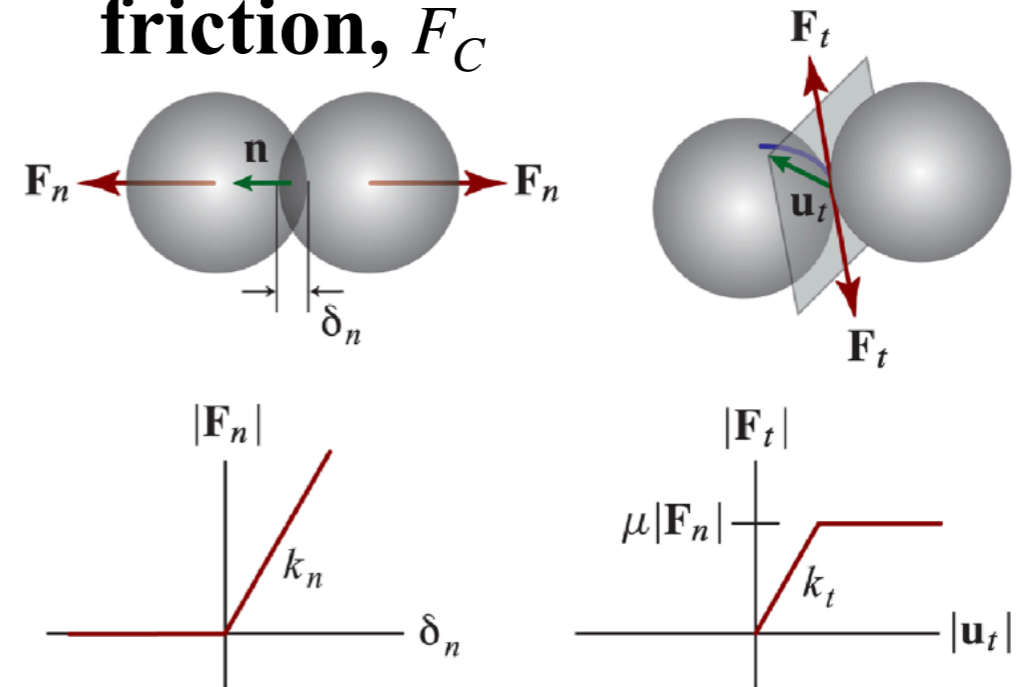
Forces

squeeze mode
lubrication, F_H

$$\vec{F}_{\text{lub}} \propto -\frac{1}{h} \vec{v}_{\text{norm}}$$



contact &
friction, F_C

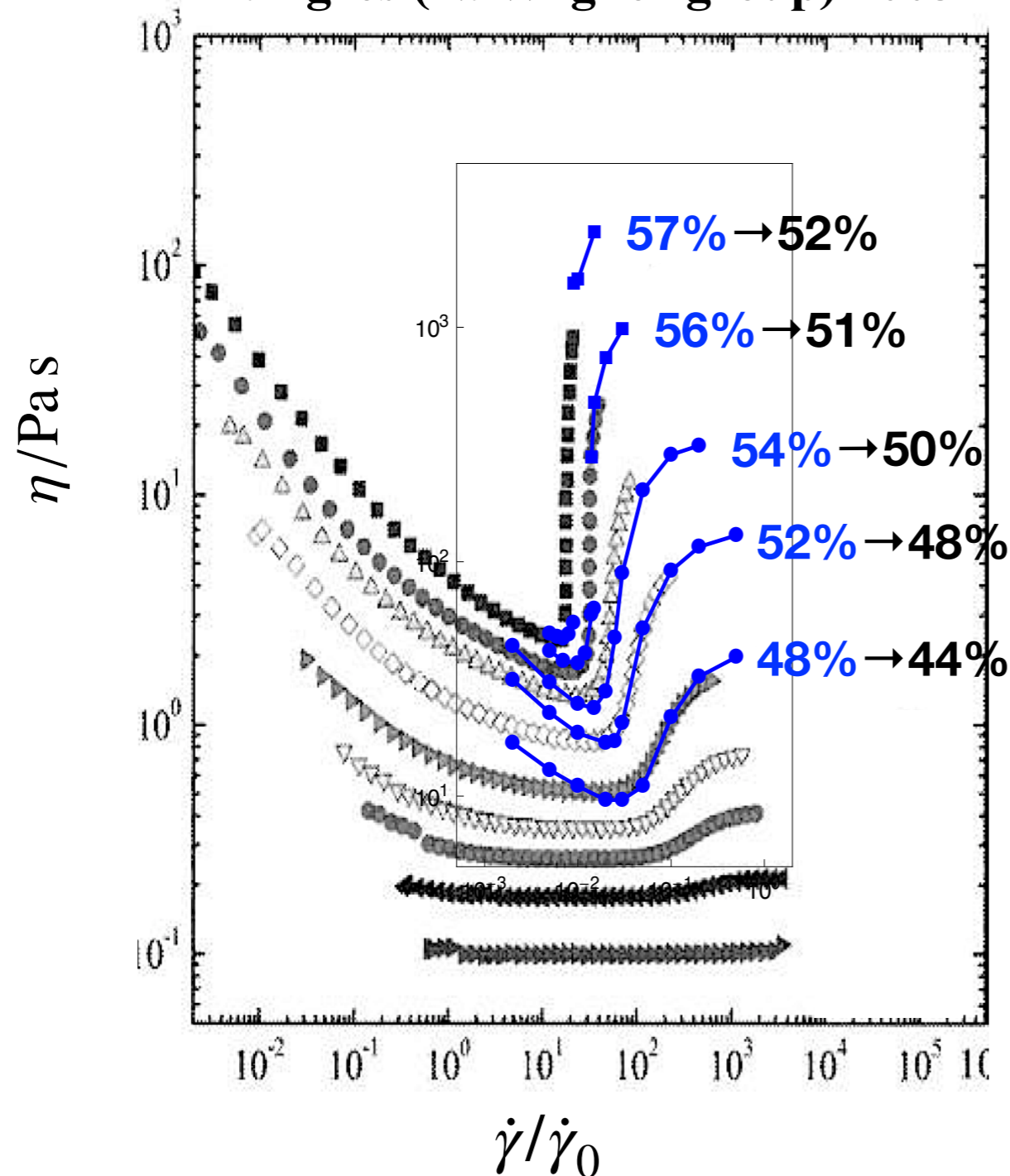


Repulsive double layer force

$$F_R = F_R(0)e^{-\kappa h}$$

Comparison with experimental data

R. Egres (N. Wagner group) 2005



Silica particles

$$a = 225 \text{ nm}$$

polyethylene glycol

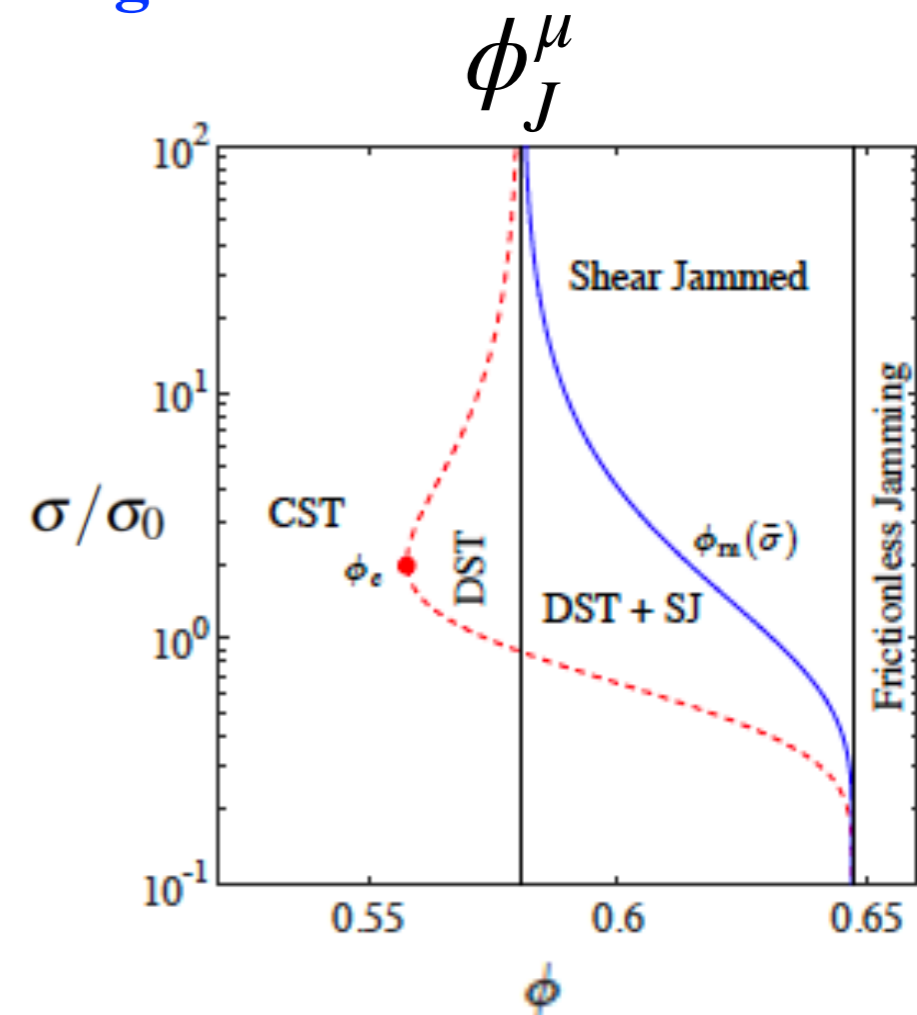
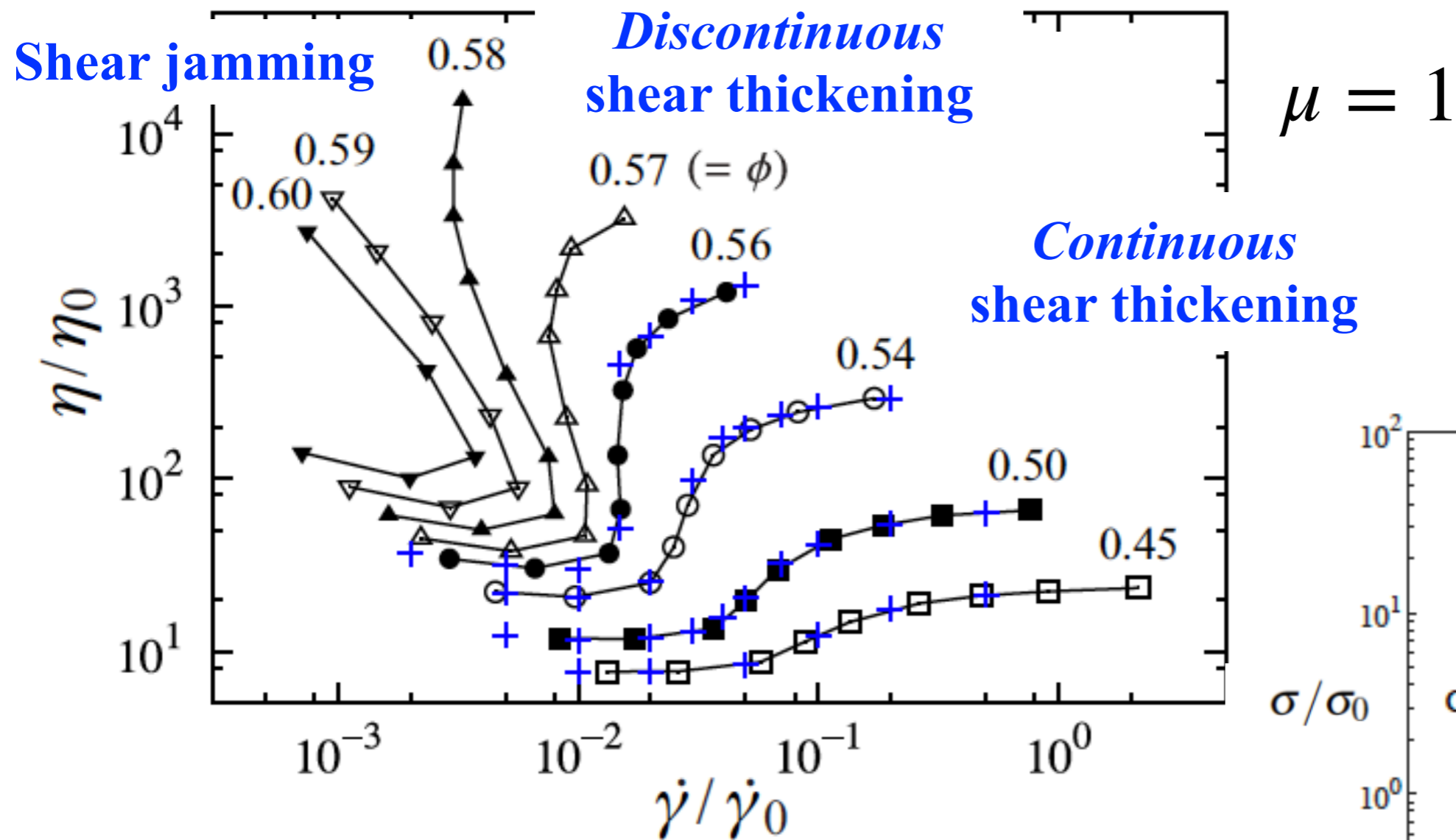
$$\eta_0 = 0.049 \text{ Pa s}$$

$$\dot{\gamma}_0 \equiv \frac{|F_R(0)|}{6\pi\eta_0 a^2} = 2 \times 10^3 / \text{s}$$

$$\longrightarrow |F_R(0)| \approx 0.1 \text{ nN}$$

See also : Y.-F. Lee, N. J. Wagner 2020 *J. Rheol.*

Scope of behavior in the lubricated-to-frictional scenario

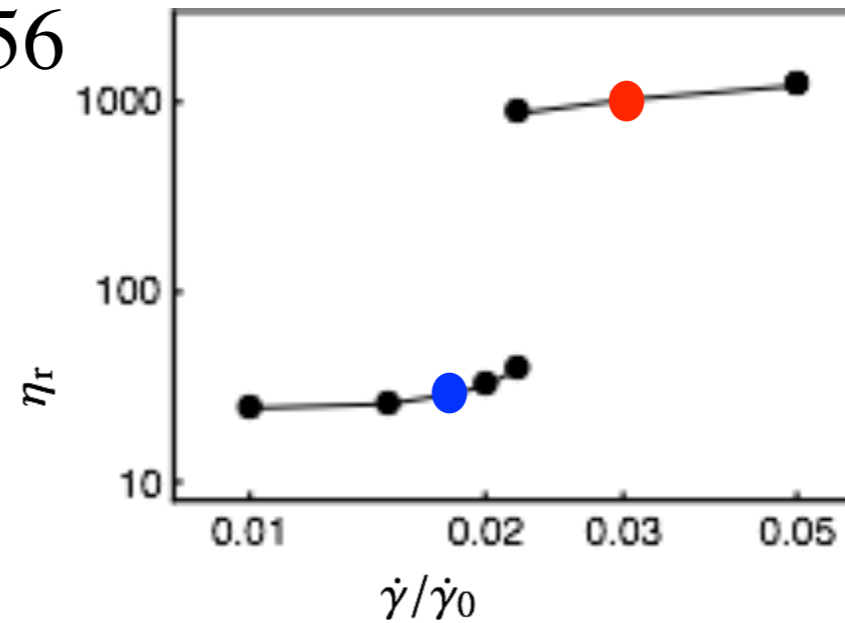


Mari, Seto, Denn & Morris *PRE* 2015

Morris *Phys. Rev. Fluids* 2018; *Ann. Rev. Fluid Mech.* 2020

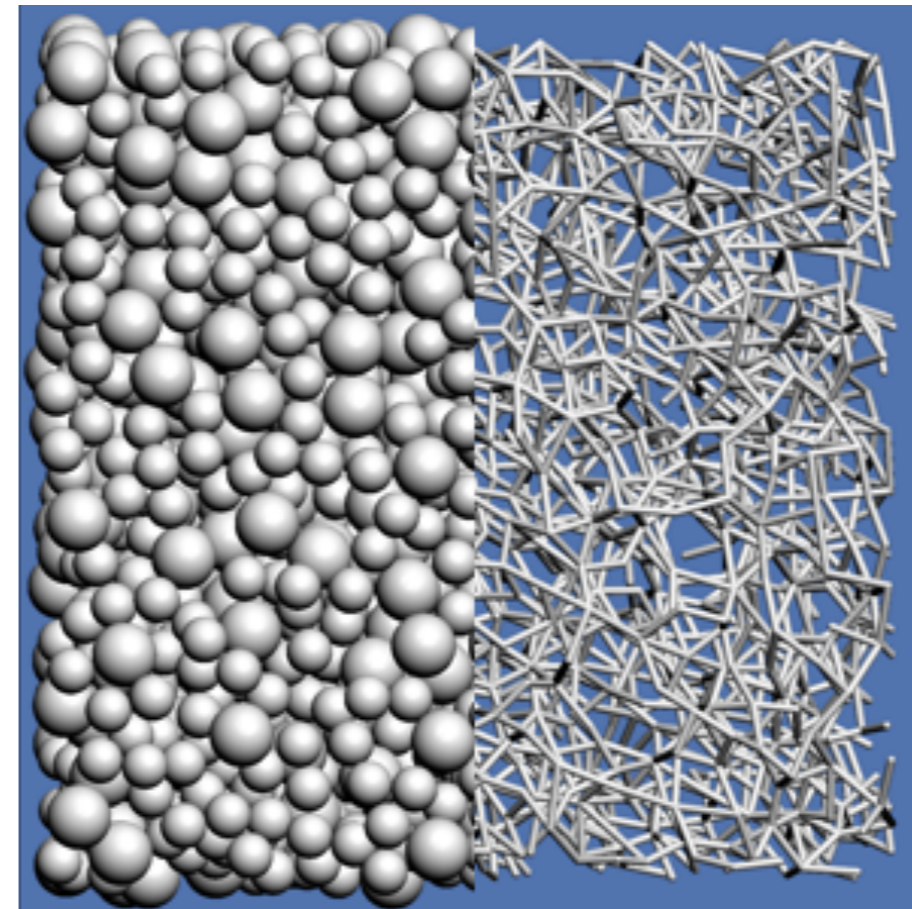
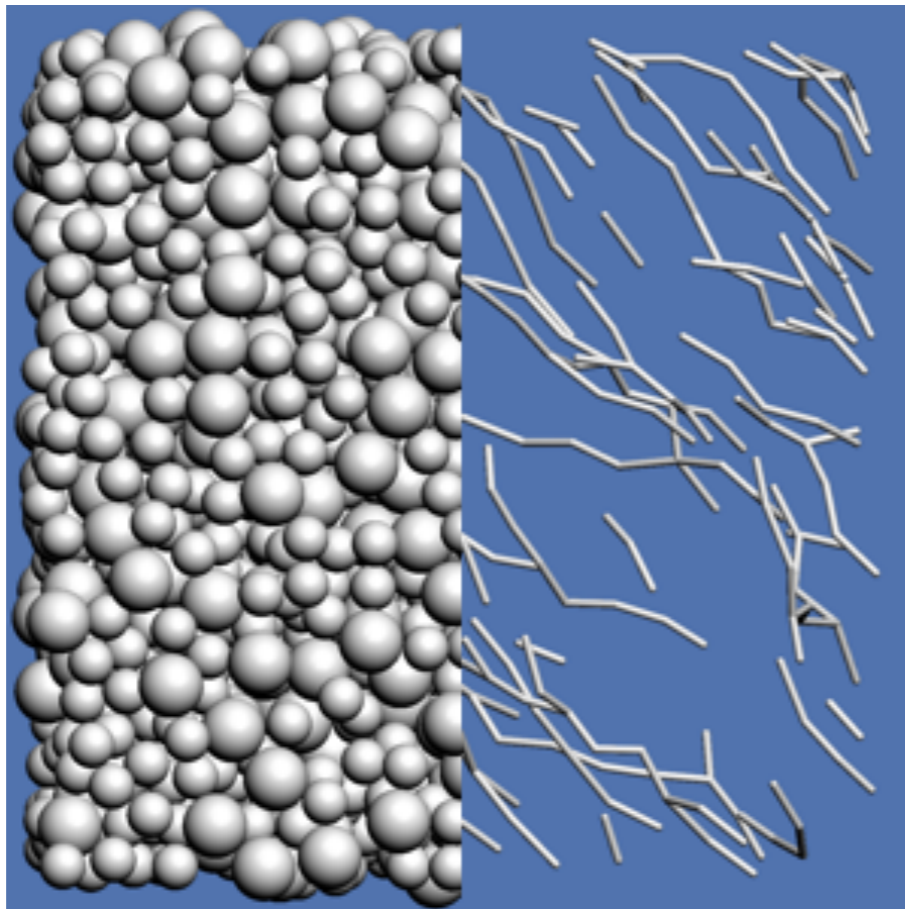
Visualizing the transition: frictional contact network

$$\phi = 0.56$$

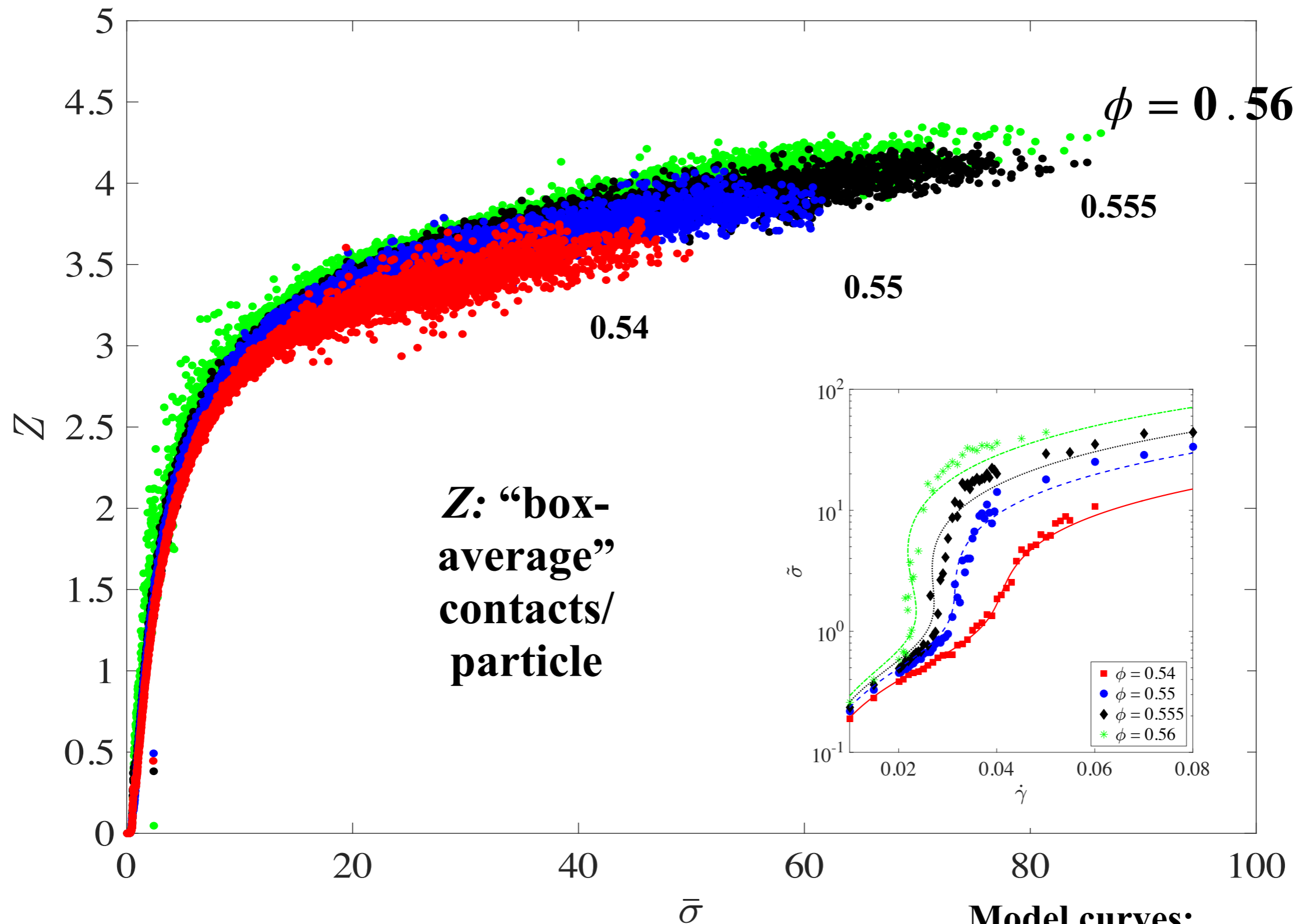


low viscosity

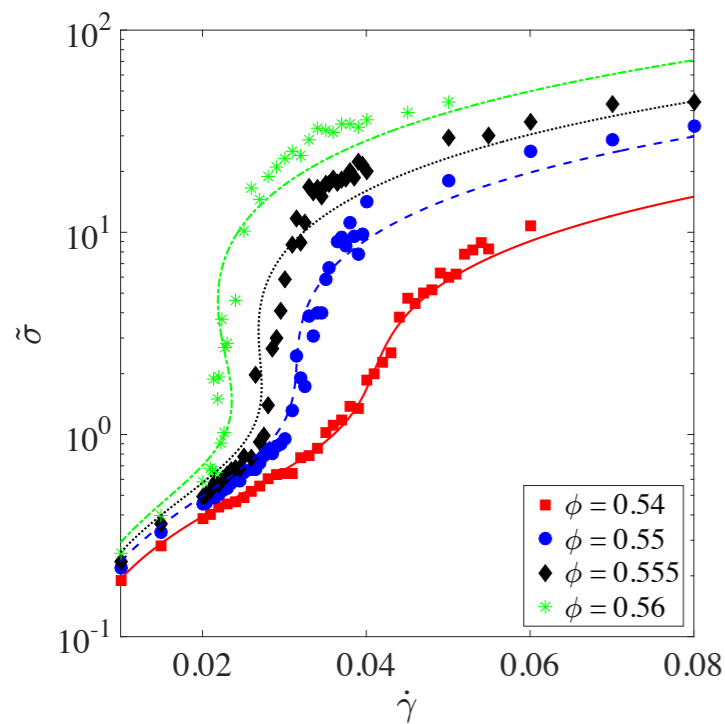
high viscosity



Stress \iff Contacts



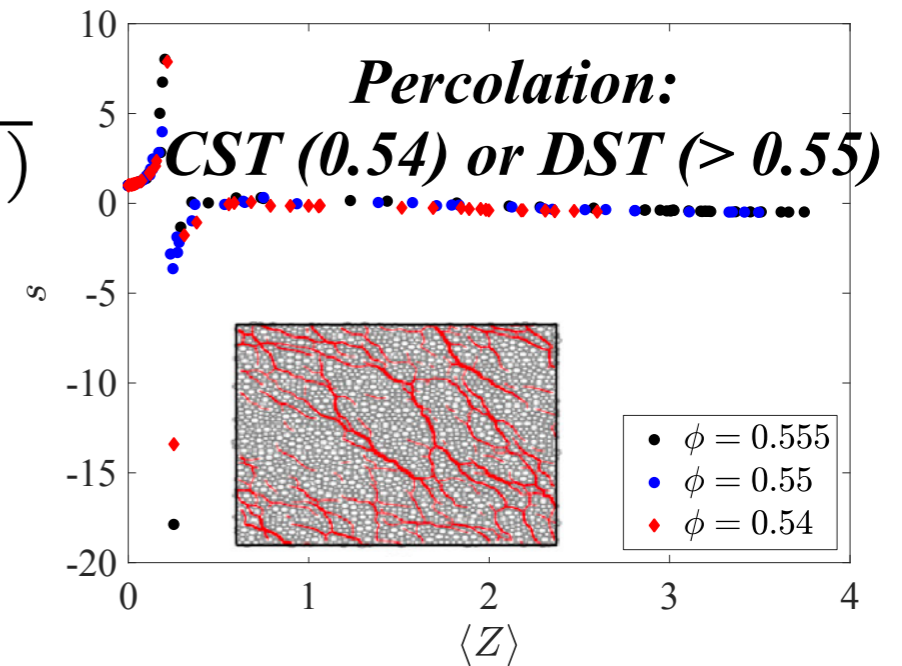
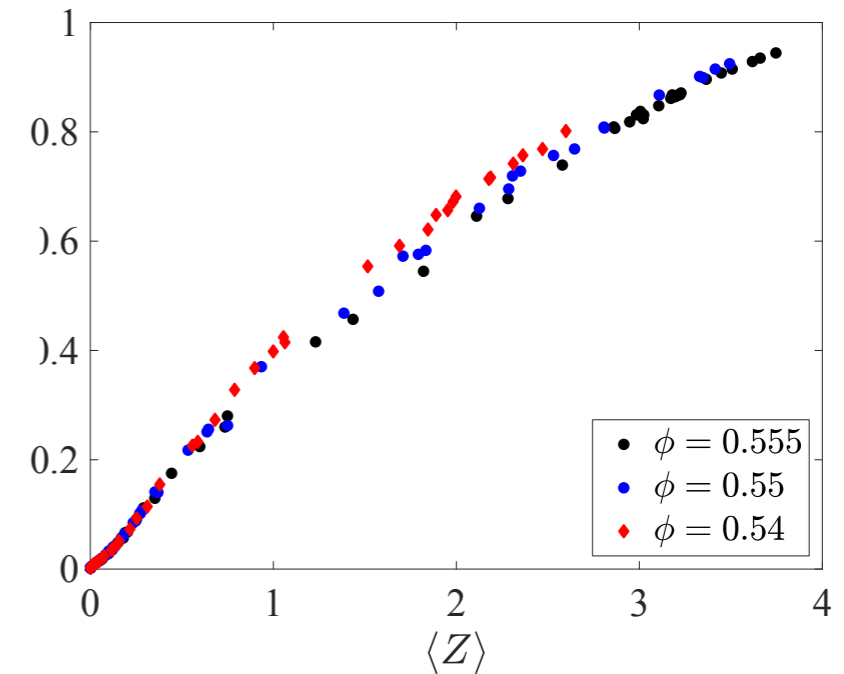
Network: begin with contacts and percolation



Largest connected component, as fraction of total particles $\langle p \rangle$

$$S \equiv \frac{1 + \langle Z \rangle^2}{(2\langle Z \rangle - \langle Z^2 \rangle)}$$

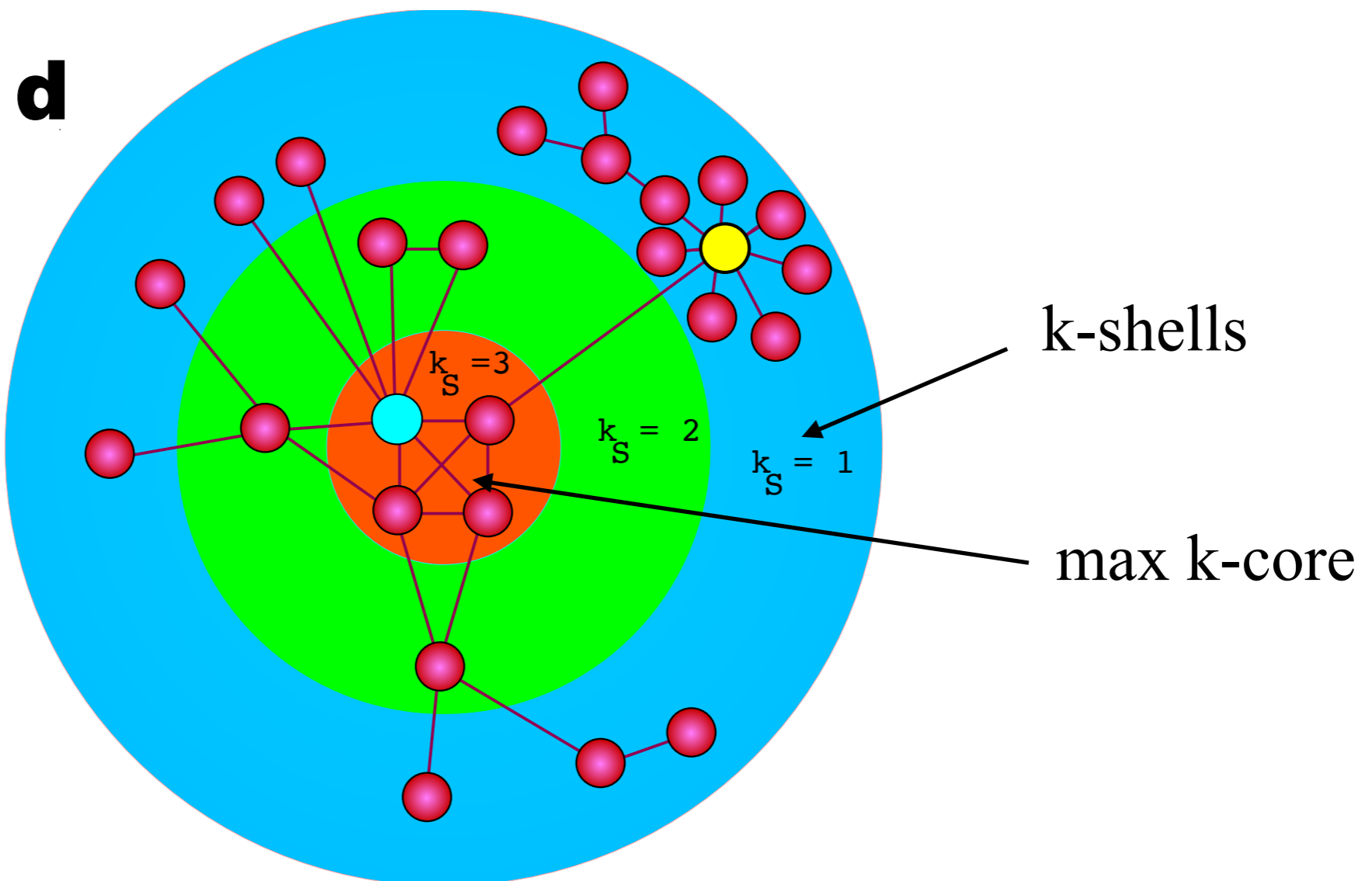
Network susceptibility: divergence at percolation



k-core network decomposition

Seidman (1983)

Given a graph $G(V,E)$: Maximal subgraph with degree at least k ,
obtained by iterative pruning

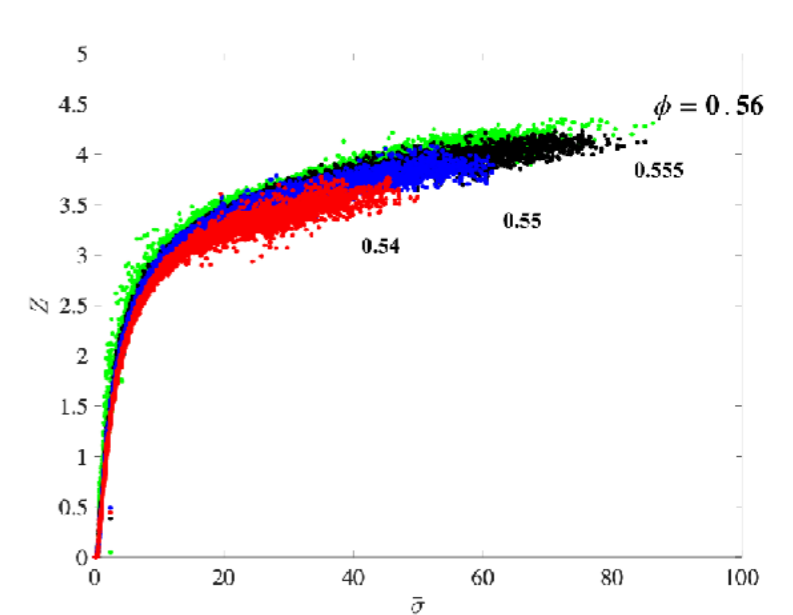
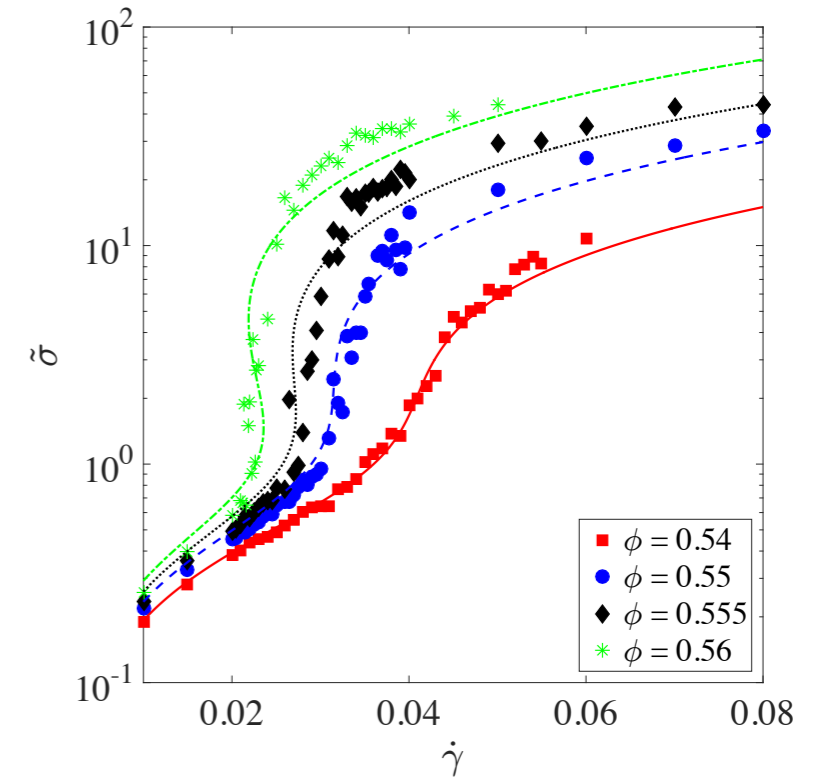
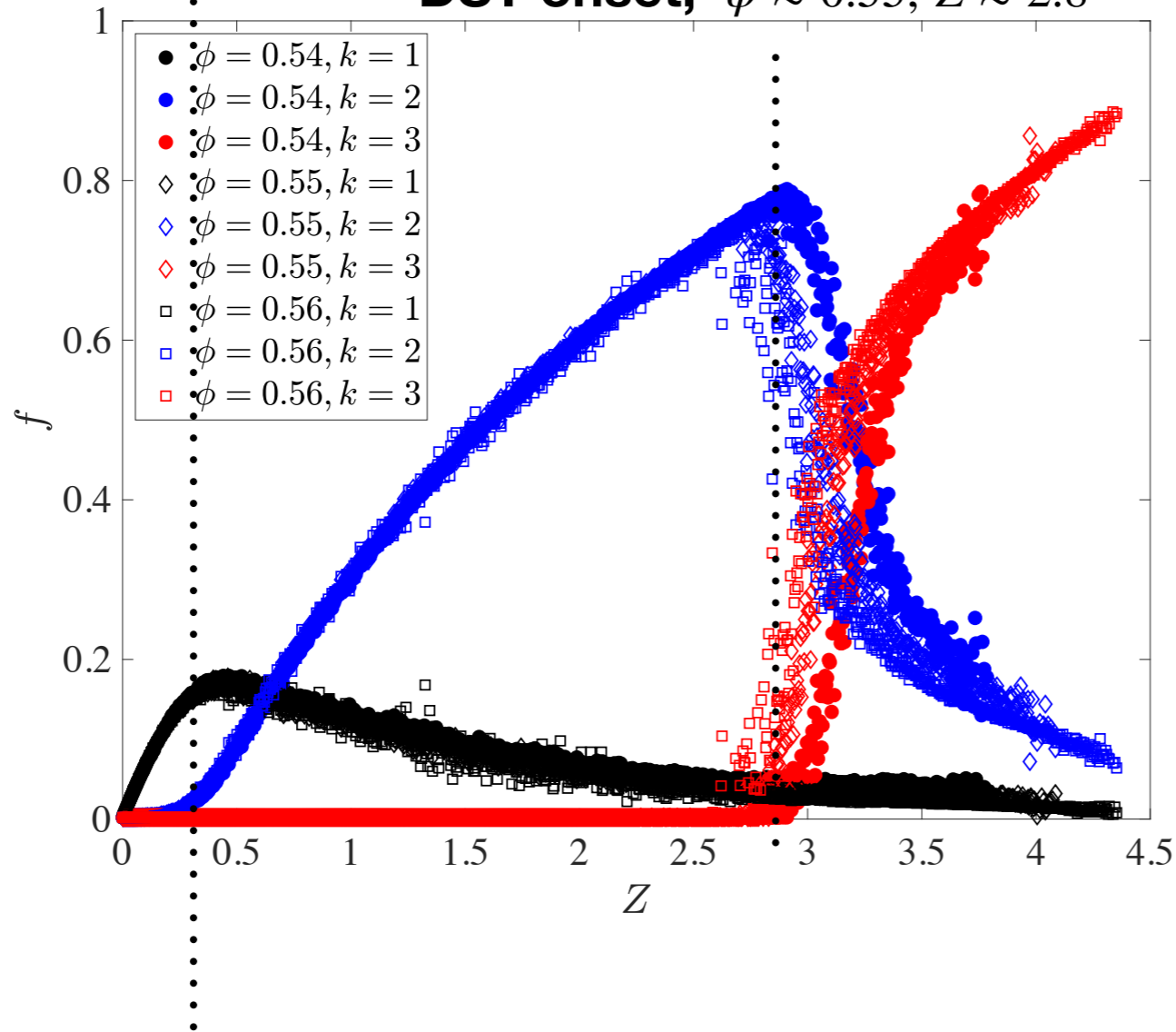


The k-shell occupancy (fully 3D simulations)

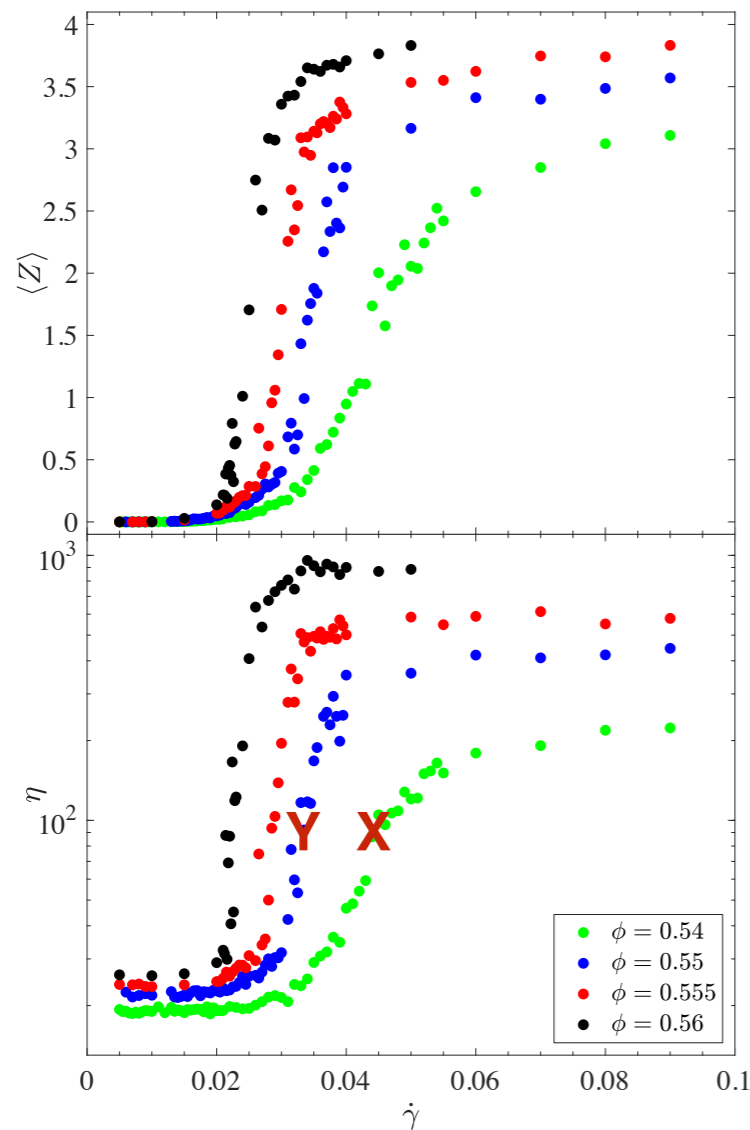
Contact percolation,

$$Z_C \approx 0.28$$

DST onset, $\phi \approx 0.55, Z \approx 2.8$

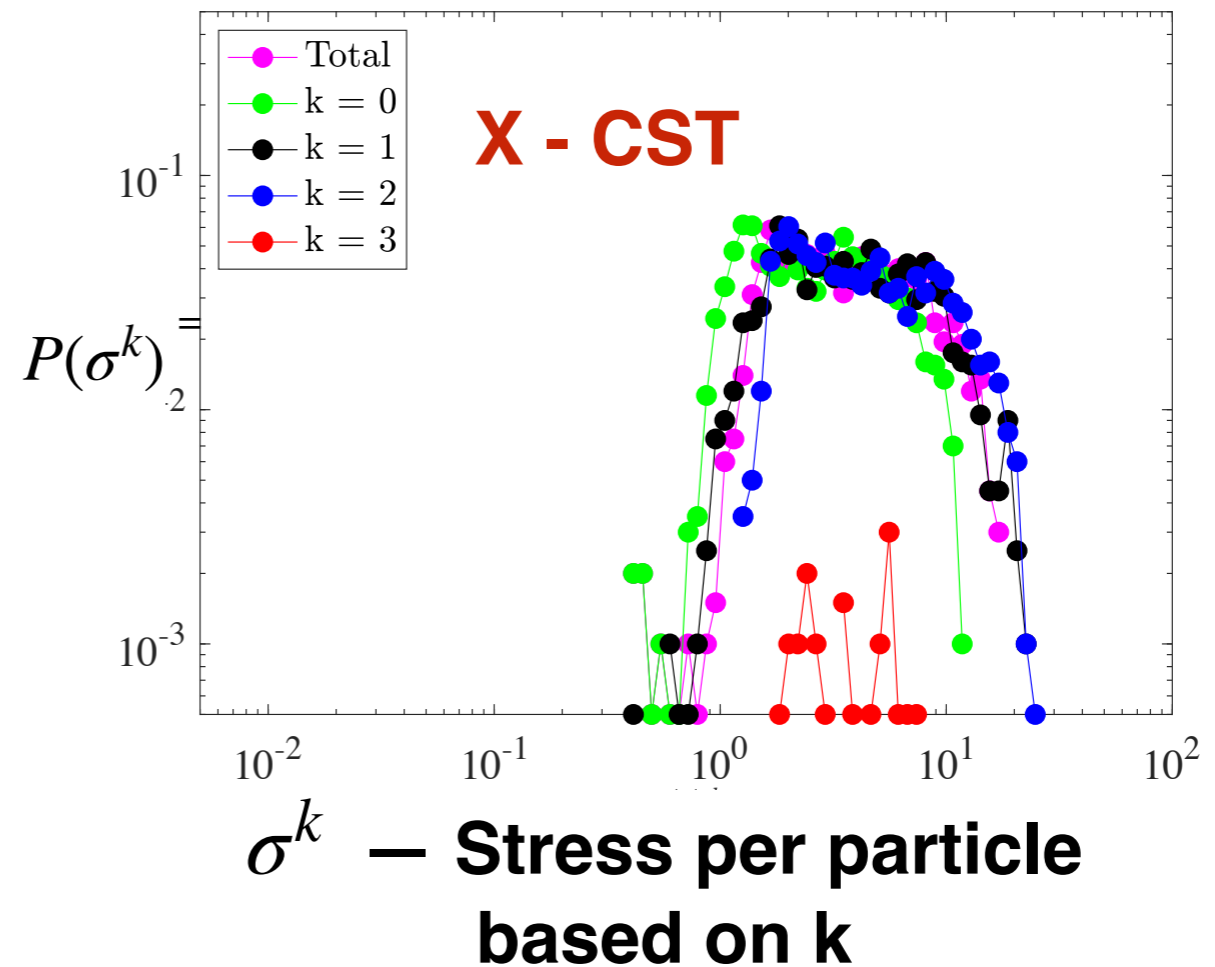


Stress per particle: by shell at onset of 3-core

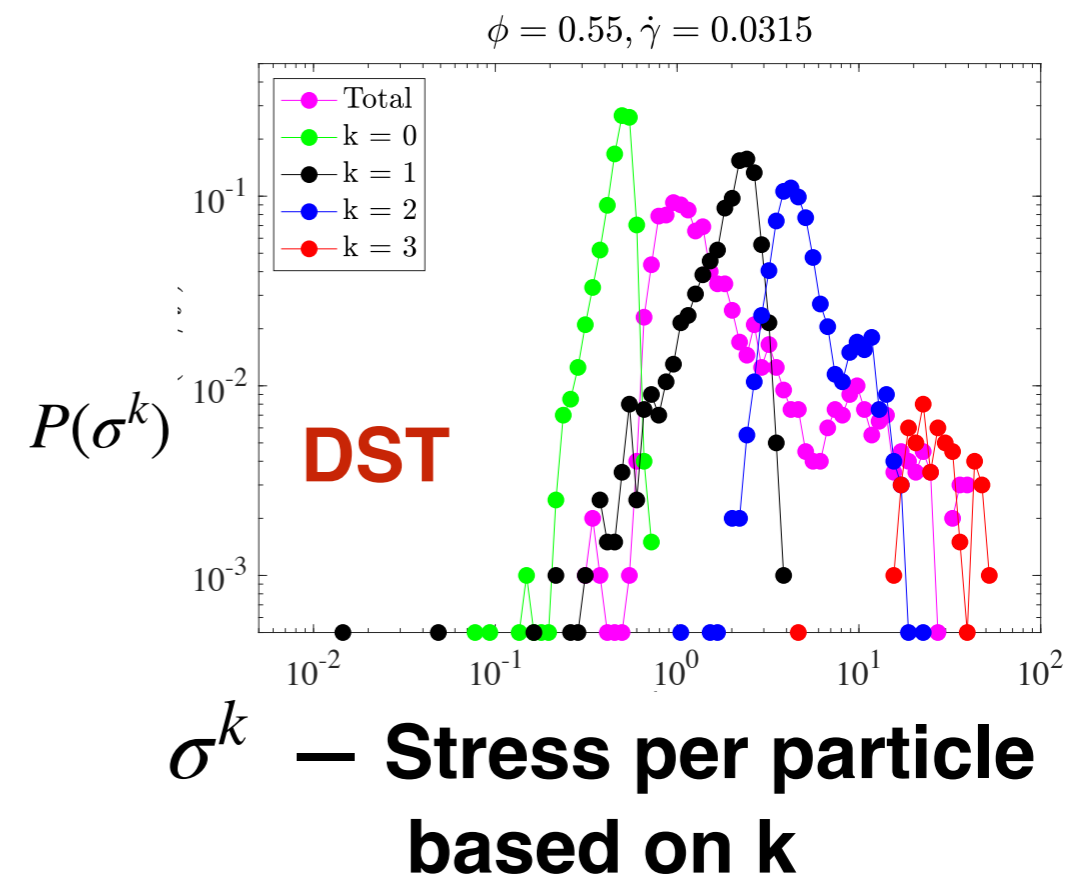
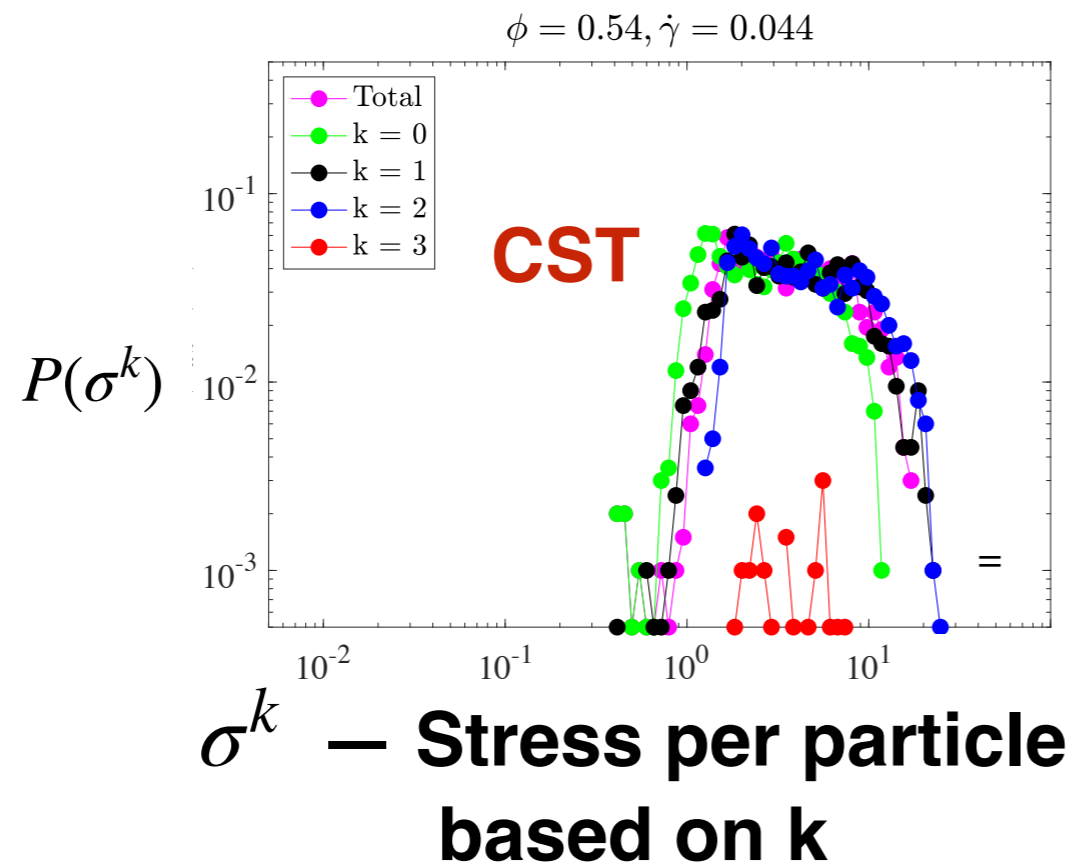


Below “critical”
concentration

$$\phi = 0.54, \dot{\gamma} = 0.044$$

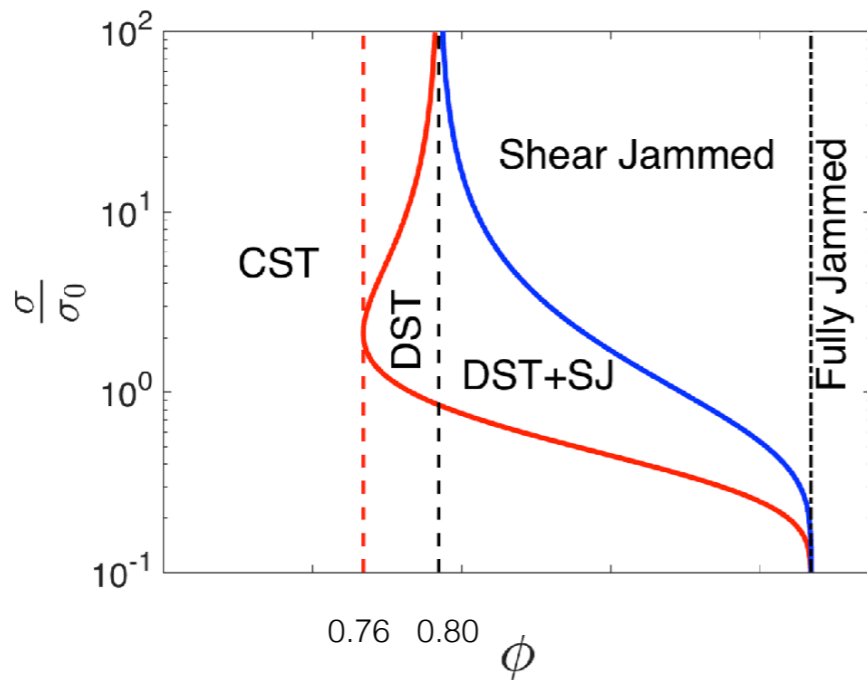
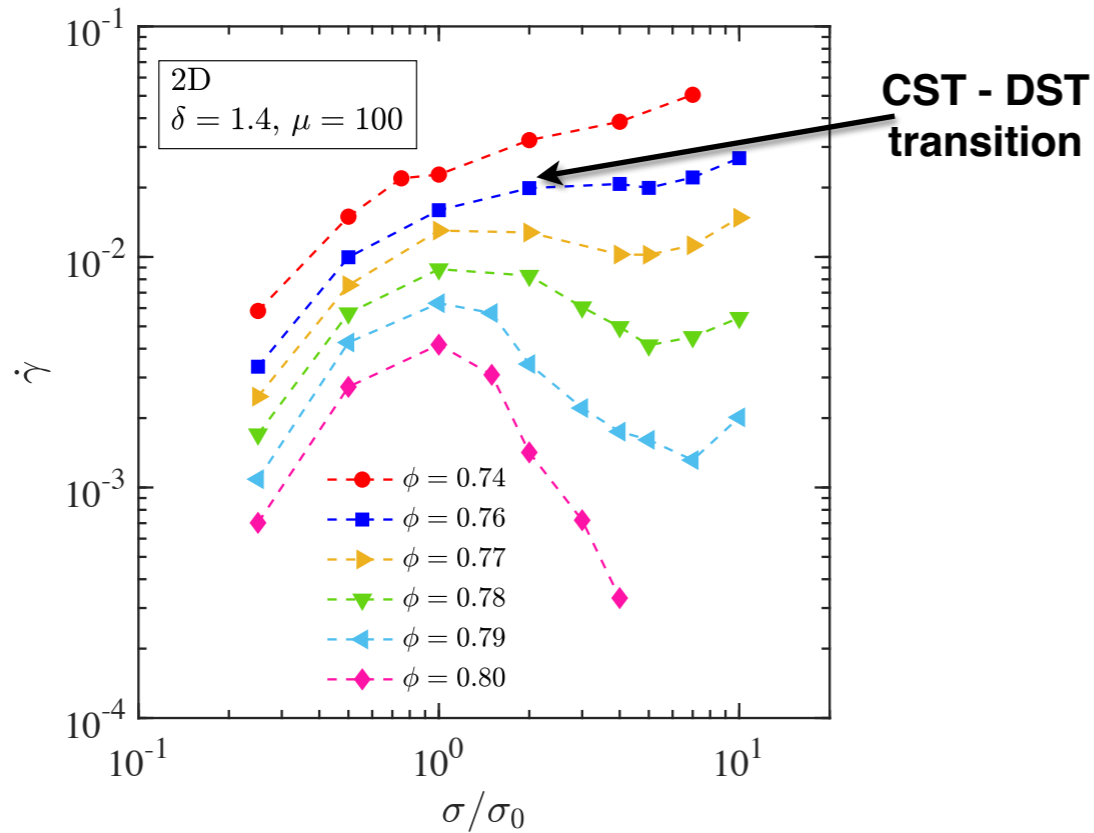


Stress per particle: by shell at onset of 3-core

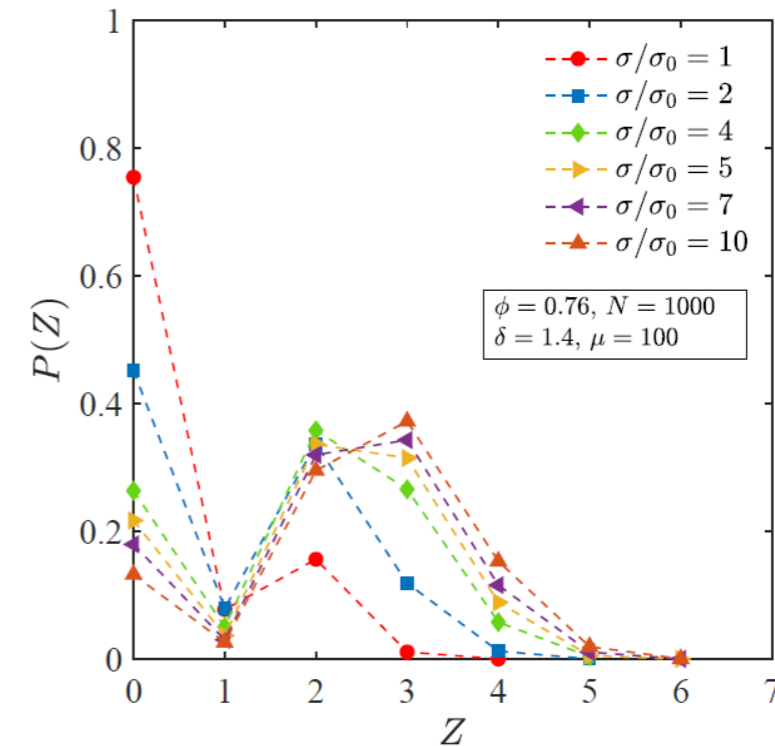
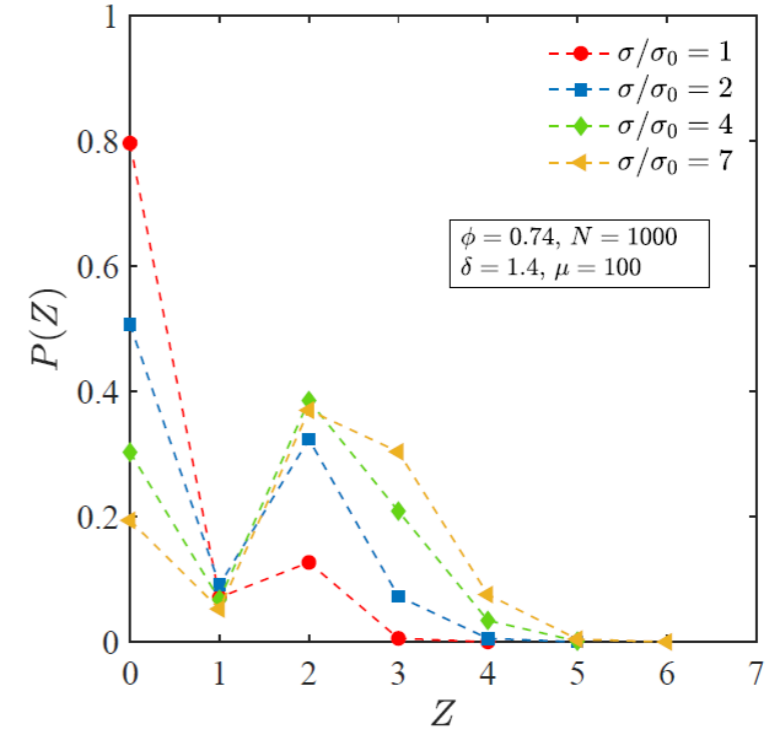


Rigid clusters in 2D: preliminaries

Friction
 $\mu \approx \infty$



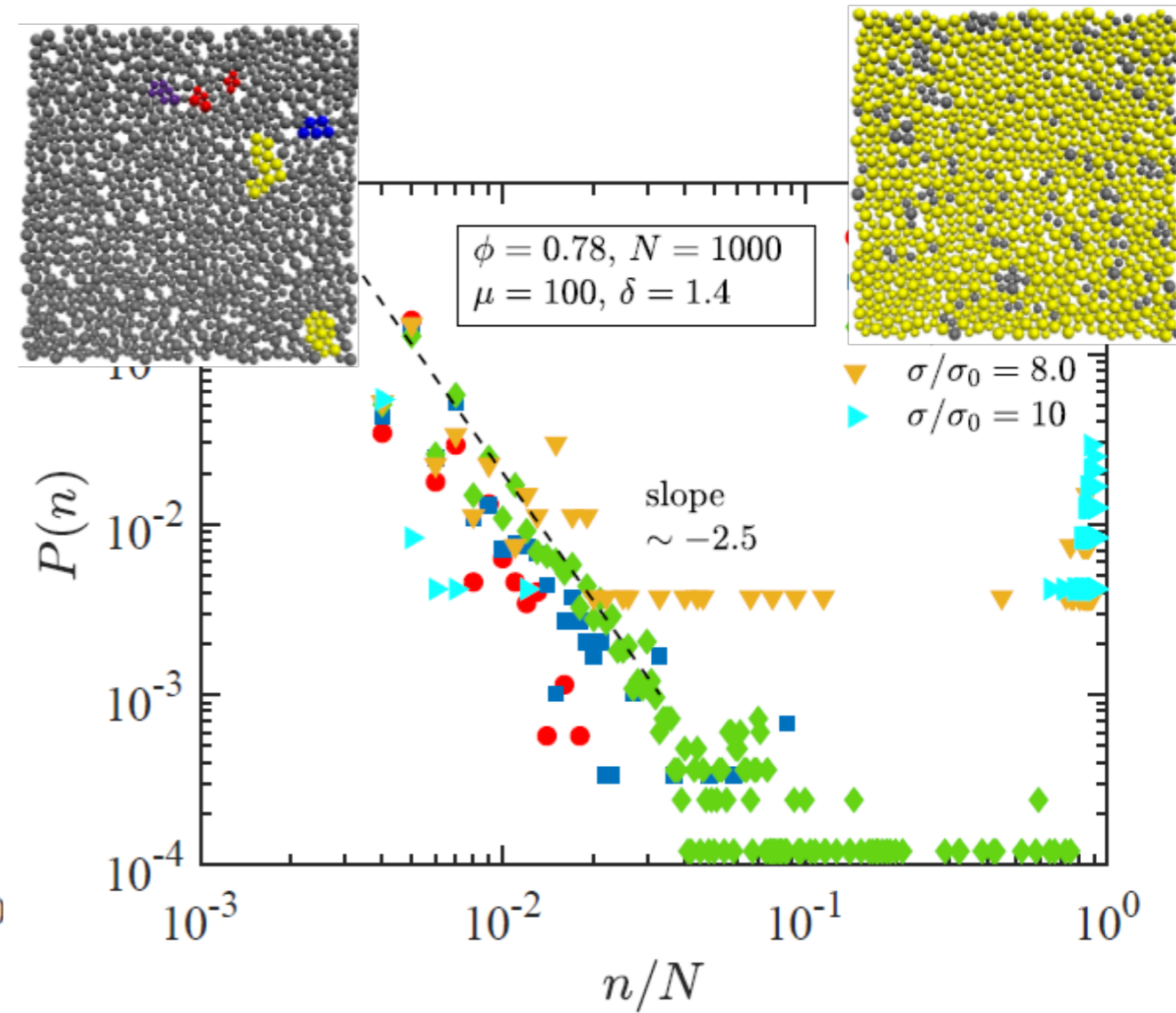
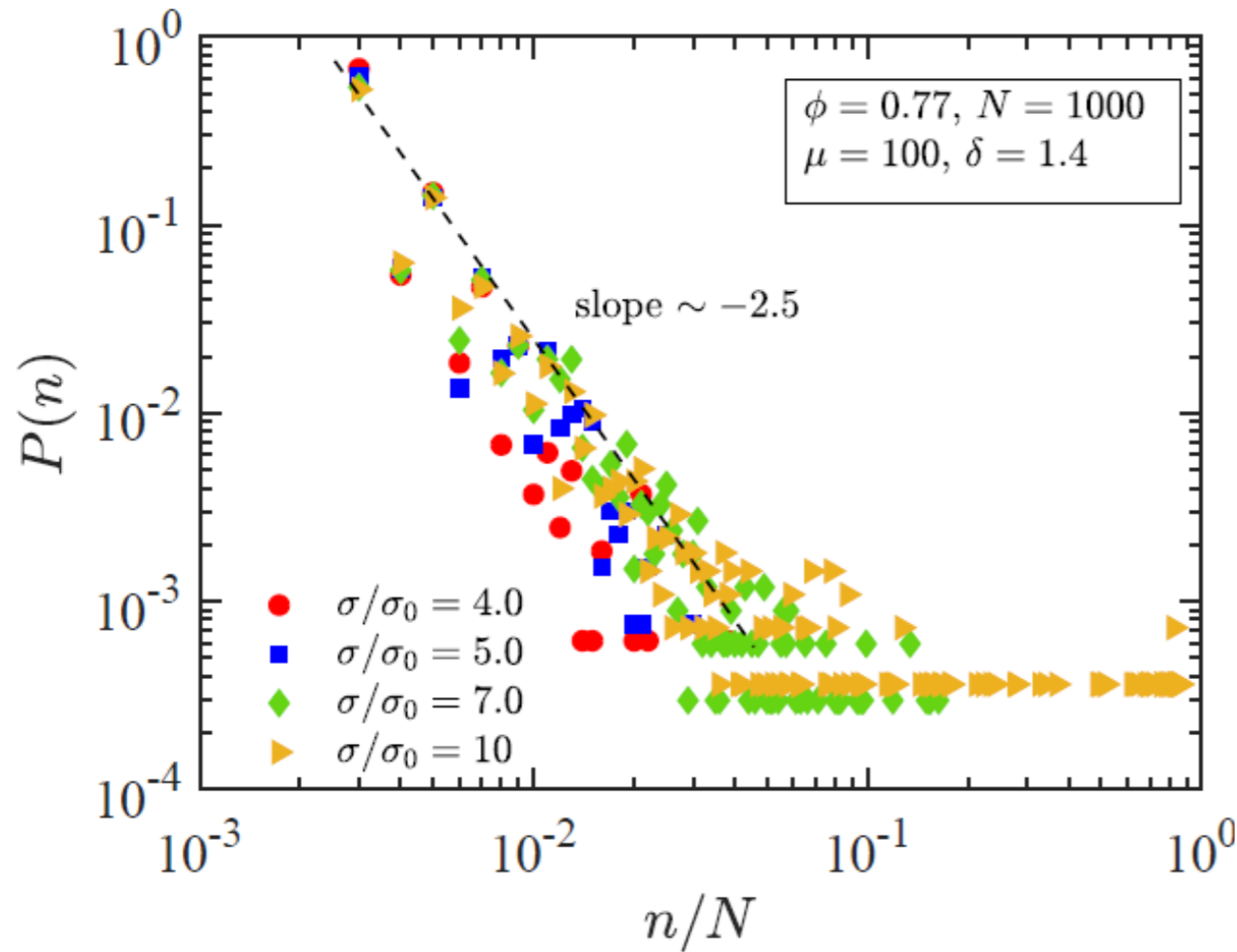
3 frictional contacts in 2D:
potential for local rigidity*



*Related ideas in 3D:

Rigid cluster distributions

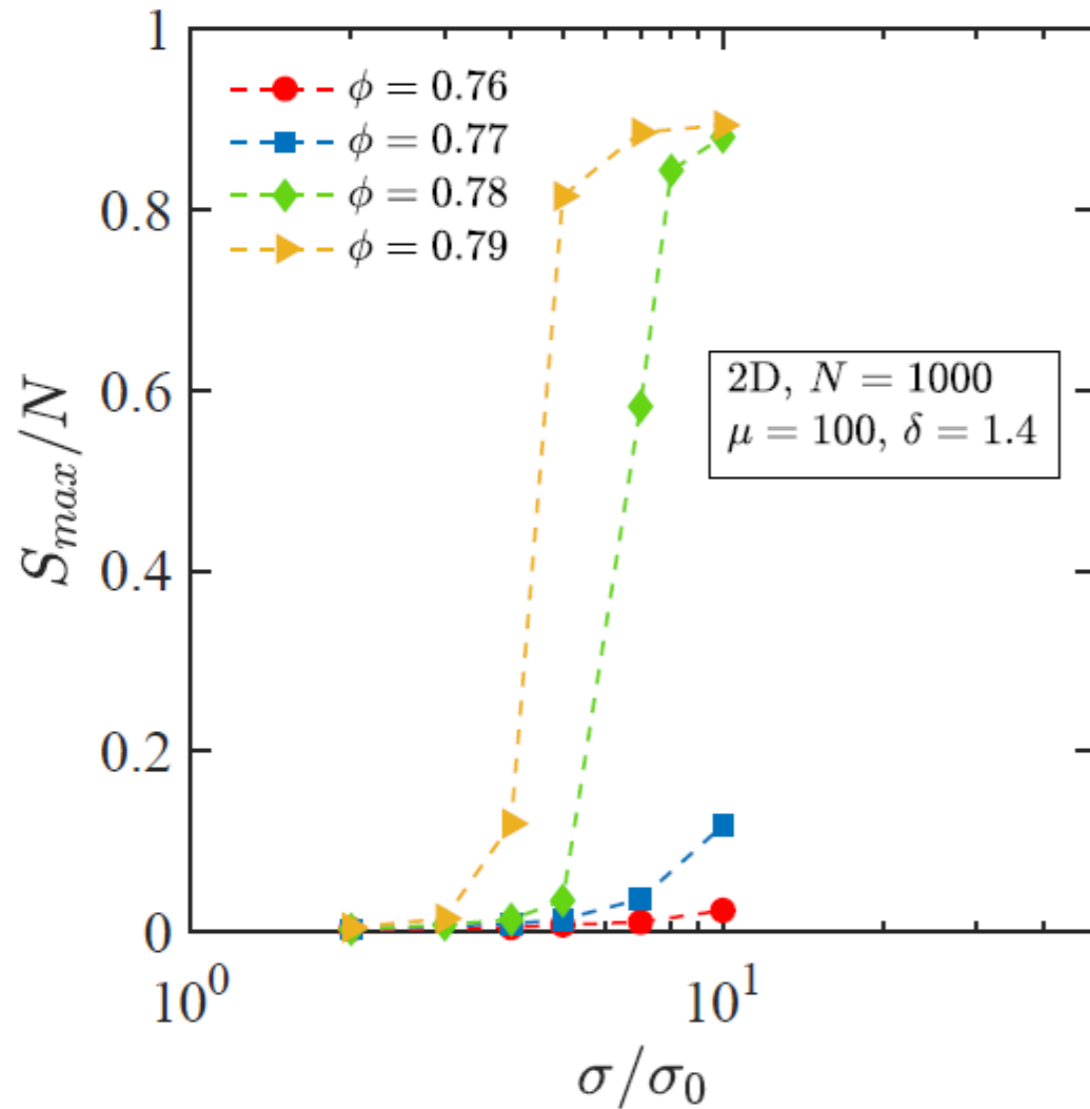
Analysis by (3,3) “pebble game”



Thanks to Mike van der Naald & Heinrich Jaeger,
Univ. of Chicago

Henkes, Quint, Fily & Schwarz *PRL* 2016
Jacobs & Hendrickson *J. Comp. Phys.* 1997

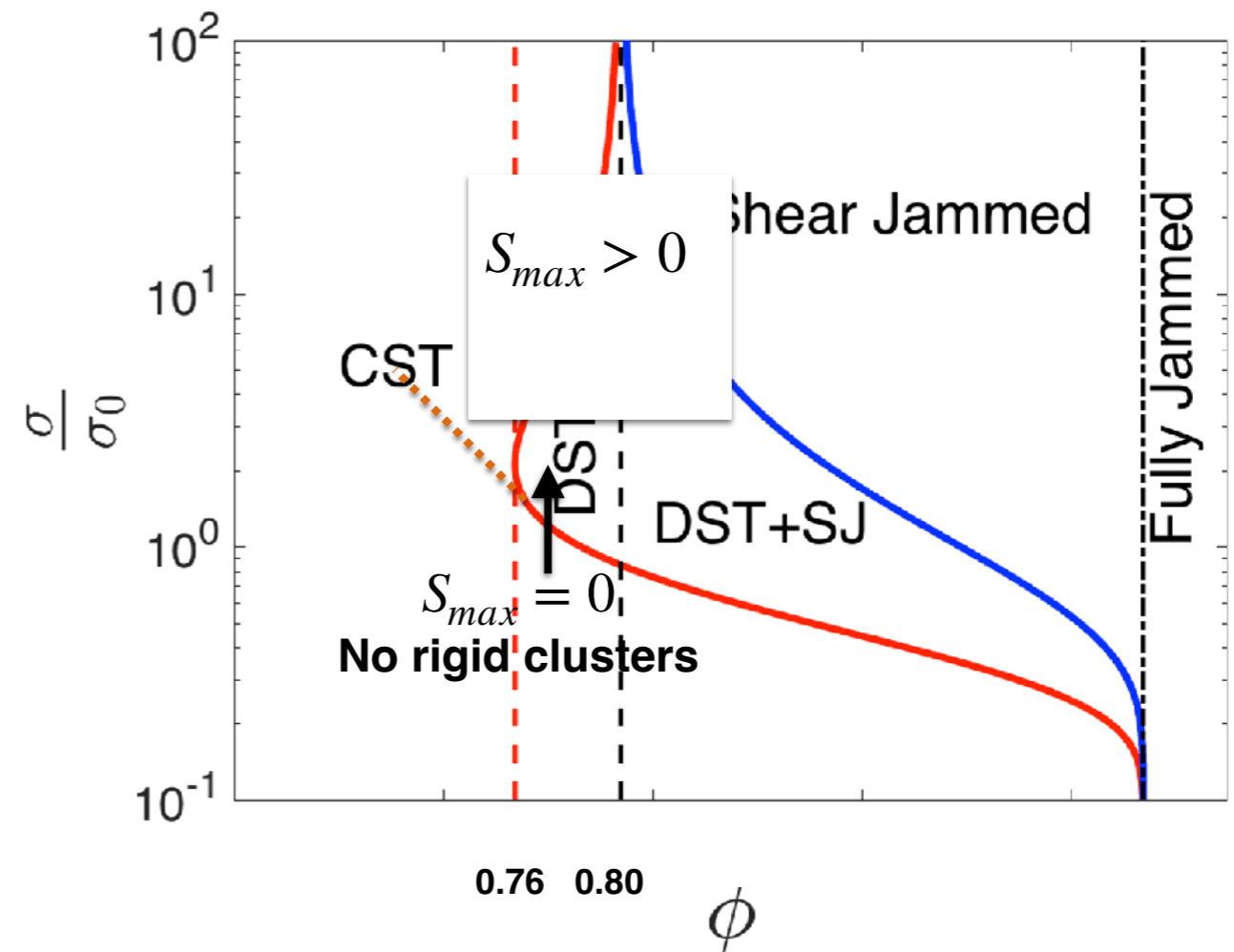
Maximum rigid cluster size



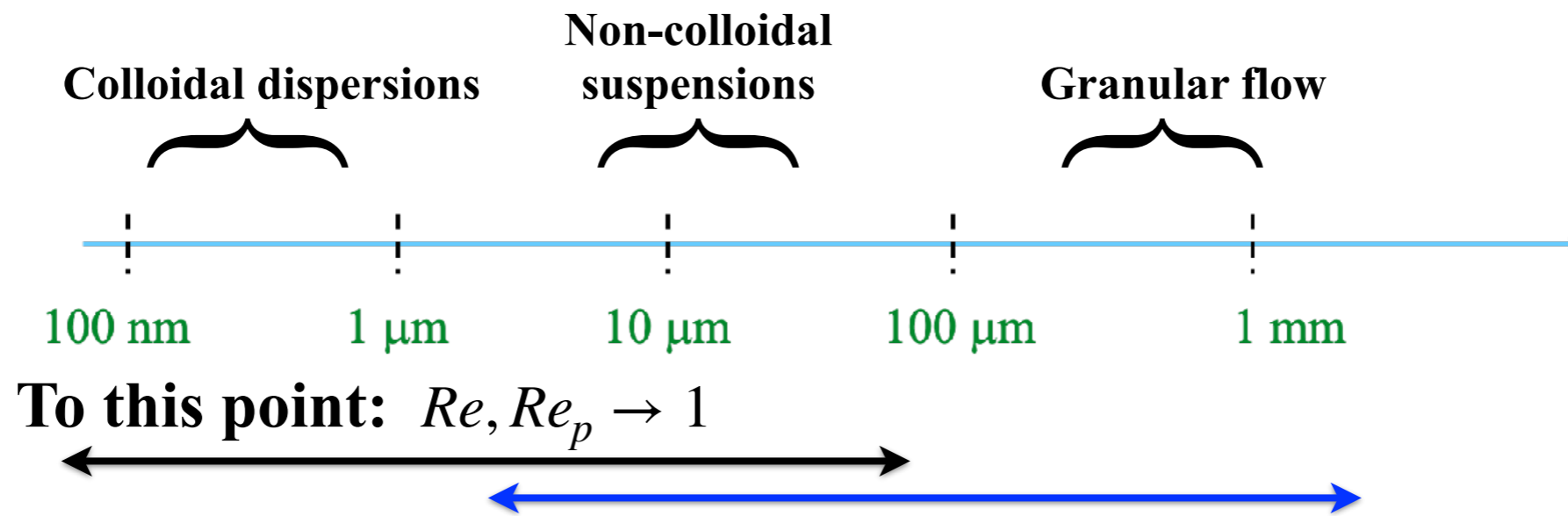
Hypothesis — rigidity is an order parameter.

Onset of rigidity \rightarrow DST.

Data seems to support, but incomplete.



Particle size a , $Re_p = \frac{\rho \dot{\gamma} a^2}{\eta}$

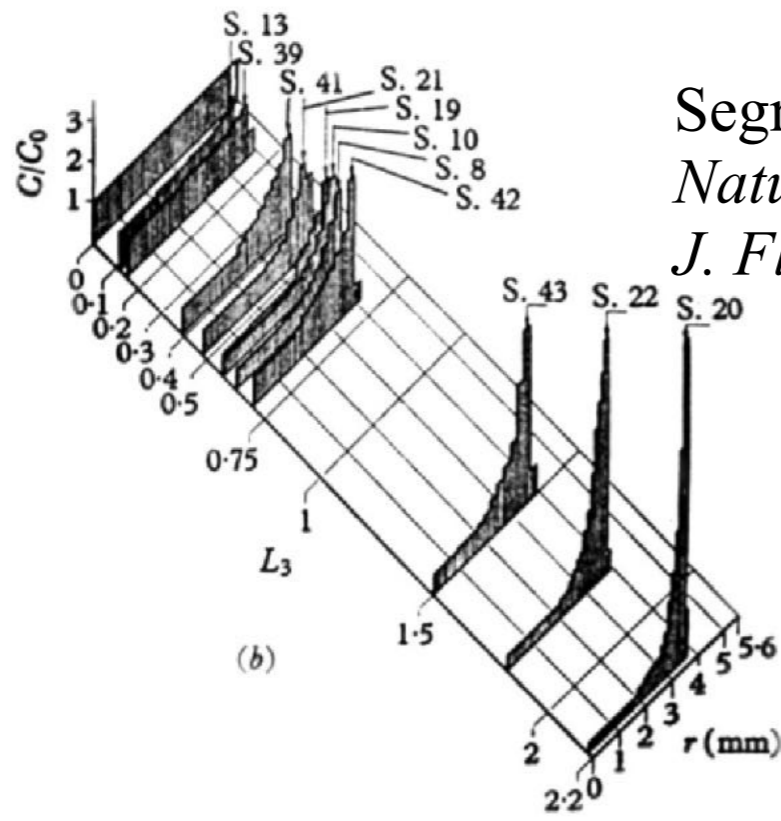


For a few minutes, consider $Re_p > 0$, $Re \gg 1$

$$Re \left(\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p + \nabla^2 \mathbf{u}$$

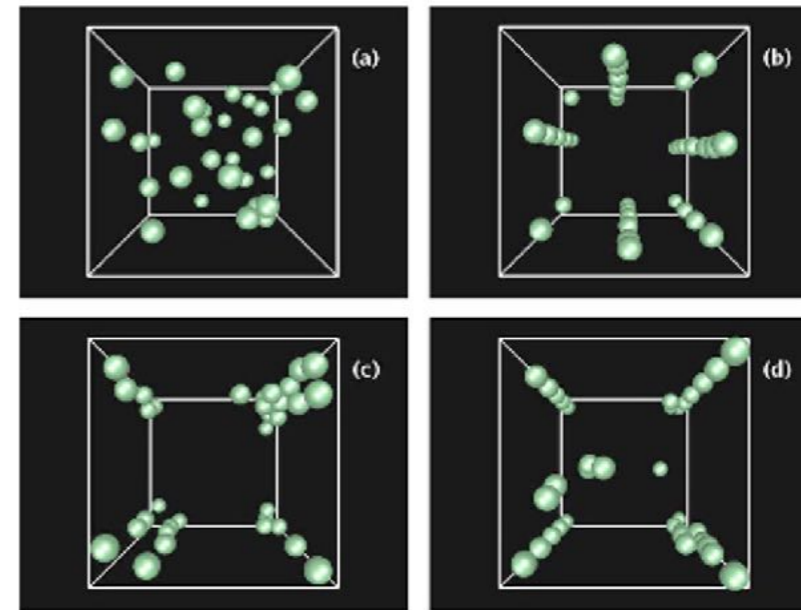
Goal: Advance the fluid mechanical paradigm for suspensions.

Inertial migration: Tubular pinch and related behavior

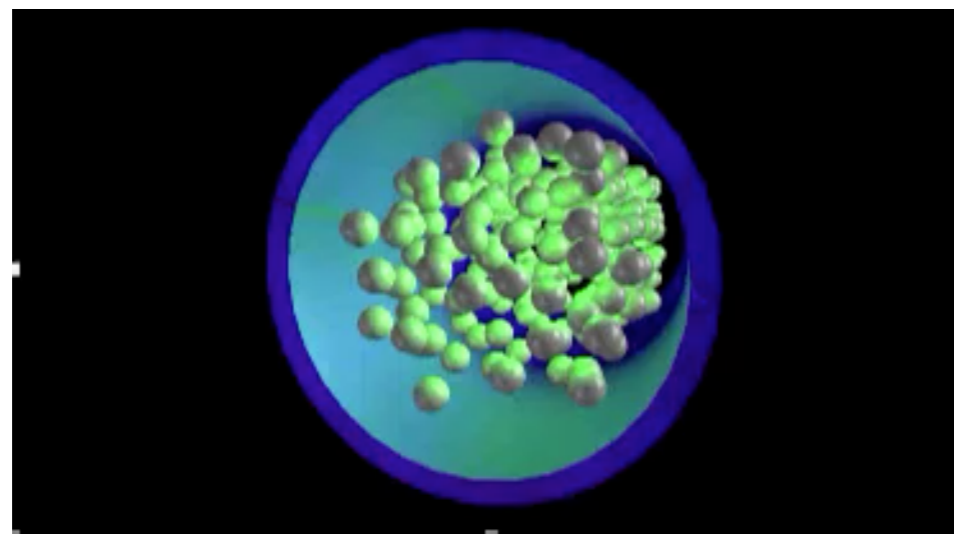
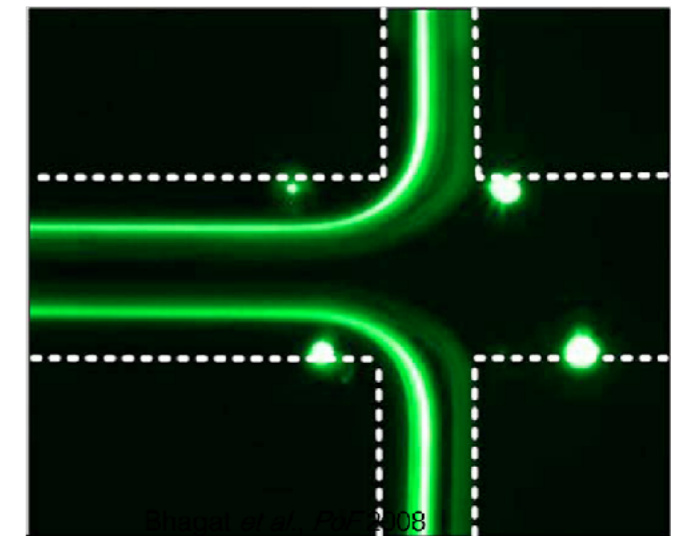
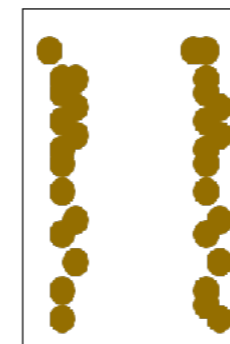


Segré & Silberberg
Nature 1961
J. Fluid Mech. 1962

Chun & Ladd *Phys Fluids* 2006



Segregation and
“filtration”



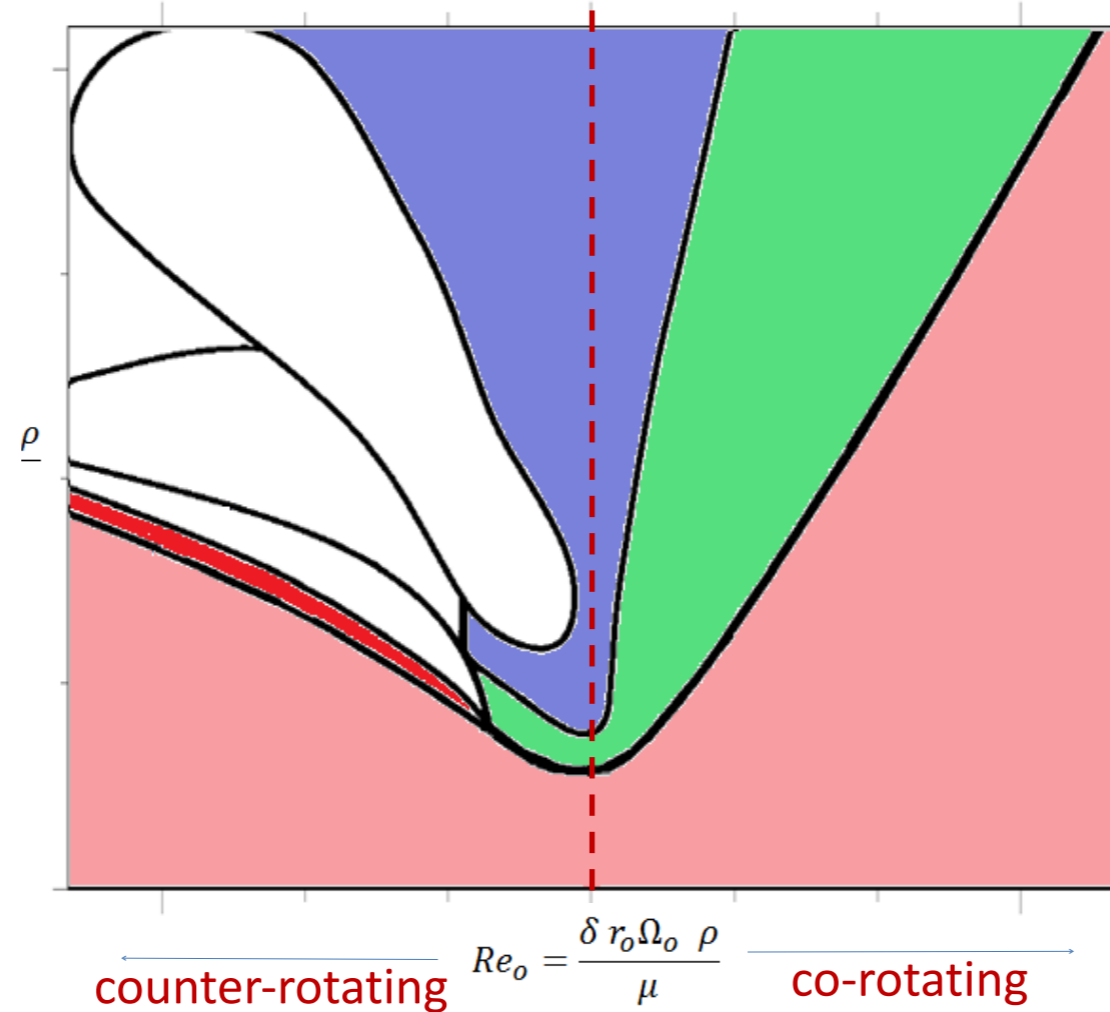
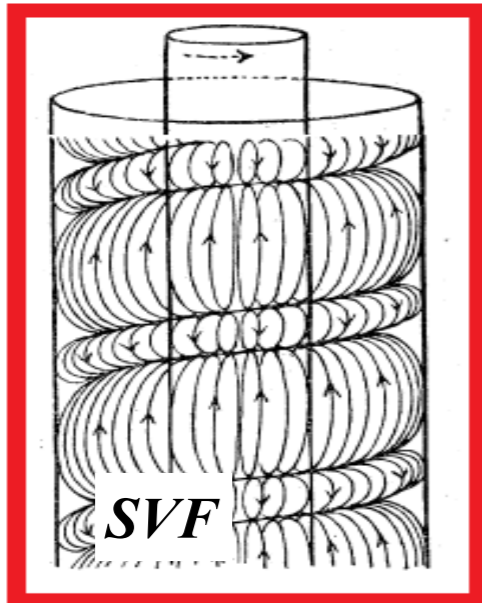
H. Haddadi, unpublished 2013

Bhagat, Kuntaegowdanahalli & Papautsky *Phys. Fluids* 2008

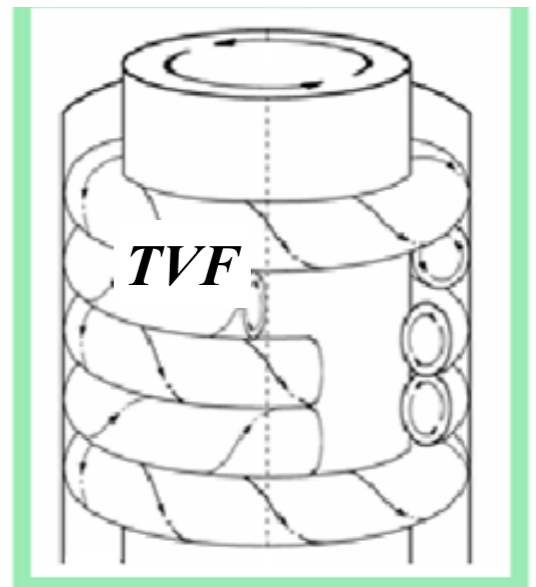
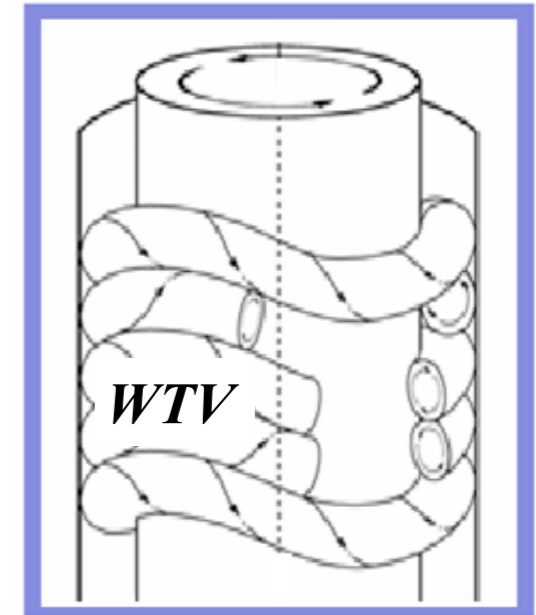
Taylor-Couette flow states

*Suspension experiments here:
only inner cylinder rotating*

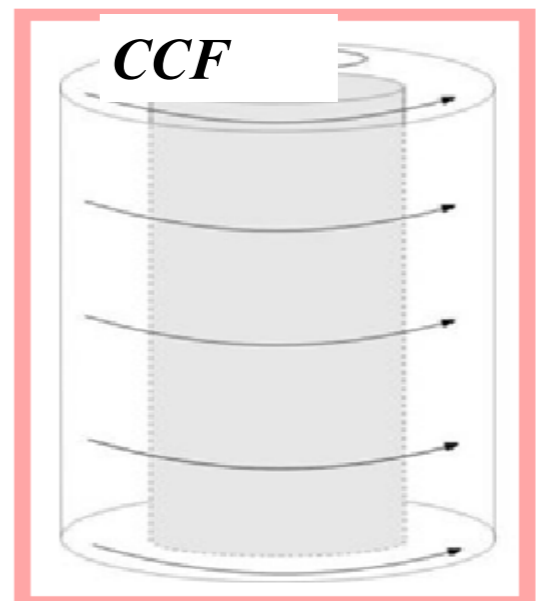
spiral vortex flow



wavy Taylor vortices



circular Couette flow



Experiments

- Stationary outer / rotating inner cylinder
- Reflective flakes: Visualization 1500x actual speed

$$Re = \frac{\rho \delta \Omega d_i}{2\eta_0} \quad \frac{L}{\delta} = 21 \quad \frac{d_i}{d_o} = 0.88$$

$$\delta = (d_o - d_i)/2$$

$$\rho_f = \rho_p = \rho$$

Majji, Banerjee & Morris *J. Fluid Mech.* 2018

Majji & Morris *Phys. Fluids* 2018

Baroudi, Majji & Morris *Phys. Rev. Fluids* 2020

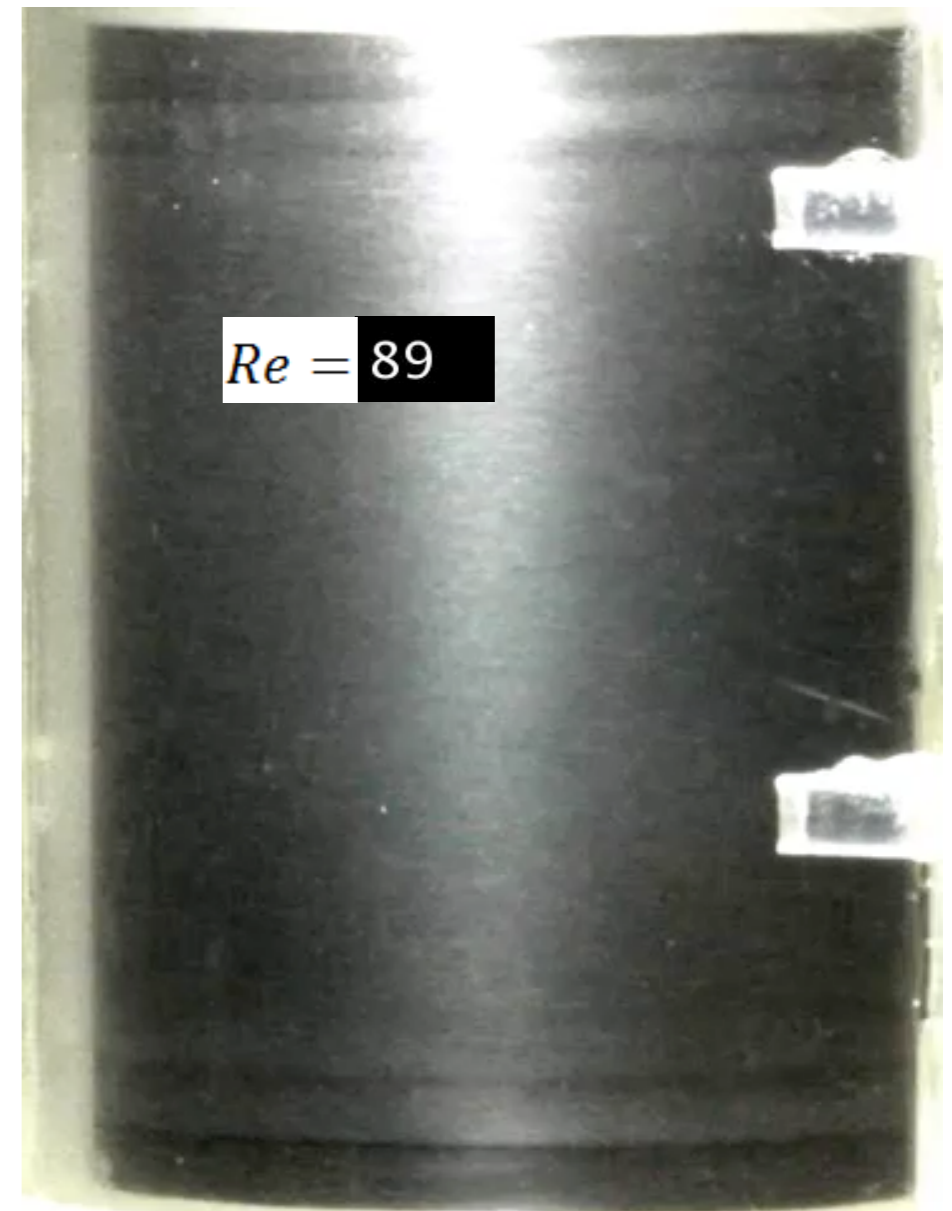
Related experiments:

Ramesh, Bharadwaj & Alam *J. Fluid Mech.* 2019

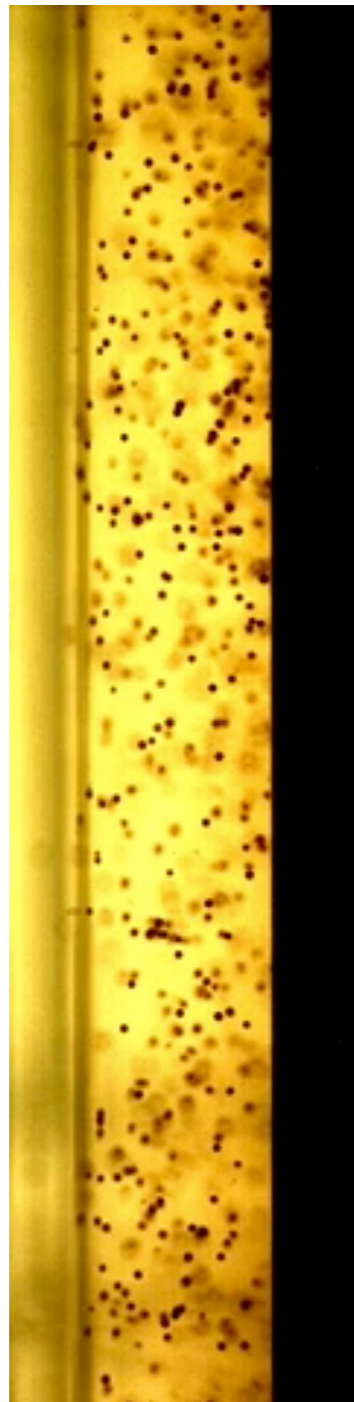
Dash, Anantharaman & Poelma *J. Fluid Mech.* 2020

Review:

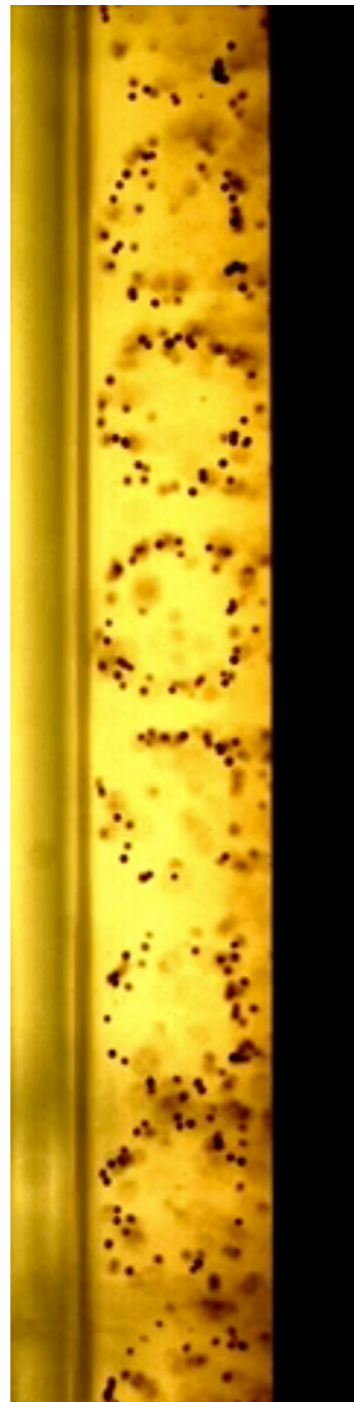
Baroudi *et al. Phil Trans A.* 2023



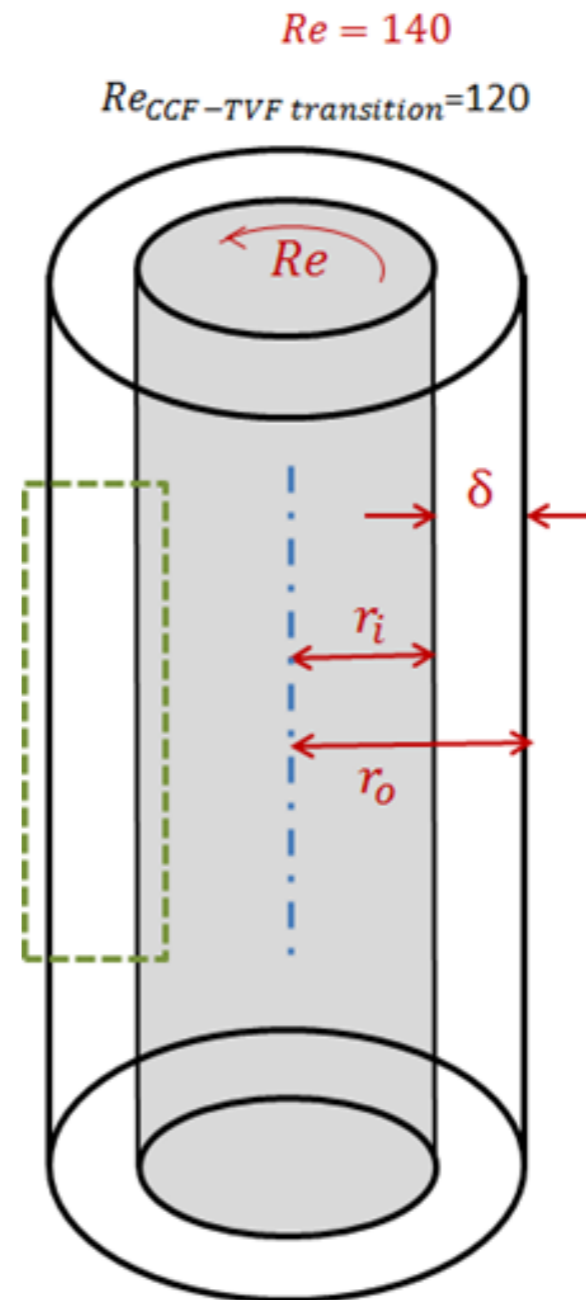
Inertial migration



time 0



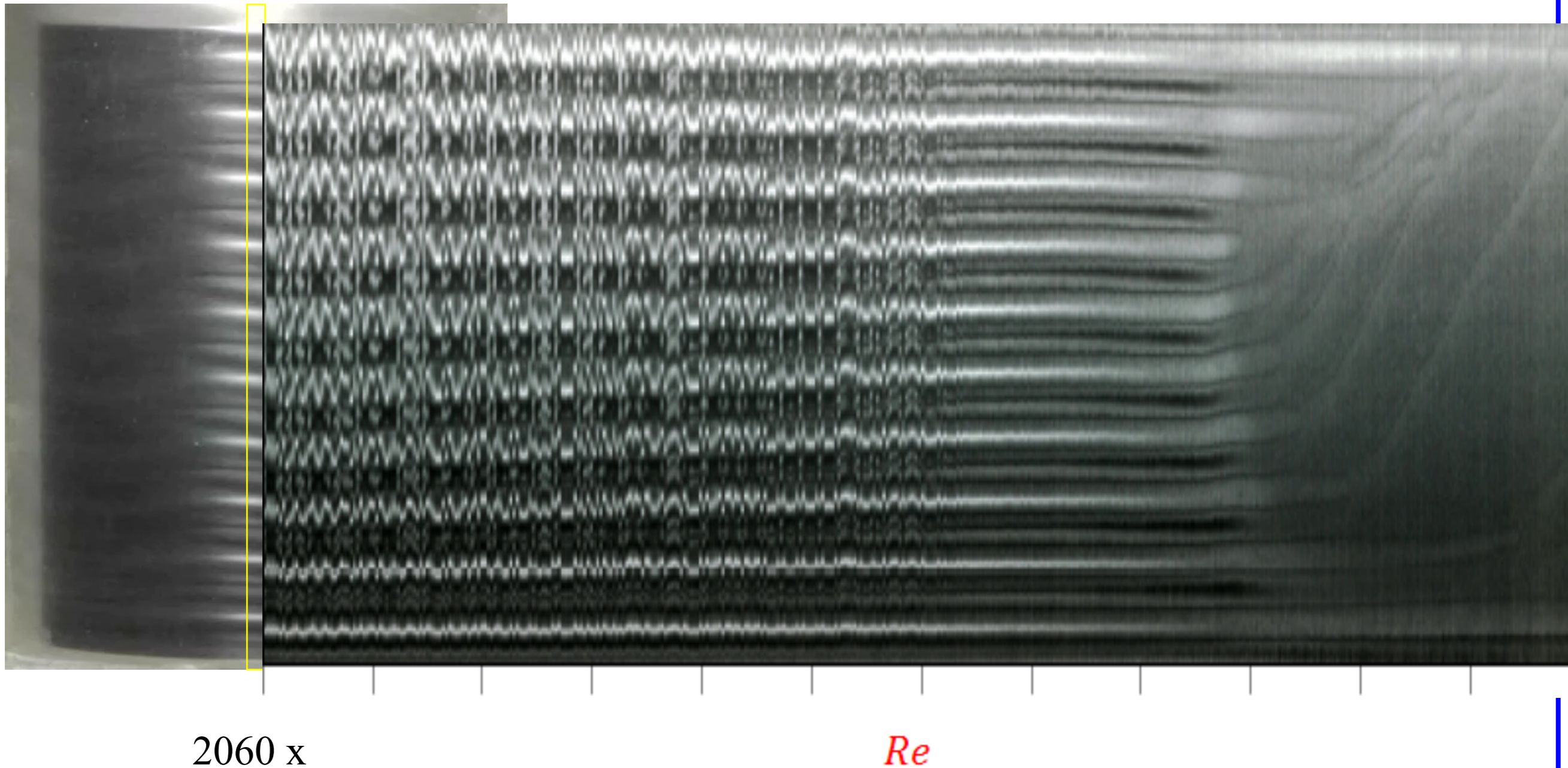
30 minutes



Majji & Morris *Phys. Fluids* 2018

Inertial migration: Segre & Silberberg *Nature* 1961

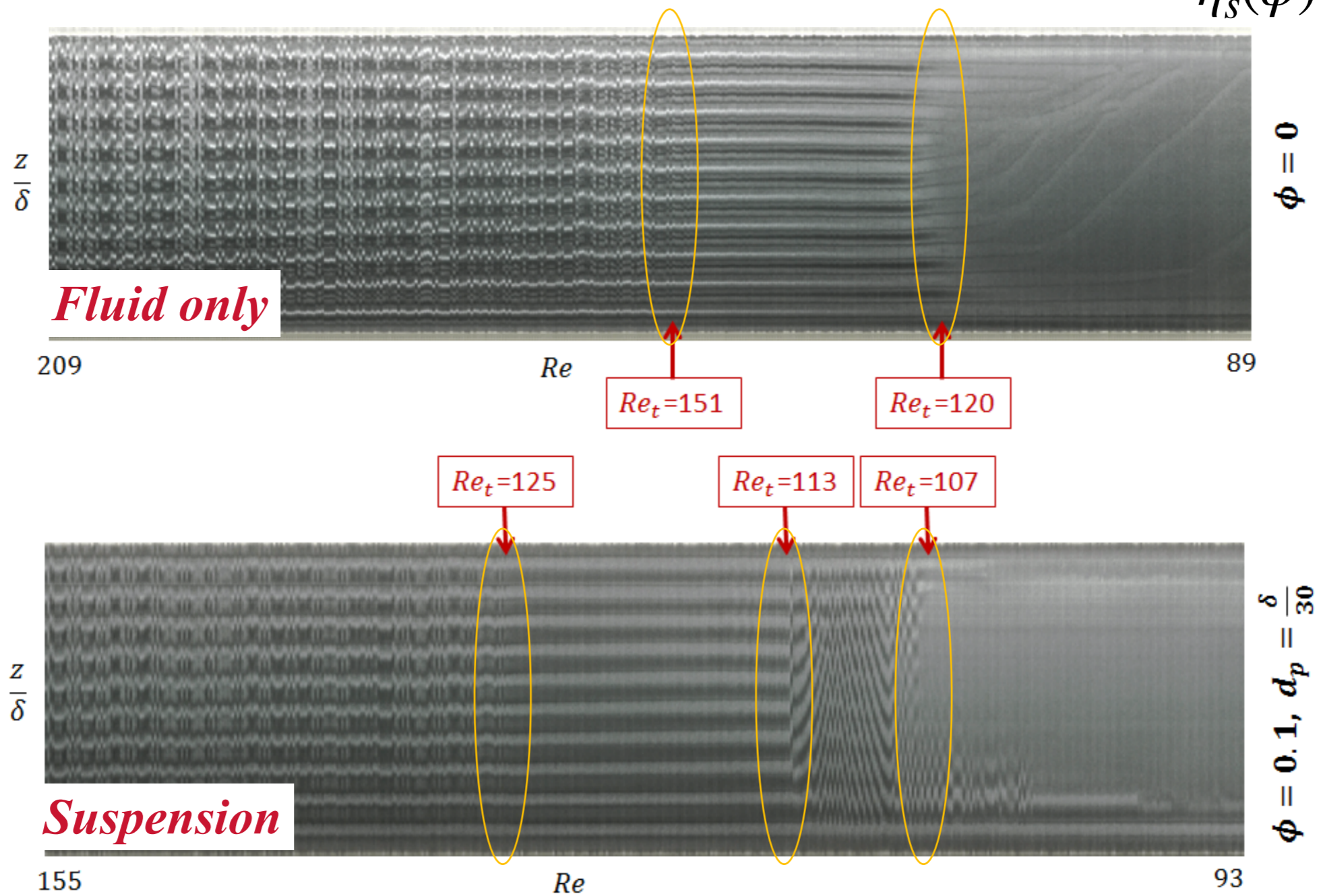
Suspension flow states — Higher solid fraction, ~ no migration

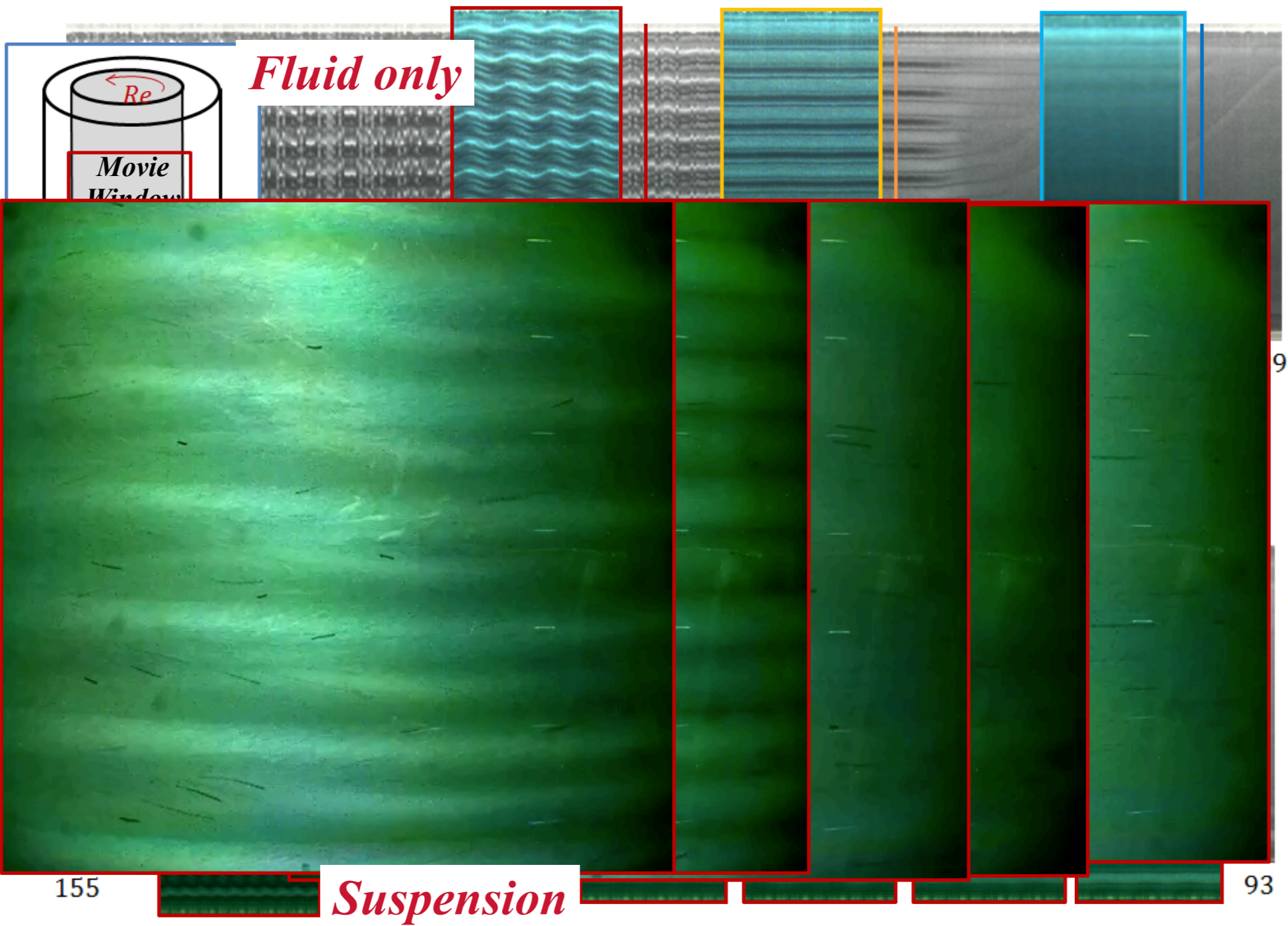


Migration effects on transition:
Baroudi *et al. Phys Rev. Fluids* 2020

Fluid vs suspension ($\phi = 10\%$) flow states

$$Re = \frac{\rho \Omega r_i \Delta r}{\eta_s(\phi)}$$





Fluid only

Movie Window

Re

$\phi = 0$

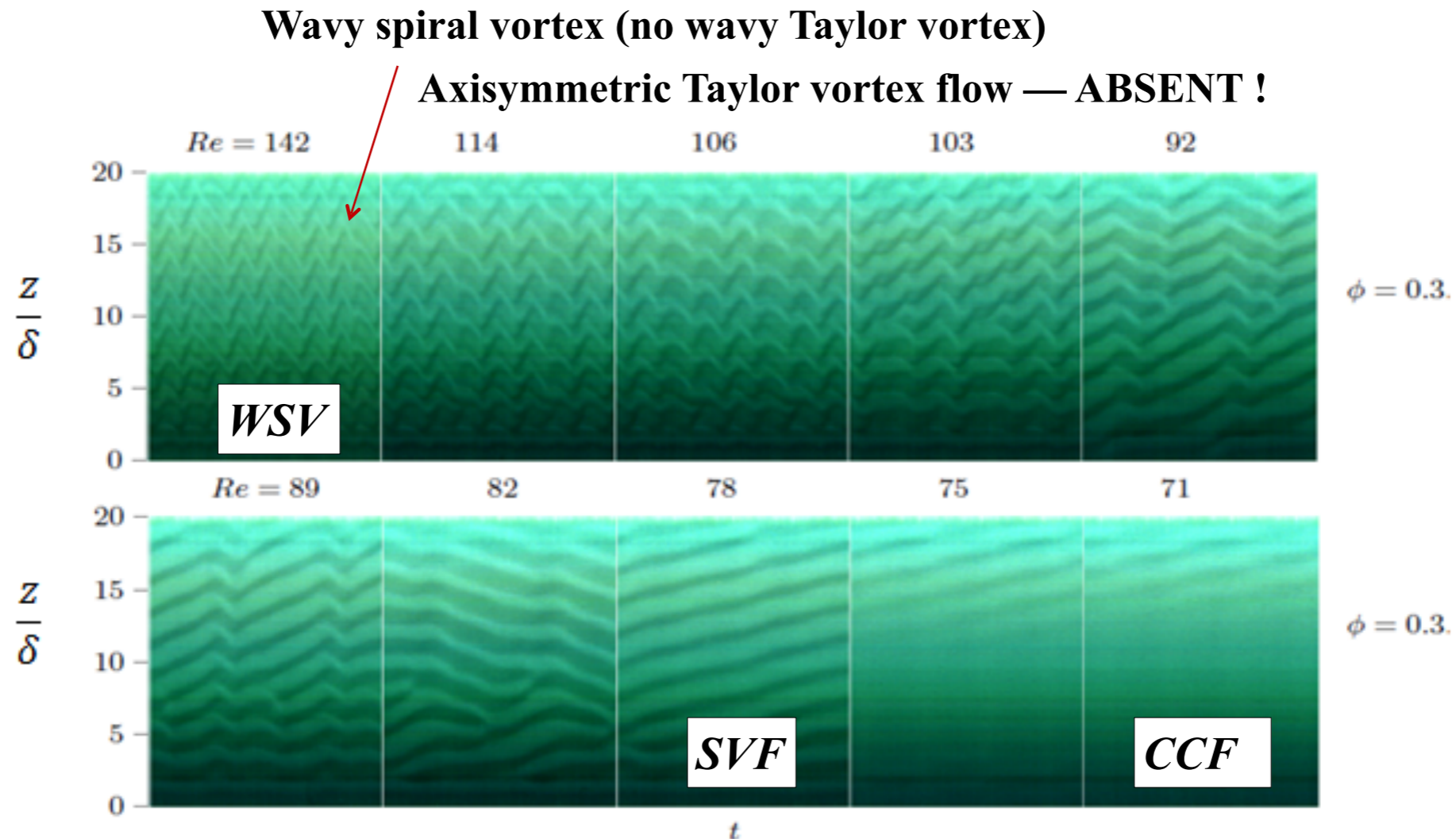
$\phi = 0.1, d_p = \frac{\delta}{30}$

155

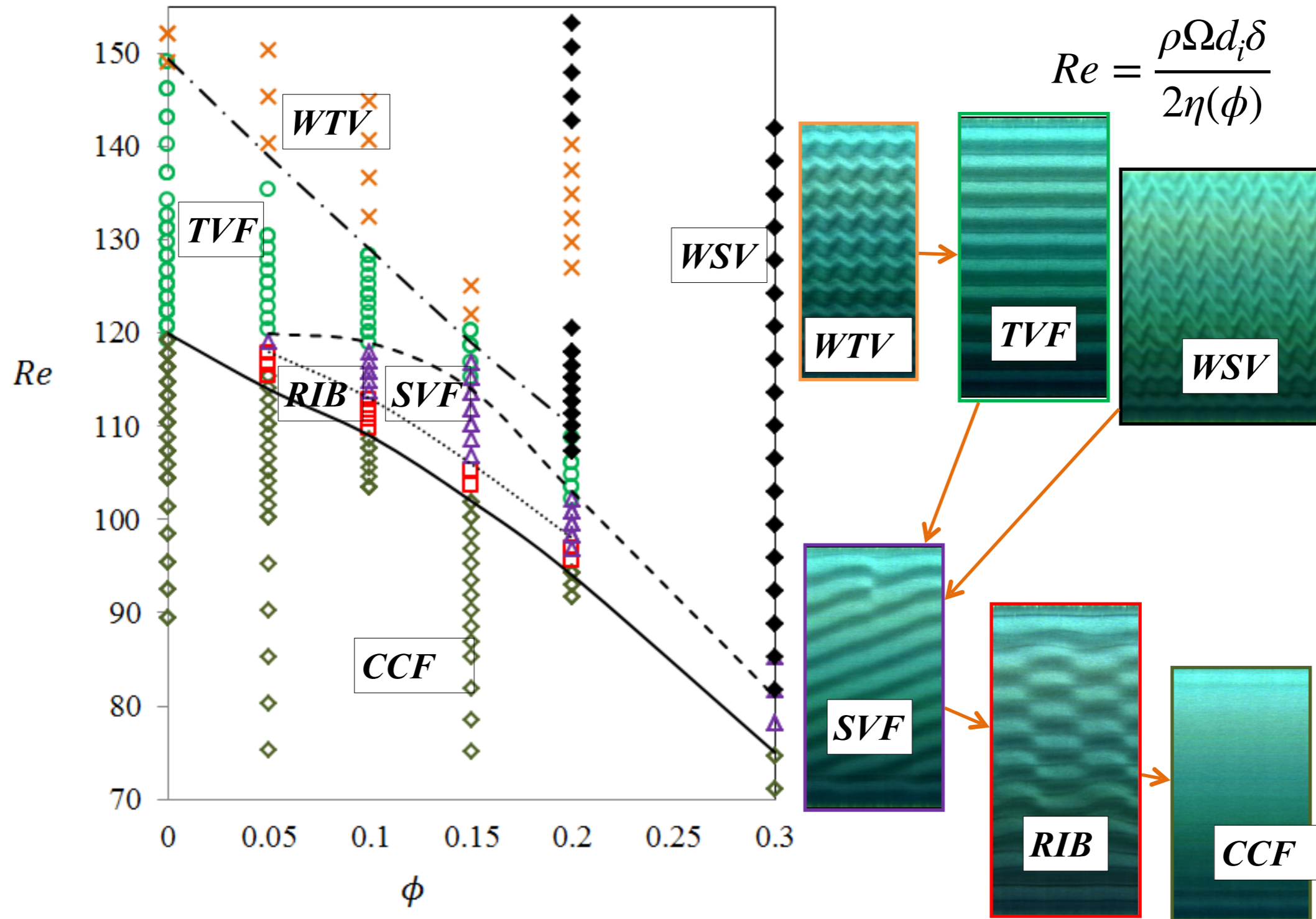
Suspension

93

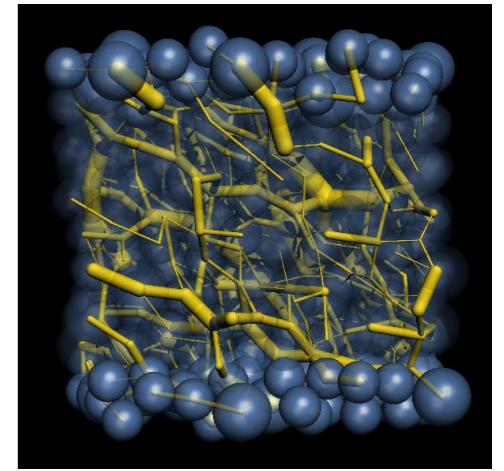
Concentrated suspension (30% solids) — No axisymmetric states seen above transition



Flow state map



Summary



Lubricated-to-frictional scenario for shear thickening:

—*hydrodynamic contacts* → *contact force chains* → *force (stress) network*
Constantly forming and breaking networks: shear-induced rigidity?

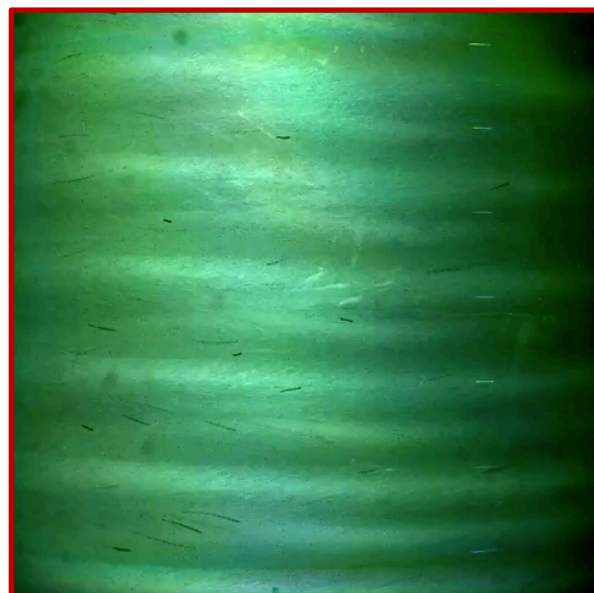
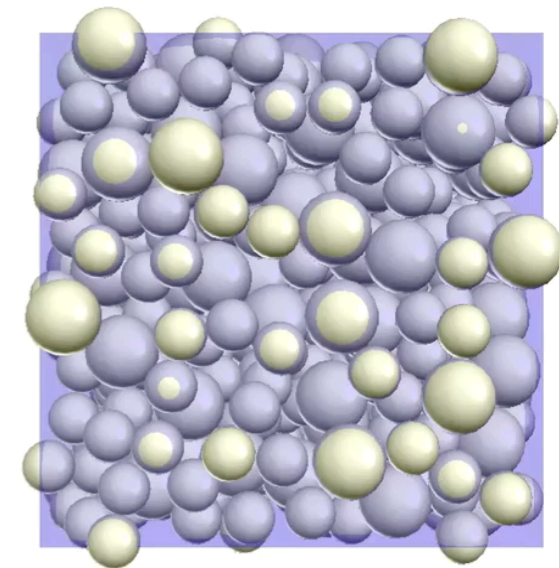
Taylor-Couette flow of suspensions:

Reduction in primary bifurcation at all ϕ

Nonaxisymmetric states (NAS)

—not seen in inner-cylinder driven Newtonian fluid

—primary bifurcations to NAS at higher ϕ



Establishing *validated models* is a key step in advancing multiphase flow analysis for the environment.

Thanks!