

BLENDING LIQUID AND GRAINS

ACCRETION DYNAMICS ON WET GRANULAR MATERIALS

Alban SAURET

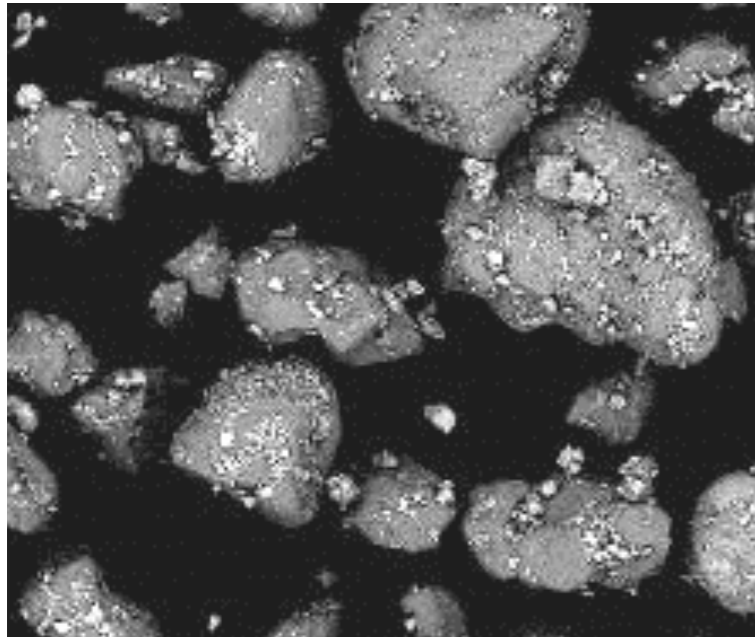
Guillaume SAINGIER, Pierre JOP

SVI, CNRS/Saint-Gobain

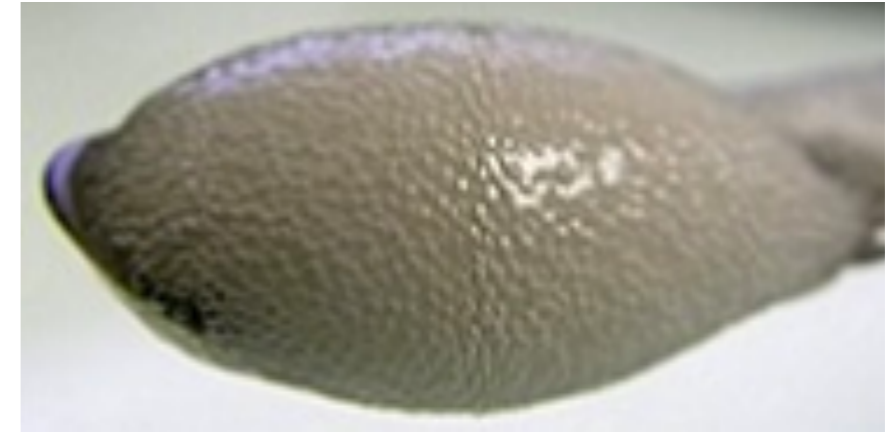


INDUSTRIAL PROCESSES : GRAINS AND SUSPENSIONS

Building materials: cement, concrete, mortars, plasters



Suspensions of bubbles in yield stress fluids

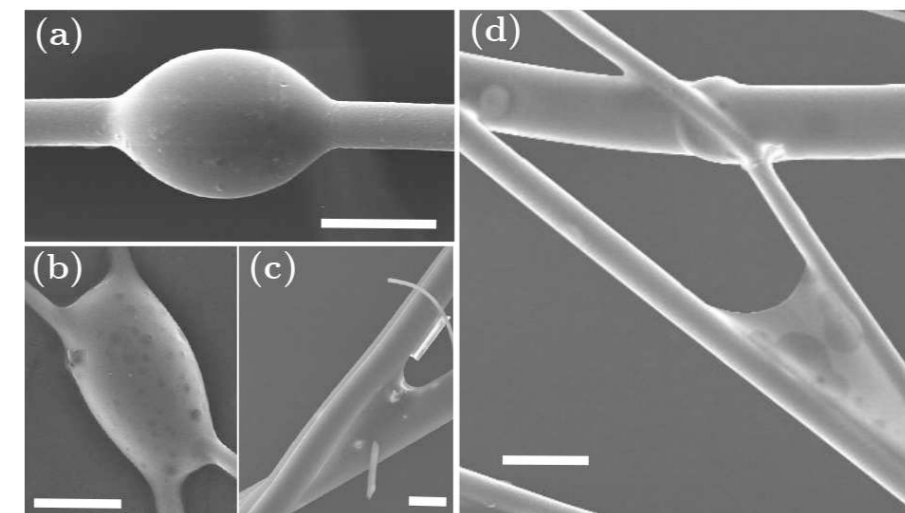


e.g. L. Ducloué, O. Pitois, J. Goyon, X. Chateau, & G. Ovarlez, *J. non-Newton. Fluid Mech.* (2015).

Glass and substrates



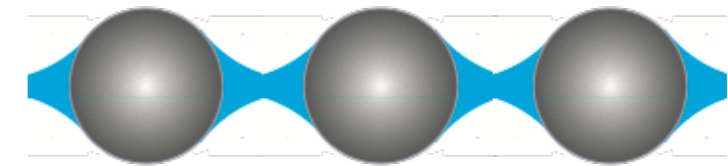
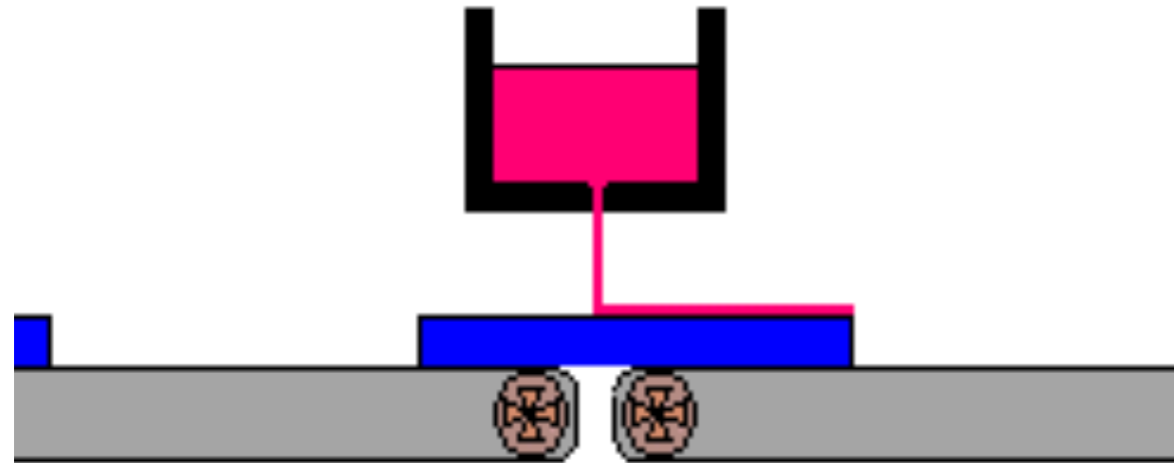
Glass wool: fibers



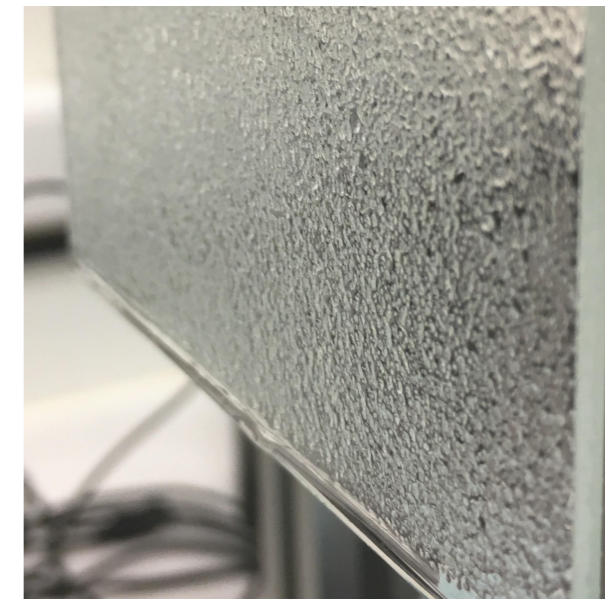
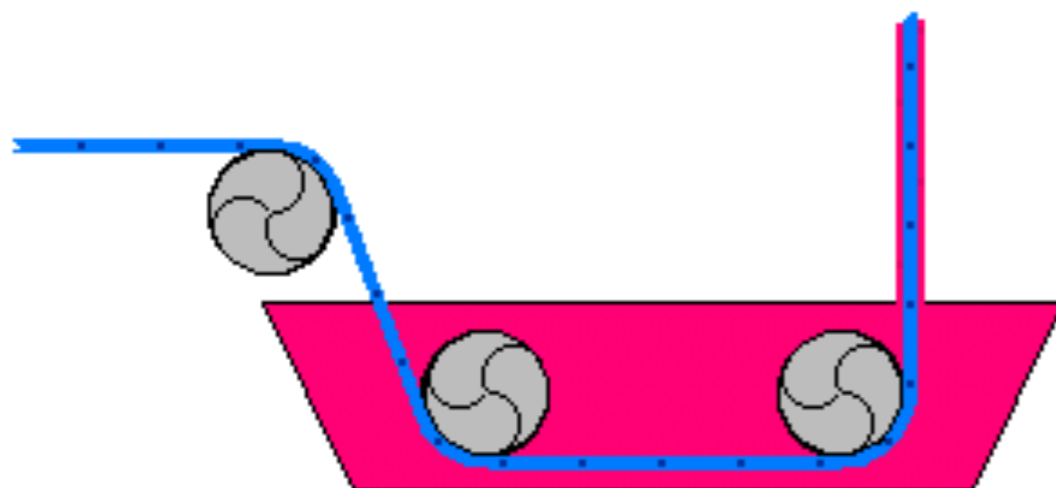
A. Sauret, F. Boulogne, E. Dressaire & H.A. Stone, *EPJE* (2015)

INDUSTRIAL PROCESSES : WET COATING

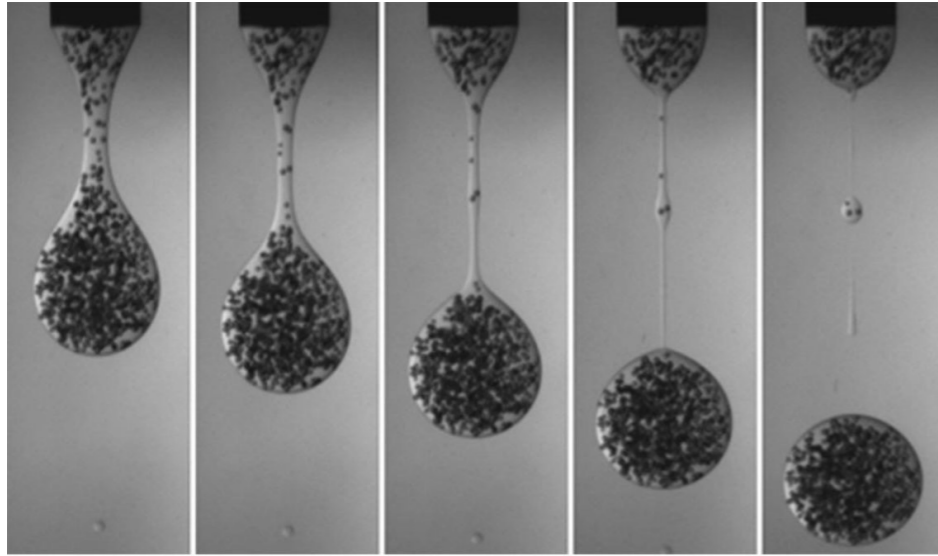
Liquid curtain



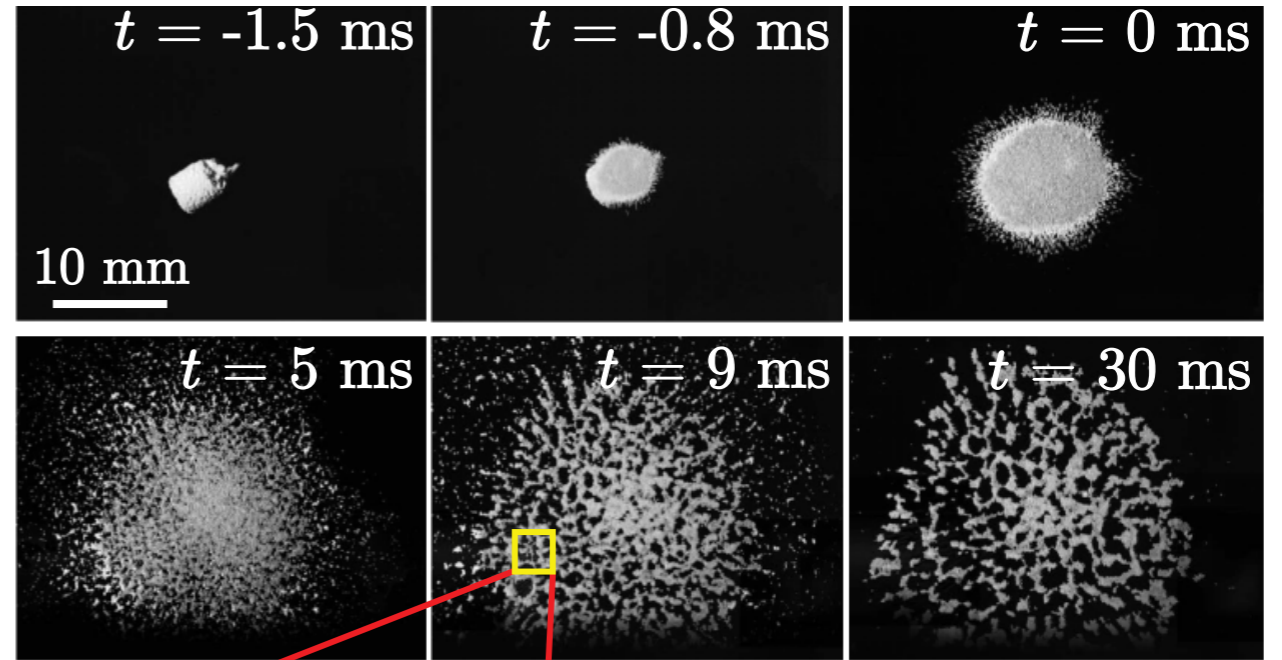
Dip-coating



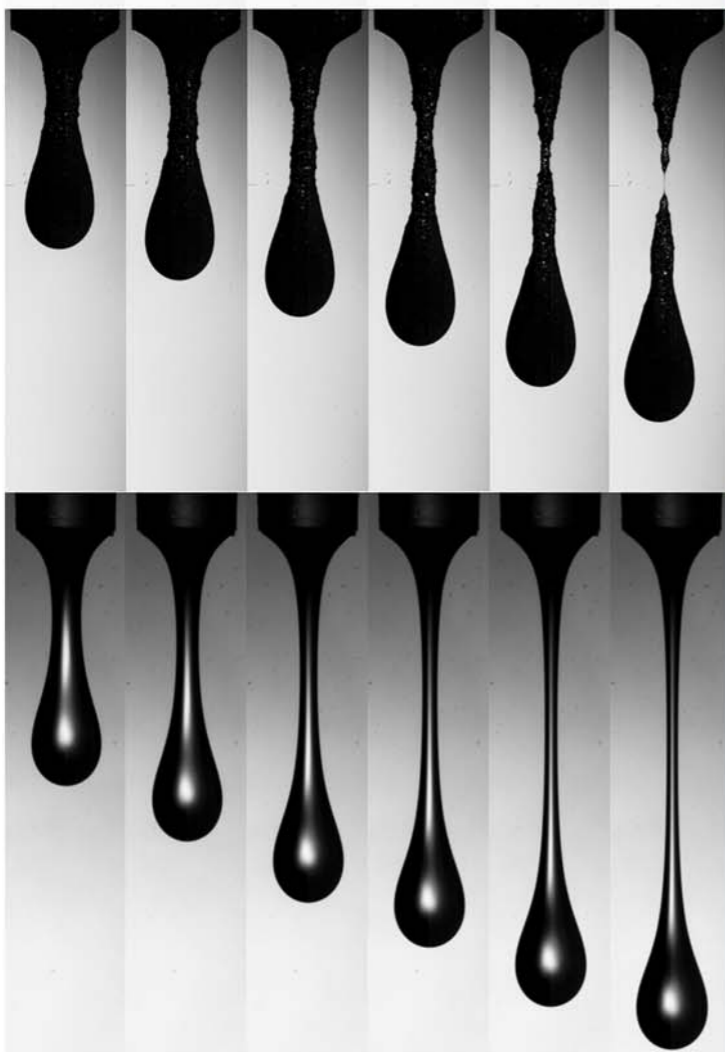
INTERFACIAL EFFECTS IN SUSPENSIONS



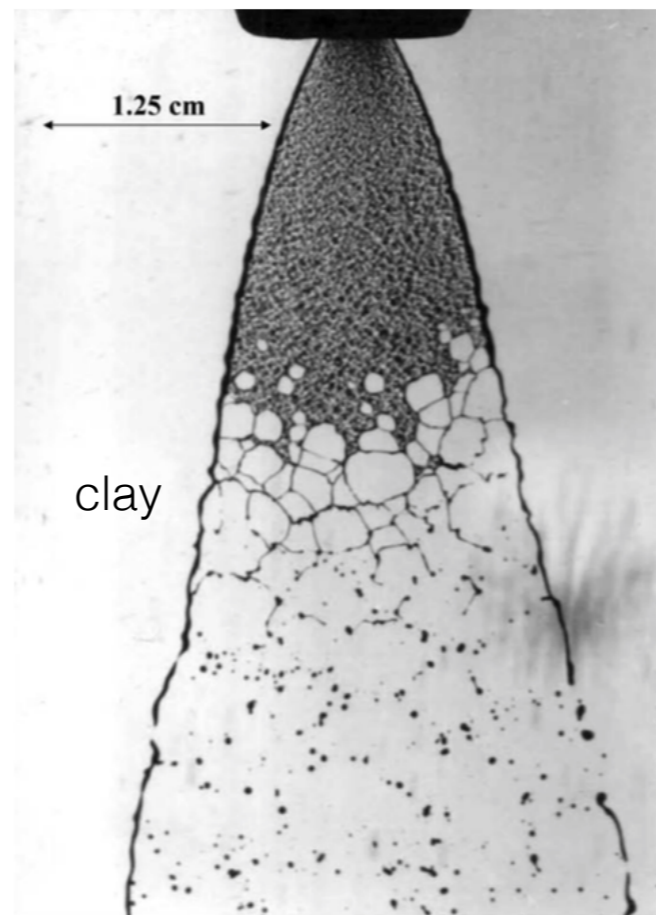
Furbank & Morris, Phys. Fluids (2004)



Lubbers *et al.*, Phys. Rev. Lett. (2014)



Bonnoit *et al.*, Phys. Fluids (2012)

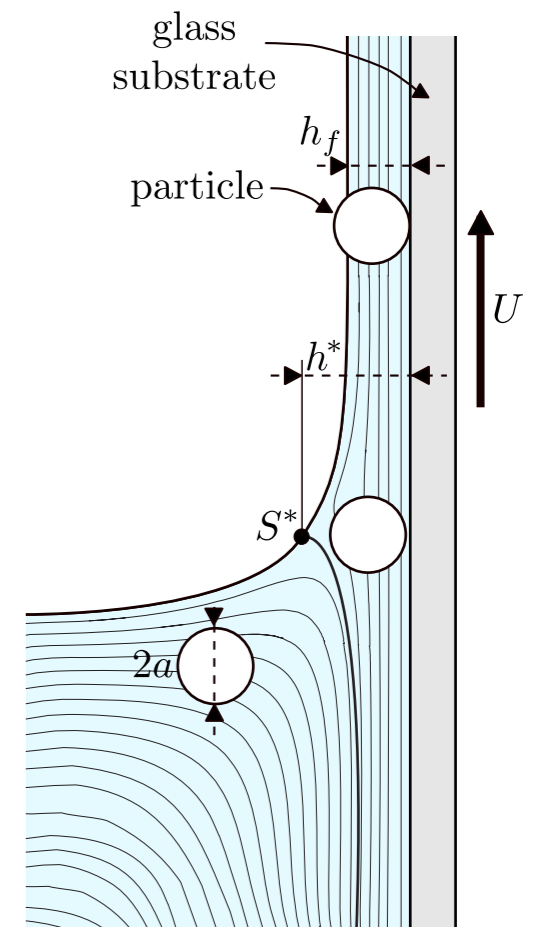
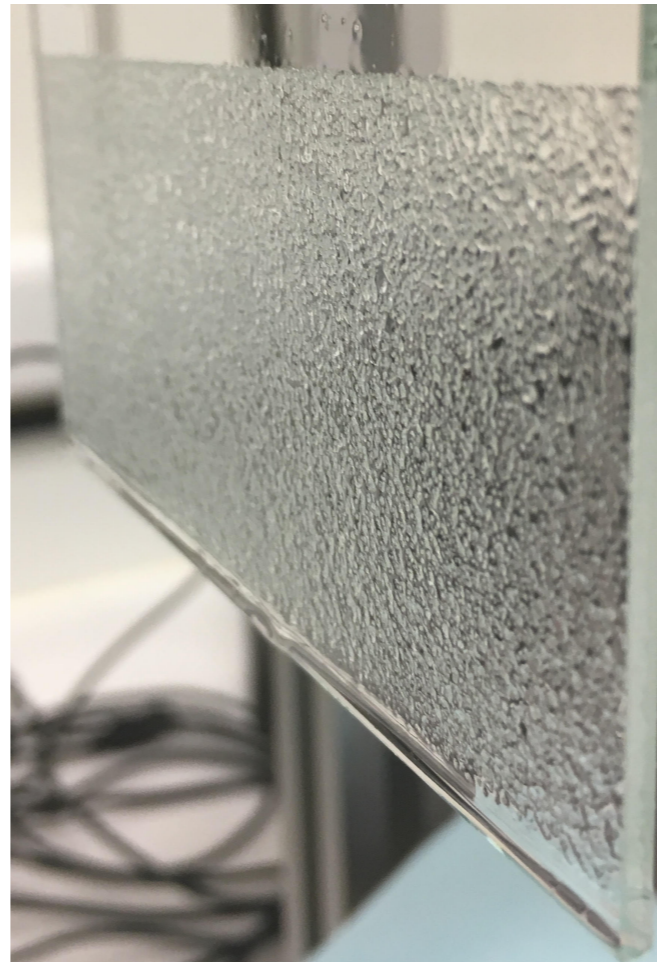
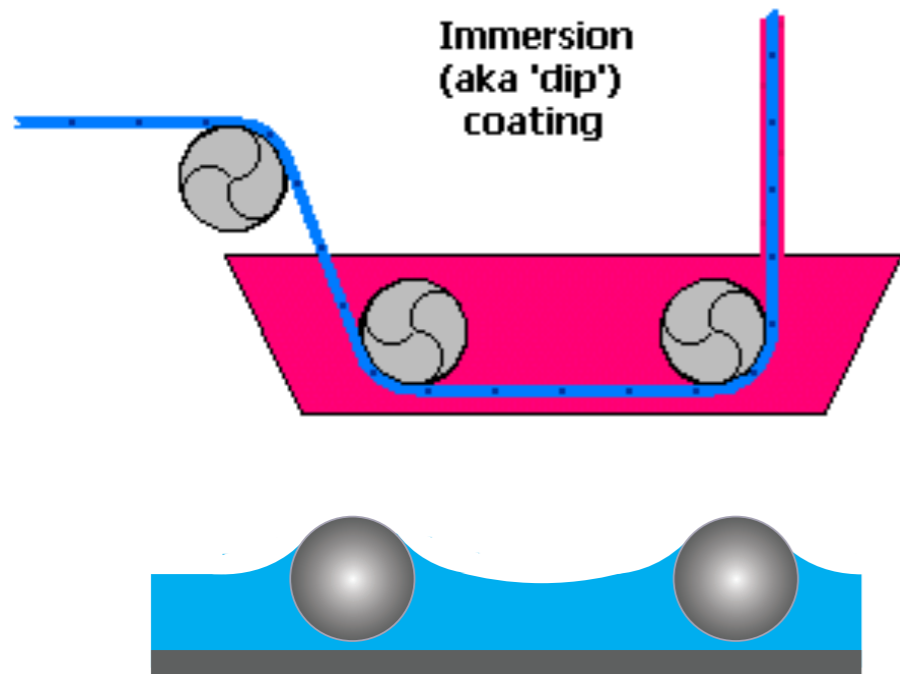


Addo-Yobo *et al.*,
AIChE (2010)



Buchanan *et al.*,
Langmuir (2007)

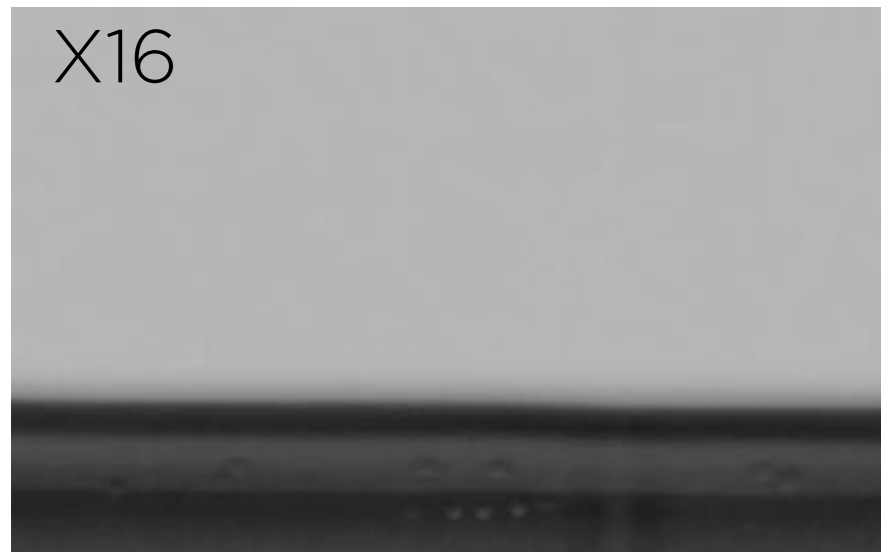
DIP COATING



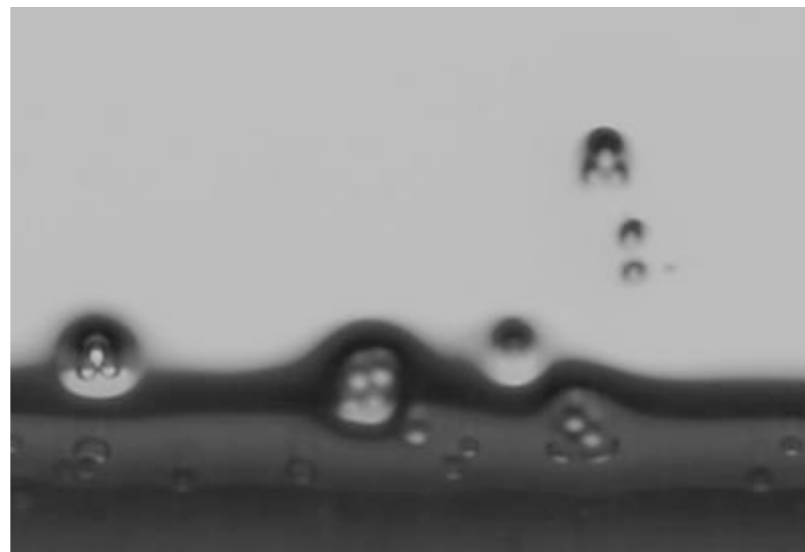
Colosqui et al.,
Phys. Rev. Lett. (2013)

Presence of particles
during coating
processes ?

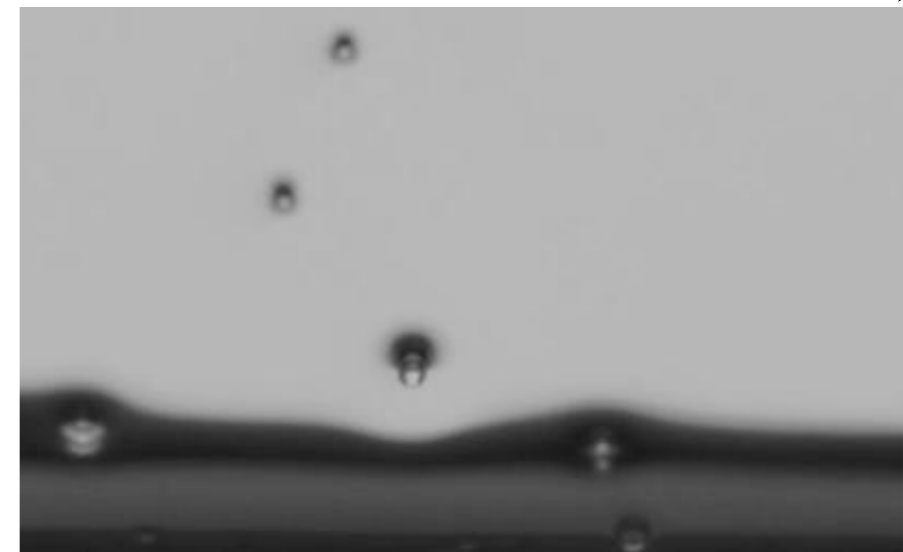
X16



$U = 7.3 \mu\text{m/s}$
 $h = 14 \mu\text{m}$

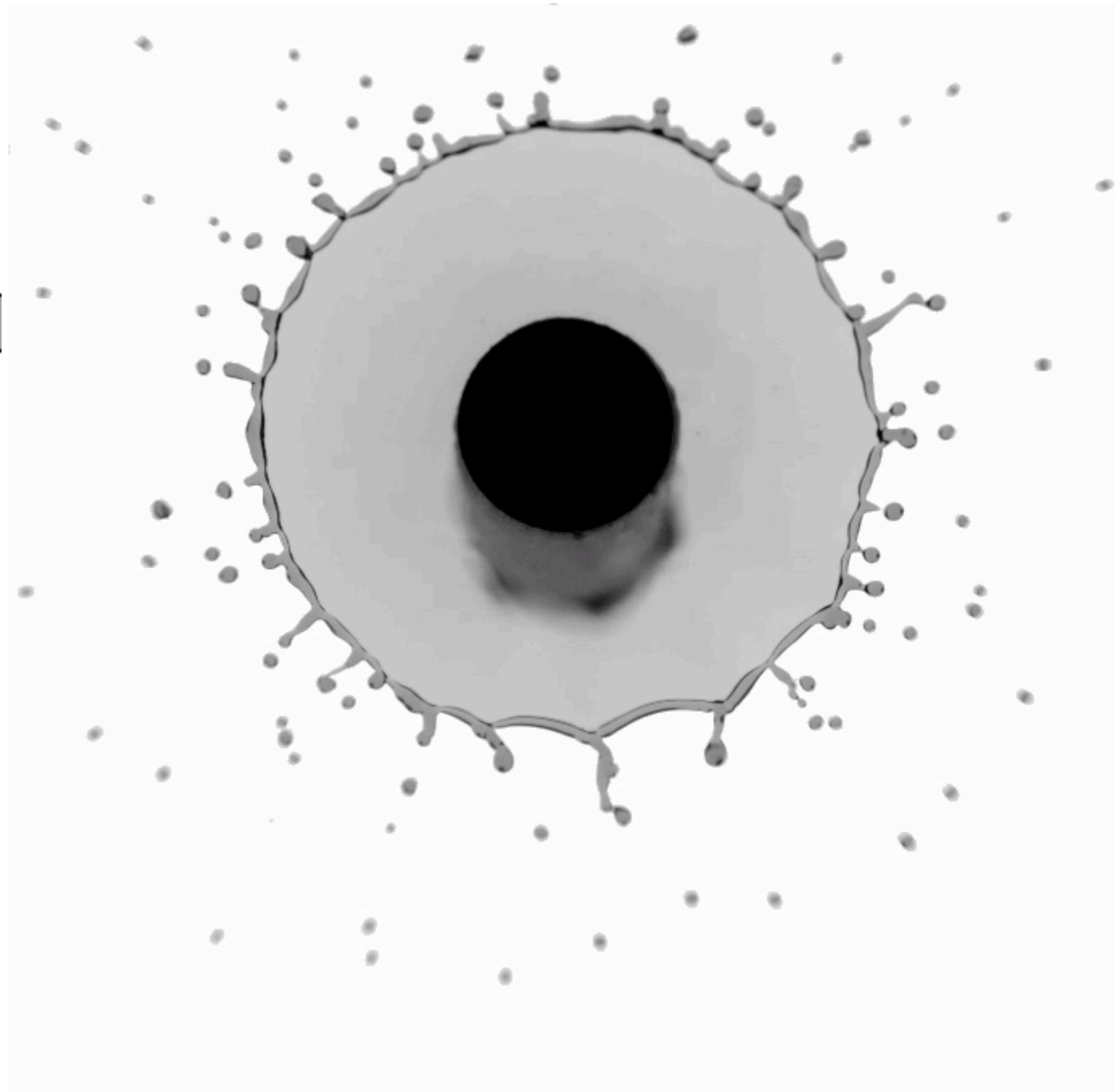
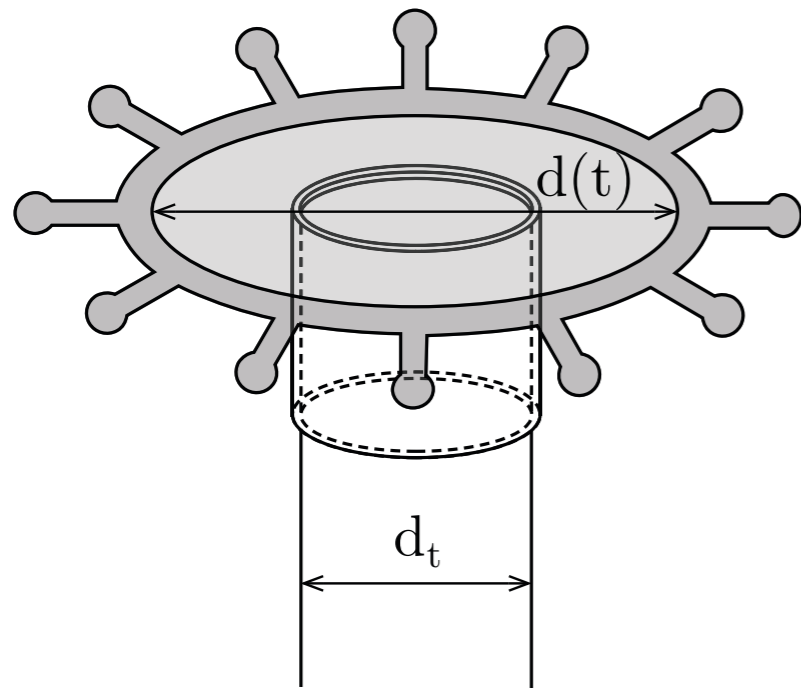
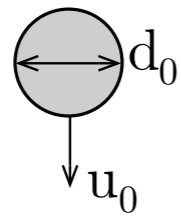
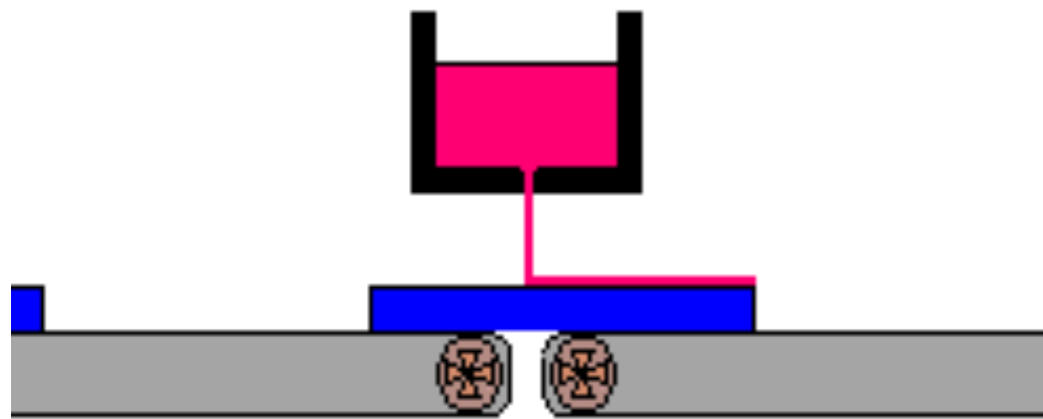


$U = 17 \mu\text{m/s}$
 $h = 24 \mu\text{m}$



$U = 36 \mu\text{m/s}$
 $h = 40 \mu\text{m}$

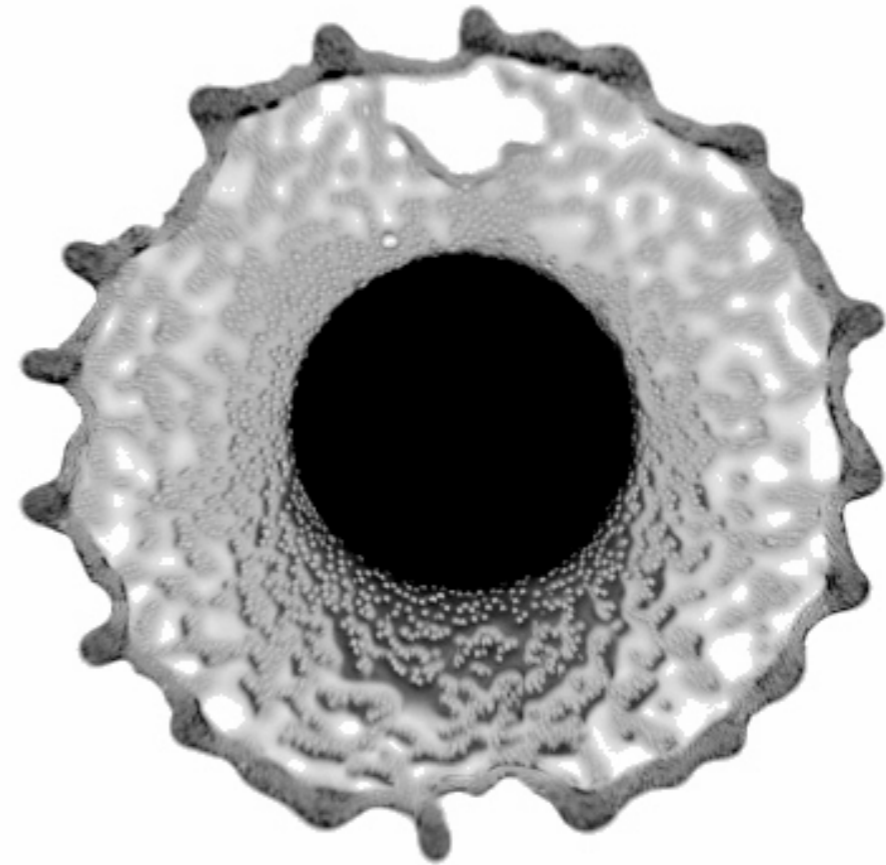
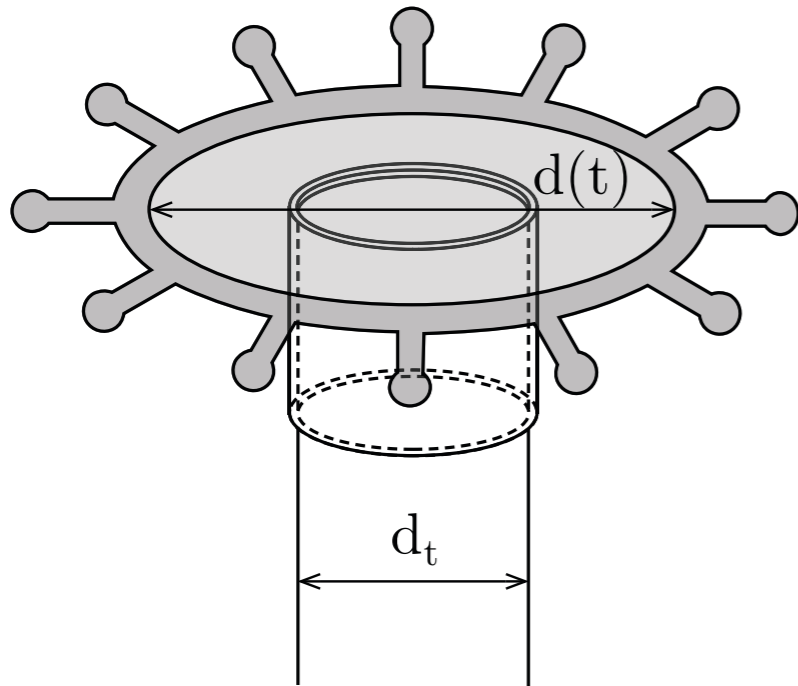
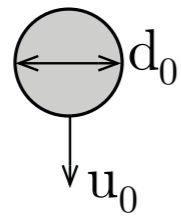
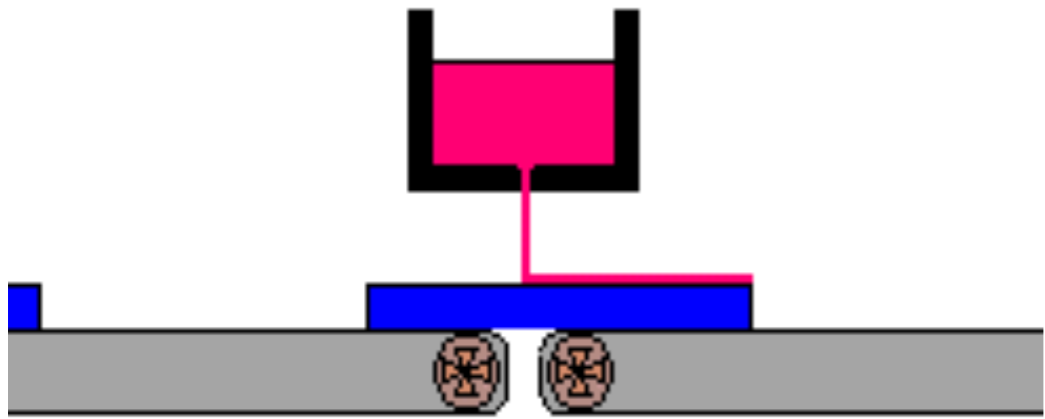
LIQUID CURTAIN



Bossa & Villermaux, JFM (2011)
Vernay et al., PRL (2015)

duration: 15 ms

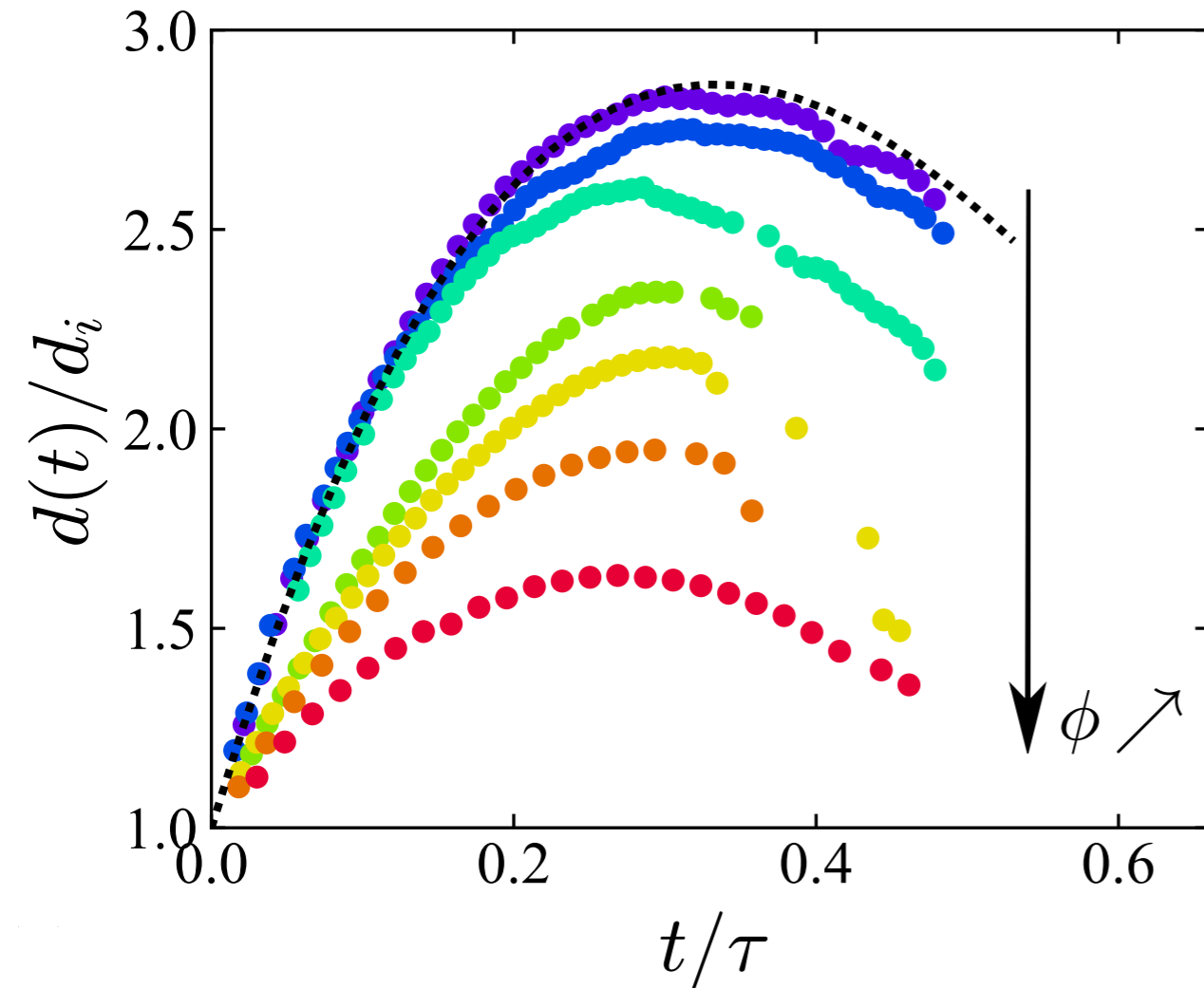
LIQUID CURTAIN



Bossa & Villermaux, JFM (2011)
Vernay et al., PRL (2015)

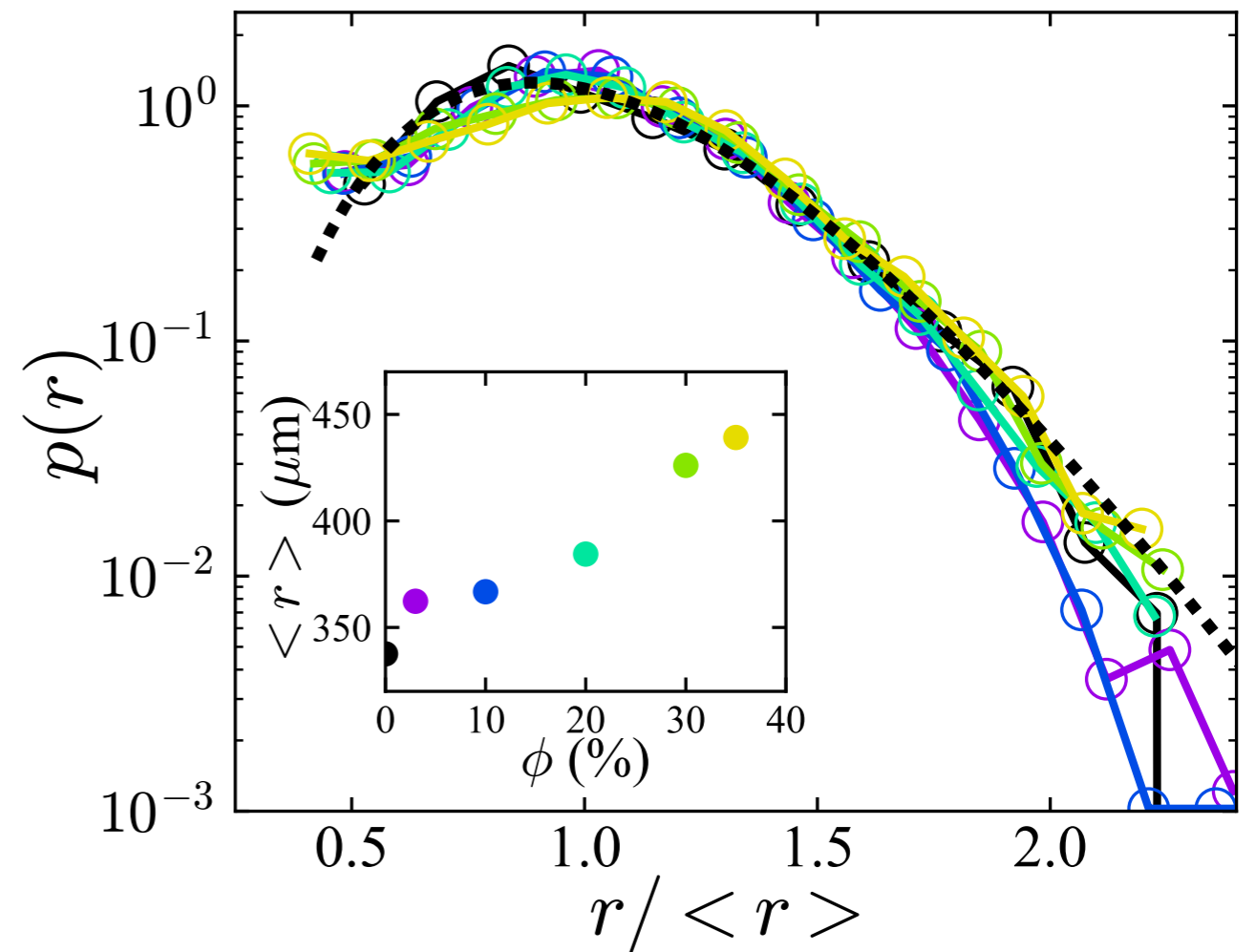
duration: 15 ms

PARTICLE-LADEN LIQUID SHEET



Expansion : captured using the viscosity of the suspension

S. Arora, C. Ligoure, & L. Ramos,
Phys. Rev. Fluids (2016)



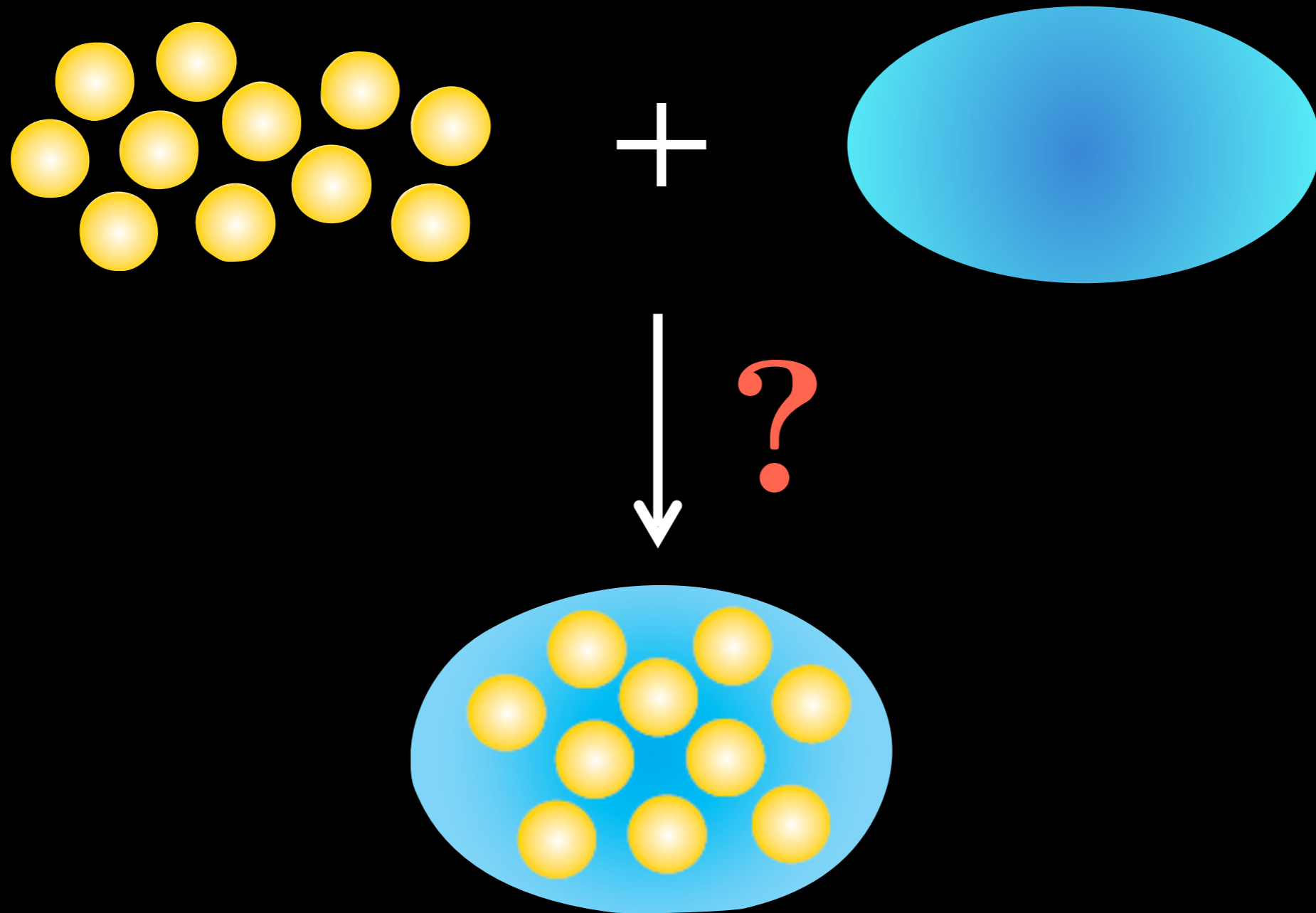
Atomization modified by the formation of clusters

$$\Gamma(n, x = d / \langle d \rangle) = \frac{n^n}{\Gamma(n)} x^{n-1} e^{-nx}$$

B. Keshavarz, E. C. Houze, J. R. Moore, M. R. Koerner & G. H. McKinley, Phys. Rev. Lett (2016).

Role of the interfacial effects in suspension flows: Particles modify thin film dynamics through viscous and local effects

BLENDING LIQUID AND GRAINS



How to prepare a dense suspension or a wet granular media ?

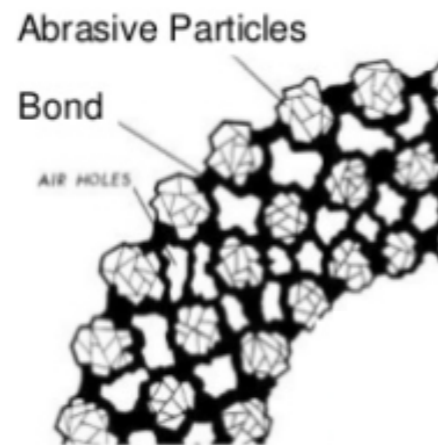
BLENDING LIQUID AND GRAINS



Hydration of plaster



Preparation of mortar



Preparation of adhesive wheels

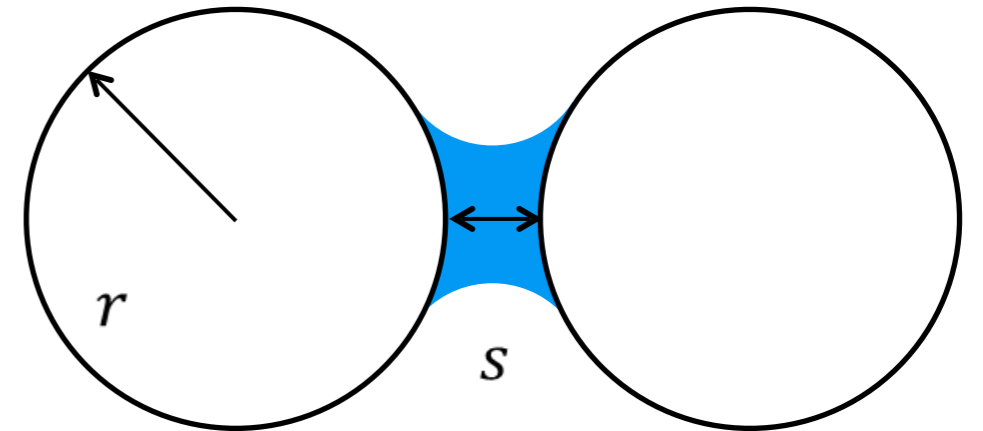
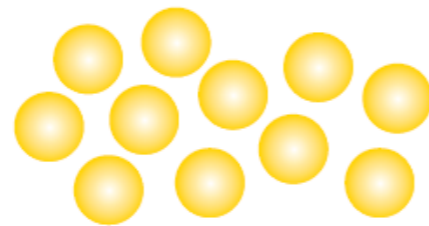


Wet granulation in powder

How to efficiently blend liquid and grains ?

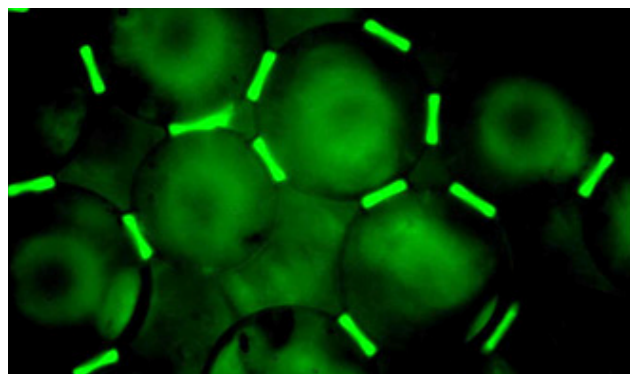
FROM DRY GRANULAR MATERIALS TO SUSPENSIONS

dry state

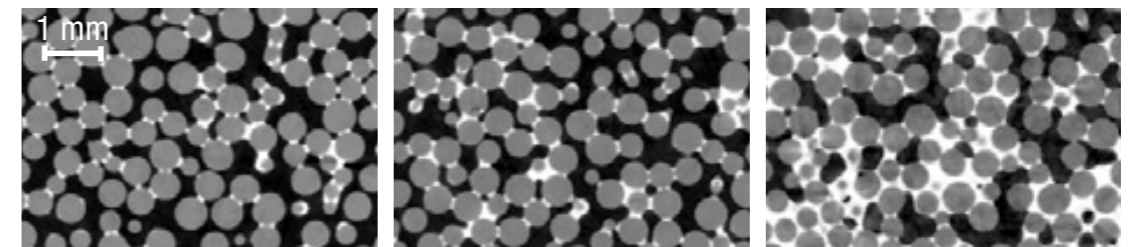
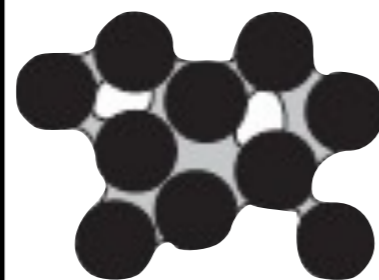


$$F_{cap} = 2\pi\gamma r \cos \theta_c$$

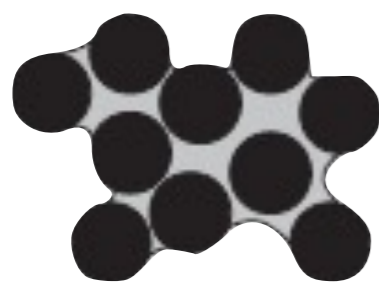
Willett et al., Langmuir (2000)



pendular

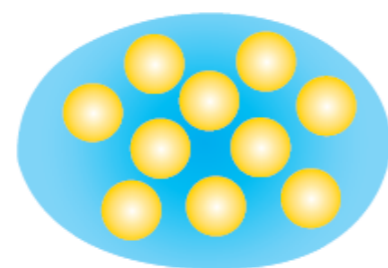


funicular

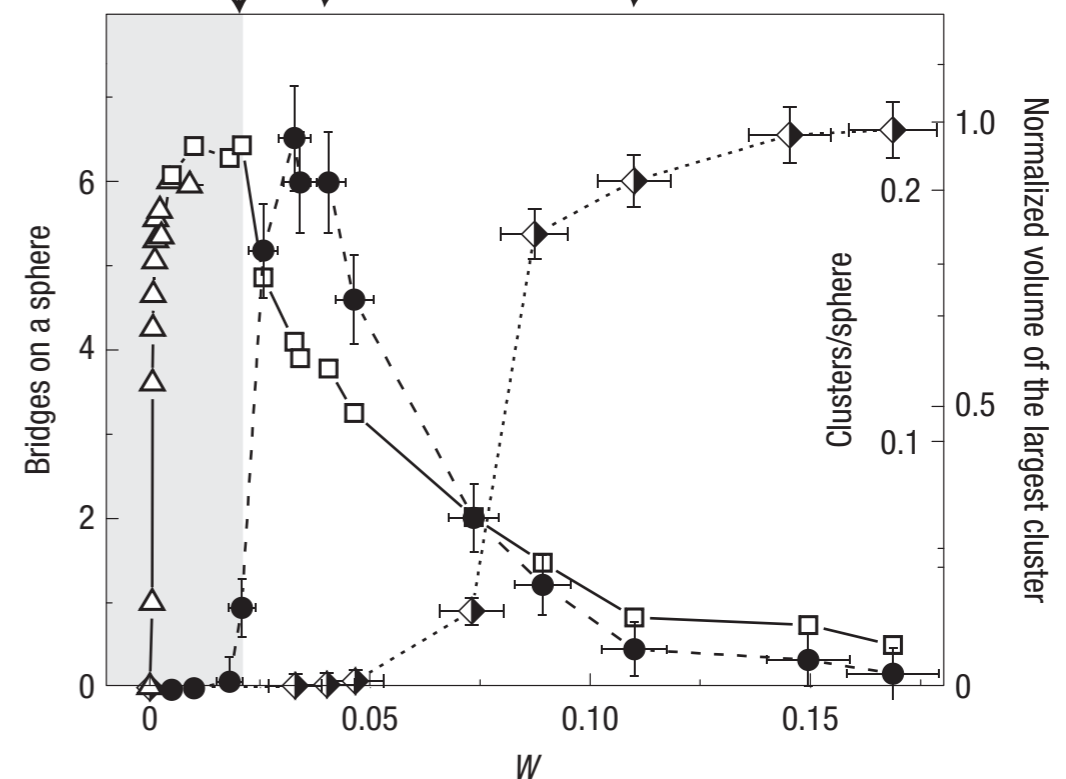


capillary

Suspension



Saturation rate



Scheel et al., Nat. Mater. (2008)

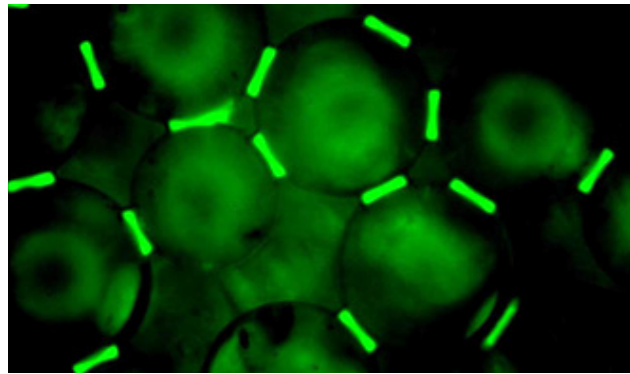
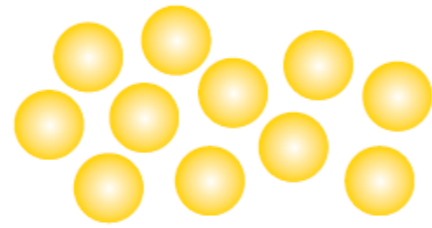
Moller & Bonn, EPL (2007)

Herminghaus Adv. Phys. (2005)

Mitarai & Nori Adv. Phys. (2006)

FROM DRY GRANULAR MATERIALS TO SUSPENSIONS

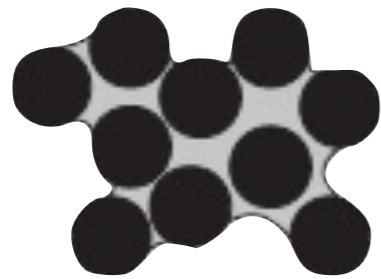
dry state



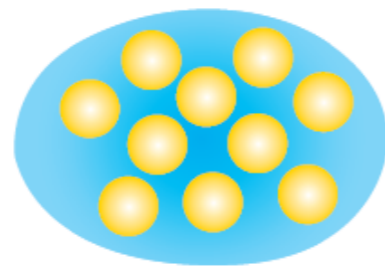
pendular



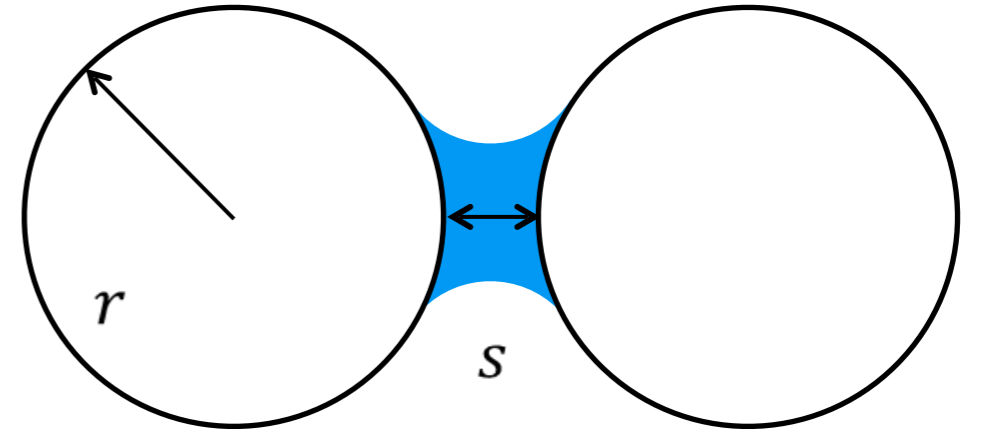
funicular



Suspension



Saturation rate



$$F_{cap} = 2\pi\gamma r \cos \theta_c$$

Willett et al., Langmuir (2000)



Pakpour et al., Sci. Rep. (2012)

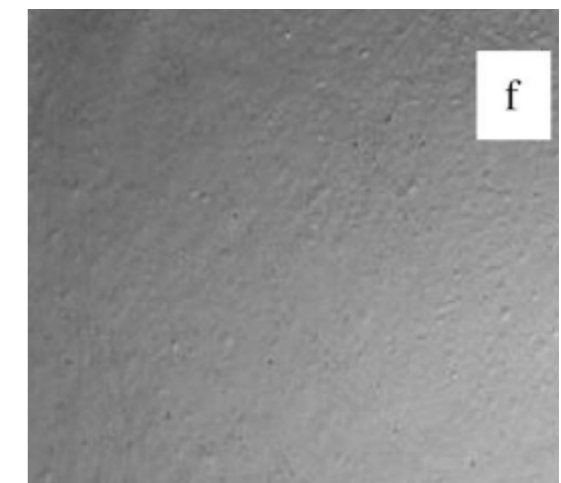
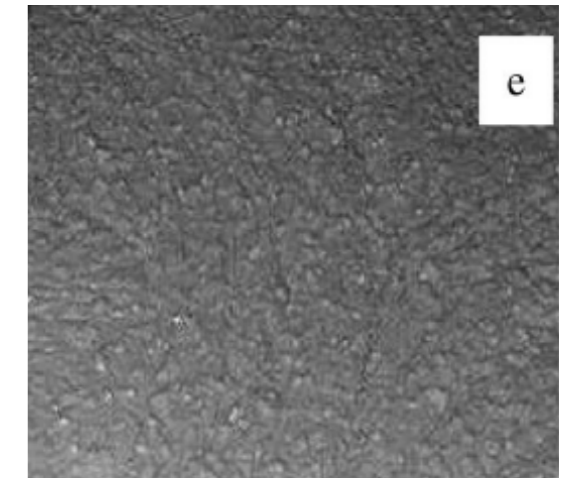
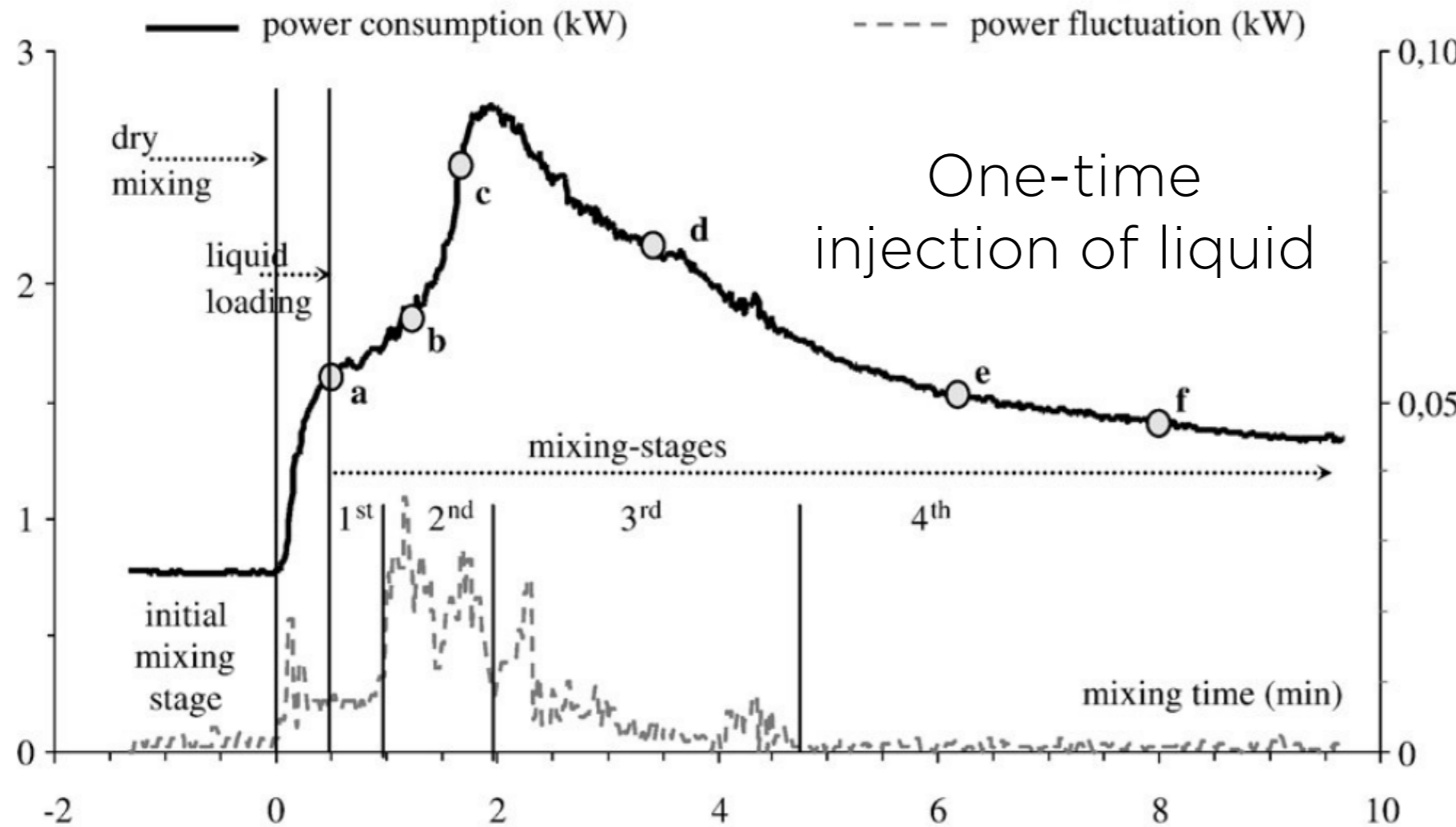
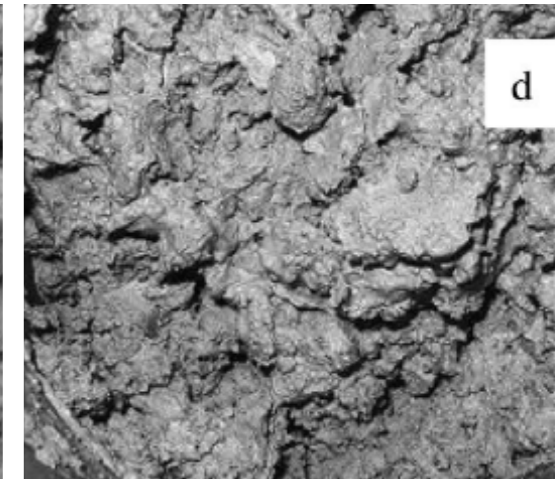
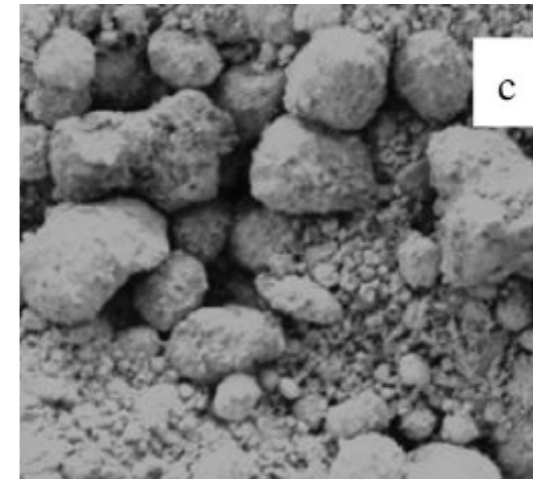
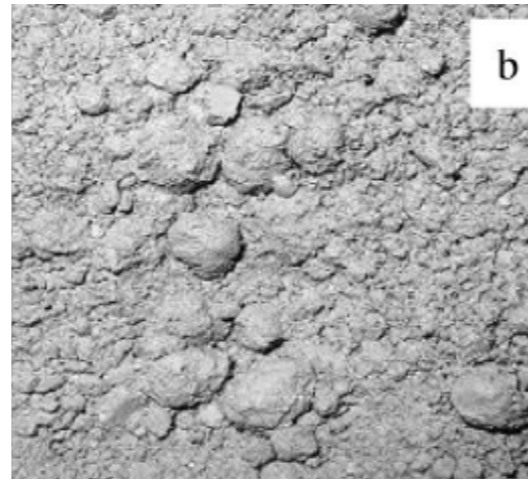
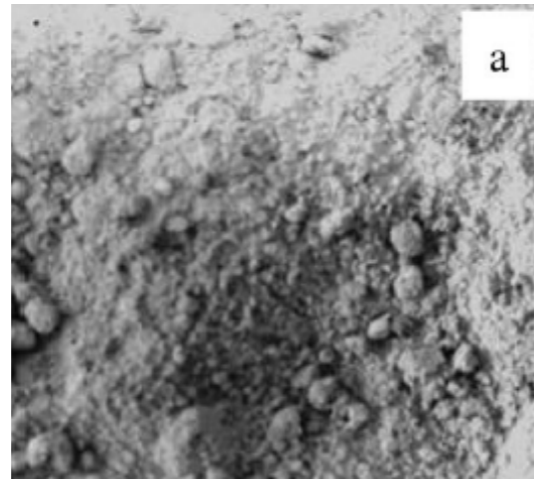
Nowak et al., Nat. Phys. (2005)

Moller & Bonn, EPL (2007)

Herminghaus Adv. Phys. (2005)

Mitarai & Nori Adv. Phys. (2006)

FROM DRY GRANULAR MATERIALS TO SUSPENSIONS

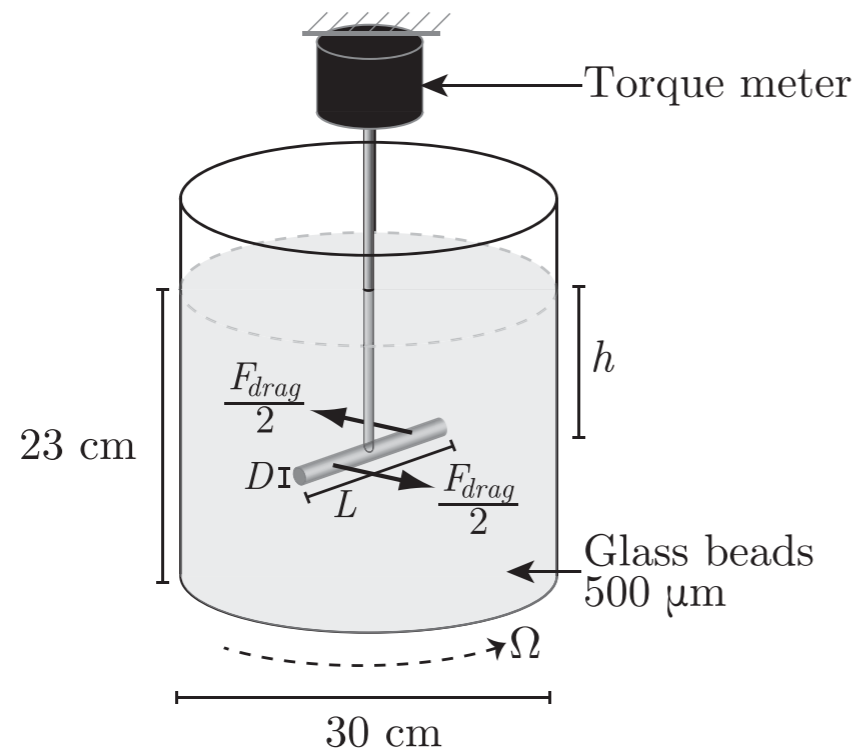


Cazacliu & Noquet, Cem. Concr. Res. (2009)

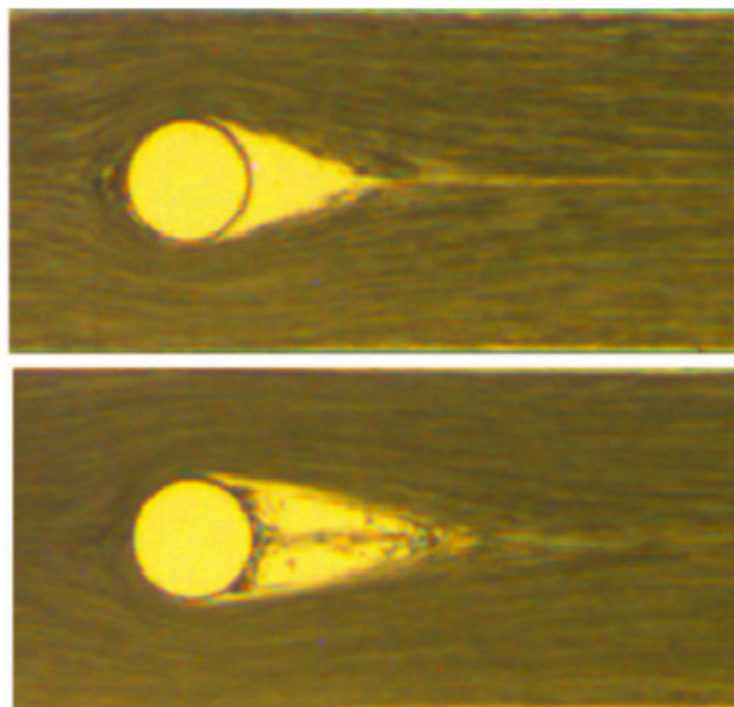
Betz et al., Int. J. Pharma. (2003)

BLENDING LIQUID AND GRAINS

Fluid/suspension interactions



Guillart et al., PRL (2013)

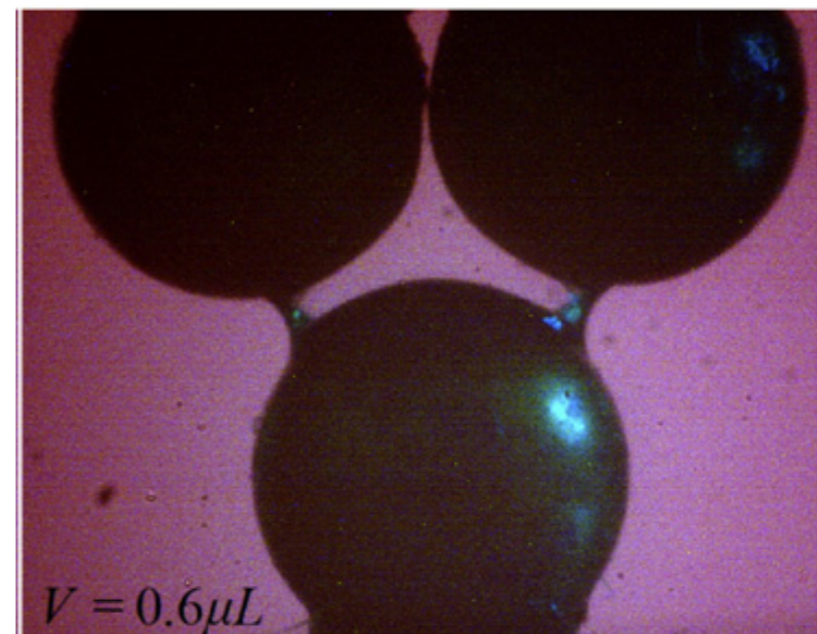


Haddadi et al., PRF (2016)

Capillary bridges



Soulie et al. EPJE (2006)

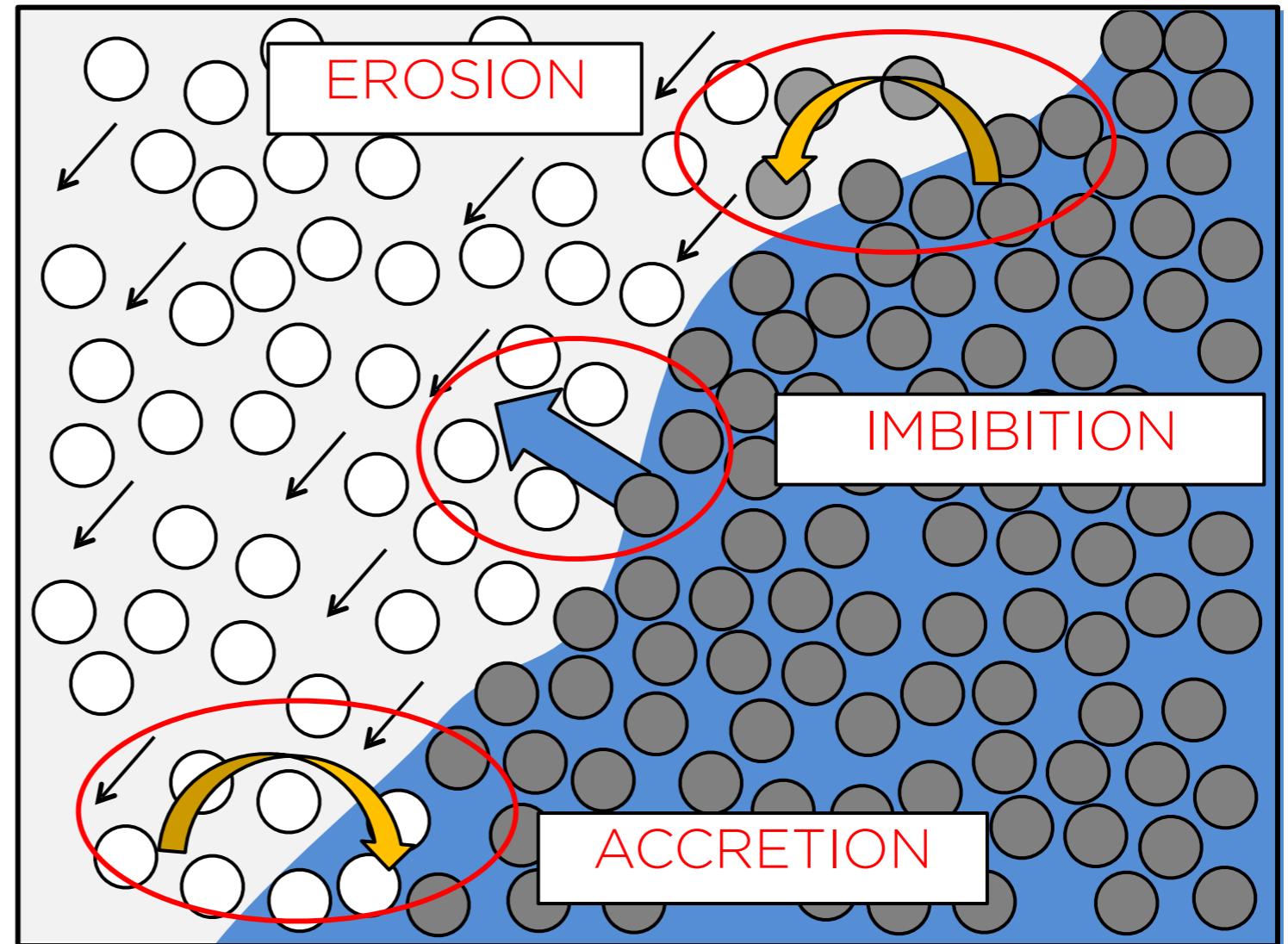


Wang et al. Powder Tech. (2017)

INTERACTION BETWEEN A GRANULAR FLOW AND A LIQUID

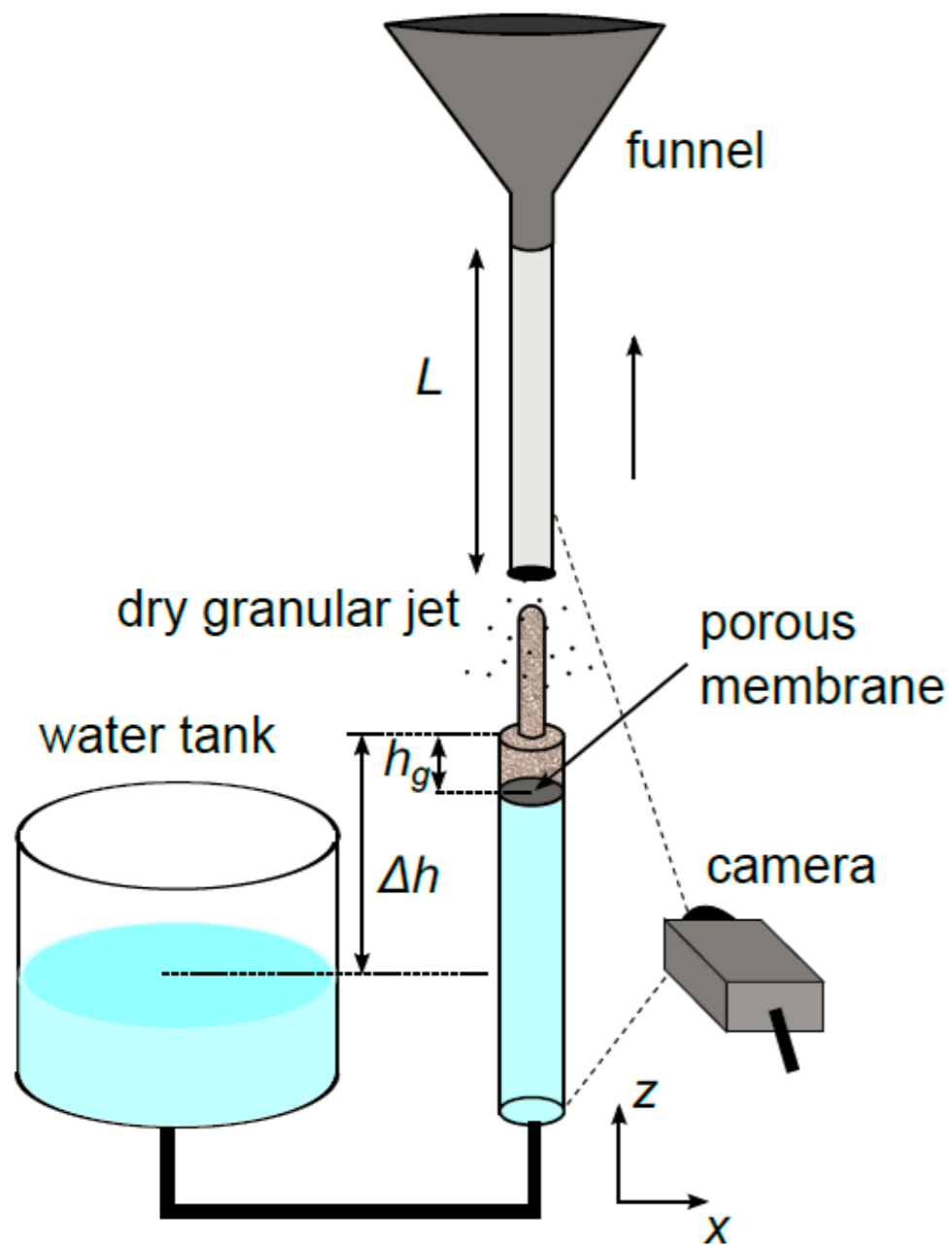


dry granular
flow



cohesive wet
grains

GRANULAR TOWER

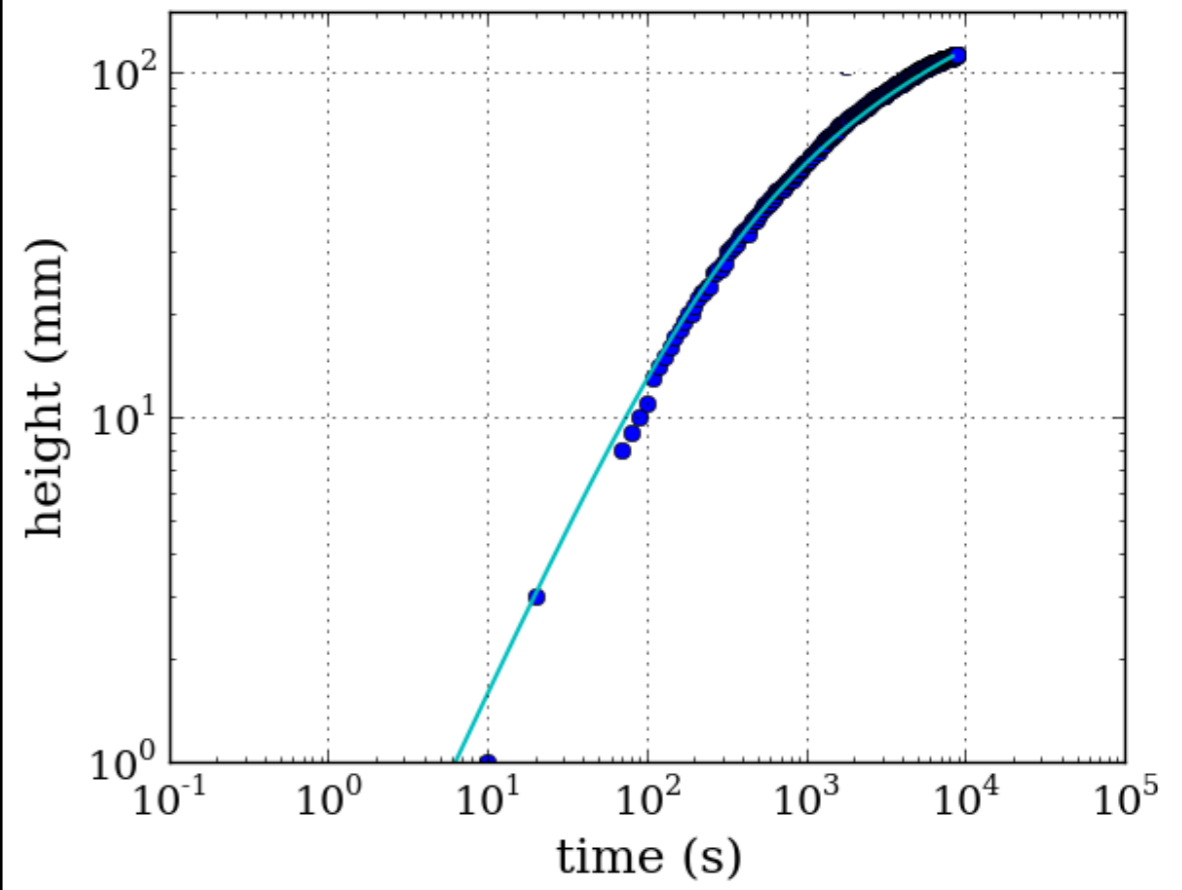
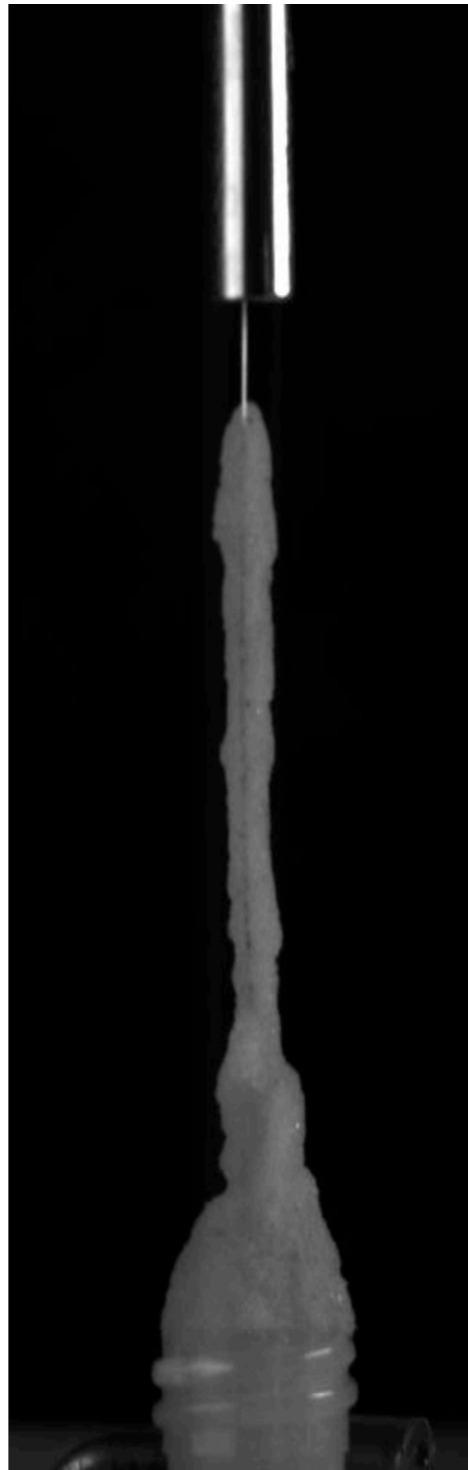
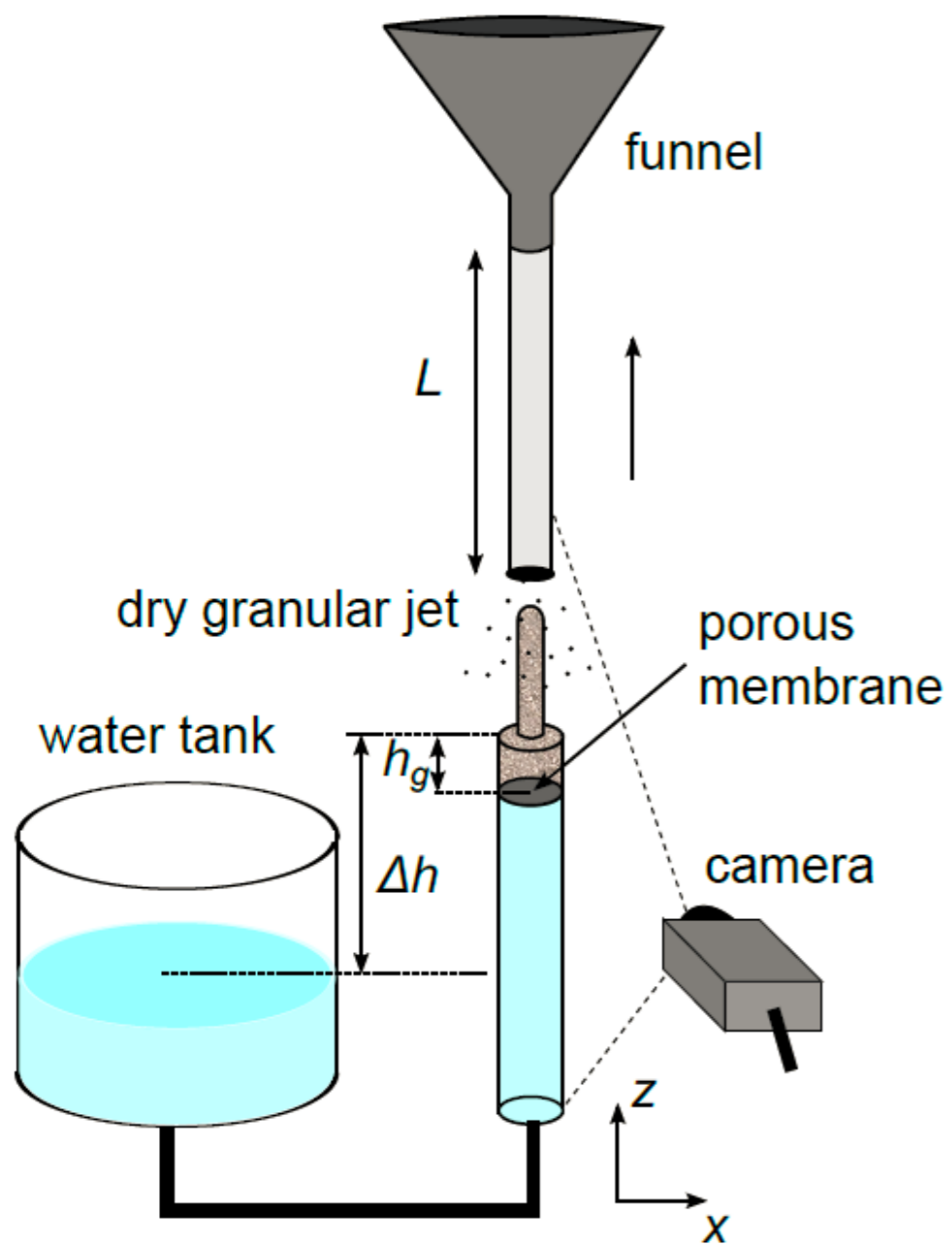


Inox tubing (2-100 cm)
Glass beads 100-315 μm

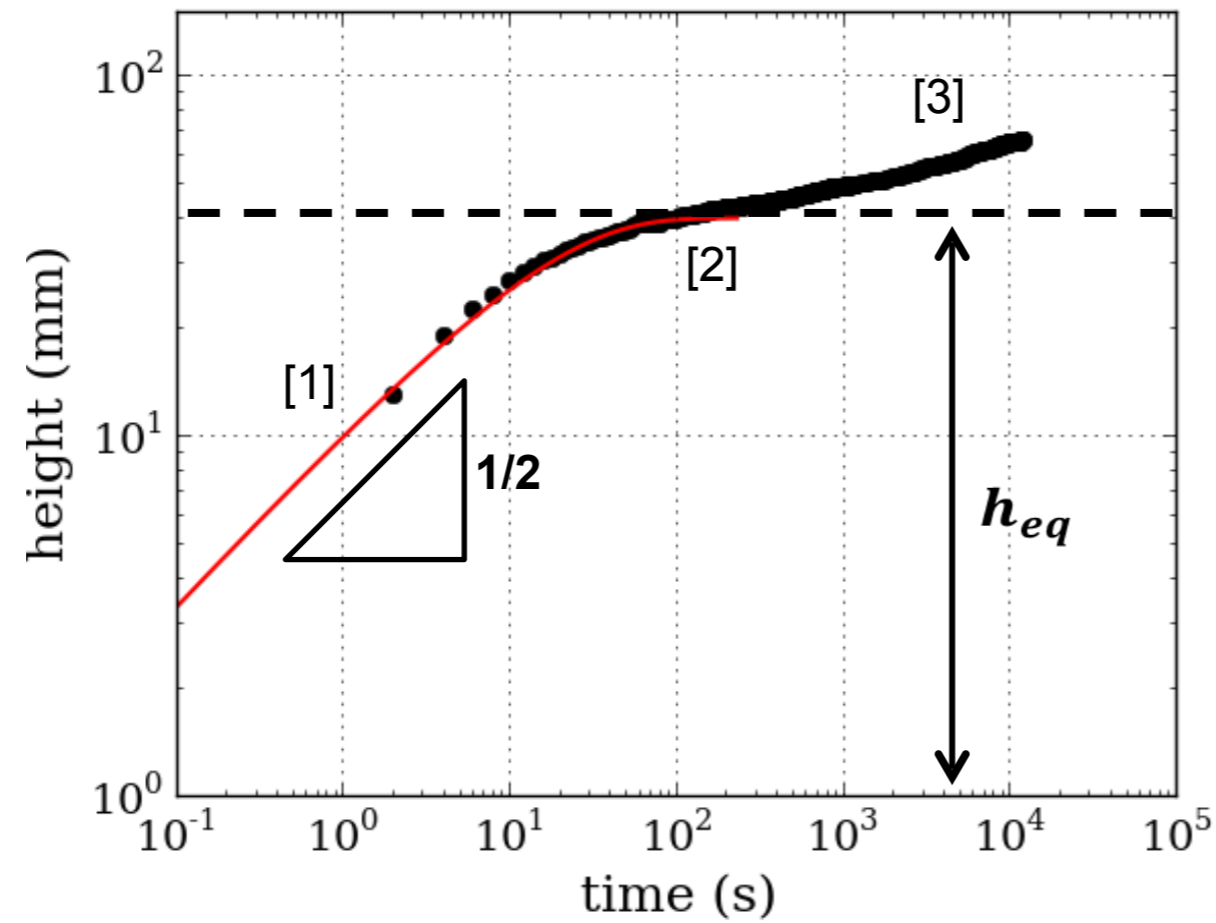
Reservoir of wet granular material

Pacheco-Vázquez *et al.*,
PRE (2012)

GRANULAR TOWER



CAPILLARY IMBIBITION VS VERTICAL ACCRETION



$$\mathbf{u} = -\frac{k}{\eta} (\nabla p - \rho \mathbf{g})$$

viscous
dissipation

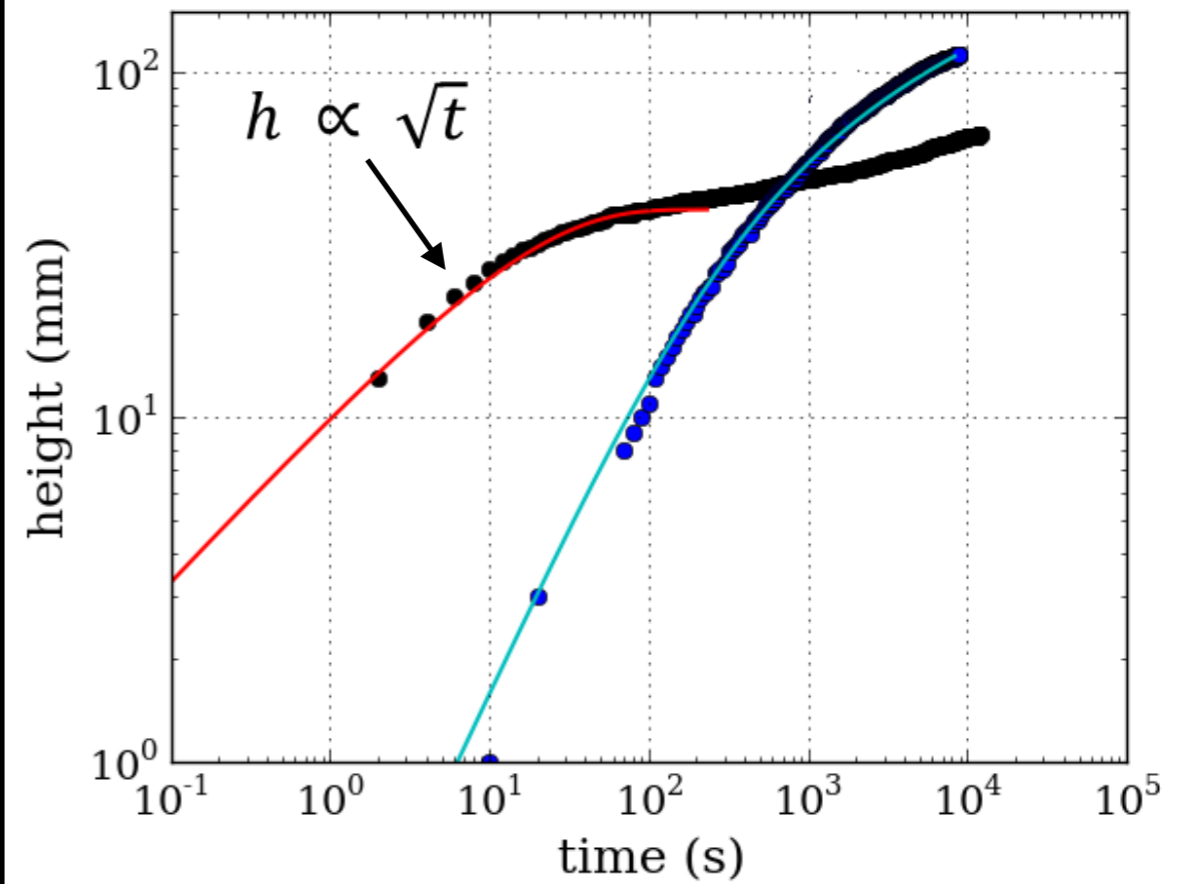
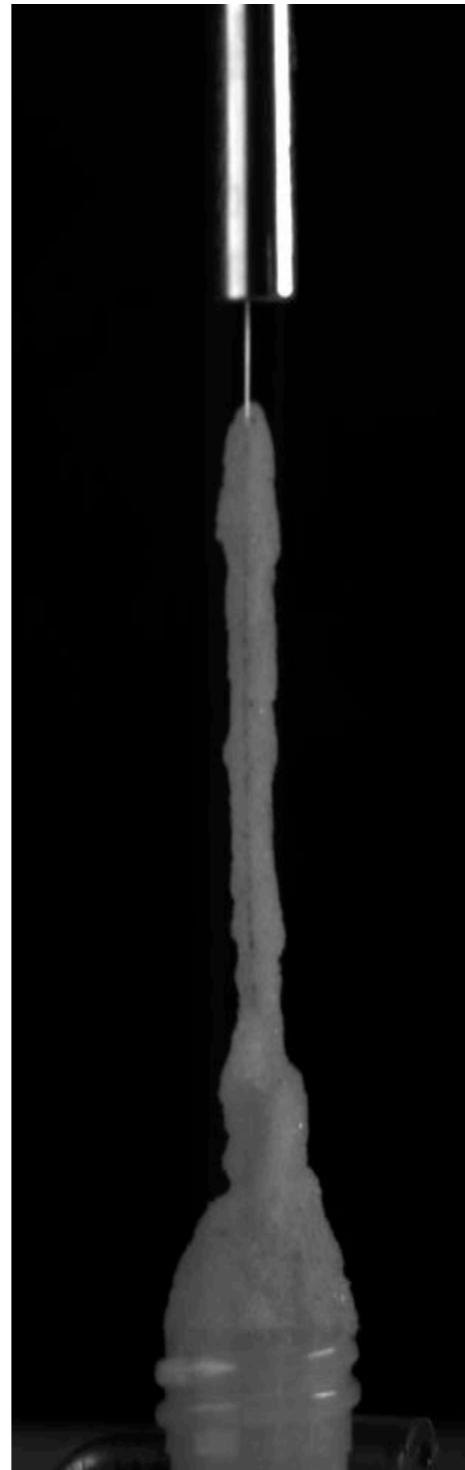
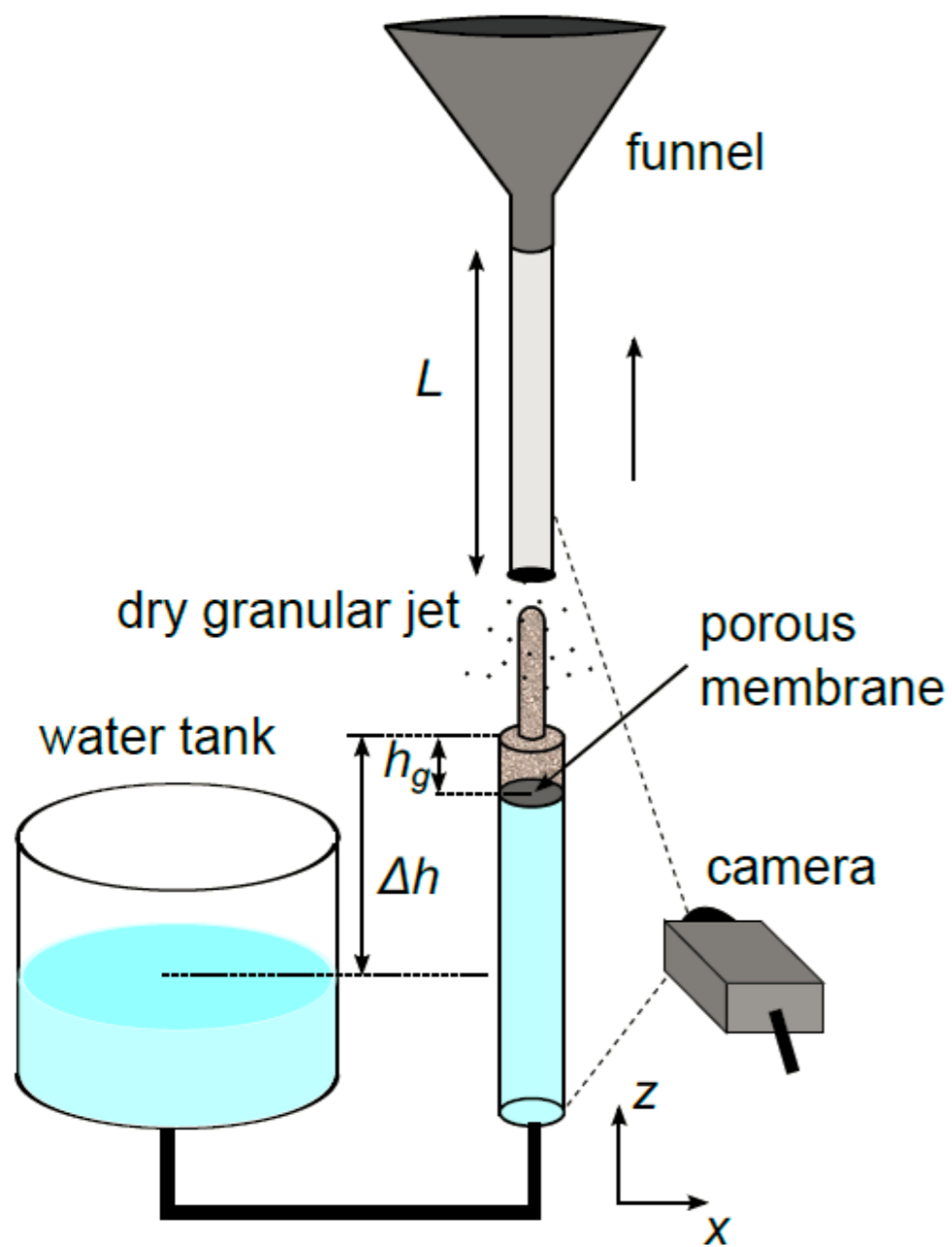
Driving
force

Pore size: $p_c = \frac{4\gamma \cos \theta_c}{d_p}$

Lucas-Washburn law: $h^2(t) \sim \frac{R\gamma \cos \theta}{\eta} t$

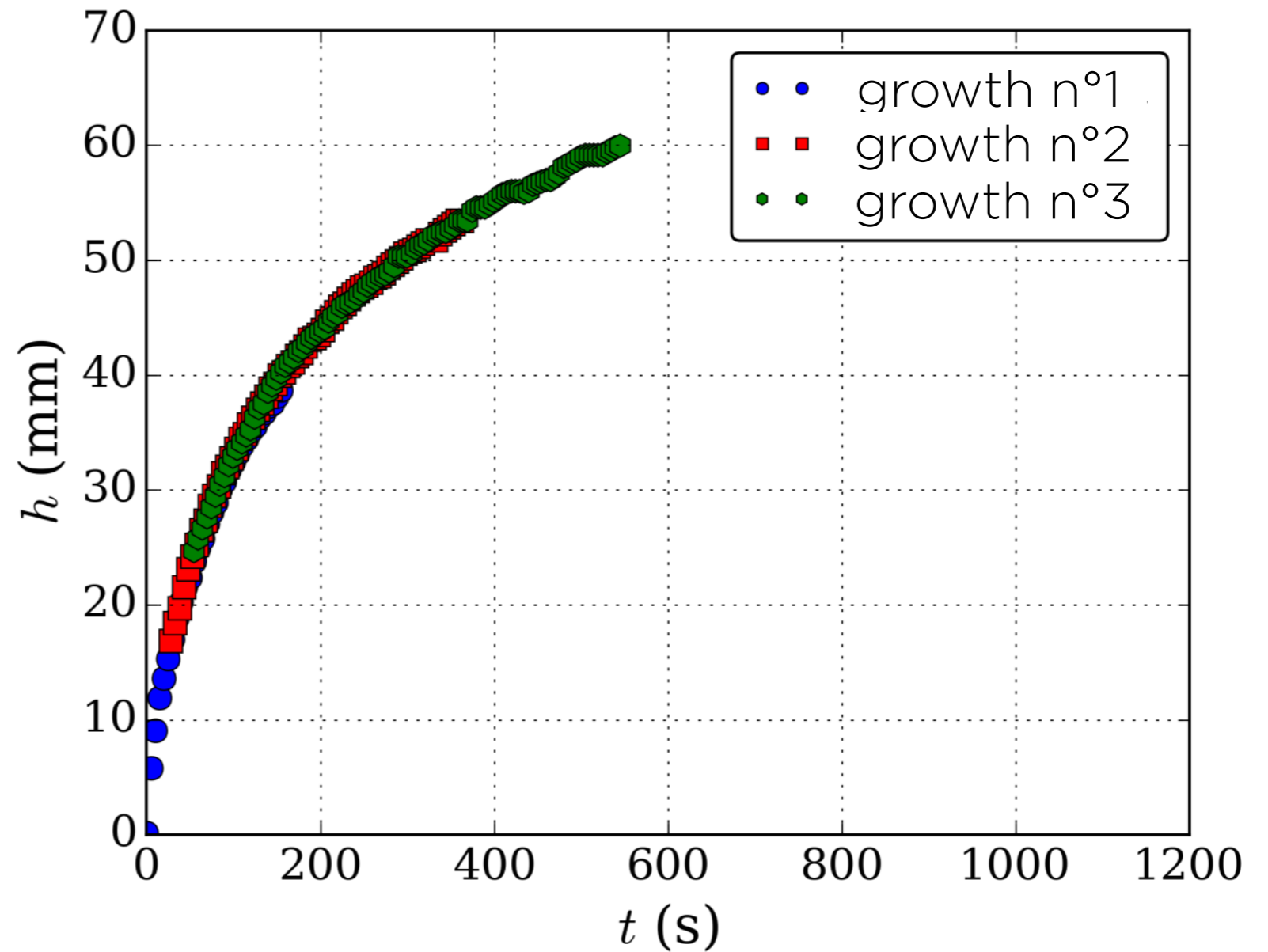
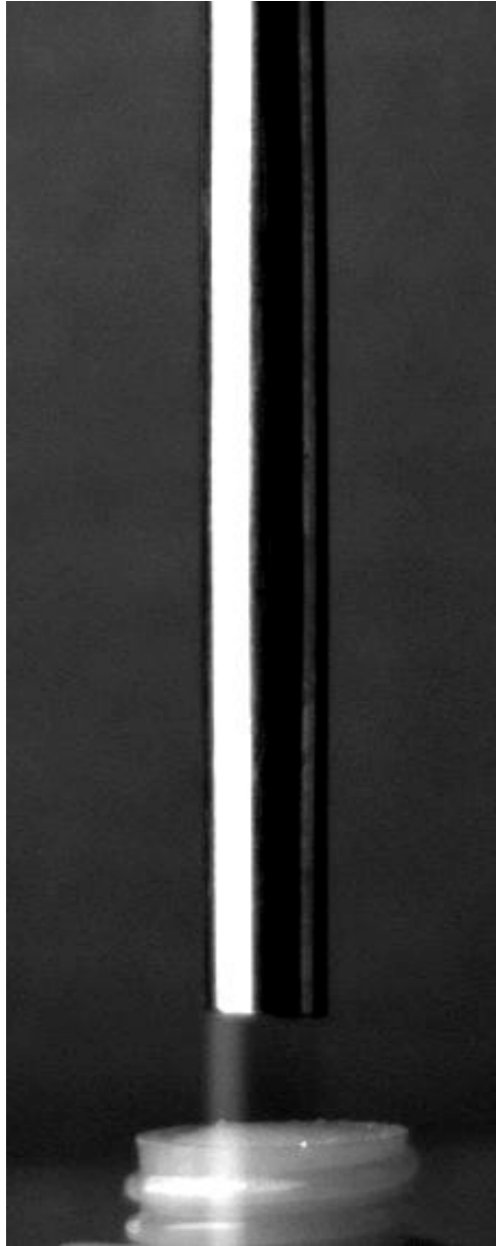
Jurin's height: $h_{max} = \frac{2\gamma \cos \theta}{\rho g R}$

GRANULAR TOWER



Growth dynamics cannot be fitted by the Lucas-Washburn law

GRANULAR TOWER

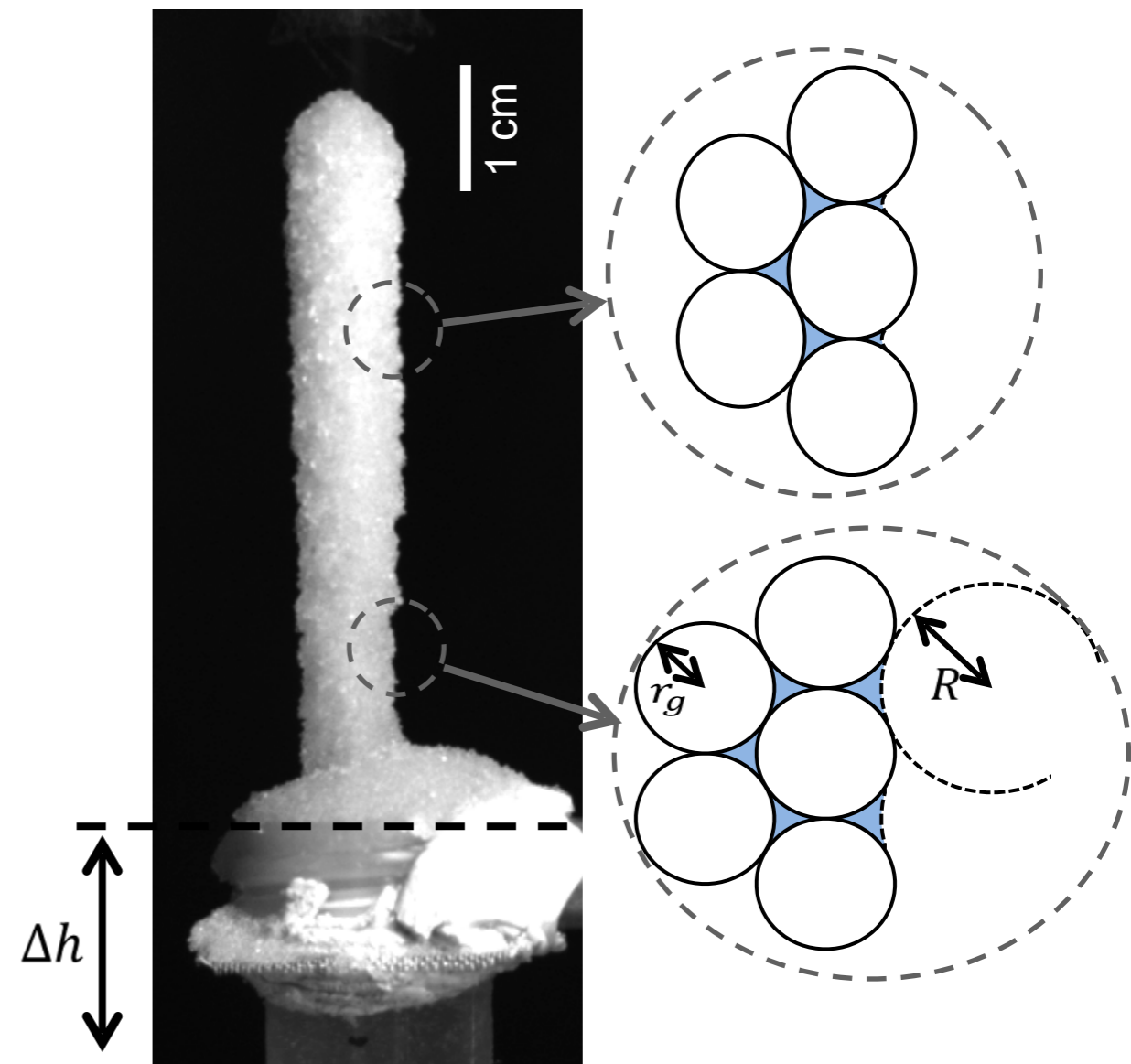
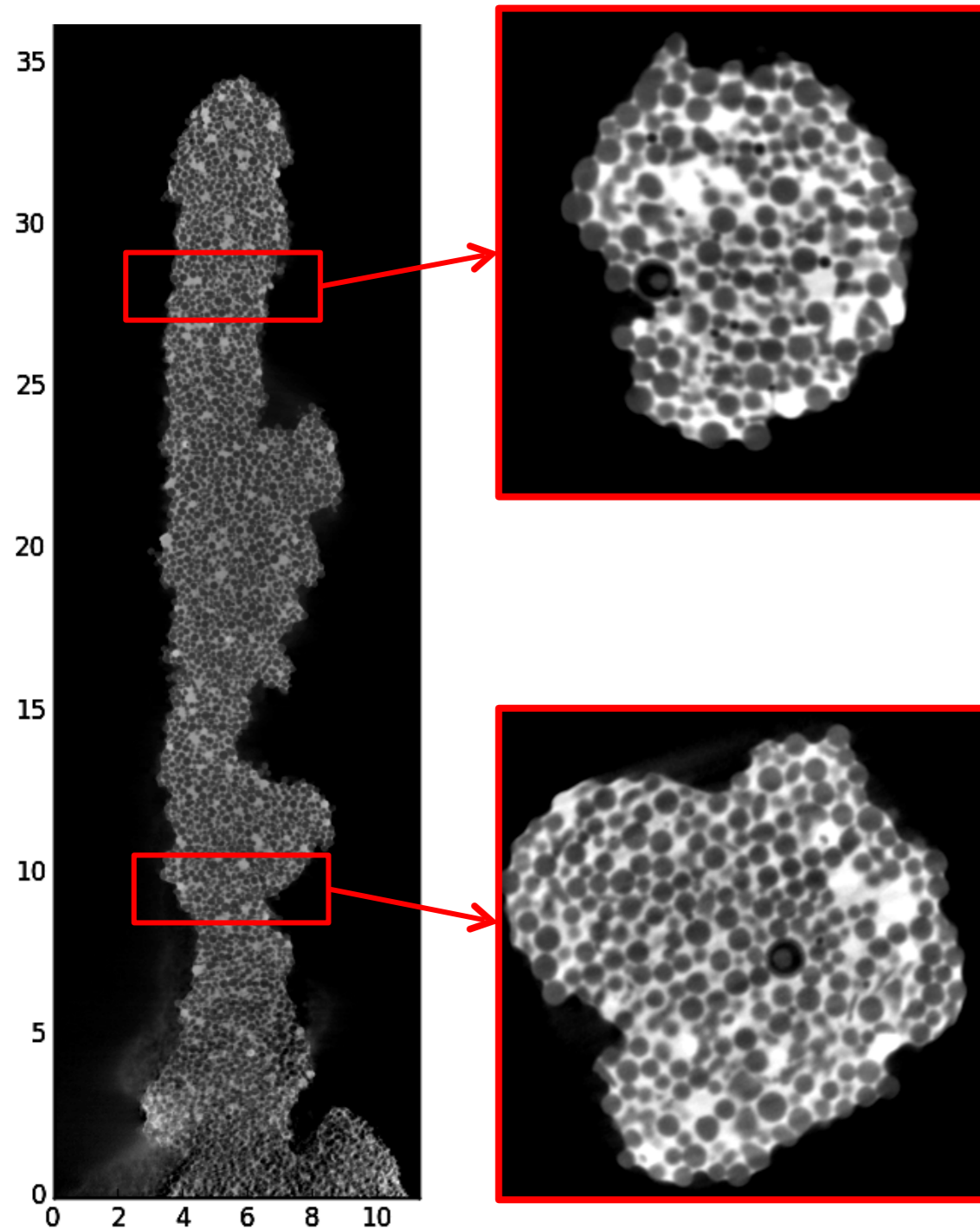


The growth of the wet aggregate only depends on the particle/liquid/air interface where the grains are impacting

Local effects

LIQUID DISTRIBUTION

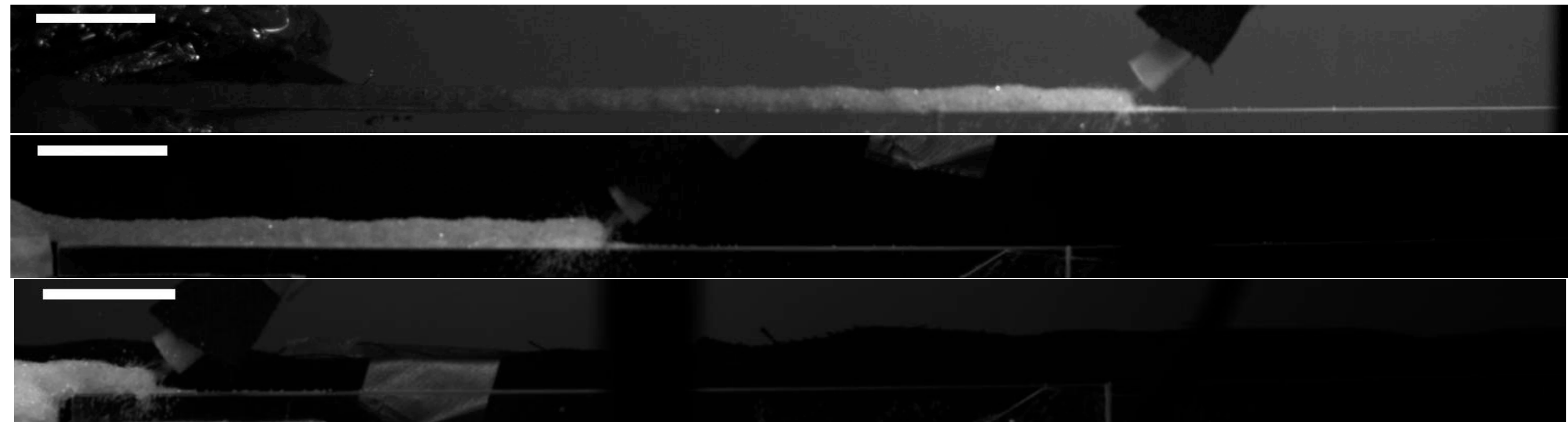
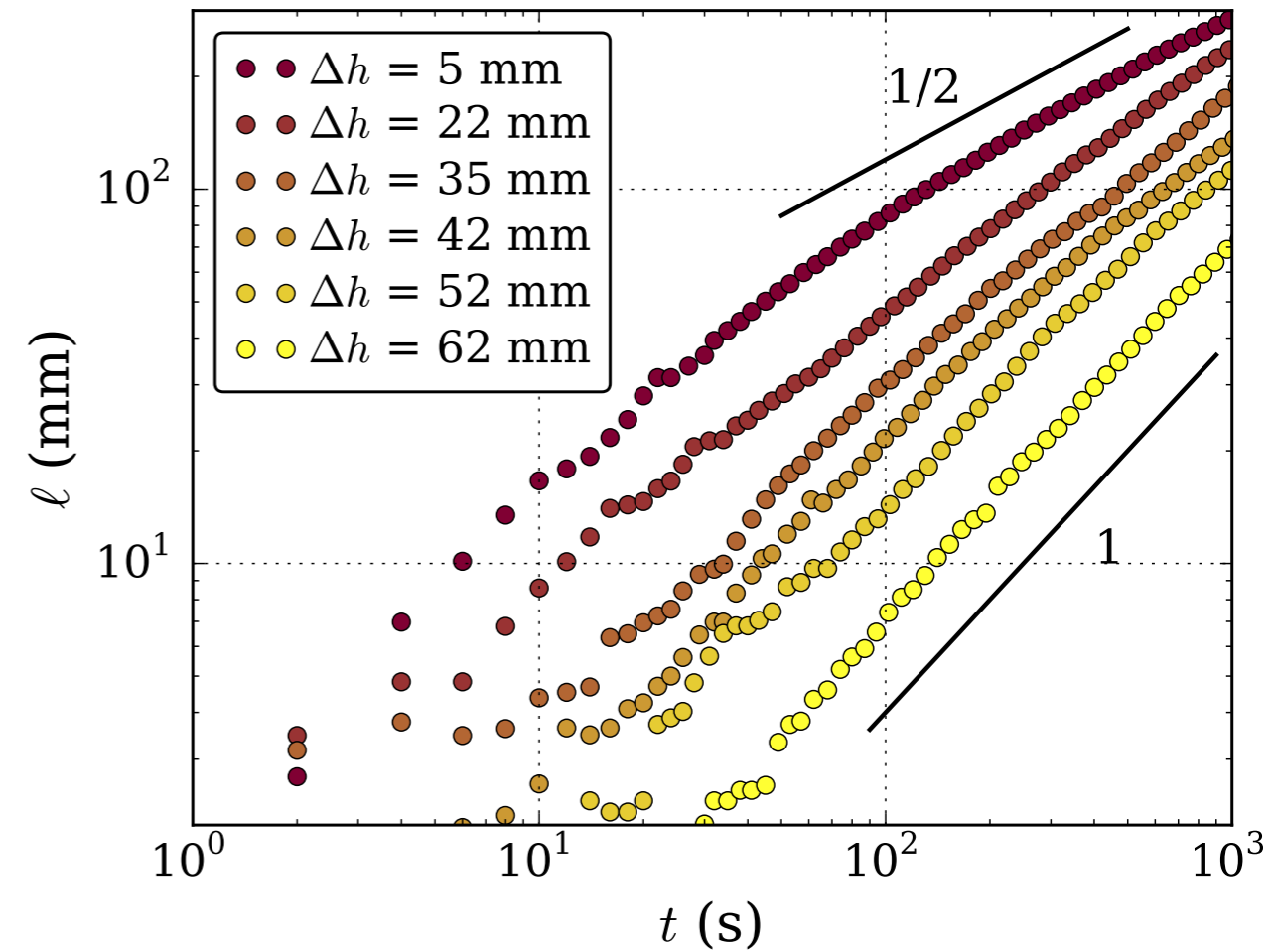
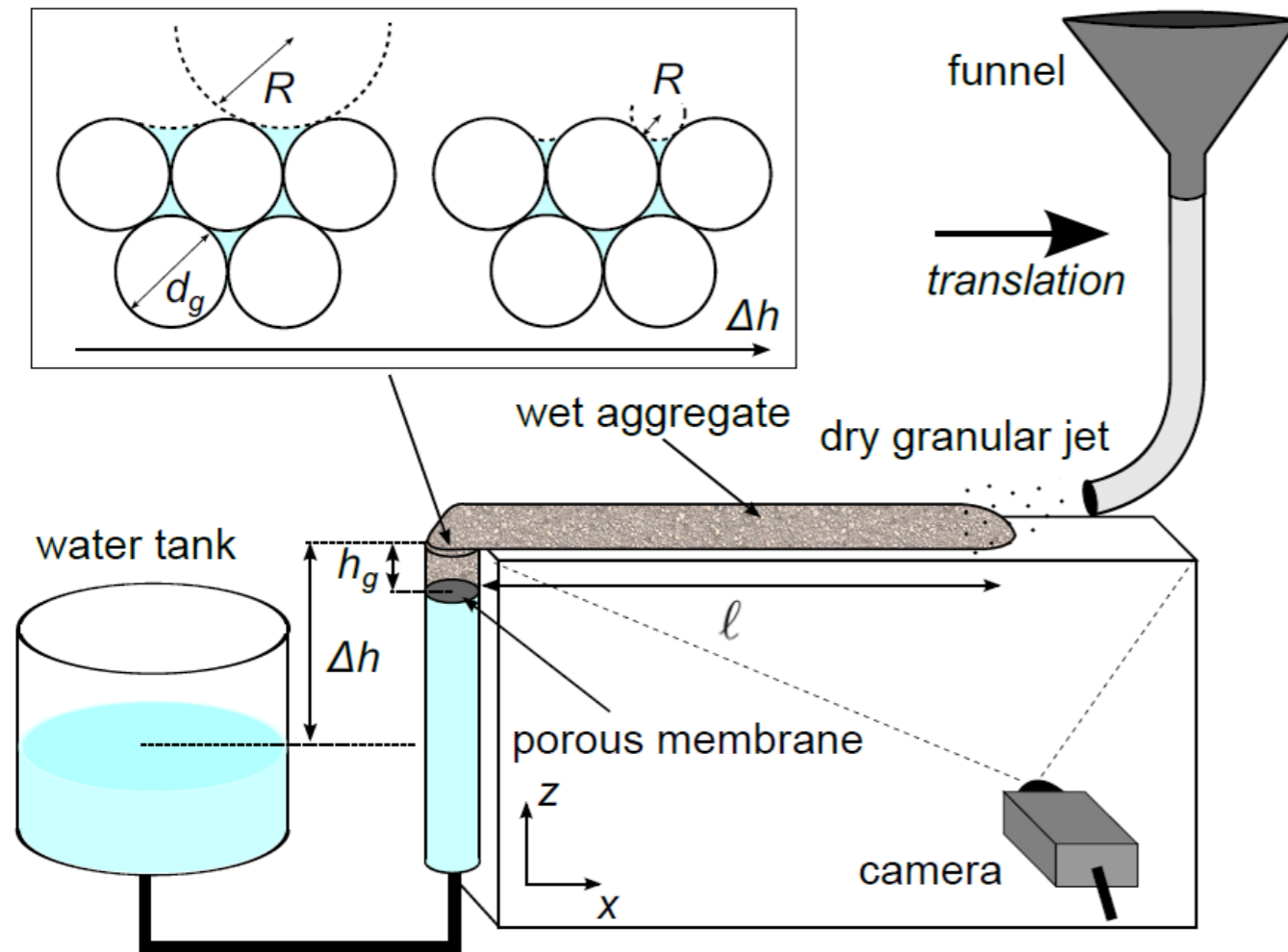
X-Ray tomography: visualization of liquid phase (water+iode), air and beads



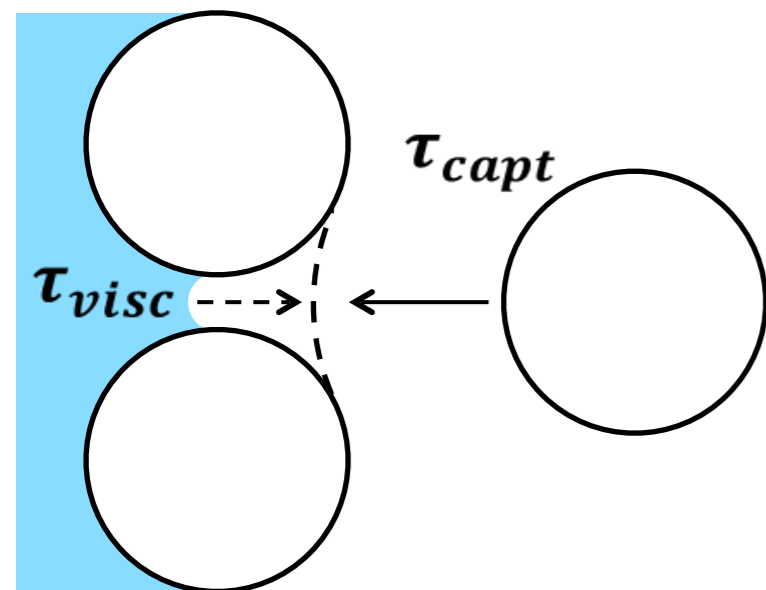
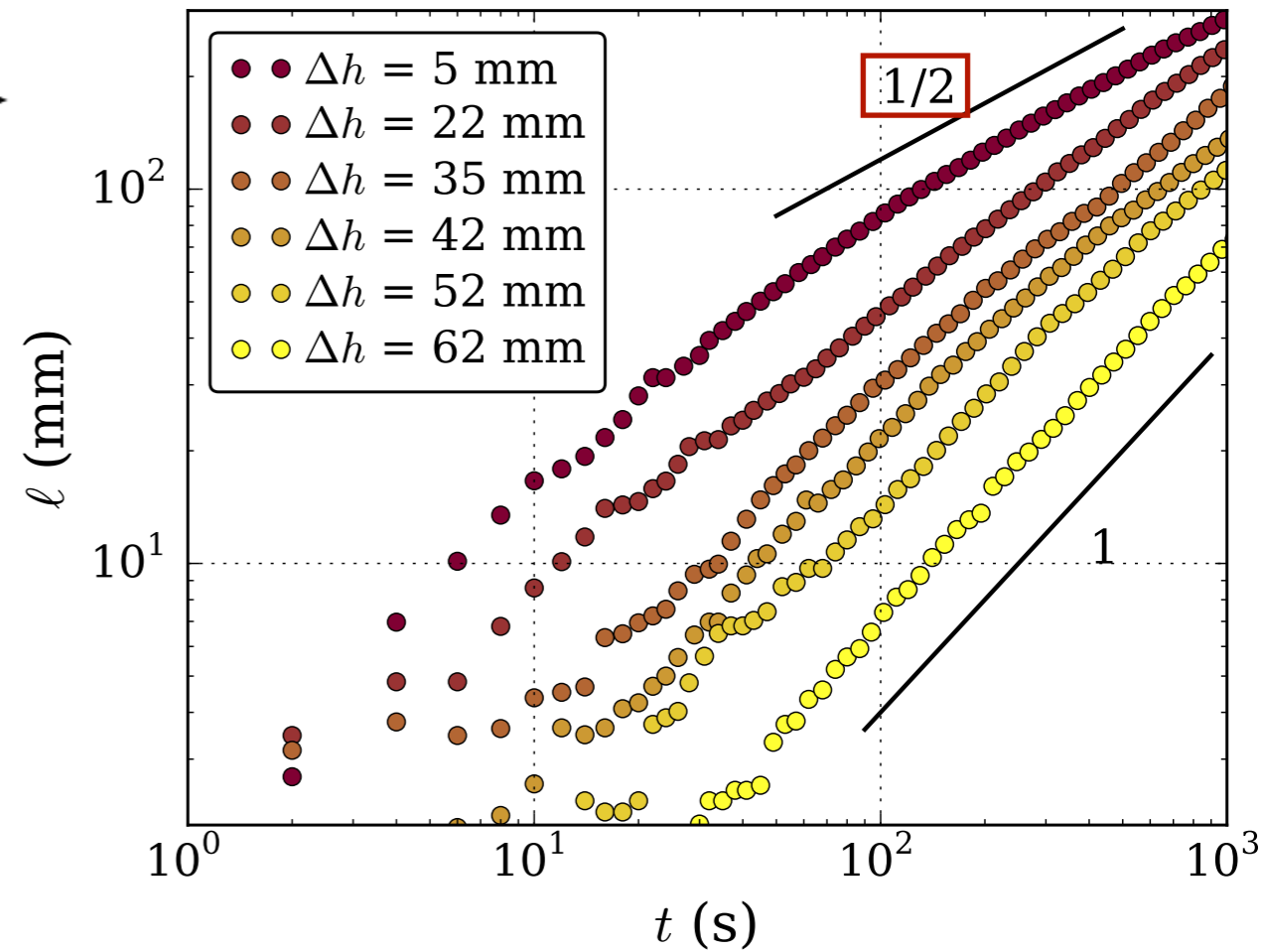
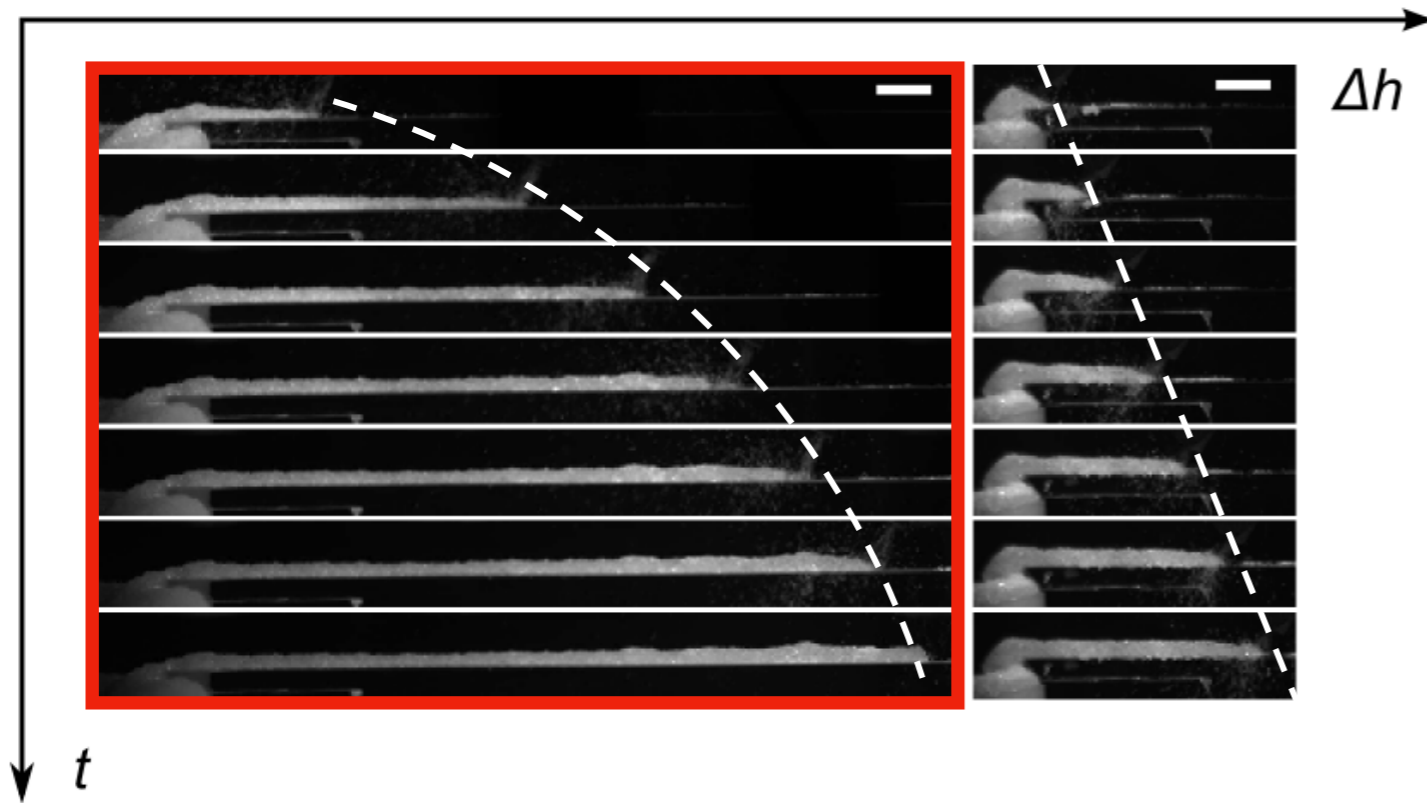
$$p_0 - \rho g z = p_0 - \frac{2\gamma \cos \theta}{R}$$

$$R = \frac{2\gamma \cos \theta}{\rho g z}$$

ACCRETION DYNAMICS



ACCRETION DYNAMICS

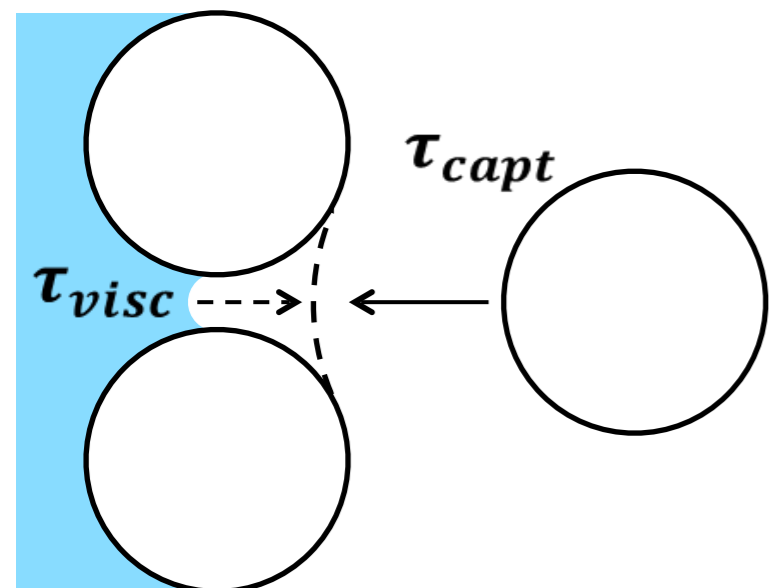
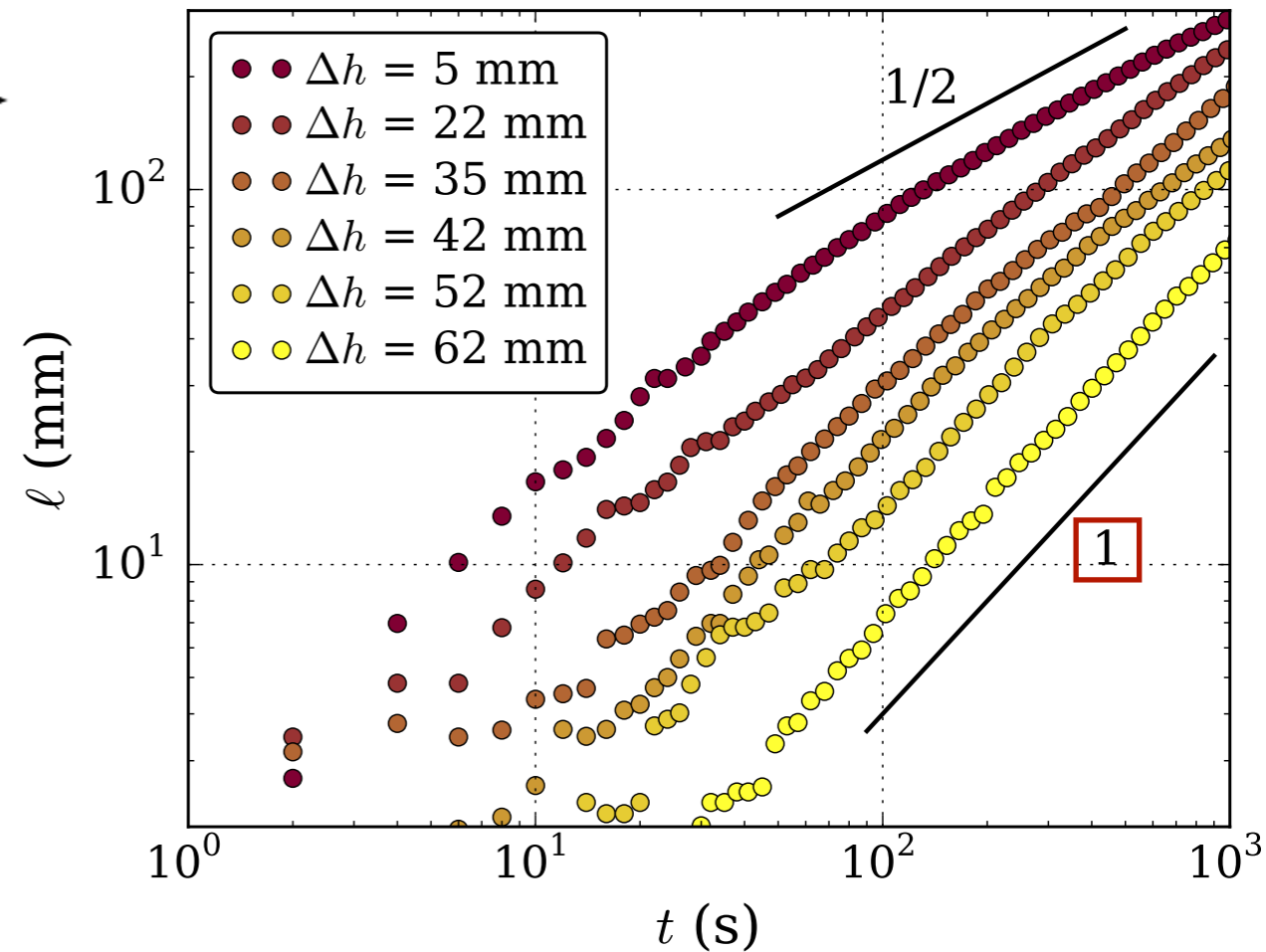
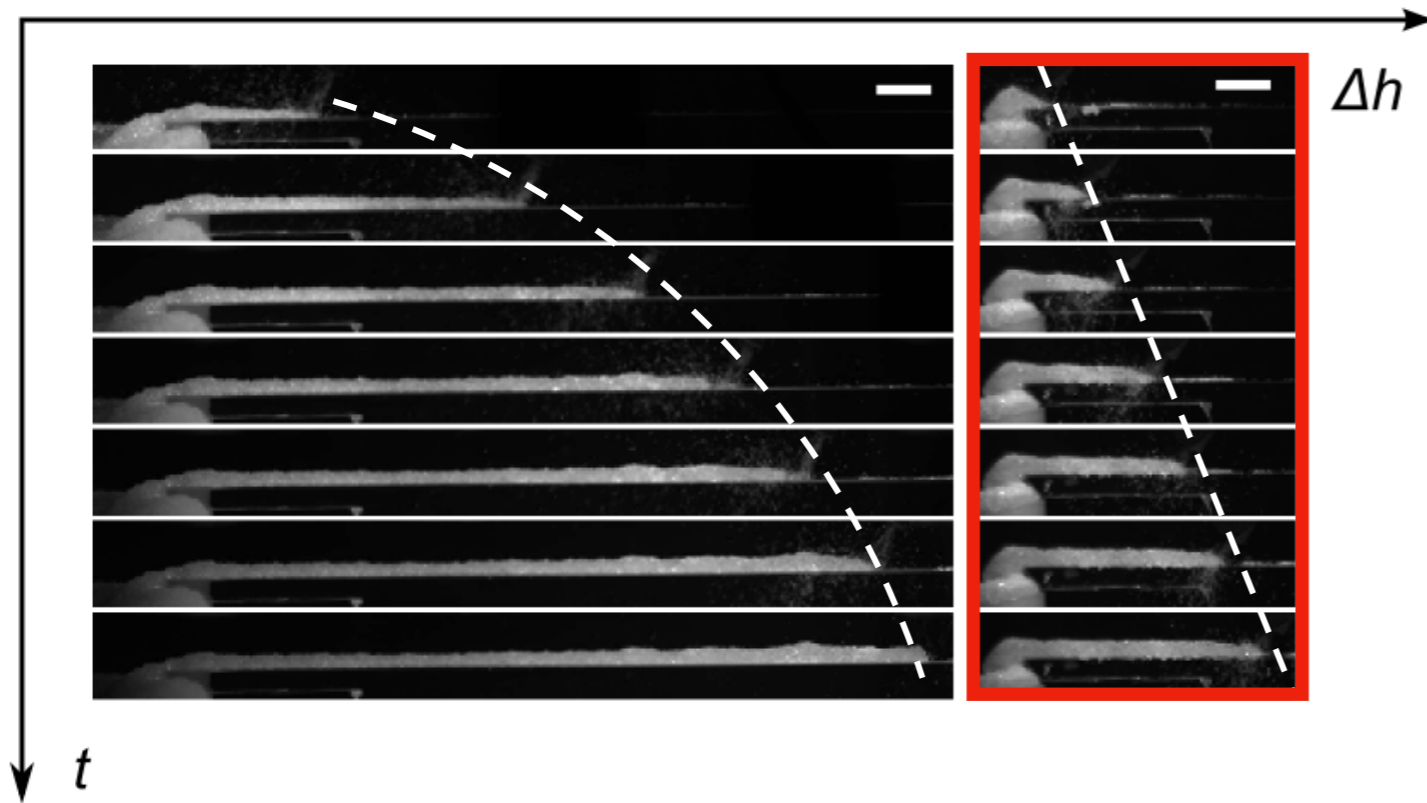


Viscous regime: $\tau_{visc} \gg \tau_{capt}$

Aggregate growth is limited by the fluid flow in the granular packing

$$l^v(t) = \sqrt{\frac{2k\Delta p}{\eta} t}$$

ACCRETION DYNAMICS



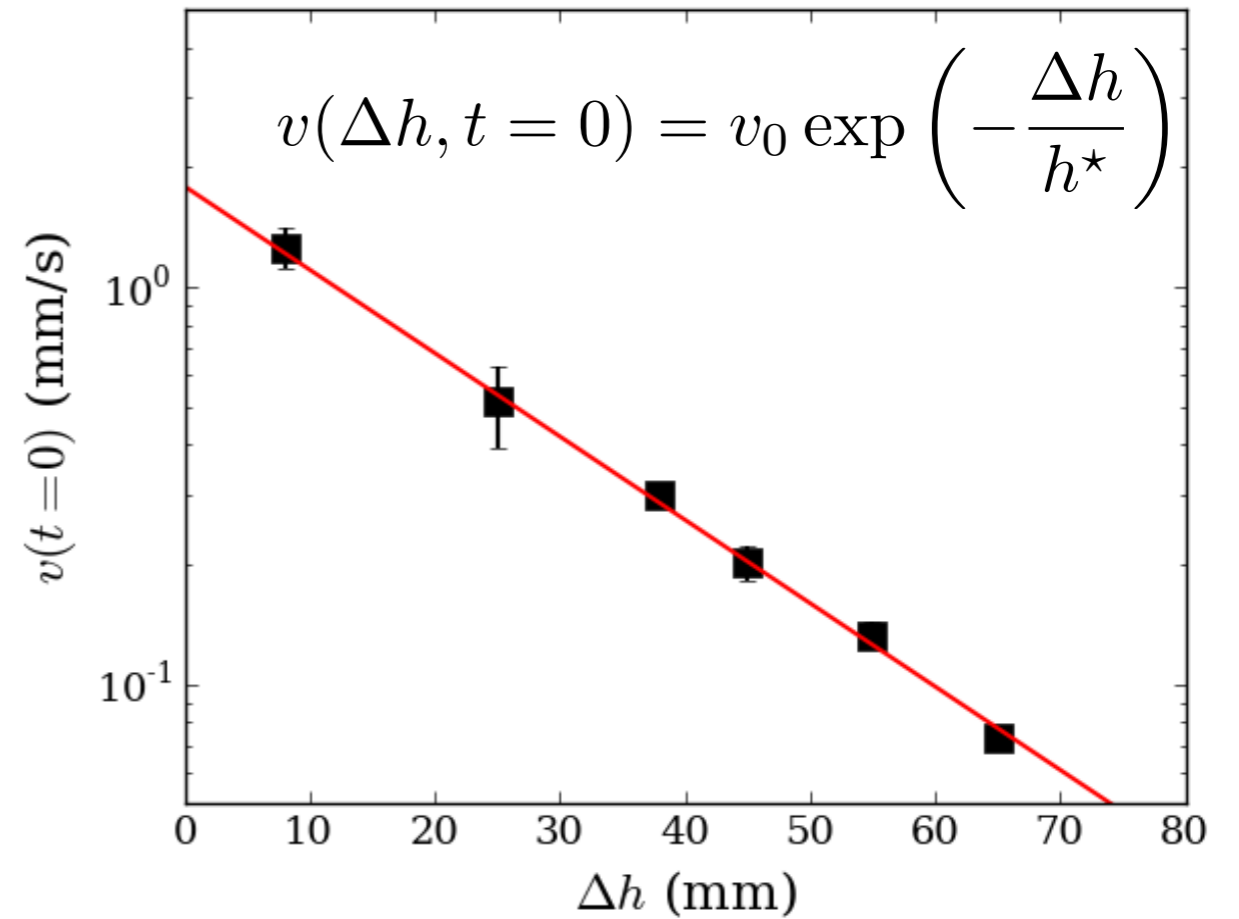
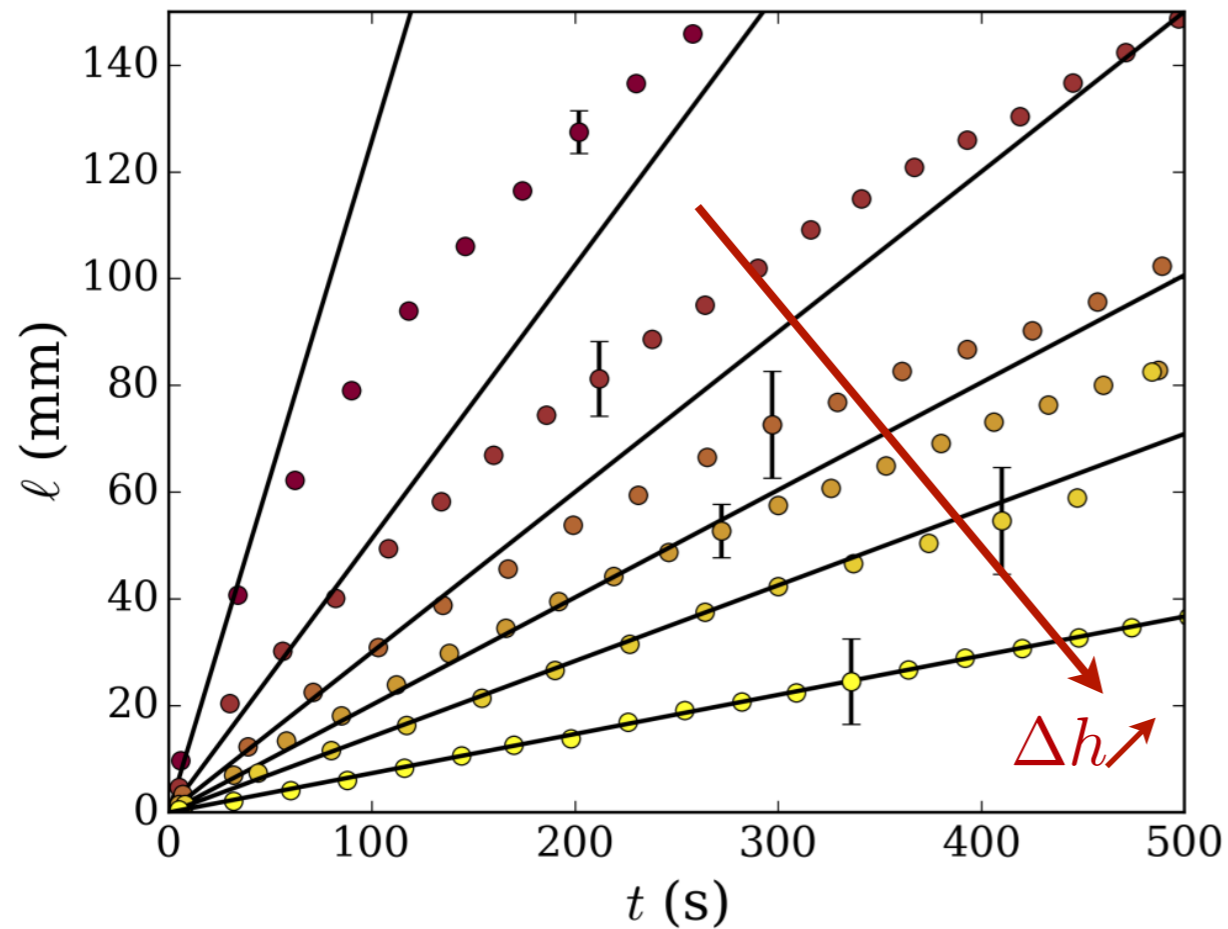
Capture regime: $\tau_{visc} \ll \tau_{capt}$

Growth limited by the fraction of dry grains trapped by the wet aggregate

$$\ell^c(t) = \frac{Q_g}{\rho_s \phi S} \mathcal{P}_{capt} t$$

INITIAL VELOCITY

Evolution of \mathcal{P}_{capt} with Δh : transition between the 2 regimes

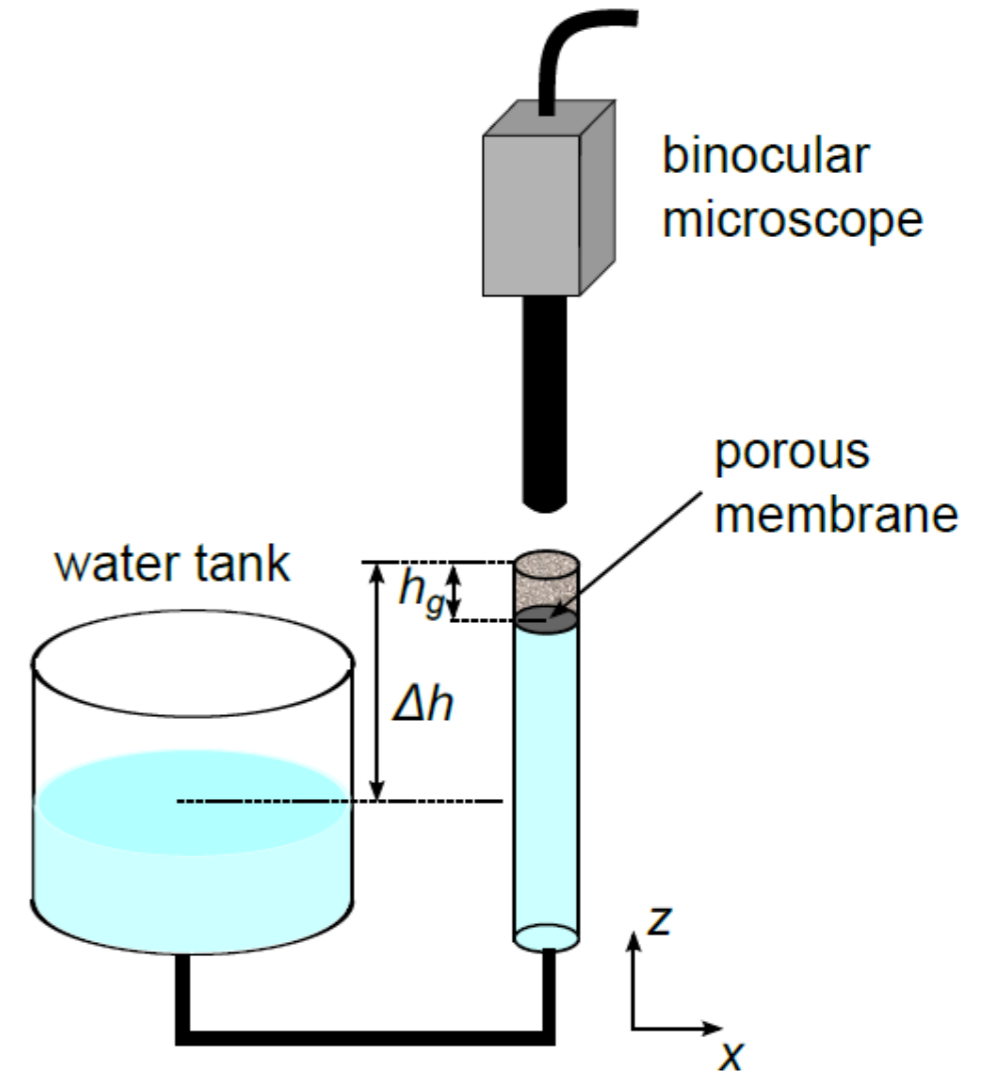
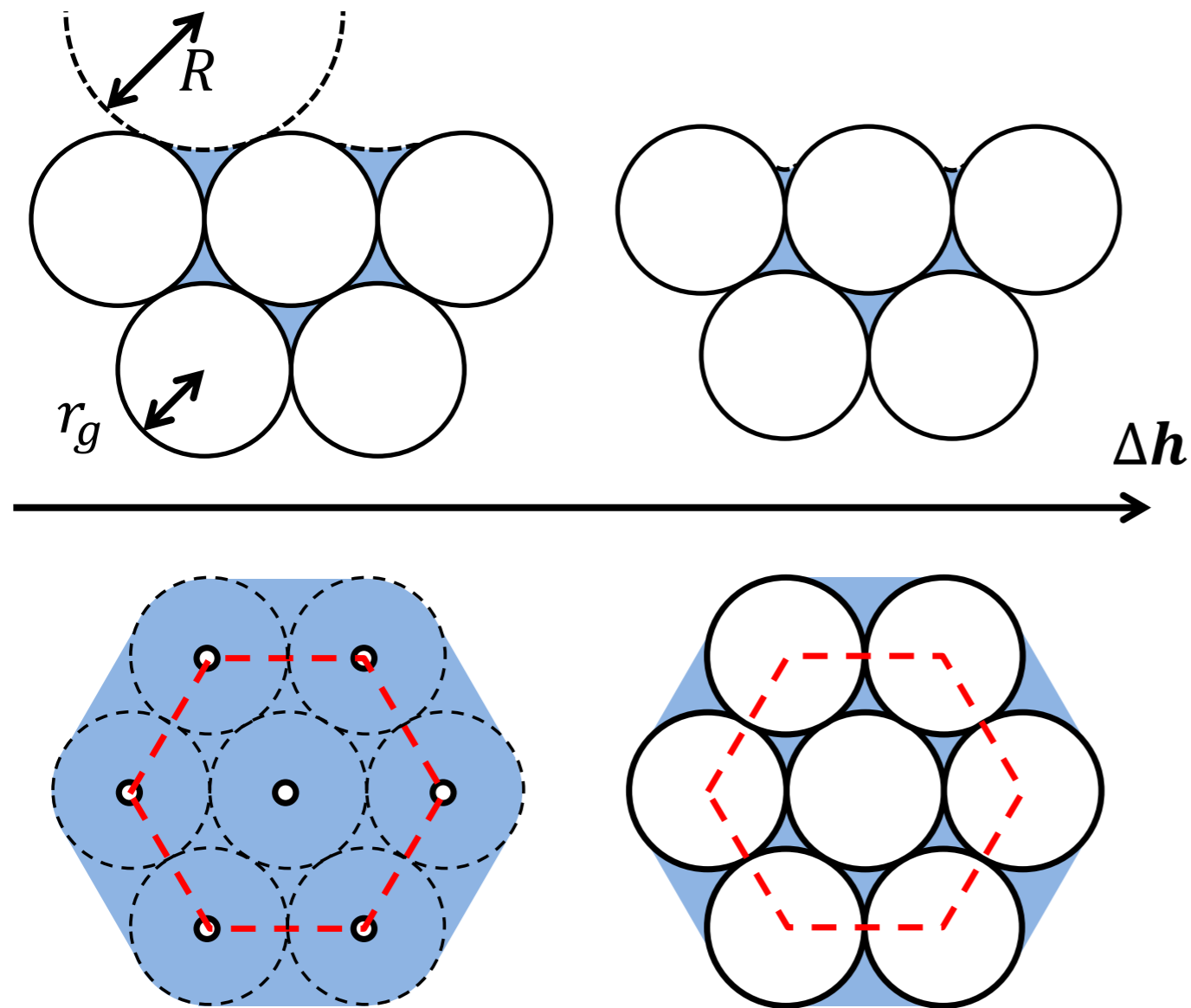


Initial growth velocity: $v(\Delta h, t = 0) = v_0 \exp\left(-\frac{\Delta h}{h^*}\right) = \frac{Q_g}{\rho_s \phi S} \mathcal{P}_{capt}(\Delta h)$

Capture probability: $\mathcal{P}_{capt}(\Delta h) = \mathcal{P}_0 \exp\left(-\frac{\Delta h}{h^*}\right)$

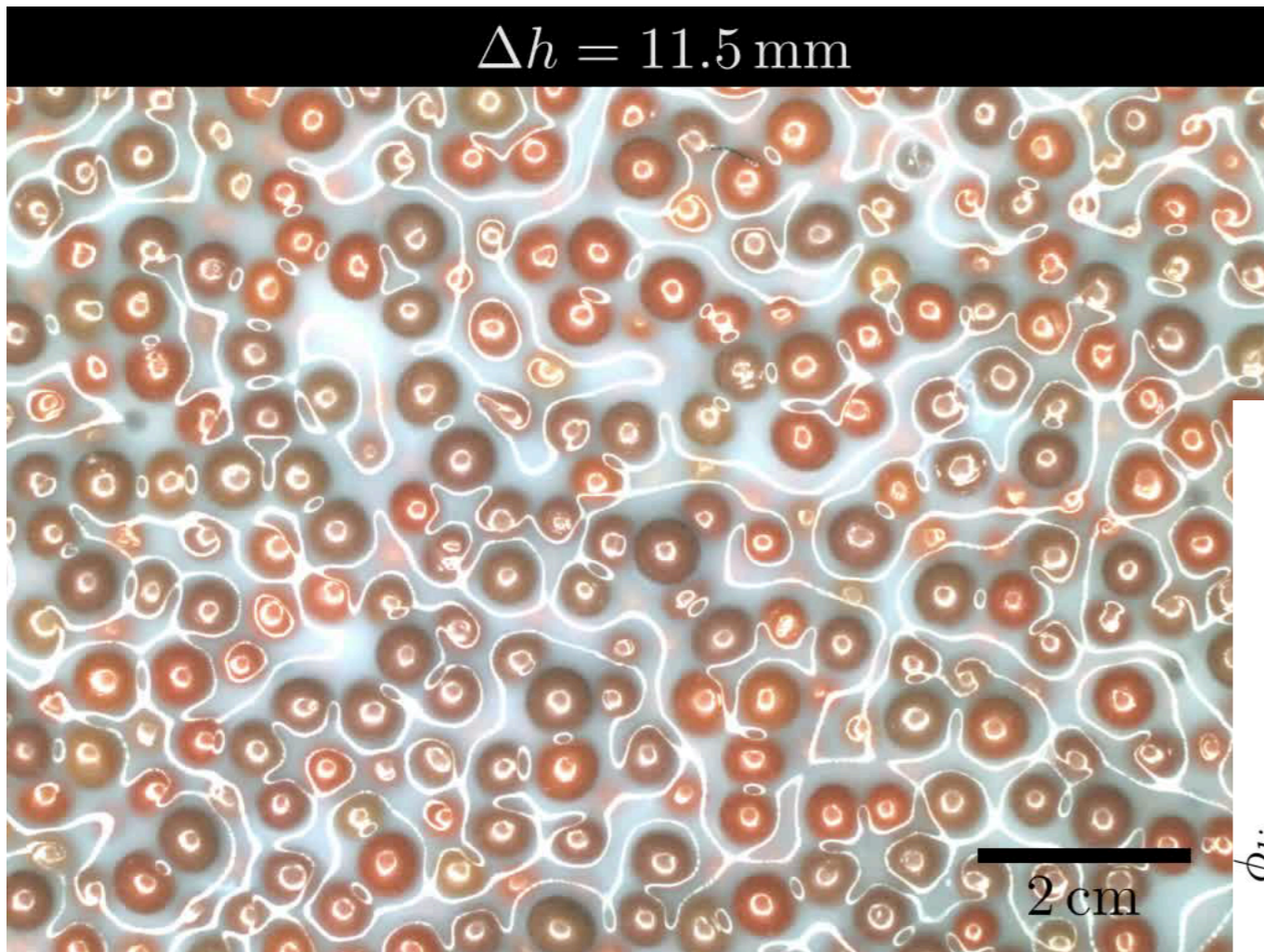
CAPTURE MECHANISM

Accretion efficiency assumed to be captured by the liquid availability at the interfaces



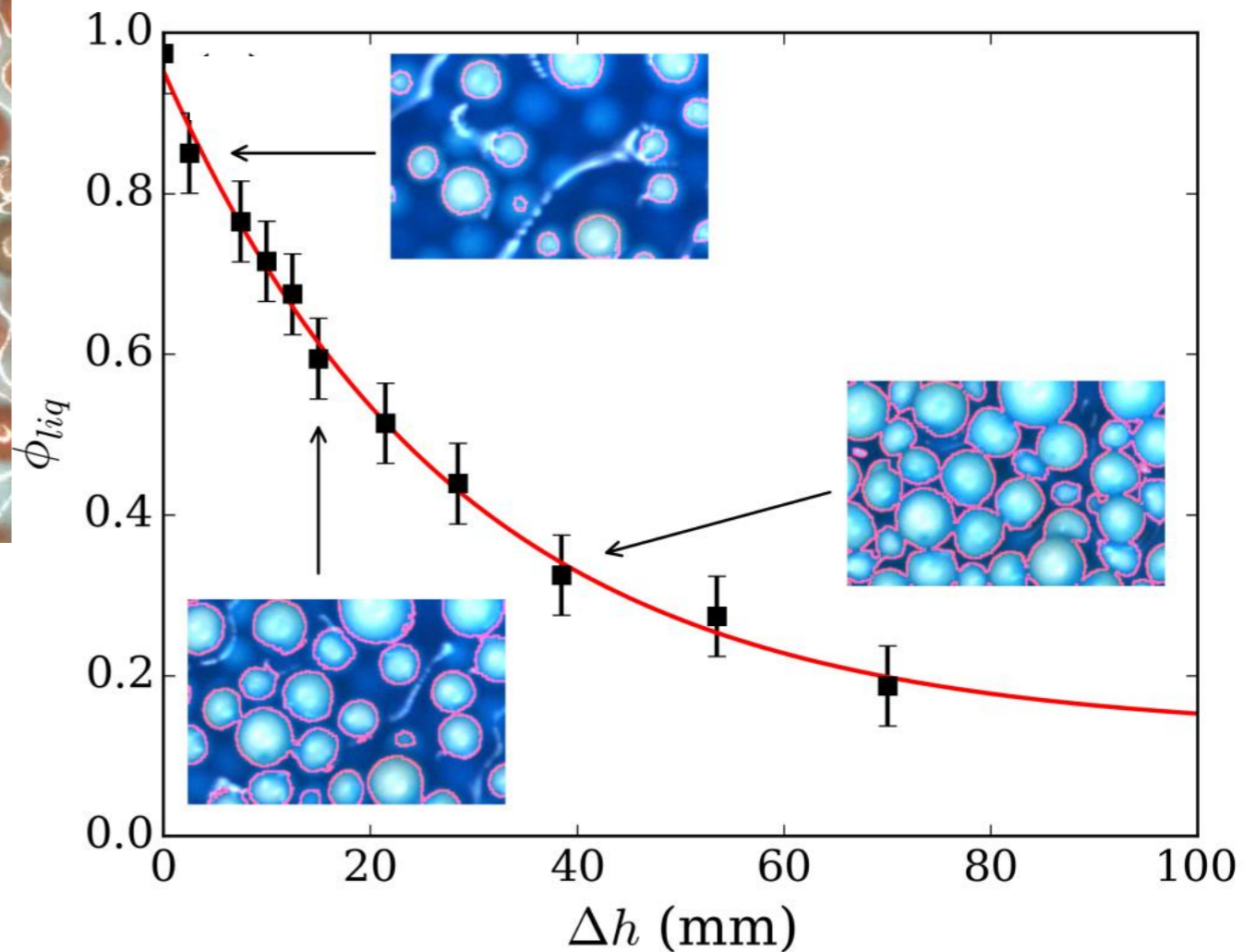
CAPTURE MECHANISM

Accretion efficiency assumed to be captured by the liquid availability at the interfaces



$$\phi_{liq}(\Delta h) = \phi_0 + (1 - \phi_0) \exp\left(-\frac{\Delta h}{h^*}\right)$$

$$\mathcal{P}_{capt} \propto (\phi_{liq} - \phi_0) \propto \exp\left(-\frac{\Delta h}{h^*}\right)$$



TRANSITION BETWEEN REGIMES

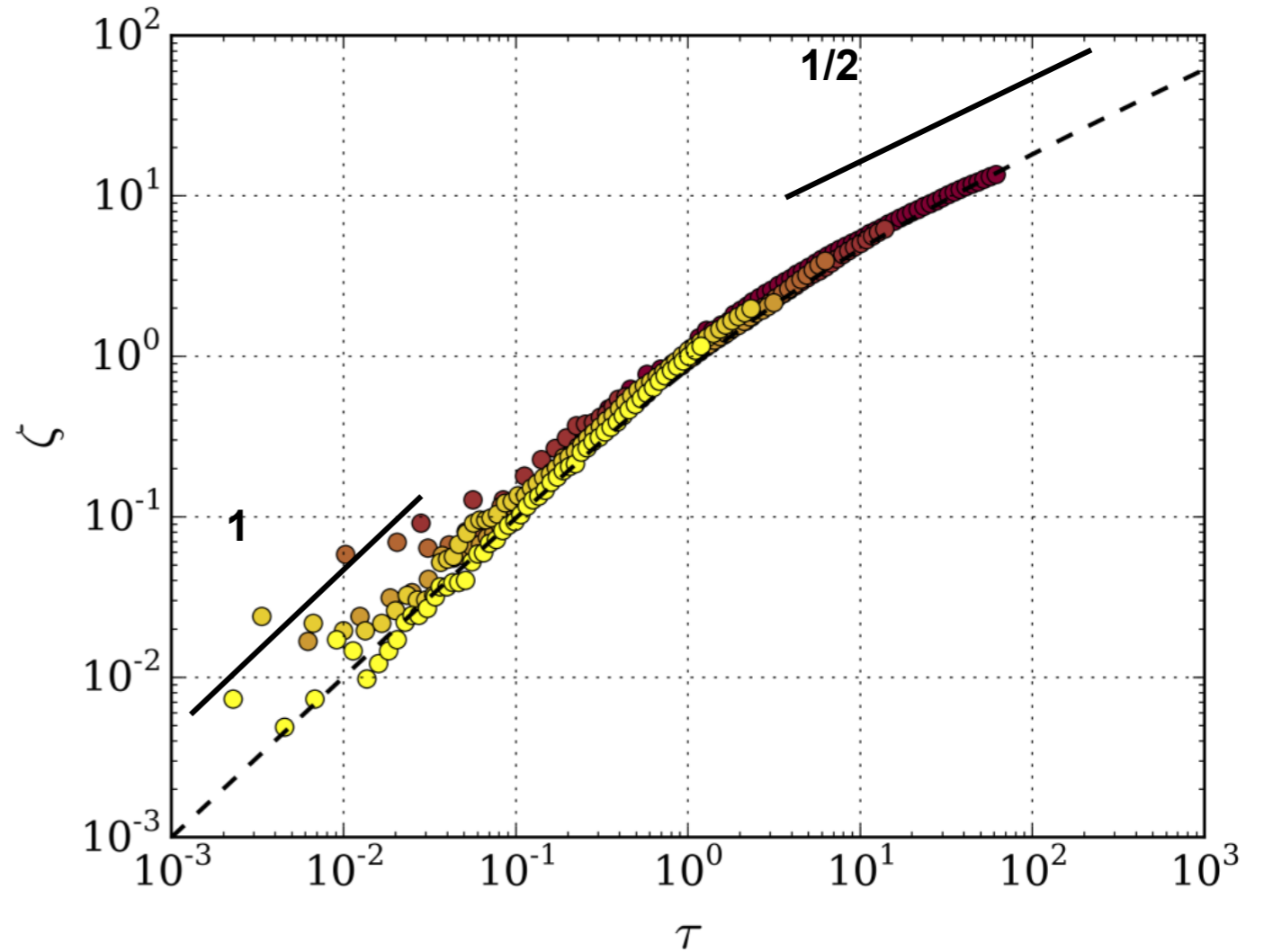
Viscous regime:

$$l^v(t) = \sqrt{\frac{2k\Delta p}{\eta} t}$$

Capture regime:

$$l^c(t) = \frac{Q_g}{\rho_s \phi S} \mathcal{P}_{capt} t$$

Transition: $u^v = u^c$

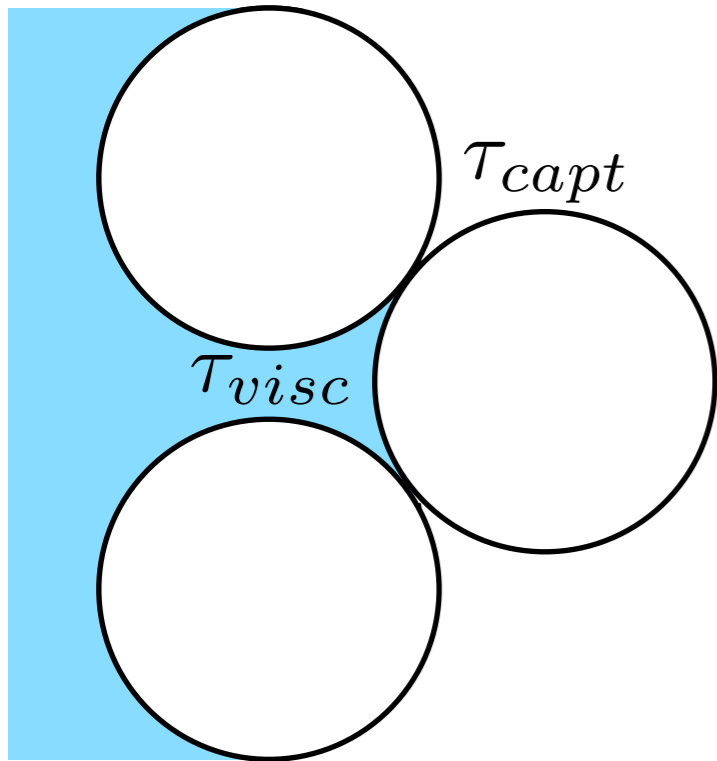


$$\left\{ \begin{array}{l} t_c = \frac{k}{2\eta} \left(\frac{\rho_g \phi S}{\mathcal{P}_{capt} Q_g} \right)^2 \Delta p \\ l_c = \frac{k}{2\eta} \frac{\rho_g \phi S}{\mathcal{P}_{capt} Q_g} \Delta p \end{array} \right.$$

$$\rightarrow \left\{ \begin{array}{l} \tau = t/t_c \\ \xi = l/l_c \end{array} \right.$$

ACCRETION DYNAMICS

Time to increase ℓ of one grain diameter d_g



$$\delta\tau = \tau_{visc} + \tau_{capt}$$

$$u_{visc} = \frac{k \Delta p}{\eta \ell} = \frac{d_g}{\tau_{visc}}$$

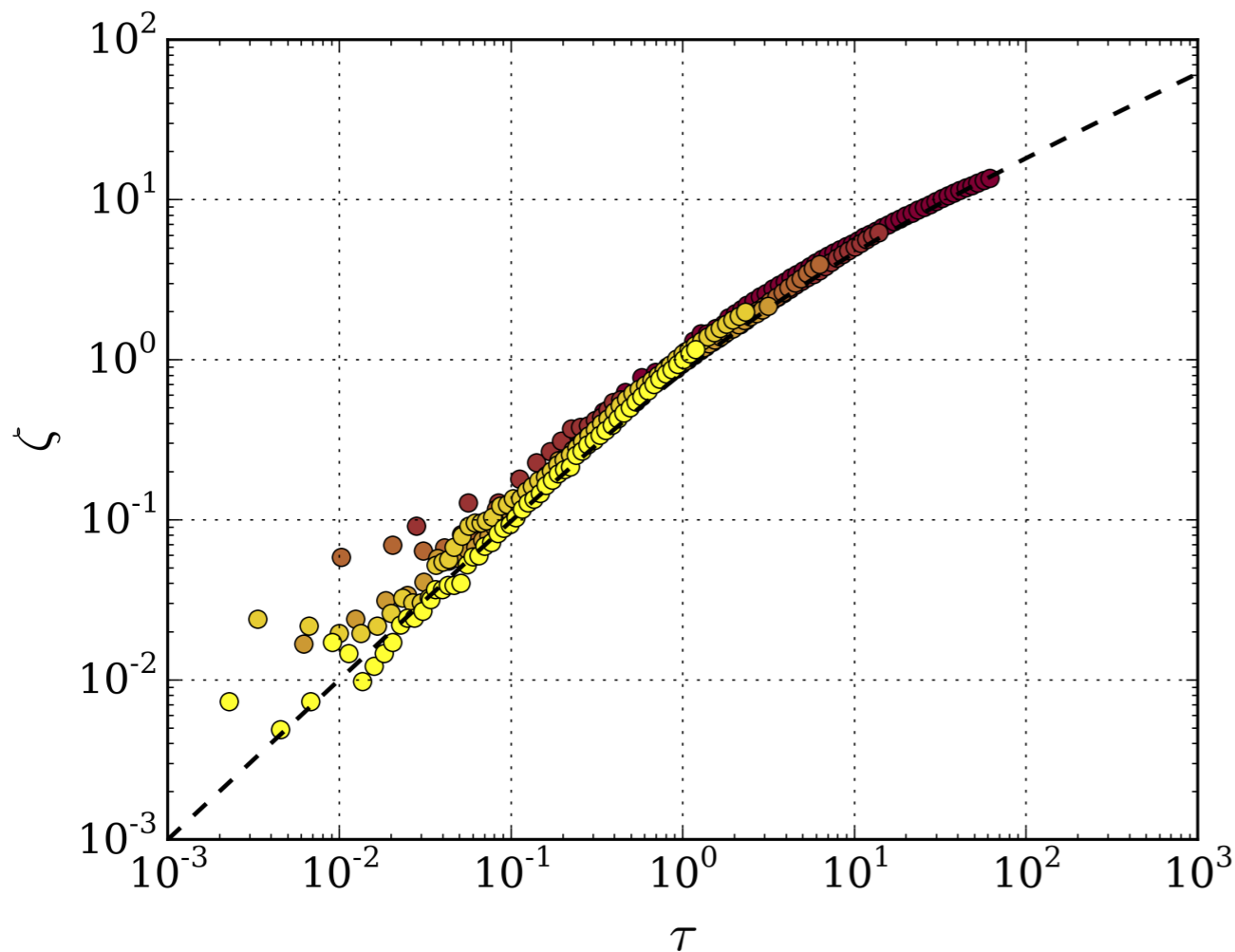
$$u_{capt} = \frac{d_g \rho \phi S}{Q_g \mathcal{P}_{capt}} = \frac{d_g}{\tau_{capt}}$$

$$\frac{d\ell}{dt} = \frac{d_g}{\delta\tau} \quad \tau = t/t_c$$

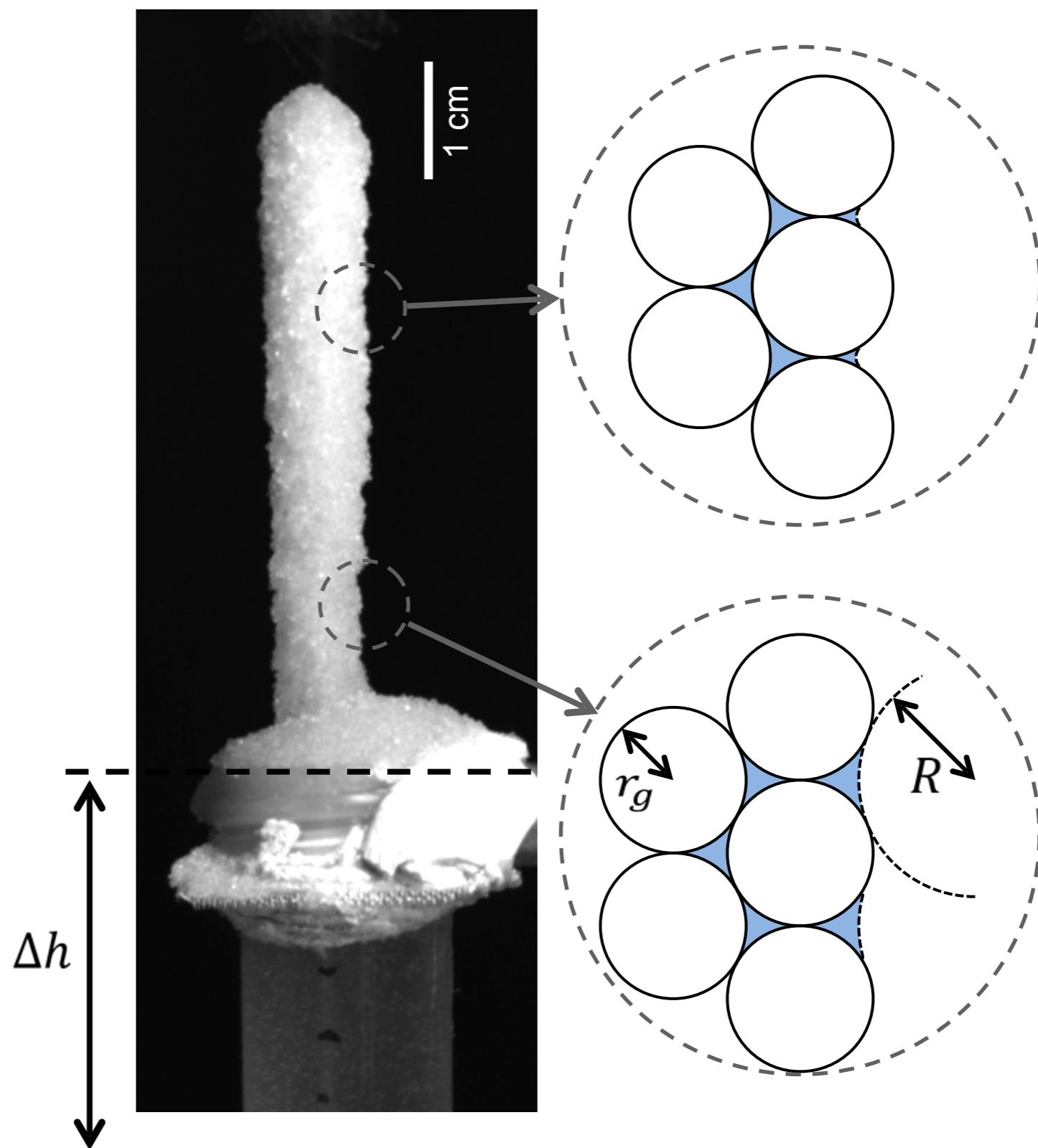
$$\xi = \ell/\ell_c$$

$$\frac{d\xi}{d\tau} = \frac{1}{1 + \xi/2}$$

$$\xi(\tau) = 2(\sqrt{1 + \tau} - 1)$$



VERTICAL GROWTH: GRANULAR TOWERS



$$\mathcal{P}_{capt}(\Delta h) = \mathcal{P}_0 \exp\left(-\frac{\Delta h}{h^*}\right)$$

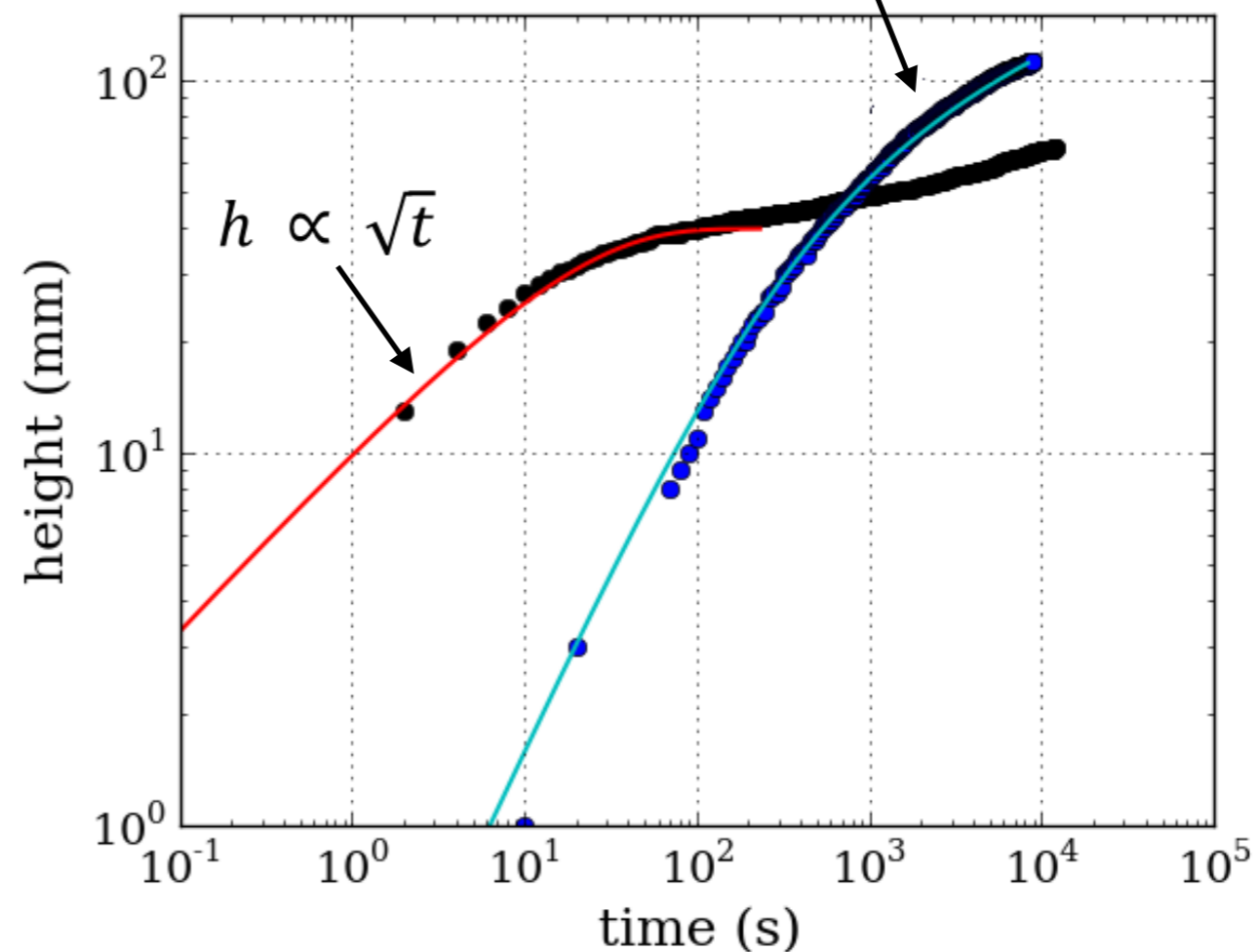
VERTICAL GROWTH: GRANULAR TOWERS



Capture probability related to the saturation rate

$$\mathcal{P}_{capt}(\Delta h) = \mathcal{P}_0 \exp\left(-\frac{\Delta h}{h^*}\right) \rightarrow v(h) = v_0 \exp\left(-\frac{h}{h^*}\right)$$

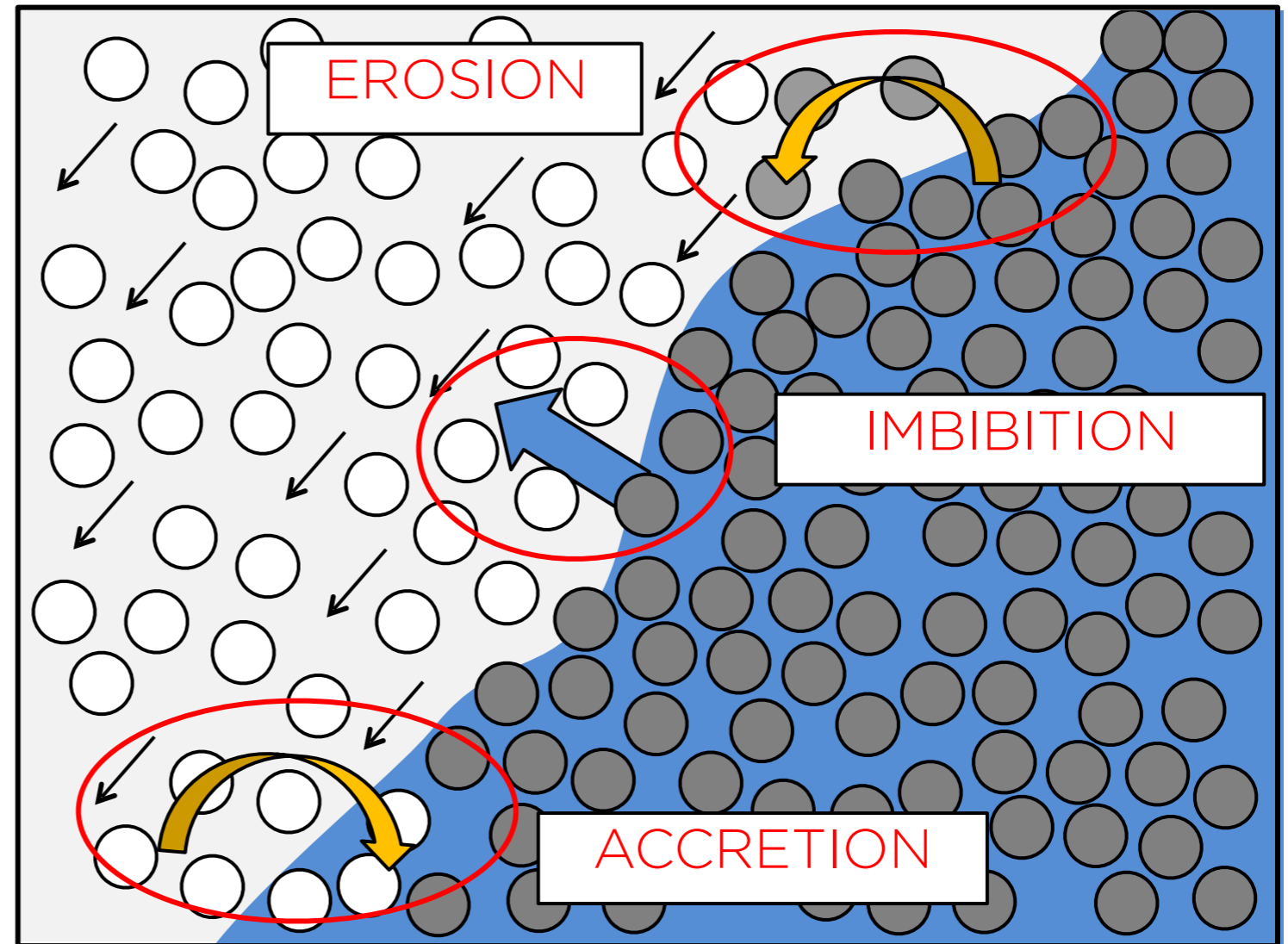
$$\rightarrow h(t) = h^* \ln\left(1 + \frac{V_0}{h^*} t\right)$$



INTERACTION BETWEEN A GRANULAR FLOW AND A LIQUID

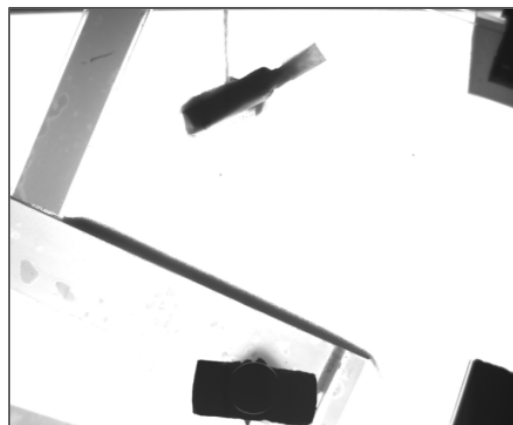
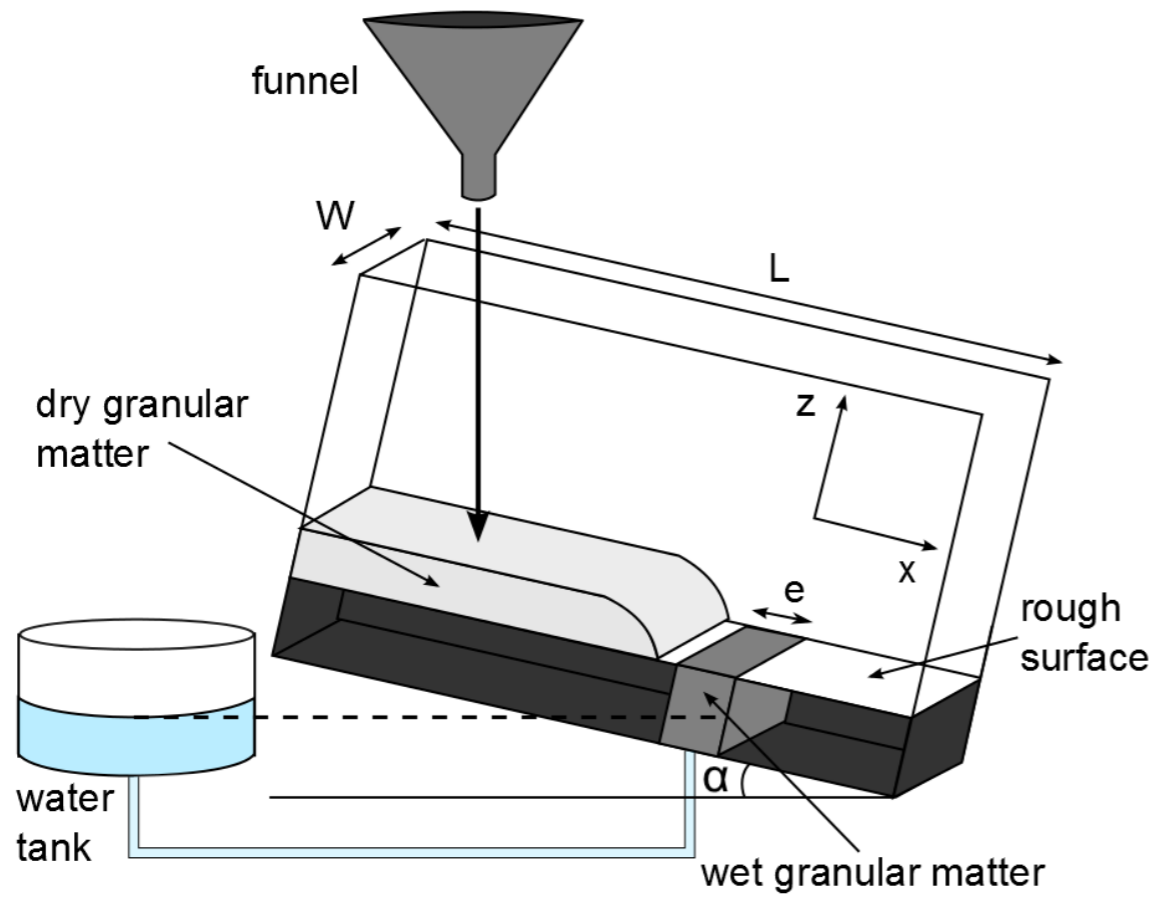


dry granular
flow

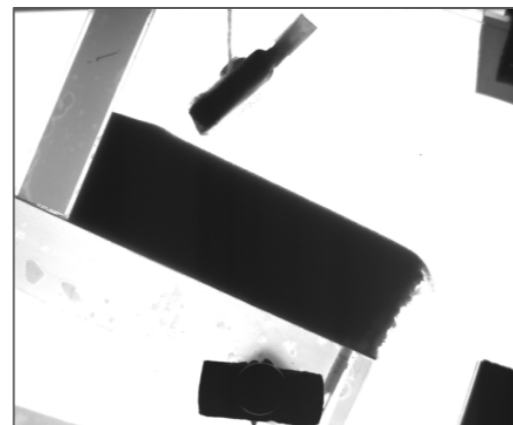


cohesive wet
grains

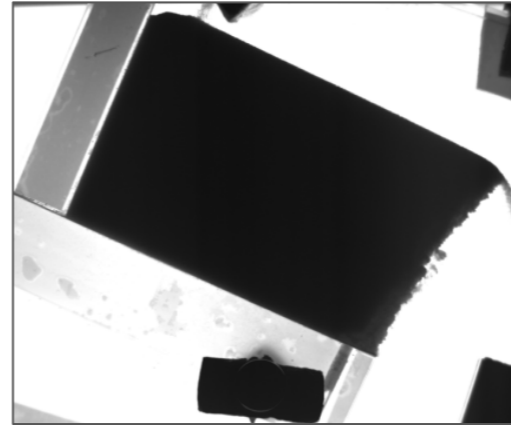
DENSE FLOW



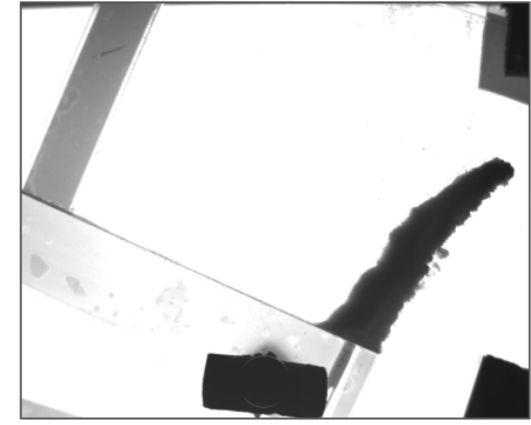
$t = 0$ min



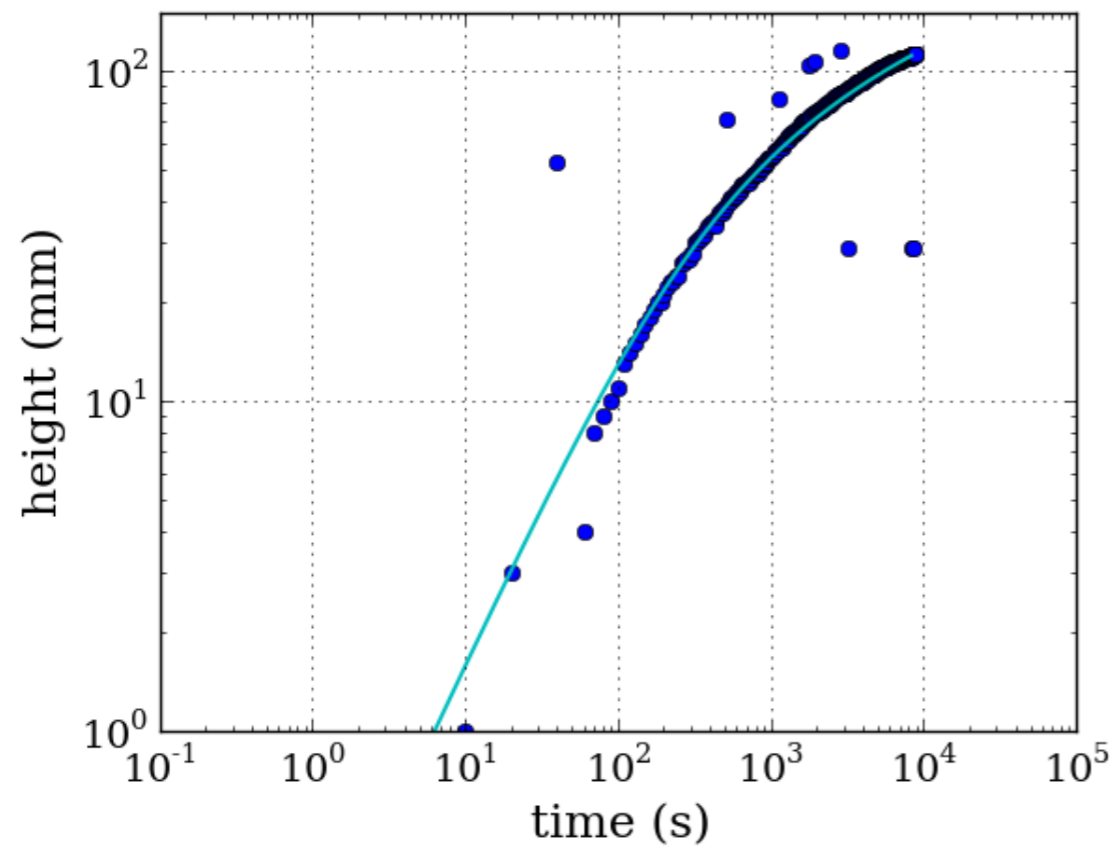
$t = 15$ min



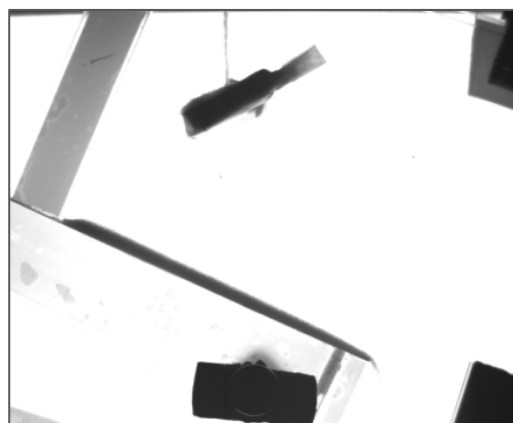
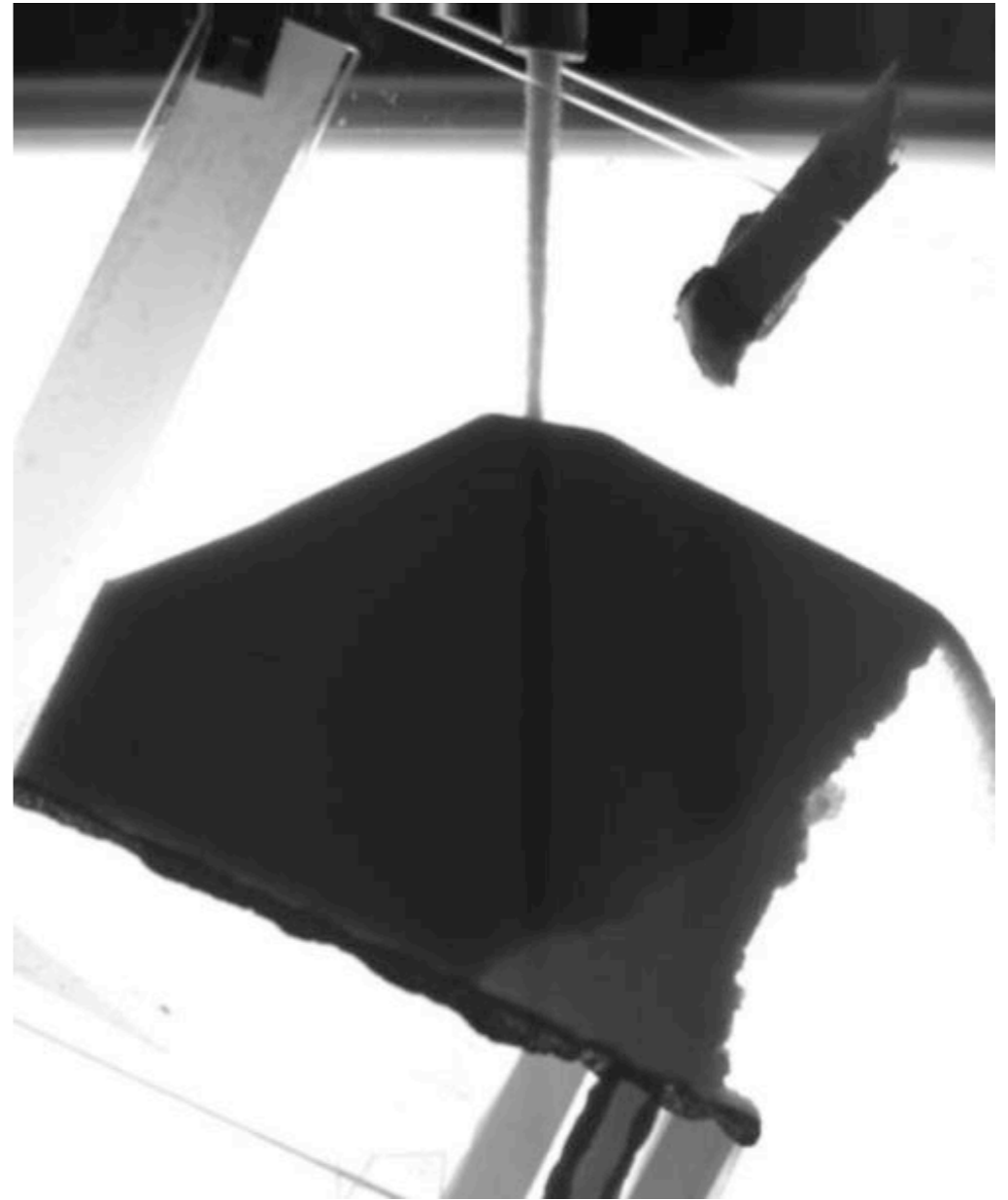
$t = 2$ h



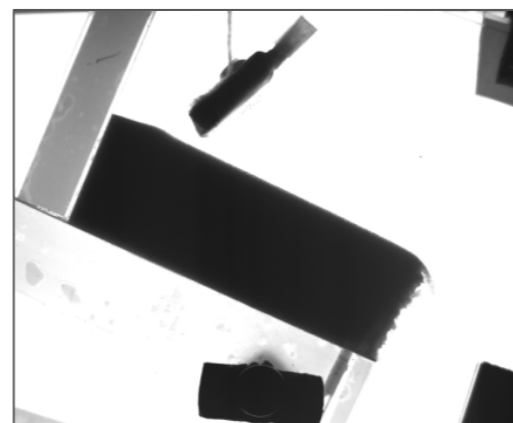
DENSE FLOW



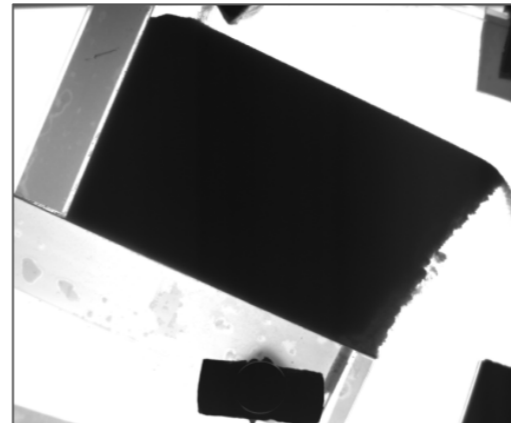
$$h(t) = h^* \ln \left(1 + \frac{V_0}{h^*} t \right)$$



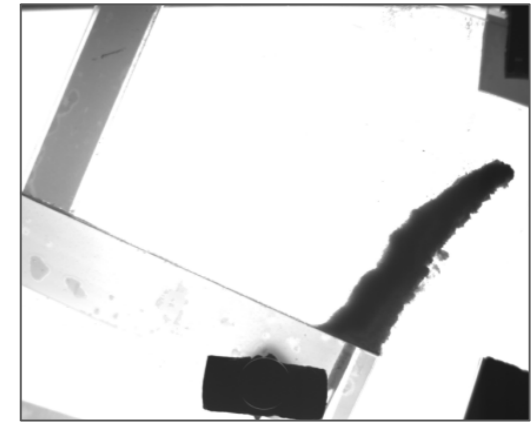
t = 0 min



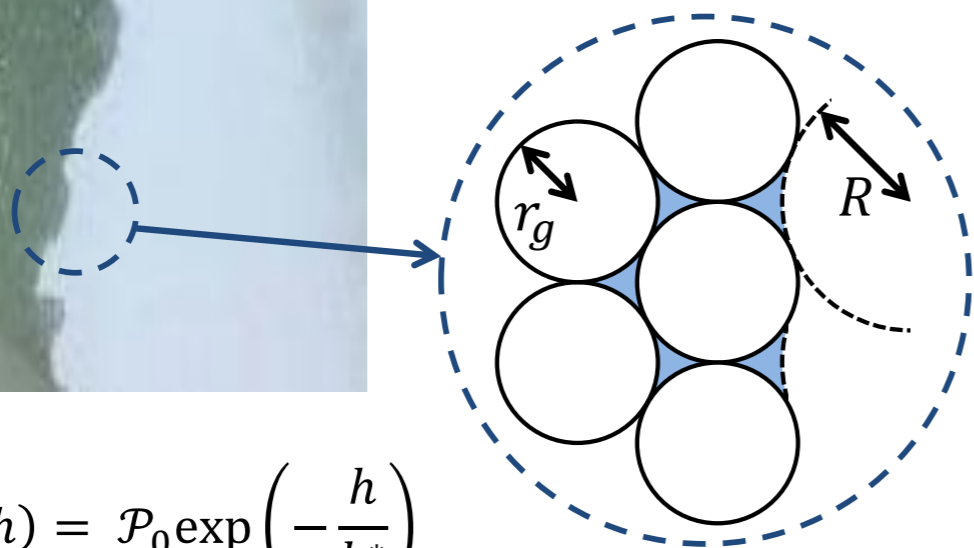
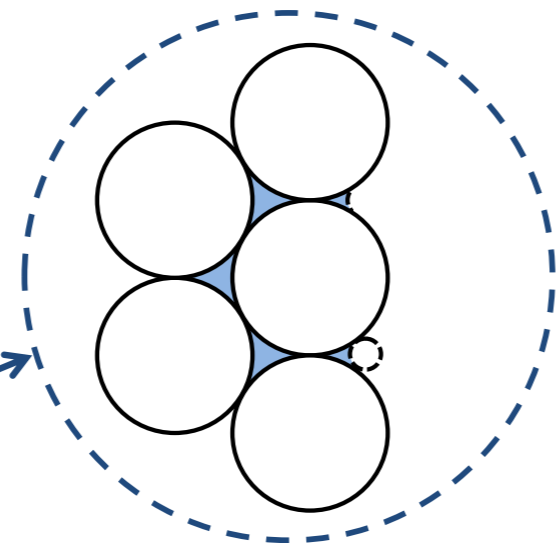
t = 15 min



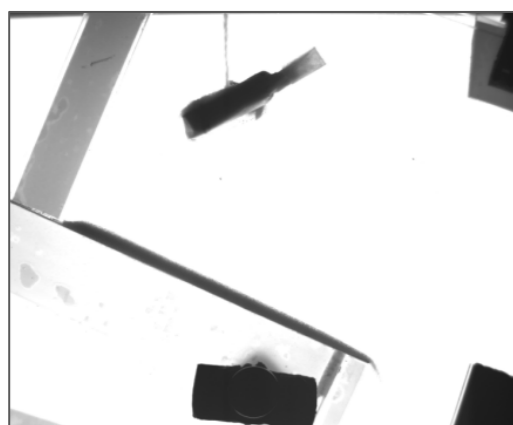
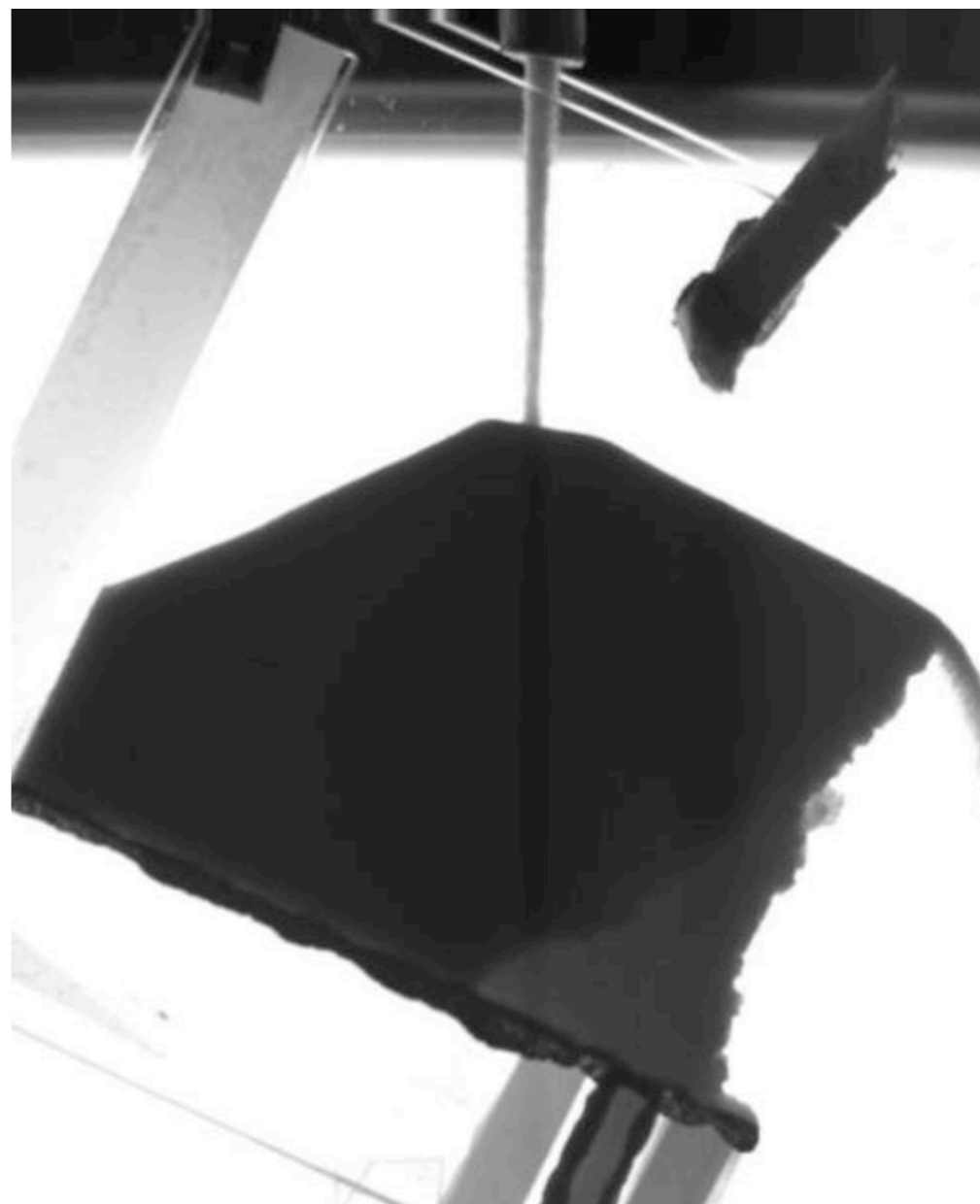
t = 2 h



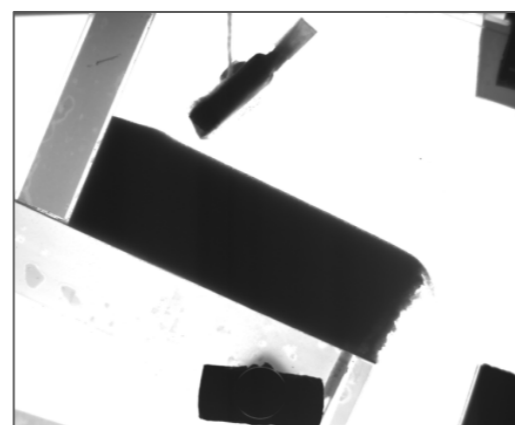
DENSE FLOW



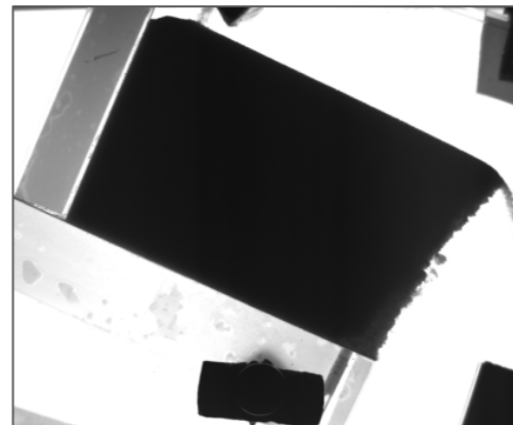
$$\mathcal{P}_{capt}(h) = \mathcal{P}_0 \exp\left(-\frac{h}{h^*}\right)$$



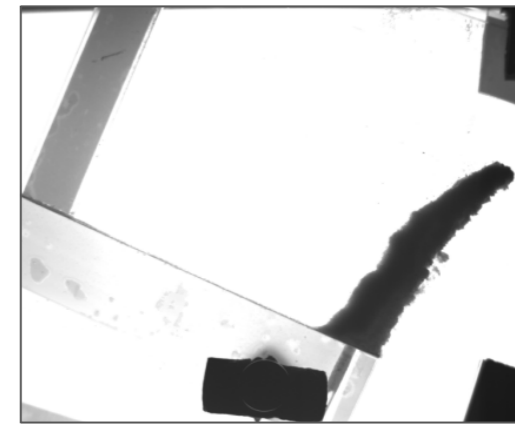
t = 0 min



t = 15 min

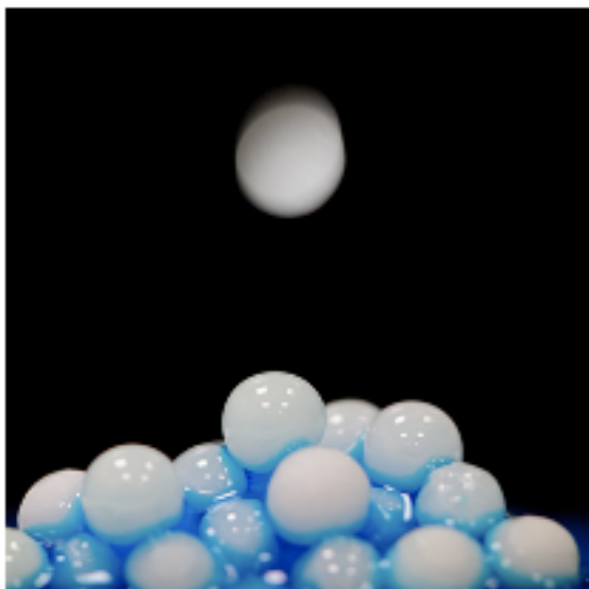


t = 2 h



SUMMARY

- Accretion: local phenomenon associated to the curvature of the meniscus
- Two regimes :
 - viscous:** limited by the fluid flow in the porous media
 - capture:** limited by trapping efficiency



EDITORS' SUGGESTION

Accretion Dynamics on Wet Granular Materials

The probability that a jet of dry grains will stick to a wet granular pile depends on the amount of liquid available at the pile's surface.

Guillaume Saingier, Alban Sauret, and Pierre Jop

[Phys. Rev. Lett. 118, 208001 \(2017\)](#)

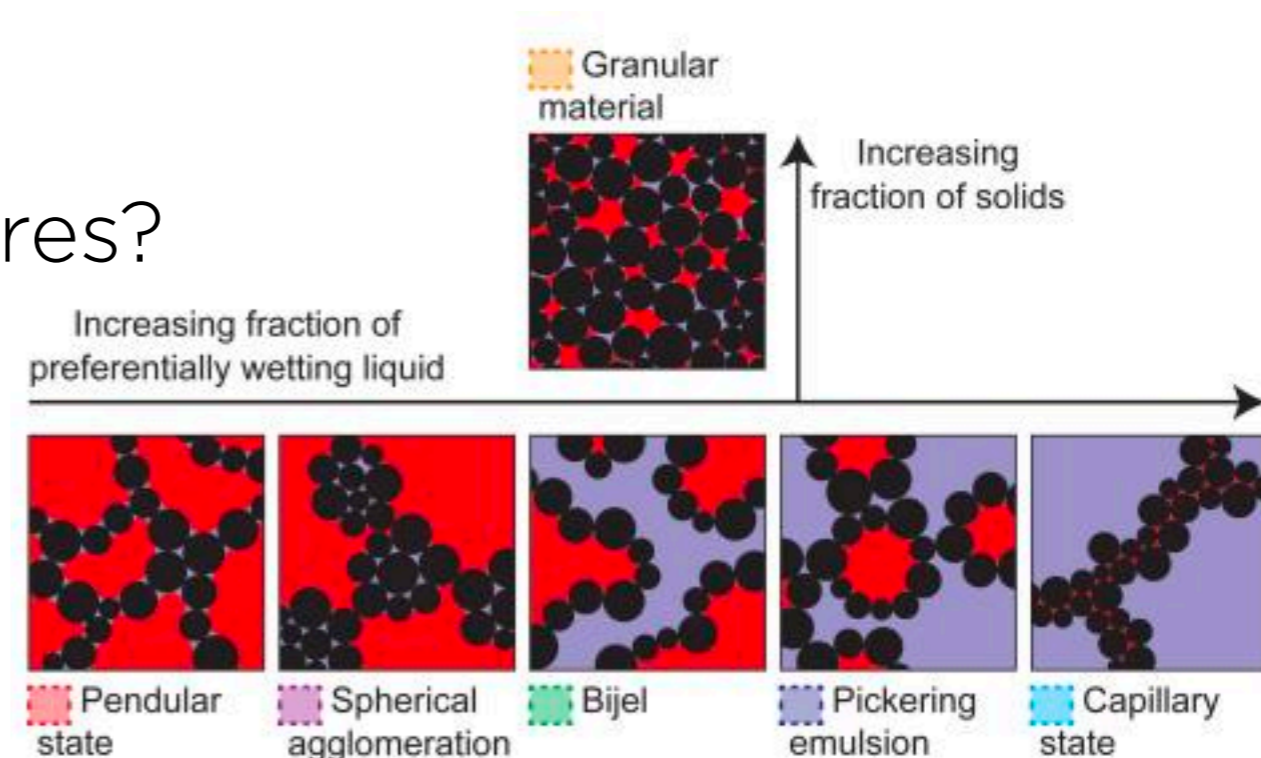


SUMMARY

- Accretion: local phenomenon associated to the curvature of the meniscus
- Two regimes :
 - viscous:** limited by the fluid flow in the porous media
 - capture:** limited by trapping efficiency

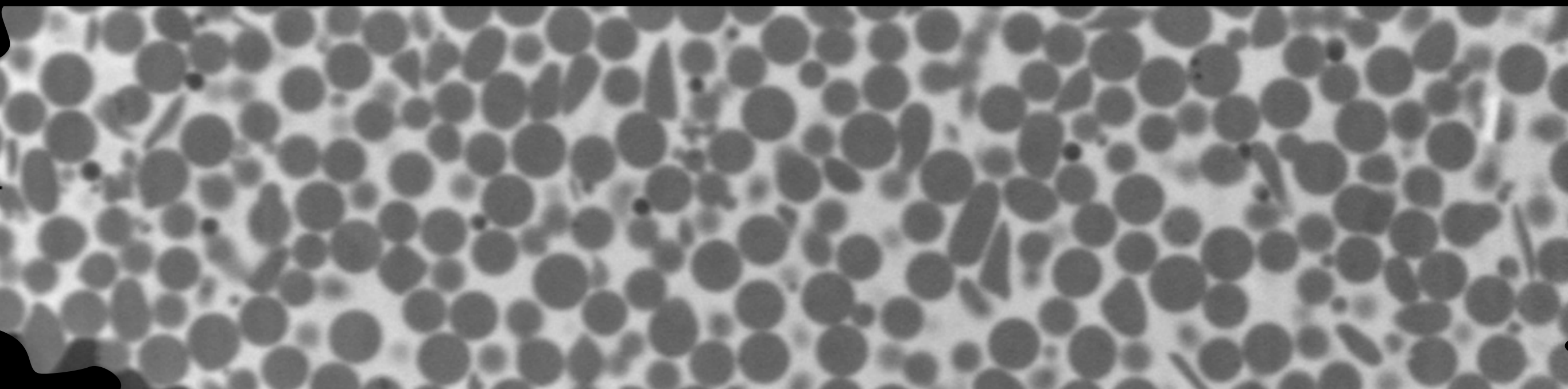
Many open questions : three-phase systems

- How does the morphology of the grains/liquid mixture couple with its rheology ?
- How does the reorganization of the capillary bridges affect the rheology ?
- Liquid/Liquid/Particles mixtures?



BLENDING LIQUID AND GRAINS

ACCRETION DYNAMICS ON WET GRANULAR MATERIALS



G. Saingier, P. Jop

P. Raux, A. Troger; M. Gomez, B. Colnet, M. Bazant,
H. A. Stone, E. Dressaire

